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Secondary organic aerosol yields of 12-carbon alkanes

C. L. Loza[1], J. S. Craven[1], L. D. Yee[2], M. M. Coggon[1], R. H. Schwantes[2], M. Shiraiwa[1,3], X. Zhang[2], K. A. Schilling[1], N. L. Ng[4], M. R. Canagaratna[5], P. J. Ziemann[6], R. C. Flagan[1,2], and J. H. Seinfeld[1,2]

[1]Division of Chemistry and Chemical Engineering, California Institute of Technology, Pasadena, CA, USA
[2]Division of Engineering and Applied Science, California Institute of Technology, Pasadena, CA, USA
[3]Multiphase Chemistry Department, Max Planck Institute for Chemistry, Mainz, Germany
[4]School of Chemical and Biomolecular Engineering and School of Earth and Atmospheric Sciences, Georgia Institute of Technology, Atlanta, GA, USA
[5]Aerodyne Research, Inc., Billerica, MA, USA
[6]Air Pollution Research Center, Department of Environmental Sciences, and Environmental Toxicology Graduate Program, University of California, Riverside, CA, USA

Correspondence to: J. H. Seinfeld (seinfeld@caltech.edu)

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Abstract. Secondary organic aerosol (SOA) yields were measured for cyclododecane, hexylcyclohexane, *n*-dodecane, and 2-methylundecane under high-NO_x conditions, in which alkyl proxy radicals (RO_2) react primarily with NO, and under low-NO_x conditions, in which RO_2 reacts primarily with HO_2. Experiments were run until 95–100 % of the initial alkane had reacted. Particle wall loss was evaluated as two limiting cases using a new approach that requires only suspended particle number-size distribution data and accounts for size-dependent particle wall losses and condensation. SOA yield differed by a factor of 2 between the two limiting cases, but the same trends among alkane precursors were observed for both limiting cases. Vapor-phase wall losses were addressed through a modeling study and increased SOA yield uncertainty by approximately 30 %. SOA yields were highest from cyclododecane under both NO_x conditions. SOA yields ranged from 3.3 % (dodecane, low-NO_x conditions) to 160 % (cyclododecane, high-NO_x conditions). Under high-NO_x conditions, SOA yields increased from 2-methylundecane $<$ dodecane $\sim$hexylcyclohexane $<$ cyclododecane, consistent with previous studies. Under low-NO_x conditions, SOA yields increased from 2-methylundecane $\sim$dodecane $<$ hexylcyclohexane $<$ cyclododecane. The presence of cyclization in the parent alkane structure increased SOA yields, whereas the presence of branch points decreased SOA yields due to increased vapor-phase fragmentation. Vapor-phase fragmentation was found to be more prevalent under high-NO_x conditions than under low-NO_x conditions. For different initial mixing ratios of the same alkane and same NO_x conditions, SOA yield did not correlate with SOA mass throughout SOA growth, suggesting kinetically limited SOA growth for these systems.

1 Introduction

Alkanes are emitted from combustion sources and can comprise up to 90 % of anthropogenic emissions in urban areas (Rogge et al., 1993; Fraser et al., 1997; Schauer et al., 1999, 2002) and 67.5 %, 56.8 %, and 82.8 % of the mass of diesel fuel, liquid gasoline, and non-tailpipe gasoline sources, respectively (Gentner et al., 2012). Upon atmospheric oxidation by OH and NO_3 radicals, alkanes form lower-volatility products that can condense as secondary organic aerosol (SOA). Ambient lifetimes against reaction with OH range, for example, from 0.5 days for *n*-hexadecane to 1.4 days for *n*-octane (Atkinson and Arey, 2003; Seinfeld and Pandis, 2006), allowing for the transport of alkanes from urban to rural areas.

SOA formation under high-NO_x conditions, in which alkyl proxy radicals (RO_2) react primarily with NO, has received much attention. Lim and Ziemann (2005, 2009a, c) developed a mechanism for linear, branched, and cyclic alkane

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oxidation that includes the formation of multi-generation oxidation products. SOA yields, defined as mass of SOA formed divided by mass of alkane reacted, have been measured in the laboratory for C_7–C_{25} alkanes with linear, branched, and cyclic structures (Lim and Ziemann, 2005, 2009b; Presto et al., 2010; Tkacik et al., 2012). In these studies, SOA yields are reported after 50–85 % of the alkane had reacted and may not represent the maximum possible yield. Generally, SOA yield was found to increase with increasing carbon number or the presence of a cyclic structure and decrease with branching of the carbon chain.

SOA formation under low-NO_x conditions, in which RO_2 reacts primarily with HO_2, has received less attention. Yee et al. (2012, 2013) developed an oxidation mechanism for *n*-dodecane and extended it to cyclic and branched compounds. Yee et al. (2012, 2013) also identified multiple generations of alkane oxidation products, and Craven et al. (2012) used positive matrix factorization to demonstrate continuous evolution of the chemical composition of SOA generated during 36 h of low-NO_x dodecane photooxidation. SOA yields for select linear and cyclic structures have been measured, and the same trends for carbon number and presence of a cyclic structure were observed under low-NO_x conditions as under high-NO_x conditions (Lambe et al., 2012).

Here we report SOA yields from 12-carbon alkanes with linear, cyclic, and branched structures under both high- and low-NO_x conditions. In each experiment, 95–100 % of the alkane, a greater percentage than those achieved in previous chamber studies, was oxidized to study the contribution of multi-generation products to SOA yield. Additionally, multiple alkane mixing ratios were used to assess the effect of precursor mixing ratio on gas-particle partitioning.

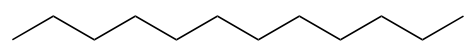
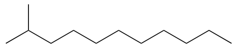
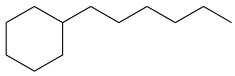
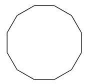
2 Materials and methods

2.1 Experimental setup

Low-NO_x experiments were conducted in the Caltech dual 28 m^3 Teflon chambers, details of which are given elsewhere (Cocker et al., 2001; Keywood et al., 2004). High-NO_x experiments were conducted in the Caltech dual 24 m^3 Teflon chambers, located in a new facility that replaced the 28 m^3 chamber facility. Most components of the old facility, including instrumentation, were moved to the new laboratory, which provides precise temperature control of the chambers (±1 °C) and flushing at a rate approximately 3 times faster than that in the 28 m^3 chamber facility. The difference in chamber volume is not expected to influence the experiment outcomes. Before each experiment, the chambers were flushed with dried, purified air for > 24 h, until the particle number concentration was < 50 cm^{-3} and the volume concentration was < 0.1 $\mu m^3 cm^{-3}$. First, hydrogen peroxide (H_2O_2, 50 % wt., Sigma Aldrich) was added to the chamber by flowing purified air over a measured volume of H_2O_2 in a glass bulb maintained at 30–35 °C. Volumes of 70 and 280 µL were used for high-NO_x and low-NO_x, experiments, respectively. Next, seed particles were injected by atomizing a 0.015 M aqueous ammonium sulfate solution. *n*-Dodecane (Sigma Aldrich, 99+ % purity), 2-methylundecane (TCI, America, > 98 % purity), or hexylcyclohexane (TCI, America, > 98 % purity) was introduced into the chamber by evaporating a known alkane liquid volume with 5 L min^{-1} of purified air. Cyclododecane (TCI, America, > 99 % purity) was introduced into the chamber by evaporating a known cyclododecane mass with 5 L min^{-1} of purified air. During each injection, the glass bulb containing the liquid or solid alkane was heated slightly to facilitate evaporation. For high-NO_x experiments, approximately 100 ppbv NO was then added to the chamber from a 510 ppmv NO in N_2 cylinder (Air Liquide). The chamber contents were allowed to mix for 1 h before beginning irradiation with 350 nm-centered UV broadband lamps (40 W Sylvania 350BL). Different light intensities were used for low- and high-NO_x experiments corresponding to $j_{NO_2} \sim 4 \times 10^{-3}$ s^{-1} and $\sim 6 \times 10^{-3}$ s^{-1}, respectively. To maintain high-NO_x conditions, 20 sccm of 510 ppmv NO was continuously injected into the chamber during the irradiation period. This additional ~ 21 L of N_2 has a negligible effect on chamber volume. The chamber contents were irradiated for 18 h and 30–36 h for high- and low-NO_x experiments, respectively, to achieve similar OH exposures in all experiments.

A suite of instruments was used to study the evolution of the gas and particle phases. Alkane mixing ratios were measured using a gas chromatograph with flame ionization detector (GC/FID, Agilent 6890N), equipped with a HP-5 column (15 m × 0.53 mm ID ×1.5 µm thickness, Agilent). Samples for injection into the GC/FID were taken by drawing 1.3 L of chamber air at a flow rate of 0.13 L min^{-3} through a glass tube packed with Tenax TA resin. The glass tube was subsequently desorbed for 10 min in the inlet of the GC/FID at 260 and 275 °C for low- and high-NO_x experiments, respectively, onto the column, held at 30 °C. After 15 min, the oven temperature was ramped at 10 °C min^{-1} to 280 °C and held at that temperature for 5 min. The mass response of the detector was calibrated for each alkane using Tenax tubes spiked with standard solutions and analyzed using the same method as the sample tubes. Relative humidity (RH), temperature, NO, NO_x, and O_3 were continuously monitored. Alkane oxidation products were detected using a custom-modified Varian 1200 triple-quadrupole chemical ionization mass spectrometer (CIMS). Details of operation can be found elsewhere (Crounse et al., 2006; Paulot et al., 2009; Yee et al., 2012, 2013). The CIMS was operated in negative mode in which CF_3O^- is used as the reagent ion. CF_3O^- clusters with the analyte, R, forming ions $[R \cdot CF_3O]^-$ at mass-to-charge ratio (m/z) $[M+85]^-$, where M is the nominal weight of R. For acidic species, the transfer product forms ions $[R \cdot F]^-$ at m/z $[M+19]^-$. Some analytes can be seen in both the cluster and

Table 1. SOA precursor and aerosol properties.

Alkane	Structure	$k_{OH} \times 10^{12\,a}$ ($cm^3\,s^{-1}$)	High-NO_x SOA density[b] ($g\,cm^{-3}$)	Low-NO_x SOA density[b] ($g\,cm^{-3}$)
n-Dodecane (Dod)		13.9[c]	1.28 ± 0.01	1.12 ± 0.03
2-Methylundecane (Mud)		13.1 ± 0.7	1.28 ± 0.01	1.12 ± 0.03
Hexylcyclohexane (Hch)		17.4 ± 0.6	1.29 ± 0.01	1.17 ± 0.03
Cyclododecane (Cdd)		14.7 ± 0.4	1.23 ± 0.02	1.28 ± 0.03

[a] Measured from a relative rate experiment at 297 K using dodecane as the reference compound. One standard deviation is given for each rate constant.
[b] SOA densities were calculated during nucleation experiments by comparing the diameter of the SOA measured by the DMA to that measured by the AMS. One standard deviation is given for each value.
[c] Jordan et al. (2008) for 298 K.

transfer product forms. The signal at each m/z represents the sum of signals from all isomers contributing to that m/z.

Aerosol size distribution and number concentration were measured continuously using a custom-built scanning mobility particle sizer consisting of a differential mobility analyzer (DMA, TSI, 3081) coupled to a condensation particle counter (CPC, TSI, 3010), henceforth referred to as the DMA. The DMA was operated in a closed-loop configuration with a recirculating sheath and excess flow of $2.67\,L\,min^{-1}$ and a 5.4 : 1 ratio of sheath to aerosol flow rates. The column voltage was scanned either from 10 to 1000 V over 100 s or 15 to 9850 V over 45 s.

Real-time particle mass spectra were collected continuously by an Aerodyne high-resolution time-of-flight aerosol mass spectrometer (AMS, DeCarlo et al., 2006; Canagaratna et al., 2007). The AMS switched between the higher resolution, lower sensitivity "W-mode" and the lower resolution, higher sensitivity "V-mode". AMS data were processed using the ToF-AMS Unit Resolution Analysis Toolkit, "SQUIRREL" (http://cires.colorado.edu/jimenez-group/ToFAMSResources/ToFSoftware/index.html), in Igor Pro Version 6.31 (Wavemetrics, Lake Oswego, OR). "V-mode" data were analyzed using fragmentation table to separate sulfate, ammonium, and organic spectra and to time-trace specific mass-to-charge ratios (Allan et al., 2004). "V-mode" and "W-mode" data were analyzed using the high-resolution spectra toolbox known as PIKA (Peak Integration by Key Analysis) to determine the chemical formulas contributing to distinct m/z ratios (DeCarlo et al., 2006). Organic ions up to m/z 305 were used to calculate elemental ratios. Craven et al. (2012) proposed formulas for organic ions with $m/z > 100$ observed for low-NO_x dodecane photooxidation SOA based on hypothesized fragmentation of products formed in the dodecane photooxidation mechanism (Yee et al., 2012). Similar analysis was applied to identify organic ions with $m/z > 100$ for SOA from all 4 alkanes investigated here under both low- and high-NO_x conditions. Organic ions CO^+ and $C_2H_4^+$ were not fit in "V-mode" due to the large interference from the N_2^+ peak, and their signals were estimated from those of particle-phase CO_2^+ and $C_2H_3^+$, respectively, using correlations determined from "W-mode" data, which has better resolution of the CO^+, N_2^+, and $C_2H_4^+$ peaks. The ratio of particle-phase CO^+ to CO_2^+ varied by experiment between 0.45 and 3.5, and a specific ratio was used for each experiment (see Table S1). The ratio of $C_2H_4^+$ to $C_2H_3^+$ was found to be 0.47 for SOA from dodecane, 2-methylundecane, and hexylcyclohexane and 0.40 for SOA from cyclododecane under both NO_x conditions. Additionally, the intensities of H_2O^+, OH^+, and O^+ were calculated from particle-phase CO_2^+ (Aiken et al., 2008). AMS data reported in this work were collected using "V-mode" and averaged over 1 h or 30 min intervals for low- or high-NO_x experiments, respectively.

Experimental OH concentrations were calculated from the measured alkane mixing ratio, the alkane concentration decay rate, estimated from the alkane mixing ratio fit to a differentiable function (typically, a 1- or 2-term exponential function), and the alkane + OH reaction rate constant. A literature OH reaction rate constant was available only for dodecane; rate constants for the other three alkanes were estimated from a relative rate experiment in which 10 ppbv of each alkane was oxidized simultaneously under low-NO_x conditions (Table 1). The measured rate constant for hexylcyclohexane is in good agreement with that calculated from structure–activity relationships (Kwok and Atkinson, 1995), $17.6 \times 10^{-12}\,cm^3\,molec^{-1}\,s^{-1}$, and the measured rate constants for 2-methylundecane and cyclododecane are lower than those calculated from structure–activity relationships,

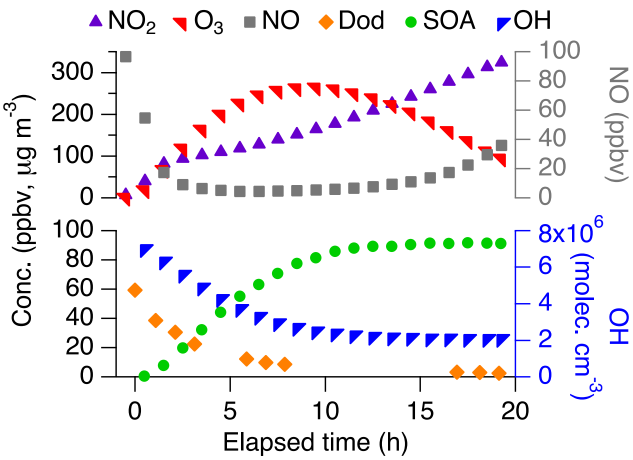


Fig. 1. Temporal trends of gas-phase species and SOA mass concentration during a typical high-NO_x experiment. On the left axis, SOA mass concentration (lower limit) is reported in $\mu g\,m^{-3}$, and dodecane, O_3, and NO_2 mixing ratios are reported in ppbv. NO and OH concentrations are given on the right axis. NO_2, O_3, NO, SOA mass, and OH concentrations are hourly averaged. Data are shown for the 57 ppbv dodecane experiment, DH2 (see Table 2). OH concentration was calculated from the dodecane decay.

13.9×10^{-12} and $17.0 \times 10^{-12}\,cm^3\,molec^{-1}\,s^{-1}$, respectively. To calculate OH exposure, an interpolated OH concentration with a time resolution of 2–3 min is calculated from a fit to experimental data, as described previously, the alkane mixing ratio decay rate, and the alkane + OH reaction rate constant. The interpolated OH concentration is multiplied by the time between data points and summed to each time point to obtain OH exposure.

Photolysis of H_2O_2 under low-NO_x conditions produced a constant OH radical concentration of $(1–3) \times 10^6\,molec\,cm^{-3}$. Under high-$NO_x$ conditions, OH radicals also were produced throughout the entire irradiation period, 18 h, with initial concentrations of $(0.7–3) \times 10^7\,molec\,cm^{-3}$ that decreased steadily to $(1–5) \times 10^6\,molec\,cm^{-3}$ after 18 h. In addition, reaction of HO_2 radicals with NO produced NO_2, which photolyzed to produce O_3. O_3 mixing ratios peaked at 200–600 ppbv approximately halfway through the experiment and then decreased as NO was continuously injected into the chamber. The variance in O_3 mixing ratio is not expected to affect SOA formation mechanisms and is discussed below. Typical vapor mixing ratios and SOA growth for a high-NO_x experiment (59 ppbv dodecane) are shown in Fig. 1.

Three oxidants, OH, O_3, and NO_3, were produced under high-NO_x conditions. All oxidant concentrations varied during the experiment due to the continuous addition of NO. While O_3 is not expected to react with most alkane photooxidation products, it can react with dihydrofurans, which also react with OH and NO_3. Variation in O_3 mixing ratios amongst the experiments could influence SOA yields by affecting the fate of dihydrofurans. In the present experiments, the ratios of dihydrofuran sinks were determined by comparing the lifetimes for dihydrofuran against reaction with OH, O_3, and NO_3 at experimental conditions. Jordan et al. (2008) estimated C_{12} dihydrofuran + OH rate constants as approximately $2.4 \times 10^{-13}\,cm^3\,molec^{-1}\,s^{-1}$. The rate constants for C_{12} dihydrofuran + O_3 and C_{12} dihydrofuran + NO_3 were taken as 3.49×10^{-15} and $1.68 \times 10^{-10}\,cm^3\,molec^{-1}\,s^{-1}$, respectively, as measured for 4,5-dihydro-2-methylfuran by Martin et al. (2002). O_3 mixing ratios were measured directly, OH concentrations were calculated from the alkane mixing ratio decay, and NO_3 concentrations were estimated from a photochemical model. The lifetime for dihydrofuran against reaction with O_3 was calculated to be at least an order of magnitude less than that against reaction with OH for all experimental conditions, and the variation in O_3 mixing ratios amongst the experiments had little effect on the fate of dihydrofurans. For the highest estimated NO_3 concentration ($1 \times 10^7\,molec\,cm^{-3}$), the lifetime for dihydrofuran against reaction with NO_3 was comparable to that against reaction with O_3, and at the lowest estimated concentration, the lifetime for dihydrofuran against reaction with NO_3 was an order of magnitude larger than that against reaction OH. In an urban area such as Mexico City with maximum OH, O_3, and NO_3 (daytime) concentrations of 4.6×10^6, $(0.74–2.0) \times 10^{12}$, and $2.4 \times 10^7\,molec\,cm^{-3}$, respectively (Molina et al., 2010; Stephens et al., 2008; Volkamer et al., 2010), the estimated lifetimes for dihydrofuran against reaction with these compounds are 15 min, 2.4–6.4 min, and 4.1 min, respectively. The conditions in the present experiments produce atmospherically relevant ratios of dihydrofuran sinks. Additionally, NO_3 was not a significant sink of either the parent alkane or RO_2 radicals even at the largest estimated NO_3 mixing ratio.

2.2 SOA yield calculations

Particles deposited to the chamber walls are accounted for when calculating the mass concentration of organic aerosol formed. Particle wall-loss corrections were made using the two limiting assumptions of gas-particle partitioning (Weitkamp et al., 2007; Hildebrandt et al., 2009; Loza et al., 2012). In one limit, no suspended vapors are assumed to condense on deposited particles. This limit is termed the lower limit because it represents the smallest possible SOA mass formed during growth. In the other limit, deposited particles are assumed to interact with suspended vapors to the same extent as suspended particles. This limit is termed the upper limit because it represents the largest possible SOA mass formed during growth. A new approach to calculate both upper and lower limit wall loss solely from suspended particle number-size distribution data is described in Appendix A. This approach is an extension of the Aerosol Parameterization Estimation model (Pierce et al., 2008) to calculate both limits to particle wall-loss corrections. Total particle volume concentration was calculated from the wall-loss corrected number-size distributions. To obtain SOA mass concentration, the seed particle volume concentration was subtracted from the total particle volume concentration, and the resulting organic particle volume concentration was multiplied by the SOA density, calculated from DMA and AMS data from a separate experiment (see Table 1).

SOA yield, Y, was calculated for both upper and lower limit SOA mass concentrations, ΔM_o ($\mu g\,m^{-3}$), using

$$Y = \frac{\Delta M_o}{\Delta HC}, \tag{1}$$

where ΔHC ($\mu g\,m^{-3}$) is the mass concentration of alkane reacted.

In addition to particle-phase wall losses, vapor-phase wall losses of 12-carbon alcohols and ketones have been observed in laboratory chambers (Matsunaga and Ziemann, 2010). If vapors condense on chamber walls instead of on particles, then SOA yields will be underestimated. Vapor wall losses were not taken into account for the yields presented here; the effect of vapor wall losses on SOA yields is discussed in Appendix B.

3 Results and discussion

For most SOA precursors, a larger initial hydrocarbon mixing ratio results in a larger source of semivolatile oxidation products, assuming that reactions occur at the same temperature and oxidizing conditions and that the vapor-phase product distributions do not vary over the range of initial hydrocarbon mixing ratios considered. The presence of more condensible products facilitates partitioning of semivolatile product species to the particle phase, leading to increased yields relative to lower mixing ratio experiments. Oxidant exposure also affects SOA yield. SOA yield increases with increasing oxidant exposure as the hydrocarbon reacts forming multiple generations of semivolatile products; however, with ever-increasing oxidation, fragmentation reactions will begin to dominate over functionalization reactions, producing volatile products that do not condense or evaporate from the condensed phase and decreasing SOA yield.

3.1 High-NO_x SOA yield measurements

Conditions for high-NO_x experiments are given in Table 2. The reported ΔM_o and yield correspond to approximately 18 h of irradiation and an OH exposure of (6–12) $\times 10^7$ molec cm^{-3} h. By this point, at least 95 % of the initial hydrocarbon had reacted. SOA growth occurred continuously as the alkane reacted. Figure 2a shows the SOA yield after approximately 18 h of irradiation as a function of hydrocarbon concentration reacted. The top and bottom of each line correspond to the upper and lower limits to the particle wall-loss correction, respectively. Experiments were

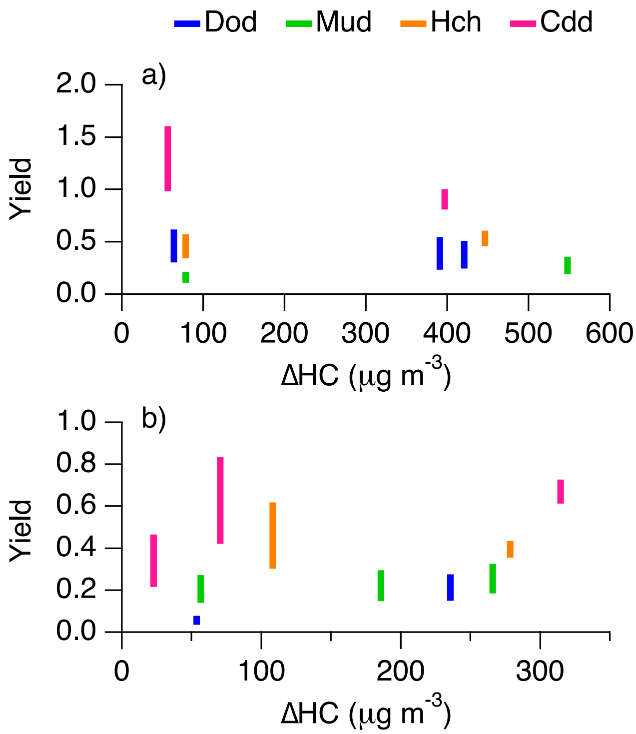


Fig. 2. SOA yield at 95–100 % of initial hydrocarbon reacted under **(a)** high- and **(b)** low-NO_x conditions. Each line shows the range between the lower limit (deposited particles do not undergo gas-particle partitioning) and upper limit (gas-particle partitioning to deposited particles is the same as that to suspended particles) SOA yields for an experiment.

run with approximately 10 ppbv (100 $\mu g\,m^{-3}$) or 60–80 ppbv (400–550 $\mu g\,m^{-3}$) initial alkane mixing ratio. In both initial alkane concentration regimes, cyclododecane produced the largest yields, while the smallest yields were observed for 2-methylundecane. Dodecane and hexylcyclohexane yields were similar. These results are consistent with the relationship between alkane structure and SOA yield observed by Lim and Ziemann (2009b) and Tkacik et al. (2012). When comparing the yields for each compound between the two initial hydrocarbon concentration regimes, no clear patterns emerge. For 2-methylundecane and hexylcyclohexane, the yield increases as initial alkane concentration increases. For dodecane and cyclododecane, the yield decreases as initial alkane concentration increases. This behavior will be discussed further in Sect. 3.4.

For cyclododecane and hexylcyclohexane, a large difference between upper and lower limit yields is observed in Fig. 2 for experiments with $\Delta HC < 100\,\mu g\,m^{-3}$. These experiments had approximately 10 ppbv initial alkane. For experiments shown in Fig. 2 with $\Delta HC > 100\,\mu g\,m^{-3}$, those with 60–80 ppbv initial alkane, SOA growth began soon after the onset of irradiation, increasing the suspended particle number-size distribution peak diameter to 250–350 nm.

Table 2. High-NO_x experimental details.

Expt.[a]	Alkane	Seed vol. ($\mu m^3\,cm^{-3}$)	NO_o[b] (ppbv)	$NO_{2,o}$[b] (ppbv)	HC_o (ppbv)	ΔHC (ppbv)	ΔM_o^c ($\mu g\,m^{-3}$)	Yield[c] (frac.)
MH1	Mud	31.7 ± 9.5	94.1 ± 0.5	6.6 ± 0.2	11.6 ± 0.4	11.6	8.5–17	0.11–0.21
MH2	Mud	41.6 ± 12.5	97.7 ± 0.5	5.8 ± 0.2	79.6 ± 2.5	79.1	100–200	0.19–0.38
DH1	Dod	30.9 ± 9.3	93.8 ± 0.5	6.3 ± 0.2	9.7 ± 0.3	9.2	19–40	0.30–0.62
DH2	Dod	26.1 ± 7.8	96.8 ± 0.5	7.1 ± 0.2	59.2 ± 1.9	56.8	91–210	0.23–0.54
DH3	Dod	30.4 ± 9.1	96.5 ± 0.5	6.1 ± 0.2	63.6 ± 2.0	61.2	100–210	0.22–0.51
HH1	Hch	34.1 ± 10.2	101 ± 0.5	2.6 ± 0.2	11.5 ± 0.4	11.5	27–45	0.34–0.57
HH2	Hch	40.0 ± 12.0	95.4 ± 0.5	2.9 ± 0.2	65.0 ± 2.1	64.9	210–270	0.46–0.61
CH1	Cdd	38.7 ± 11.6	95.6 ± 0.5	6.8 ± 0.2	8.5 ± 0.3	8.5	56–91	0.98–1.6
CH2	Cdd	37.7 ± 11.3	93.4 ± 0.5	7.9 ± 0.2	61.0 ± 2.0	58.6	320–400	0.80–1.0

[a] The first letter of each experiment identifier refers to the alkane, and the second letter refers to high- (H) or low- (L) NO_x conditions.
[b] One standard deviation is reported, as measured by the instrument manufacturer.
[c] The range of values listed correspond to the two limiting assumptions for suspended vapor-deposited particle gas-particle partitioning. The smaller and larger values correspond to the upper and lower partitioning limits, respectively.

During the experiments with ~ 10 ppbv initial alkane, SOA growth did not begin immediately, and the suspended particle number-size distribution peak diameter remained below 200 nm for most of the experiment. The temporal trend of suspended particle number-size distribution peak diameter for the high-NO_x cyclododecane experiments is shown in Fig. S1. In the Caltech chambers, particle wall-loss rate constants are lowest for 200–300 nm particles (Fig. S1, right panel). Typical seed particle number-size distribution peak diameters are 40–60 nm. Because particle growth is slower in ~ 10 ppbv initial alkane experiments and particles remain at a smaller diameter for longer times, more particles are lost to the wall before and during SOA growth in ~ 10 ppbv initial alkane experiments than in those with 60–80 ppbv initial alkane, owing to the size-dependence of particle wall loss. Therefore, a large difference between lower and upper limit yields is observed for the ~ 10 ppbv initial alkane experiments. The difference between upper and lower limit yields for dodecane and 2-methylundecane is similar for all ΔHC. Less overall SOA growth is observed for dodecane and 2-methylundecane; as a result, less difference is observed between the lower and upper limit yields.

SOA yields from cyclododecane were close to or greater than 1 depending on the wall-loss correction method used. SOA yields can be > 1 if most of the functionalized oxidation products generated from a non-functionalized parent hydrocarbon condense to form SOA. SOA yields > 1 have been observed previously from longifolene photooxidation under high-NO_x conditions (Ng et al., 2007a). To determine if the SOA mass produced violated mass conservation, an estimation of maximum potential SOA mass concentration was calculated assuming that all oxidation products formed from the reacted cyclododecane condensed. For the estimation, the average SOA molecular weight was calculated from the oxygen-to-carbon (O : C), hydrogen-to-carbon (H : C), and nitrogen-to-carbon (N : C) ratios measured by the AMS, assuming that condensed species retain 12 carbon atoms. Note that ions NO^+ and NO_2^+ are included in these calculations and will be discussed further in Sect. 3.4. To calculate the maximum potential SOA mass concentration, the molar concentration of cyclododecane reacted is multiplied by the average SOA molecular weight. This SOA mass concentration is then compared to the observed SOA mass concentration. For experiment CH1 (cyclododecane), the maximum potential SOA formed was 84 $\mu g\,m^{-3}$, which is greater than the lower wall-loss limit ΔM_o but less than the upper wall-loss limit ΔM_o. For experiment CH2 (cyclododecane), the maximum potential SOA formed was 519 $\mu g\,m^{-3}$, which is greater than both the lower and upper bound limit ΔM_o. All observed cyclododecane yields except for the upper wall-loss limit yield for CH1 do not violate mass conservation. It is likely that uncertainties in deposited particle growth rates calculated in the upper limit wall-loss correction method (see Appendix A) cause the upper limit yield for CH1 to be overestimated.

Previous studies exist of SOA yields under high-NO_x conditions for dodecane, 2-methylundecane, and cyclododecane. Lim and Ziemann (2009b) measured SOA yields for all three compounds with initial alkane mixing ratios of approximately 1 ppmv, of which 76–83 % was oxidized at the point at which yields were calculated. In the present work, yields were calculated for lower initial alkane mixing ratios with a larger fraction of the initial alkane reacted. Because higher initial alkane mixing ratio and lower extent of alkane reacted have opposite effects on SOA yield that are difficult to decouple, comparison of absolute measurements between Lim and Ziemann (2009b) and the present work are not instructive. Presto et al. (2010) reported SOA yields for dodecane oxidation for 19.1 and 57.8 ppbv initial alkane, and Tkacik et al. (2012) reported SOA yields from 2-methylundecane oxidation for a low alkane mixing ratio (initial alkane mixing ratios were not specified). Both studies parameterized yields using the volatility basis set (VBS)

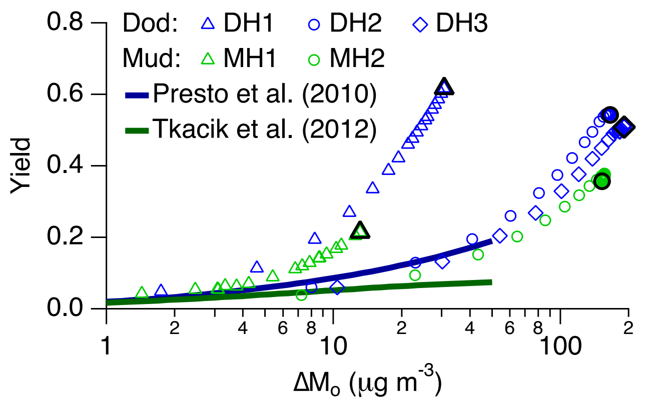


Fig. 3. Comparison of SOA yields as a function of organic aerosol mass concentration, ΔM_o, observed in the present study with those reported in previous studies. For the present study, final yields (after 95–100 % alkane reacted) are denoted by the black markers.

for $\Delta M_o < 50\,\mu g\,m^{-3}$. A comparison of the present work to these studies is shown in Fig. 3. Both Presto et al. (2010) and Tkacik et al. (2012) report the upper limit to particle wall losses. For comparison to these previous studies, the upper limit to particle wall losses and a unit SOA density were used to calculate yields for experiments DH1, DH2, DH3, MH1, and MH2 shown in Fig. 3. The dodecane VBS parameterization presented by Presto et al. (2010) matches the higher final ΔM_o dodecane experiments, DH2 and DH3, for $\Delta M_o < 50\,\mu g\,m^{-3}$; however, it does not match the lower final ΔM_o dodecane experiment, DH1. This discrepancy can be attributed to different OH exposure. Presto et al. (2010) achieved an OH exposure of approximately 1.2×10^7 molec cm^{-3} h and did not react all of the parent alkane, whereas OH exposure in the present experiments was approximately 7×10^7 molec cm^{-3} h and at > 95 % of the parent alkane reacted. Similar results are observed when comparing 2-methylundecane yields from Tkacik et al. (2012) with those in the present study. The OH exposure achieved in Tkacik et al. (2012), 6×10^6 molec cm^{-3} h, was also lower than that achieved in the present work.

3.2 Low-NO_x SOA yield measurements

Conditions for low-NO_x experiments are presented in Table 3. ΔM_o and SOA yield measurements are reported after 30–36 h irradiation, corresponding to OH exposures of (6–12) $\times 10^7$ molec cm^{-3} h, for which at least 95 % of the initial alkane reacted. Figure 2b shows the SOA yield after 30–36 h irradiation, and, as for the high-NO_x data, the top and bottom of each line correspond to the upper and lower limits to the particle wall-loss correction, respectively. The highest yields are observed for cyclododecane, followed by hexylcyclohexane, with the yields for dodecane and 2-methylundecane being similar. The ordering of hexylcyclohexane, dodecane, and 2-methylundecane yields is different from that observed under high-NO_x conditions and will be discussed further in Sect. 3.4. As with the high-NO_x yields, there are no compound-specific trends for SOA yield with initial alkane concentration.

SOA yields under low-NO_x conditions have not been reported previously for the compounds studied here. SOA yields under low-NO_x conditions have been reported for *n*-decane and *n*-pentadecane in a Potential Aerosol Mass flow reactor (Lambe et al., 2012). Lambe et al. (2012) reported maximum yields of 0.39 and 0.69 at OH exposures of 1.4×10^8 and 9.7×10^7 molec cm^{-3} h and SOA concentrations of 231 and 100 $\mu g\,m^{-3}$ for decane and pentadecane, respectively. The dodecane SOA yield is expected to lie between those for longer and shorter chain alkanes; however, the dodecane SOA yields measured in the present study (Table 3) are less than that measured for 231 $\mu g\,m^{-3}$ decane, a much larger initial concentration than those used in the present experiments, by Lambe et al. (2012) at similar OH exposure. Lambe et al. (2012) note that the maximum SOA yield for pentadecane at 16 $\mu g\,m^{-3}$ is 0.21, which is in much better agreement with the dodecane SOA concentrations and SOA yields in the present study.

3.3 SOA growth parameterization

In Fig. 3, it is interesting to note that different SOA yields are observed from the same alkane and ΔM_o for different initial alkane mixing ratios (e.g., at $\Delta M_o = 10\,\mu g\,m^{-3}$, the yield from 9 ppbv dodecane, DH1, is 0.27, whereas the yield from 57–61 ppbv dodecane, DH2 and DH3, is 0.06). This trend is observed for all four compounds under both high- and low-NO_x conditions and suggests that there may be an alternative to parameterizing yields for these alkanes in terms of ΔM_o (i.e., assuming quasi-equilibrium growth).

Shiraiwa et al. (2013) predicted that the behavior of the particle size distribution during low-NO_x dodecane photooxidation is consistent with kinetically limited, rather than quasi-equilibrium, growth. Other ambient and laboratory studies also suggest that SOA growth can be kinetically limited (Riipinen et al., 2011; Perraud et al., 2012). For kinetically limited SOA growth, SOA yield should be a function of total particle surface area; however, for the same alkane and NO_x conditions and a given particle surface area, different SOA yields were observed, similar to the results presented in Fig. 3. Instead, SOA yields were parameterized by number of semivolatile organic compound (SVOC)-particle collisions. Total SVOC concentration was simulated for the case of dodecane low-NO_x photooxidation using a kinetic multilayer model of gas-particle interactions (KM-GAP) (Shiraiwa et al., 2012; Shiraiwa and Seinfeld, 2012; Shiraiwa et al., 2013). KM-GAP explicitly resolves mass transport and chemical reactions in the gas and particle phases. The cumulative number of SVOC-particle collisions per unit chamber volume, C_{sum}, was calculated from the SVOC concentration and total particle surface area. Details of these calculations

Table 3. Low-NO_x experimental details.

Expt.[a]	Alkane	Seed vol. ($\mu m^3\,cm^{-3}$)	HC_o (ppbv)	ΔHC (ppbv)	ΔM_o^b ($\mu g\,m^{-3}$)	Yield[b] (frac.)
ML1	Mud	21.8 ± 6.5	8.5 ± 0.3	8.4	7.9–15	0.14–0.27
ML2[c]	Mud	16.7 ± 5.0	28.9 ± 0.9	28.1	28–58	0.15–0.31
ML3	Mud	15.9 ± 4.8	40.2 ± 1.3	38.1	49–86	0.19–0.33
DL1	Dod	16.7 ± 5.0	8.2 ± 0.3	7.9	1.8–4.2	0.033–0.078
DL2[c]	Dod	12.1 ± 3.6	34.0 ± 1.1	33.6	35–65	0.15–0.28
HL1[c]	Hch	11.2 ± 3.4	15.6 ± 0.5	15.5	33–70	0.30–0.65
HL2	Hch	20.0 ± 6.0	41.3 ± 1.3	40.8	99–120	0.35–0.44
CL1	Cdd	18.9 ± 5.7	3.5 ± 0.1	3.4	4.9–11	0.22–0.46
CL2[c]	Cdd	15.3 ± 4.6	10.4 ± 0.3	10.3	30–62	0.42–0.86
CL3	Cdd	21.5 ± 6.5	46.6 ± 1.5	45.1	200–230	0.61–0.73

[a] The first letter of each experiment identifier refers to the alkane, and the second letter refers to high- (H) or low- (L) NO_x conditions.
[b] The range of values listed corresponds to the two limiting assumptions for suspended vapor-deposited particle gas-particle partitioning. The smaller and larger values correspond to the upper and lower partitioning limits, respectively.
[c] Due to chamber volume limitations, these experiments were run in two parts. The initial conditions for the two separate experiments are listed Table S2.

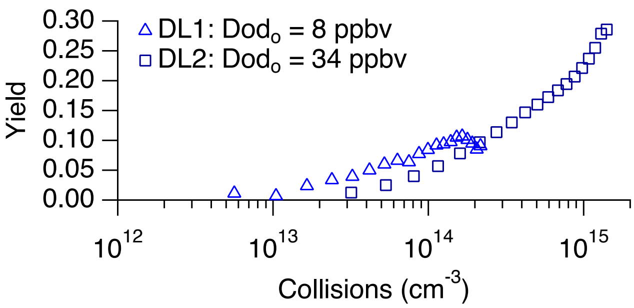


Fig. 4. SOA yield (upper limit) as a function of estimated cumulative SVOC-particle collisions per unit chamber volume for low-NO_x dodecane photooxidation experiments.

are given in Appendix C. Figure 4 shows yield as a function of C_{sum} for the dodecane low-NO_x photooxidation system. Calculations were made with a time resolution of 3 min, but hourly averaged data are displayed. The SOA yields from both experiments trend similarly with C_{sum}. This result indicates that analysis of chamber experiments for any SOA system with kinetic-flux modeling is instructive and provides an alternative to parameterizing SOA yields as a function of ΔM_o.

3.4 Aerosol chemical composition

Organonitrates have been identified previously as products from alkane high-NO_x photooxidation and are expected to be present in the particle phase (Lim and Ziemann, 2005). The AMS can detect organic nitrates as NO^+ and NO_2^+, but inorganic nitrates also contribute signal to these ions (Farmer et al., 2010). During the high-NO_x experiments, NO^+ and NO_2^+ trend with organic growth measured by the AMS. During this time, nitric acid is also formed from reaction of NO_2 with OH and can partition to particles and interact with the ammonium sulfate seed. The ratio of $NO^+ : NO_2^+$ observed during photooxidation experiments is higher than that from AMS ionization efficiency calibrations, in which ammonium nitrate is atomized into the AMS, indicating that the NO^+ and NO_2^+ signals are not likely from inorganic nitrates. Because there is evidence that the signals for NO^+ and NO_2^+ likely come from organonitrates in the present experiments, these ions are included when calculating the total organic mass from AMS data. According to a proposed decomposition pathway for organonitrates (Francisco and Krylowski, 2005; Farmer et al., 2010), the oxygens in NO^+ and NO_2^+ are not bound directly to a carbon atom. Therefore, the ion signals at NO^+ and NO_2^+ were not included in elemental ratios used to calculate average carbon oxidation state.

Average carbon oxidation state, $\overline{OS}_C$, (Kroll et al., 2011) was calculated from AMS measurements for comparison of the alkane systems. SOA $\overline{OS}_C$ from each parent alkane showed similar trends with respect to initial alkane mixing ratio, NO_x conditions, and OH exposure; therefore, data only for cyclododecane are shown in Fig. 5. Under both high- and low-NO_x conditions, SOA formed from a lower initial cyclododecane mixing ratio was characterized by a higher $\overline{OS}_C$. This trend has been observed in other systems (Shilling et al., 2009) and is expected because a higher initial alkane mixing ratio increases the mixing ratios of semivolatile products, which have lower $\overline{OS}_C$ than low volatility products, in both the gas and particle phases. Under low-NO_x conditions, SOA $\overline{OS}_C$ decreases for OH exposures of 0–2×10^7 molec cm^{-3} h and then gradually increases with increasing OH exposure. Other studies have reported similar trends for O : C formed under low-NO_x conditions (Lambe et al., 2012; Loza et al., 2012). This trend is attributed to

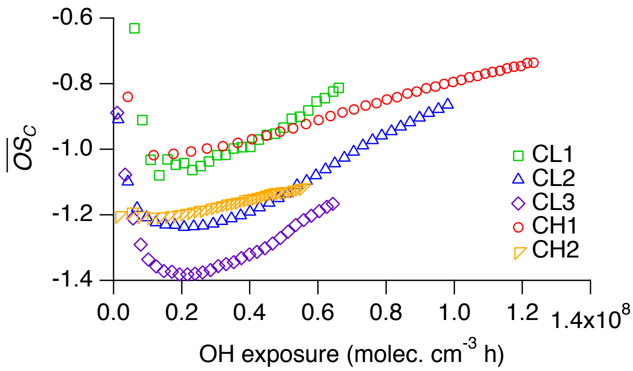


Fig. 5. SOA average carbon oxidation state as a function of OH exposure for high- and low-NO_x cyclododecane photooxidation.

initial condensation of a small amount of low-volatility oxidation products followed by condensation of semivolatile products as the SOA mass increases, and then condensation of more low-volatility products as gas-phase oxidation progresses. Under low-NO_x conditions, over 95 % of the aerosol mass measured by the AMS in the present experiments comes from ions with chemical formulae of $C_xH_y^+$, $C_xH_yO^+$, and $C_xH_yO_2^+$. Note that for both NO_x conditions, the ions O^+, HO^+ and H_2O^+ are included in the mass fraction of $C_xH_yO_2^+$ ions because these concentrations of these ions are calculated from that of CO_2^+. Initially, the contributions of ions with formula $C_xH_y^+$ are approximately equal to the sum of those with formulae $C_xH_yO^+$ and $C_xH_yO_2^+$, but as OH exposure increases to 2×10^7 molec cm^{-3} h, the contributions from ions with formula $C_xH_y^+$ begin to dominate, presumably as more semivolatile species condense. At OH exposures above 2×10^7 molec cm^{-3} h, contributions from ions with formulae $C_xH_yO^+$ and $C_xH_yO_2^+$ increase and those with formula $C_xH_y^+$ decrease but still comprise a majority of the organic mass. For low-NO_x alkane photooxidation, it has been suggested that peroxyhemiacetal formation triggers initial SOA growth (Yee et al., 2012, 2013; Shiraiwa et al., 2013). The hydroperoxides thought to contribute to initial peroxyhemiacetal formation, such as the carbonyl hydroperoxide, have multiple functional groups, which could explain the initial, higher $\overline{OS}_C$ values. As the particles grow, other, less functionalized oxidation products can also condense, decreasing $\overline{OS}_C$. As oxidation continued, multiple generations of gas-phase oxidation products, such as hydroxy carbonyl hydroperoxides and dicarbonyl hydroperoxides, were observed in dodecane photoxidation and proposed for cyclododecane photoxidation and also could partition to particles, increasing $\overline{OS}_C$. Although the proposed SOA products have multiple oxygen moities, much of the carbon chain is not functionalized, and $C_xH_y^+$ fragments are expected to dominate the mass spectrum.

Under high-NO_x conditions, an initial decrease in $\overline{OS}_C$ was not prominent, and the increase in $\overline{OS}_C$ as OH exposure increased was less when compared to that under low-NO_x conditions. When comparing high- and low-NO_x experiments with similar initial cyclododecane mixing ratio (CL2 with CH1 or CL3 with CH2), SOA formed under high-NO_x conditions has a higher $\overline{OS}_C$ during SOA growth but similar $\overline{OS}_C$ after all cyclododecane reacted. These trends indicate that less OH exposure is required to form low-volatility products under high-NO_x conditions than under low-NO_x conditions. A similar trend was observed by Presto et al. (2009), who used a thermodenuder to measure the volatility of heptadecane SOA formed under high- and low-NO_x conditions. The estimated vapor pressures of many of the condensible species produced under high- and low-NO_x dodecane photooxidation are similar (Jordan et al., 2008; Yee et al., 2012), but the experimental conditions control the rate at which these compounds are formed.

Alkane oxidation by OH generates RO_2, which can react with NO, HO_2, or another RO_2. RO_2 can also react with NO_2, but the peroxynitrates formed quickly decompose back to RO_2 and NO_2; this pathway will not be considered here. In the present experiments, RO_2 reacted primarily with HO_2 under low-NO_x conditions and with NO under high-NO_x conditions. NO mixing ratio was measured directly and varied from 2–100 ppbv, and HO_2 concentration was estimated from a photochemical model as approximately 1×10^{10} cm^{-3} (Yee et al., 2012). Using RO_2 reaction rate constants from the Master Chemical Mechanism 3.2 (http://mcm.leeds.ac.uk/MCM; Jenkin et al., 2003; Saunders et al., 2003), the lifetimes of RO_2 reaction with NO and HO_2 are estimated as 0.04–2 and 4 s, respectively. Shorter RO_2 lifetimes under high-NO_x conditions will allow low-volatility products to form at lower OH exposures.

3.5 Effect of gas-phase fragmentation reactions on SOA yield

For a number of SOA systems, SOA yields are higher under low-NO_x conditions than under high-NO_x conditions (e.g., Song et al., 2005; Ng et al., 2007a; Eddingsaas et al., 2012). A likely explanation is that alkoxy radicals (RO) produced from the reaction of alkyl peroxy radicals (RO_2) and NO undergo fragmentation to form higher volatility species, whereas hydroperoxides produced from the reaction of RO_2 and HO_2 do not. With less fragmentation under low-NO_x conditions, the carbon chain is preserved, resulting in higher yields when compared with those observed for high-NO_x conditions. For linear alkanes with > 6 carbons, isomerization of RO is favored over fragmentation reactions or reaction with O_2, preserving the carbon chain and producing compounds of lower volatility than fragmentation products (Lim and Ziemann, 2009a). As a result, yields under low- and high-NO_x conditions for these larger alkanes are similar, as shown in Fig. 2.

Additional trends between alkane structure, bulk SOA chemical composition, and SOA yield can be observed from

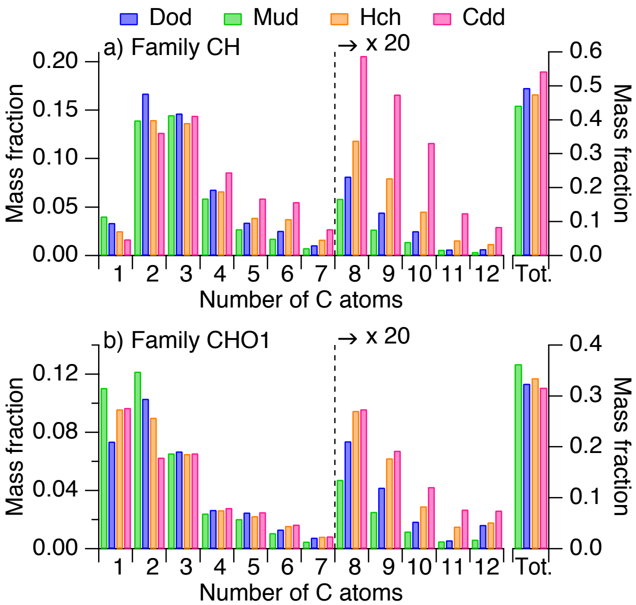


Fig. 6. Contribution of ions detected in the AMS to the bulk organic mass concentration for high-NO_x alkane photooxidation. Ions are grouped into families according to the ion atomic composition and displayed as a function of carbon atoms in the ion. Tot. is the sum over all carbon atom numbers for each family. The data represent a 30 min average of the SOA formed after 95–100 % of the initial alkane had reacted. The data presented are from experiments DH2, MH2, HH2, and CH2.

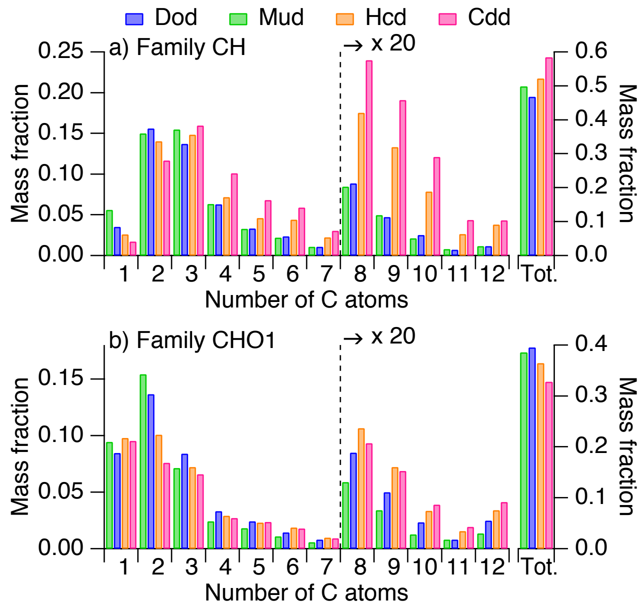


Fig. 7. Contribution of ions detected in the AMS to the bulk organic mass concentration for low-NO_x alkane photooxidation. Ions are grouped into families according to the ion atomic composition and displayed as a function of carbon atoms in the ion. Tot. is the sum over all carbon atom numbers for each family. The data represent a 60 min average of the SOA formed after 95–100 % of the initial alkane had reacted. The data presented are from experiments DL2, ML2, HL2, and CL3.

the AMS mass spectra. Ions can be grouped into "families" according to their elemental composition. The mass spectra are dominated by ions in family CH, ions with formula $C_xH_y^+$, and family CHO1, ions with formula $C_xH_yO^+$. Figures 6 and 7 show the contribution of ions in each family as a function of the number of carbon atoms in each ion and the total family contribution for a 30 min averaged sample obtained after 95–100 % of the initial alkane mixing ratio reacted. Only data from experiments with higher alkane mixing ratio (> 50 ppbv and > 25 ppbv for high- and low-NO_x, respectively) are shown; similar trends were observed in experiments with lower initial alkane mixing ratios. In the present study, an increase in yield is characterized by larger mass fractions of ions containing nine or more carbon atoms for both families CH and CHO1. Pearson's correlation coefficients for each carbon number are given in Tables S4 and S5 for family CH and family CHO1, respectively. Under high-NO_x conditions, the total mass fractions of family CH ions for cyclododecane and dodecane SOA are higher than those for 2-methylundecane and hexylcylohexane SOA (Fig. 6a), and the trend is reversed for ions in family CHO1 (Fig. 6b). The same trend is not observed under low-NO_x conditions; although, compounds with a larger mass fraction of family CH ions have smaller mass fractions of family CHO1 ions. These trends provide insight into the significance of gas-phase fragmentation reactions under high- and low-NO_x conditions.

During photooxidation, the prevalence of branching in a compound is expected to lead to increased fragmentation, requiring more functionalization to produce condensible species. Greater functionalization increases the oxygen content of product molecules, thus it is reasonable that SOA from branched compounds, 2-methylundecane and hexylcyclohexane, has a higher mass fraction of family CHO1 ions than that from compounds with less branching, cyclododecane and dodecane. These trends are not as apparent under low-NO_x conditions, suggesting that the fragmentation pathway may not be as important under low-NO_x conditions as under high-NO_x conditions. It should be noted that while fragmentation occurs for cyclododecane oxidation products, it results in ring-opening, which preserves the carbon backbone and does not produce a higher-volatility species. Hexylcyclohexane is also a cyclic compound, and an alkoxy radical on the ring α to the branch point may result in ring-opening, which preserves the carbon backbone; thus, fragmentation of hexylcyclohexane will not always result in generation of species with fewer carbon atoms than the parent molecule.

Gas-phase fragmentation products from high-NO_x alkane photooxidation were detected using the CIMS (Table S3). The proposed products have been grouped into "families" by functionality: carboxylic acid ($C_nH_{2n}O_2$), hydroxy carboxylic acid ($C_nH_{2n}O_3$), carbonyl nitrate ($C_nH_{(2n-1)}NO_4$), or hydroxynitrate ($C_nH_{(2n+1)}NO_4$), where n is the number of carbon atoms in the proposed molecule. For the CIMS ions presented here, the carbon chain is preserved as ionization occurs, whereas heating and ionization in the AMS tends to break the carbon chain, and the ions presented in Figs. 6 and 7 could come from longer chain parent molecules. Figure 8 shows the signal for each product, normalized by ΔHC for a 30 min averaged sample obtained after 95–100 % of the initial alkane mixing ratio reacted. The data are presented assuming that CIMS sensitivity is independent of n for a given family and that sensitivity is the same for all isomers (including cyclic and branched structures) for a given n and family. Mixing ratio calibrations were not performed for all species presented, and trends of ion signal with carbon number are not evaluated. Because the CIMS has unit mass resolution and can detect ions produced as transfer ($m/z = [M+19]^-$) and cluster ($m/z = [M+85]^-$) products, the signals in Fig. 8b could come from an acid or a hydroperoxide. Under high-NO_x conditions, hydroperoxide production is not expected. For almost all products shown in Fig. 8, signals in the cyclododecane experiment are lower than those for the other three alkanes, suggesting that cyclododecane oxidation products undergo little fragmentation, consistent with trends obtained from AMS data. More fragmentation of 2-methylundecane and hexylcyclohexane oxidation products is expected than for those of dodecane; however, the signal from fragmentation products for most families are similar for dodecane, 2-methylundecane, and hexylcyclohexane, suggesting that some fragmentation also occurs during dodecane high-NO_x photooxidation.

Gas-phase fragmentation reactions can also occur under low-NO_x conditions from hydroperoxide photolysis (Yee et al., 2012, 2013). Photolysis of a hydroperoxide forms an alkoxy radical, which can isomerize or decompose depending on the carbon backbone structure. For dodecane, hydroperoxide photolysis is expected to be a minor reaction pathway compared with OH oxidation. The specific case of photolysis of a hydroperoxy group adjacent to a carbonyl produces an aldehyde, which has been shown to react with hydroperoxides to form peroxyhemiacetals. Peroxyhemiacetal formation is proposed to initiate SOA growth in the alkane low-NO_x photooxidation system (Yee et al., 2012, 2013; Shiraiwa et al., 2013). In this case, fragmentation reactions depend more on the relative position of hydroperoxy and carbonyl groups than the structure of the carbon backbone.

When comparing SOA yields between low- and high-NO_x conditions for each compound (Fig. 2), three dominant trends are observed. (1) Under high-NO_x conditions, SOA yields at 95-100 % of the initial hydrocarbon reacted (i.e., the yield at the largest OH exposure for each experiment), for dodecane and cyclododecane are larger for lower initial alkane mixing ratio. (2) For hexylcyclohexane and, more noticeably, 2-methylundecane, SOA yields under high-NO_x conditions are higher when the initial alkane mixing ratio is higher. (3) SOA yields for dodecane and cyclododecane are higher under high-NO_x conditions than under low-NO_x conditions. Trends (1) and (2) arise from the role of fragmentation under high-NO_x conditions. At higher initial alkane mixing ratios, semivolatile species can condense preferentially to particles, whereas, for lower initial alkane mixing ratios, semivolatile species remain in the gas phase for further oxidation. For linear or cyclic compounds, further oxidation decreases compound volatility, resulting in additional SOA formation and higher SOA yields. However, for branched compounds, further oxidation results in fragmentation, leading to higher volatility species that do not condense to form additional SOA. At sufficiently high OH exposures, fragmentation will become important for all systems that form SOA (Lambe et al., 2012), but those conditions were not reached in the present experiments. Trend (3) results from differences in the extent of fragmentation under both NO_x conditions. Dodecane and 2-methylundecane have almost identical chemical structures, and one may expect these two compounds to have similar SOA yields. Under low-NO_x conditions, the SOA yields for experiments ML2 and DL2 are 15–31 % (however, the SOA yield observed in ML1 is higher than that observed in DL1), whereas under high-NO_x conditions, higher SOA yields are observed for dodecane than for 2-methylundecane (see Tables 2 and 3). High-NO_x SOA yields are greater than low-NO_x yields for unbranched compounds, but high- and low-NO_x SOA yields are similar for branched compounds as a result of enhanced fragmentation under high-NO_x conditions.

4 Conclusions

In the present study SOA yields have been measured for linear, cyclic, and branched 12-carbon alkanes under high- and low-NO_x conditions in which 95–100 % of the alkane reacted. The highest SOA yields were observed from cyclic alkanes, and the presence of branch points decreased SOA yield, primarily under high-NO_x conditions where vapor-phase fragmentation reactions were more likely to occur. Uncertanties arise in the SOA yield measurements due to particle and vapor wall losses and result in a factor of 2–3 difference between upper and lower limits to SOA yield. Recently, Gentner et al. (2012) assessed SOA formation from diesel and gasoline vehicles and noted that SOA yields for cyclic alkanes with five- and six-membered rings, which comprise 37 % of diesel and 11 % of gasoline, were not well-characterized. This study presents data for one such compound, hexylcyclohexane. Hexylcyclohexane SOA yield was similar to that of dodecane under high-NO_x conditions and greater than dodecane under low-NO_x conditions. Lim and Ziemann (2009b) measured SOA yields for two other branched-cyclic compounds, n-butylcyclohexane and

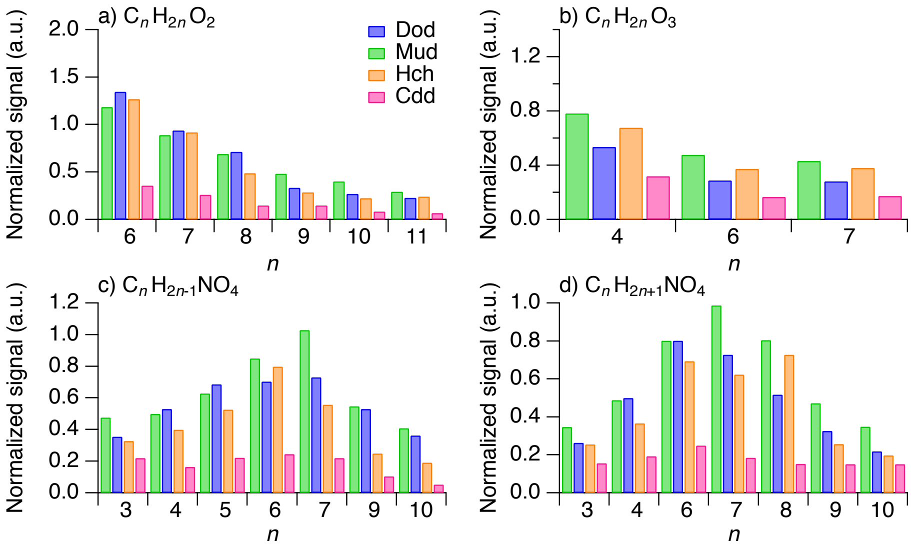


Fig. 8. Comparison of gas-phase fragmentation reaction products from high-NO_x alkane photooxidation measured by the CIMS. The signal is normalized by the mixing ratio of alkane reacted. All molecular formulae are proposed assignments. The data represent a 30 min average of gas-phase species after 95–100 % of the initial alkane had reacted. The ions monitored and their proposed chemical assignments are given in Table S3. The data presented are from experiments DH3, MH2, HH2, and CH2.

n-decylcyclohexane, under high-NO_x conditions but with initial alkane mixing ratios much higher than ambient mixing ratios, approximately 1 ppmv. The authors found that the SOA yield for butylcyclohexane was higher than that for decane, but the yield for decylcyclohexane was less than that for hexadecane. Further characterization of yields from branched-cyclic compounds is necessary to better identify trends and provide more data for models.

Although alkanes are emitted primarily in urban areas under high-NO_x oxidizing conditions, their relatively slow OH reaction rates allow for transport to rural areas with lower NO_x conditions. SOA yields measured in the present study are higher or the same under high-NO_x conditions in comparison to those measured for low-NO_x conditions. Therefore, alkanes exhibit the largest SOA formation potential in urban areas close to their sources.

Appendix A

Particle wall-loss calculations

Pierce et al. (2008) developed the Aerosol Parameter Estimation model to determine the time variance of particle wall-loss rates during an environmental chamber experiment. We have adapted this model to calculate the mass growth rate of suspended particles throughout an experiment. These mass growth rates are then applied to deposited particles to calculate lower and upper limit wall-loss corrections.

The model utilized in the current work is based on the aerosol General Dynamic Equation (Seinfeld and Pandis, 2006):

$$\frac{\partial n_s(D_p,t)}{\partial t} = \left(\frac{\partial n_s(D_p,t)}{\partial t}\right)_{\text{coag}} + \left(\frac{\partial n_s(D_p,t)}{\partial t}\right)_{\text{cond}} + \left(\frac{\partial n_s(D_p,t)}{\partial t}\right)_{\text{wl}}, \tag{A1}$$

where $n_s(D_p,t)$ ($\text{cm}^{-3}\,\text{cm}^{-1}$) is the suspended particle number-size distribution, D_p (cm) is particle diameter, t (s) is time, and coag, cond, and wl represent the change in suspended particle size-number distribution due to coagulation, condensation, and particle-phase wall loss, respectively.

The change in the suspended particle number-size distribution due to coagulation is described by

$$\left(\frac{\partial n_s(D_p,t)}{\partial t}\right)_{coag} = \frac{1}{2}\int_0^{D_p} K\left(\left(D_p^3-q^3\right)^{\frac{1}{3}},q\right) n_s\left(\left(D_p^3-q^3\right)^{\frac{1}{3}},t\right) n_s(q,t)\,\mathrm{d}q - n_s(D_p,t)\int_0^{\infty} K(q,D_p)\, n_s(q,t)\,\mathrm{d}q, \tag{A2}$$

where $K(D_{p1},D_{p2})$ ($\text{cm}^3\,\text{s}^{-1}$) is the coagulation coefficient for collisions of particles with diameters D_{p1} and D_{p2} (Seinfeld and Pandis, 2006). The DMA measures particle number-size distributions using discrete size bins, and the coagulation coefficient must also be discretized to be applied to these data. The change in suspended particle number-size distribution due to coagulation becomes

$$\left(\frac{\partial n_{\mathrm{s}}\left(D_{\mathrm{p}},t\right)}{\partial t}\right)_{\mathrm{coag}} = \frac{1}{2}\sum_{i}\sum_{j} f_{\mathrm{c}}\left(D_{\mathrm{p}i},D_{\mathrm{p}j}\right) K\left(D_{\mathrm{p}i},D_{\mathrm{p}j}\right) N\left(D_{\mathrm{p}i},t\right) N\left(D_{\mathrm{p}j},t\right) - \sum_{i} K\left(D_{\mathrm{p}i},D_{\mathrm{p}k}\right) N\left(D_{\mathrm{p}i},t\right) N\left(D_{\mathrm{p}k},t\right), \tag{A3}$$

where $f_{\mathrm{c}}\left(D_{\mathrm{p}i},D_{\mathrm{p}j}\right)$ expresses whether the collision of a particle in size bin i with a particle in size bin j produces a particle in size bin k, bounded by diameters $D_{\mathrm{p}k-}$ and $D_{\mathrm{p}k+}$:

$$f_{\mathrm{c}}\left(D_{\mathrm{p}i},D_{\mathrm{p}j}\right) = 1 \quad \text{if} \quad D_{\mathrm{p}k-} \le 2\left(\left(\frac{D_{\mathrm{p}i}}{2}\right)^{3} + \left(\frac{D_{\mathrm{p}j}}{2}\right)^{3}\right)^{\frac{1}{3}} < D_{\mathrm{p}k+} \tag{A4}$$

$$f_{\mathrm{c}}\left(D_{\mathrm{p}i},D_{\mathrm{p}j}\right) = 0 \quad \text{otherwise.} \tag{A5}$$

Particles are not allowed to form outside of the measured size range (Verheggen and Mozurkewich, 2006).

The change in suspended particle number-size distribution due to condensation is described by

$$\left(\frac{\partial n_{\mathrm{s}}\left(D_{\mathrm{p}},t\right)}{\partial t}\right)_{\mathrm{cond}} = -\frac{\partial}{\partial D_{\mathrm{p}}}\left[I\left(D_{\mathrm{p}},t\right) n\left(D_{\mathrm{p}},t\right)\right], \tag{A6}$$

where $I\left(D_{\mathrm{p}},t\right)$ ($\mathrm{cm\,s^{-1}}$) is the rate of change of particle diameter as a result of condensation. Assuming spherical particles with a density ρ_{p} ($\mathrm{g\,cm^{-3}}$) that is not a strong function of time,

$$I\left(D_{\mathrm{p}},t\right) = \frac{\mathrm{d}D_{\mathrm{p}}}{\mathrm{d}t} = \frac{2\sum J_i}{\pi D_{\mathrm{p}}^{2}\rho_{\mathrm{p}}}, \tag{A7}$$

where J_i ($\mathrm{g\,s^{-1}}$) is the mass flux of species i to the particle. J_i is defined as

$$J_i = \frac{2\pi D_{\mathrm{p}} D_i M_i}{RT} f\left(Kn,\alpha_i\right)\left(p_{\infty,i} - p_{\mathrm{s},i}\right), \tag{A8}$$

where D_i ($\mathrm{cm^2\,s^{-1}}$) is the diffusion coefficient for species i in air, M_i ($\mathrm{g\,mol^{-1}}$) is the molecular weight of species i, R ($\mathrm{g\,cm^2\,s^{-2}\,mol^{-1}\,K^{-1}}$) is the gas constant, T (K) is temperature, $f\left(Kn,\alpha_i\right)$ is a correction factor for non-continuum effects and surface accommodation effects, $p_{\infty,i}$ ($\mathrm{g\,cm^{-1}\,s^{-2}}$) is the vapor pressure of species i in far from the particle, and $p_{s,i}$ ($\mathrm{g\,cm^{-1}\,s^{-2}}$) is the partial pressure of species i at the surface of the particle. Substituting Eqs. (A7) and (A8) into Eq. (A6) yields

$$\left(\frac{\partial n_{\mathrm{s}}\left(D_{\mathrm{p}},t\right)}{\partial t}\right)_{\mathrm{cond}} = \frac{-4}{RT\rho_{\mathrm{p}}}\left[\sum_{i} D_i M_i f\left(Kn,\alpha_i\right)\left(p_{\infty,i} - p_{\mathrm{s},i}\right)\right] \frac{\partial}{\partial D_{\mathrm{p}}}\left[\frac{1}{D_{\mathrm{p}}} n_{\mathrm{s}}\left(D_{\mathrm{p}},t\right)\right] \tag{A9}$$

Here we are assuming that ρ_{p} is constant with respect to D_{p} at a given time t. If many size bins are used to describe the particle number-size distribution, then ρ_{p} is likely constant over a small range of D_{p}, and the magnitude of the error that this assumption produces is reduced. Following Pierce et al. (2008), the unknown parameters in Eq. (A9) can be combined into a single factor, F_{c} ($\mathrm{cm^2\,s^{-1}}$), defined as

$$F_{\mathrm{c}} = \frac{4}{RT\rho_{\mathrm{p}}}\sum_{i} D_i M_i f\left(Kn,\alpha_i\right)\left(p_{\infty,i} - p_{\mathrm{s},i}\right). \tag{A10}$$

Substituting F_{c} into Eq. (A9) and differentiating gives the final form for the change in suspended number-size distribution due to condensation:

$$\left(\frac{\partial n_{\mathrm{s}}\left(D_{\mathrm{p}},t\right)}{\partial t}\right)_{cond} = -F_{\mathrm{c}}\left[-\frac{1}{D_{\mathrm{p}}^{2}} n_{\mathrm{s}}\left(D_{\mathrm{p}},t\right) + \frac{1}{D_{\mathrm{p}}}\frac{\partial n_{\mathrm{s}}\left(D_{\mathrm{p}},t\right)}{\partial D_{\mathrm{p}}}\right] \tag{A11}$$

The model varies F_{c} to produce a number-size distribution that best fits the observed number distribution.

The change in suspend particle number-size distribution due to particle wall deposition is assumed to follow first-order kinetics with particle size-dependent rate constants, $\beta\left(D_{\mathrm{p}}\right)$ ($\mathrm{s^{-1}}$):

$$\left(\frac{\partial n_{\mathrm{s}}\left(D_{\mathrm{p}},t\right)}{\partial t}\right)_{wl} = -\beta\left(D_{\mathrm{p}}\right) n_{\mathrm{s}}\left(D_{\mathrm{p}},t\right). \tag{A12}$$

A theoretical determination of β is described in Crump and Seinfeld (1981) and McMurry and Rader (1985); however, parameters needed to calculate β values are difficult to quantify from theory alone for environmental chambers. Instead, β values can be determined from calibration experiments (Keywood et al., 2004; Ng et al., 2007b; Loza et al., 2012) or can be specified as unknowns in an aerosol general dynamic model (Pierce et al., 2008). The present model employs the former parameterization of β values. β values for AS particles are measured during calibration experiments in which wall deposition is the dominant process affecting the number distribution. Particles containing organics are assumed to behave the same as pure AS particles.

To implement the model, the General Dynamic Equation is solved numerically between each time step for a given experimental data set. First the General Dynamic Equation is discretized into diameter size bins corresponding to those of the measured number-size distribution. Then the model is initialized with a measured number-size distribution at time step t and a guess for the parameter F_{c}. The model is solved using a Dormand Price pair 4th and 5th order Runge–Kutta method to produce a number-size distribution at time step $t+1$. The fit of the predicted to the observed number-size distributions at time step $t+1$ is quantified using various diameter moments. The ith diameter moment is calculated as follows

$$M_i = \int_{0}^{\infty} D_{\mathrm{p}}^{i} n_{\mathrm{s}}\left(D_{\mathrm{p}}\right)\mathrm{d}D_{\mathrm{p}} = \sum_{k} D_{p,k}^{i} N_{\mathrm{s}}\left(D_{p,k}\right), \tag{A13}$$

where k is the size bin and N_s (cm^{-3}) is the suspended particle number concentration. The best fit of the predicted to the observed number distribution is that which minimizes χ^2:

$$\chi^2 = \sum_{a=1}^{9} \left(\frac{M_{i(a),p} - M_{i(a),o}}{M_{i(a),o}} \right)^2, \tag{A14}$$

where $i(a)$ is the set of diameter moments $[-1, -0.5, 0, 0.5, 1, 1.5, 2, 2.5, 3]$ and moment subscripts p and o are predicted and observed, respectively.

Once values for F_c have been estimated, they can be used in wall-loss corrections to parametrize the growth of particles lost to the chamber walls. The change in the deposited particle number-size distribution also is governed by the the aerosol General Dynamic Equation, but only wall loss and condensation process affect the number-size distribution:

$$\frac{\partial n_w(D_p,t)}{\partial t} = \beta(D_p)\, n_s(D_p,t) - F_c \omega \left[-\frac{1}{D_p^2} n_w(D_p,t) + \frac{1}{D_p} \frac{\partial n_w(D_p,t)}{\partial D_p} \right], \tag{A15}$$

where $n_w(D_p,t)$ (cm^{-3}) is the deposited particle number-size distribution, and ω is a factor that describes the extent of condensation to deposited particles. ω has a value between 0 (no condensation to deposited particles) and 1 (condensation to deposited particles is the same as that to suspended particles). ω values of 0 and 1 correspond to the lower and upper limits of particle wall-loss corrections, respectively. The aerosol General Dynamic Equations for suspended and deposited particles are solved simultaneously between each time step using the previously determined value for F_c at that time step and a constant value for ω. In the current work, wall-loss corrections were calculated with $\omega = 0$ and $\omega = 1$ to evaluate the limits of condensation behavior to deposited particles.

Appendix B

Effect of vapor wall losses on SOA yields

Condensible species can partition to suspended particles, deposited particles, and the chamber walls. The SOA yields reported here account for the first two processes, but vapor wall losses are not considered. If vapors are lost to the wall instead of forming SOA, then SOA yield will be underestimated. Matsunaga and Ziemann (2010) observed vapor wall losses for alkanes, ketones, and alcohols that are relevant to compounds formed in the present systems. The extent of vapor phase wall losses in both of the Caltech chamber facilities was investigated using experiments in which a known volume of dodecanone, dodecanol, or dodecane was injected into a chamber filled with purified air. The signal for each species was monitored over a period of several hours. Dodecane wall losses were not significant in either chamber. In the 28 m^3 chamber used for low-NO_x experiments, 2-dodecanone wall losses followed first-order kinetics with a rate constant of $k_w = 2.2 \times 10^{-6}\,s^{-1}$ ($\tau = 5.3$ days). In the 24 m^3 chamber used for high-NO_x experiments, 2-dodecanol wall losses followed first-order kinetics with a rate constant of $k_w = 1.5 \times 10^{-6}\,s^{-1}$ ($\tau = 7.7$ days). Matsunaga and Ziemann (2010) observed 20 % wall loss of 2-dodecanol in 80 min and 25 % wall loss of 2-dodecanone in 25 min, which equate to first order wall-loss rate constants of $k_w = 3.4 \times 10^{-4}\,s^{-1}$ ($\tau = 49$ min) and $k_w = 9.2 \times 10^{-4}\,s^{-1}$ ($\tau = 18$ min) for 2-dodecanol and 2-dodecanone, respectively; after the initial decrease, the 2-dodecanone mixing ratio remained constant for 400 min, presumably after equilibrium was achieved between the suspended vapors and those sorbed to the walls. Equilibrium was not observed for either compound in the Caltech chambers over a 22 h period, and it was not possible to detect rapid initial losses in the Caltech chambers as a result of the chamber setup and injection procedures. The time required to inject measurable mixing ratios of each compound into the chamber was at least 25 min, and because there is no active mixing in the Caltech chambers, it was necessary to wait an additional 20 min after the end of the injection for the chamber contents to mix. Rapid vapor wall losses occurring during this time period are difficult to distinguish from changes in compound mixing ratio due to injection and mixing. Finally, alkane photooxidation generates a variety of products with multiple functionalization; however, only singly-functionalized compounds were tested for wall loss. Matsunaga and Ziemann (2010) showed that vapor wall loss is a function of compound vapor pressure and structure; therefore, it is difficult to extrapolate wall-loss rates of 2-dodecanol and 2-dodecanone to all compounds formed from alkane photooxidation. In an attempt to quantify vapor wall losses, Shiraiwa et al. (2013) assumed vapor wall losses follow pseudo-first order kinetics and varied vapor wall-loss rate constants of SVOCs generated in KM-GAP simulations of dodecane low-NO_x photooxidation. Using $k_w = 9.6 \times 10^{-6}\,s^{-1}$, the highest value considered, led to a decrease of the SOA mass concentration by approximately 30 %. As a result, SOA yield would increase by 30 %. The combined uncertainties of vapor and particle phase wall-loss result in a factor of 2–3 difference between the upper and lower limits to SOA yields in each system.

Appendix C

SVOC-particle collision calculations

In KM-GAP, the collision flux of SVOC at the particle surface, J_A (molec $cm^{-3}\,s^{-1}$), is

$$J_A = \frac{1}{4} c_A \bar{c}_A, \tag{C1}$$

where c_A is the SVOC concentration (molec cm^{-3}) and $\bar{c}_A$ is the mean molecular speed of SVOC (cm s^{-1}). J_A can be calculated for discrete time points, i, in an experiment corresponding to particle surface area measurements. The following summation is used to calculate cumulative number of SVOC-particle collisions per unit chamber volume, C_{sum} (cm^{-3}),

$$C_{sum} = \sum_{i=1}^{n} J_{A,i} S_i \Delta t_i \,, \qquad (C2)$$

where n is the total number of data points, S_i is the particle surface area ($cm^2\,cm^{-3}$), and Δt_i is the time between data points i and $i+1$ (s). Here the upper limit wall-loss corrected surface area concentration is used to correspond to the model, which does not simulate particle wall losses.

Supplementary material related to this article is available online at http://www.atmos-chem-phys.net/14/1423/2014/acp-14-1423-2014-supplement.pdf.

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