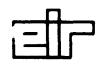
Eidg. Institut für Reaktorforschung Würenlingen Schweiz

High Temperature Reaction of Uranium Carbides and Transient Metal Chiorides in Molten Chloride Media

M. Taube, J. Strejcek, F. Dietler



Würenlingen, Juni 1973

We regret that some of the pages in the microfiche copy of this report may not be up to the proper legibility standards, even though the best possible copy was used for preparing the master fiche.

EIR-Bericht Nr. 238

HIGH TEMPERATURE REACTION OF URANIUM CARBIDES AND TRANSIENT METAL CHLORIDES IN MOLTEN CHLORIDE MEDIA

M. Taube, J. Strejcek, F. Dietler

June 1973

Contents

page

	Summary	1
1.	Introduction, objective, principles	2
2.	Experimental techniques	12
3.	Kinetics: results and discussion	15
4.	Equilibrium: results and discussion	24
5.	The Impact of the 'inert' metal chlorides	35
6.	General remarks	41

Summary

The reaction of uranium monocarbide with molten metal chlorides (AlCl₃, ZnCl₂, CdCl₂, HgCl₂, MnCl₂) in molten alkali chlorides (NaCl, KCl, RbCl, CsCl and eutectics NaCl/KCl, NaCl/CaCl₂) in temperature region between 600 to 970 ^OC in sealed silica ampules was investigated. The kinetics (half time of dissolution) and the equilibrium was measured. In the system UC/MnCl-NaCl for the equilibrium state, the concentrations of uranium in both solid and liquid phases are roughly equal, which permitted to allowed the investigation of the influence of the secondary components as small amounts of uranium oxycarbide, uranium sesquicarbide and the impact of different alkali metals ions. The activity coefficient of uranium trichloride in this media was assested.

1. Introduction, objective, principles

The aim of this paper is to discuss some particular problems concerning the kinetics and equilibrium of the reaction between uranium monocarbide and transient metal chlorides in molten chloride media in temperature range up to 1000 $^{\circ}$ C.

The reason for such a study is: (1). The development of uraniumplutonium carbide as a solid fuel for fast breeder reactors (e.g. see Schumacher 1971). (2) The possibility that pyrochemical processes might be employed with molten chloride media for reprocessing and preparation of uranium carbide fuel (Vogler, Argonne Nat. Lab. 1965, Beucherie 1966, Taube, Schumacher 1970). (3) The investigation of the properties of uranium trichloride in molten chloride media for possible use as fuel or blanket/ coolant material in a molten salt fast breeder reactor (Taube, Ligou 1972) (see also Harder, Long 1969).

The most intensive investigation of the chlorination of uranium (or thorium) carbide in molten salt media was carried out using a strong chlorination agent (Ishihara 1964) or electrolysis (Hansen 1963). In the work described in this paper the use of strong chlorination agents was abandoned since the aim was the investigation of more subtle mechanisms which can be conveniently studied near the equilibrium state, in which both in the primary solid phase (uranium monocarbide) and in the secondary liquid phase (uranium trichloride in molten alkali chloride medium), the uranium concentrations are of the same order of magnitude.

The most appropriate carriers of chlorine for these investigations are the transient metal chlorides and especially manganese dichloride. The criteria for the selection of the appropriate metal chloride are discussed later.

Only one earlier paper, so far as is known to the authors, concerns work which is close to the experiments described here. It is that of Robinson and Chictti (1964) in which a system of uranium monocarbide in molten metallic zinc media is equilibrated with molten zinc chloride in KCl/LiCl media. The use of a molten metallic phase in the equilibrium state makes this investigation less important for the present case.

In this paper the reaction of uranium monocarride with metal dichlorides is investigated, which as a first approximation can be written as follows:

$$\langle UC \rangle + \frac{3}{x}$$
 (MeCl_x) \gtrsim (UCl₃) + $\frac{3}{x}$ $\langle Me \rangle$ + $\langle C \rangle$ 1)

where 〈 〉 is solid phase
 () is liquid solution in alkali chloride medium.

The next step may be the formation of metal carbide which is represented by:

$$\langle Me \rangle + z \langle C \rangle \gtrsim \langle MeC_z \rangle$$
 2)

In some cases a further step of chlorination is possible - the uranium (III) to uranium (IV) oxidation:

$$(\text{UCl}_3) + \frac{1}{x} (\text{MeCl}_x) \geq (\text{UCl}_4) + \frac{1}{x} \langle \text{Me} \rangle$$
 3)

The uranium monocarbide used is almost always a uranium oxycarbide which influences reaction 1) in the following simplified manner:

$$\frac{y}{y-x} \langle UC_{(1-x)} \circ_{x} \rangle + \frac{3}{x} \quad (Me \ Cl_{x}) \geq (UCl_{3}) + \frac{y}{y-x} \langle UC_{(1-y)} \circ_{y} \rangle$$
$$+ \frac{3}{x} \langle Me \rangle + \langle C \rangle \qquad 4)$$

Only in extreme cases is the following reaction of uranium dioxide precipitation also possible

$$\frac{2}{2-y} \langle U \circ_{y} c \rangle + \frac{3}{x} \quad (Me \ Cl_{x}) \geq (UCl_{3}) + \frac{y}{2-y} \quad \langle Uo_{2} \rangle +$$

$$+ \frac{3}{x} \langle Me \rangle + \frac{2-2y}{2y} \quad \langle c \rangle \qquad 5)$$

but a farther conversion of uranium dioxide to uranium tetrachloride is also possible

$$\langle UO_2 \rangle + \frac{4}{x} \text{ Me Cl}_x \geq (UCl_4) + \frac{4}{x} \langle Me O_{x_2} \rangle$$
 6)

The last - but not the least important factor which influences the reactions is the components of the 'inert' media, in this case the alkali metals or the alkali earth metal chlorides. Ir the present work we investigated:

NaCl, NaCl/KCl eutectic, KCl, RbCl, CsCl and particularly NaCl/CaCl₂ eutectic.

Both the molten chlorides - the substrate $MeCl_x$ and the product UCl_3 dissolve in this molten chloride media resulting in more or less stable complexes which of course altered the equilibrium of the entire system. This effect can be represented by means of the equation

$$\langle UC \rangle + \frac{3}{x} (MeCl_x \cdot y MCl) \ge (UCl_3 \cdot y MCl) + \frac{3}{x} \langle Me \rangle + \langle C \rangle 7)$$

where MCl - inert metal chloride with, in most cases M an alkali metal.

An important role is played by the metal chlorides which influence both the kinetics and the equilibrium of the system under investigation. Where we used $HgCl_2$, $CdCl_2$, $ZnCl_2$ and $MnCl_2$ with $5d^{10}$, $4d^{10}$, $3d^{10}$ level electrons (in order of decreasing free enthalpy of formation) and $AlCl_3$ (without d electrons).

The main object of the investigation was uranium 'monocarbide', nominally UC and for part of the study also uranium sesquicarbide $UC_{1.5}$ (U_2C_3).

The temperature range of equilibrium and kinetics study was 550 $^{\circ}$ C to 970 $^{\circ}$ C.

The kinetics and equilibrium measurements were done for 1/4, 1/2, 1, 2, 4, 8 up to 24 hours or longer.

The operations being sensitive against atmospherilia were carried out in glove boxes under a controlled nitrogen atmosphere with approximately 10 ppM 0₂ and 10 ppM H₂O. In some cases the 0₂ concentration was a factor of 10 higher which could have influenced the results.

Components

The criteria for the selection of the appropriate compounds for the postulated system represented by equation 1 are as follows: The desired free enthalpy change Δ G of this reaction should be as near to zero as possible in the temperature range $600^{\circ} - 900^{\circ}$ C. Not only will the value of the equilibrium constant K be close to 1 but also the distribution ratio D for uranium, where

$$D = \frac{\text{molar fraction of UCl}}{\text{molar fraction of UC}}$$

In such a case the determination of uranium in both phases - the molten (in the form of UC1₃) and the solid (in the form of UC) will be most exact, enabling the effect of other relatively small influences (e.g. 'inactive' molten salt media) to be readily measured.

From a general point of view the electronegativity of any here choosen metal chloride should lie between a value of 1.2 (the electronegativity of uranium and plutonium) and 1.6. For higher electronegativity values the equilibrium moves towards uranium

chloride and makes the value of the equilibrium constant and ditribution ratio large and difficult to measure because of very small amounts of uranium carbide. Selection of a metal of appropriate electronegativity thus leads to a choice of the following: Mg, Al, Mn, Zn, Cd, Hg.

For the same reasons the 'inert' or non-reacting component metals were selected from those with an electronegativity no greater than 1, i.e. alkali metal chlorides NaCl, NaCl/KCl, KCl CsCl and, as an alkali earth chloride CaCl₂ (Fig. 1).

For the reaction 1, for the temperature 1100 K we can write:

RTlnK ^{1100 K} eq	=	ΔG _U - ΔG _{Me}	=	$\Delta G_{reaction}^{1100 K}$
ΔG _U	=	∆G ^{f(1100K)} (UC1 ₃)	-	∆G ^{F(1100K)} ≺UC>

$$\Delta G_{Me} = \Delta G_{MeCl}^{f(1100K)}$$

(f = formation)

Taking the value of $\Delta G_{UCl_3}^{f}$ from the recent experimental measurement and excellent critical review of Ferris (1972) and for T = 1100K

 $\Delta G_{UC1_3}^{1100K} = -605 \text{ KJ.mol}^{-1} \text{ UC1}_3$

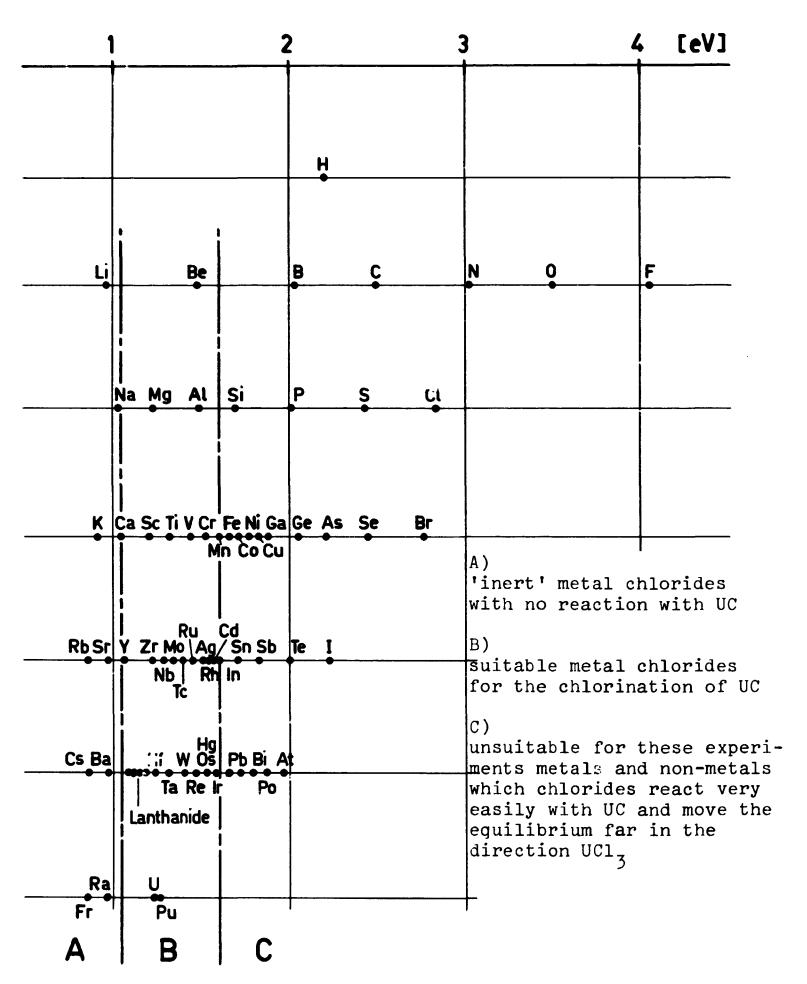


Fig. 1 Electronegativity calculated using the Allred-Rochov formula (according to Cotton, Wilkinson, 1966)

From Potter (1972)

$$\Delta G_{UC}^{1100K} = -107 \text{ KJ. mol}^{-1} \text{ UC}$$

then the change of free enthalpy

$$\Delta G_{reaction}^{1100K} = -498 \text{ KJ. mol}^{-1} \text{ U, say } \sim 500 \text{ KJ. mol}^{-1}$$

Because of the experimental techniques (fittness of analysis of uranium ir both phases) we postulate as a first approximation a concentration in both phases equal to the case where the free enthalpy of reaction is zero

$$\Delta G_{\text{reaction}}^{1100K} = 0; \quad K_{\text{eq}}^{1100K} \cong 1; \quad D_{\text{U}}^{1100K} \cong 1$$

Then the approximate metal chloride must have a free enthalpy of formation

$$\Delta G_{MeCl_{X}}^{f(1100K)} = \frac{500}{3} \text{ KJ.mol}^{-1} \text{ Cl}$$

$$\cong 167 \text{ KJ.mol}^{-1} \text{ Cl}$$

so that we could say, on the basis of data from figure 2, that (1) the following metal chlorides will shift the equilibrium so far that practically no uranium carbide will be measurable: $HgCl_2$ (Hg_2Cl_2), AgCl, $CdCl_2$, $ZnCl_2$. 2) the following will result in an equilibrium in which the uranium is present in both phases molten salt and solid (carbide) in clearly measurable amounts; $MnCl_2$, $AlCl_3$. 3) metal chlorides which practically do not react with UC in other words 'inert' salts; NaCl, KCl, RbCl, CsCl, CaCl₂ and BaCl₂ (Fig. 2).

On the basis of reaction 1 we write

$$K_{eq} = \frac{N_{UCl_3}}{N_{UC}} \cdot \frac{N_{Me}^{3/x}}{N_{MeCl_x}^{3/x}} \cdot \frac{\gamma_{UCl_3}}{\gamma_{UC}} \cdot \frac{\gamma_{Me}^{3/x}}{\gamma_{MeCl_x}^{3/x}} \cdot N_C \gamma_C \quad 8)$$

where N = molar fraction

 γ = activity coefficient

but of course

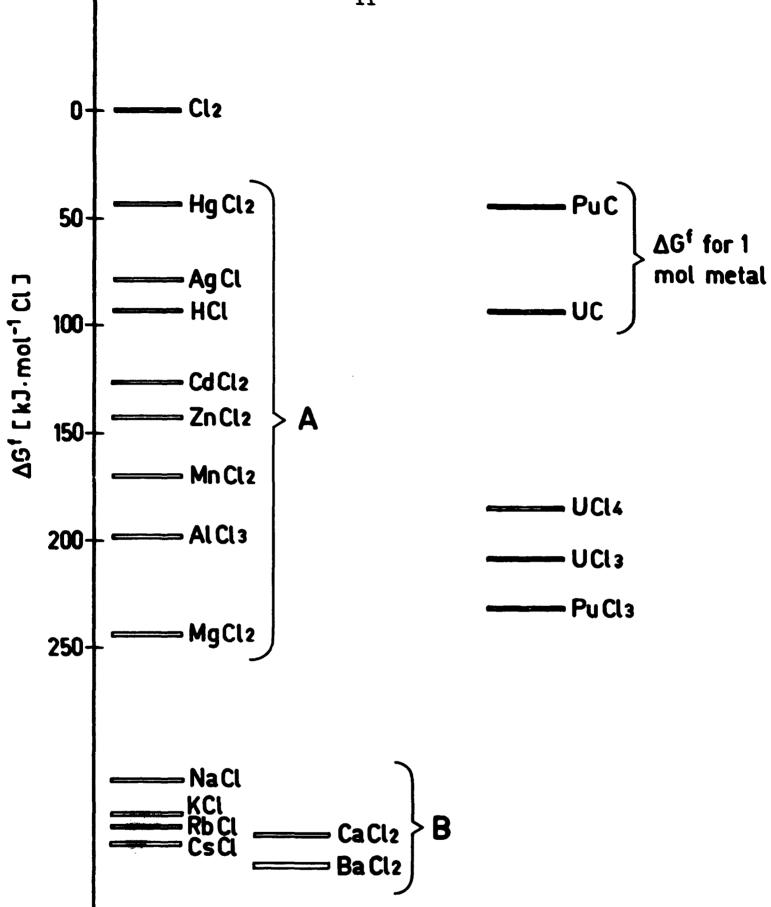
 γ_{UC} = 1; γ_{Me} = 1; γ_C = 1

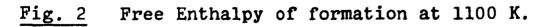
and activity coefficient quotient: $\pi_{\gamma} = \frac{\gamma UCl_3}{\frac{3/2}{\gamma MeCl_2}}$

distribution ratios:

$$D_{U} = \frac{N_{UC1_{3}}}{N_{UC}}$$

$$D_{Me} = \frac{N_{Me}}{N_{MeC1_{2}}}$$





- A) Reactive chloride metals
- B) "Inert" salt compounds

Then
$$K_{eq} = D_U \cdot D_{Me}^{3/x} \cdot \pi_{\gamma} \cdot N_C$$
 9)

If we use the following composition of substrates

 $1 \text{ mol UC} + Q \frac{3}{x} \text{ mol MeCl}_{x}$

then in equilibrium we obtain

$$(1-w) \cdot \langle UC \rangle + \frac{3}{x} (Q-w) \operatorname{MeCl}_{x} \geq w(UCl_{3}) + \frac{3}{x} \cdot w \langle Me \rangle + w \cdot \langle C \rangle$$

$$10)$$

then
$$D_U = \frac{W}{1-W}$$
 $D_{Me} = \frac{W}{Q-W}$

2. Experimental techniques

From the point of view of experimental techniques the following problems are of importance:

 The stability of the substrates and products against the container materials - in this case silica ampules e.g. (for sake of simplicity without stoichiometric coefficients)

 $UCl_3 + SiO_2 \rightarrow UO_2 + SiCl_4 + USi_3$

2) The stability of the substrates and products against the atmosphere, in this case oxygen, water vapour:

- 3) The purity of substrates, especially the readily hydrolysing and oxidising components: UCl₃, UC, MeCl_y
- 4) The selectivity of the separation methods: for instance the selective solution only of UCl₃ in the presence of uranium carbide.
- 5) The accuracy of the determination method: here the amperometric titration of uranium chlorides soluted in aqueus phase.

The problem mentioned above(II,1) of the possible interaction of UCl₃ in molten salt media with silica requires further study. McIver (1966) writes: "The most obvious choice for a vessel is silica as this does not react with UCl₃. However, if free uranium is present in the melt silica is attacked and mixtures of UO₂ and USi₃ formed."

Brown (1972) states that "uranium trichloride partially with silica at the temperature 850 $^{\circ}$ - 900 $^{\circ}$ C the product being UO₂."

In these experiments for dry substrates the reaction between UCl₃ and SiO₂ is very slow and only after 6-8 hours is the amount of UO₂ formed significant.

On point 2. the components used and the method of purification (drying) was is follows

- AlCl₃ produced by Fluka AG in sealed ampules no special purification used only for rough tests
- CaCl₂·2H₂O produced by Merck, purified as follows:

dry HCl (Molecular sieve $\cdot 4$ Å) for five hours from 20 °C up to 300 °C;

removal of HCl and cooling in the N₂ stream. (N₂ - purified with Oxisorb F, 0_2 <1 vpM, H₂O vapour < 0.5 vpM)

- Cd Cl₂, x H₂O - purified as for Ca Cl₂
$$\cdot$$
 2H₂O and dried

- Hg Cl₂ (Merck) no purification for rough checks experiments only
- MgCl₂ · 6H₂O (pro analysis, Merck) purified as for CaCl₂ · 2H₂O but a residue of MgO was left (seen as suspension in molten salt:)
- MnCl₂ · 4H₂O (pro analysis, Merck) purified as CaCl₂ · 2H₂O
- NaCl (pro analysis Merck) partially dried in vacuum and then heated after 4 hours from 20 °C up to 200 °C
- ZnCl₂ (pro analysis Merck) (SnO ~ 1,2 %) purified as CaCl₂
 2H₂O
- CaCl₂-NaCl eutectic was electrolysed with tungsten electrode
 (Ø 0.3 mm, 10 cm long) at ~ 1 volt the measured current was:

at 740 $^{\circ}$ C : 15 m A at 550 $^{\circ}$ C : 2 m A

- UC (produced by Nukem) nominal UC 0.987 dried in glove box in vacuum extractor for 1 hour our analysis gave UC 0.985 0.015.
- Silica ampule vacuum dried, 2 hours, 150 °C sealed after filling.

On point 4. For the analytical procedure a very important step is the separation of both phases: the salt phase and the chloride phase. Here we choose the method of solution in water at approx. 10 ^OC for periods of 20 minutes. This problem is partly discussed in in the literature.

Besson (1963) writes: "UC reacts readily with water only above 60 $^{\circ}$ C. The dissolution of UC in hydrochloric acid is not complete when the concentration of acid is too low". Bradley (1962) has observed during the hydrolysis of UC in water at 25 $^{\circ}$ C for 1 hour a very small gas evolution. The time required to hydrolise a 3 - 4 g irregularly shaped specimen at 25 $^{\circ}$ C was up to a week. Robinson (1964) separated UC from Zn metal by solution in HNO₃. The UC is not dissolved.

In this paper a series of hydrolyses of UC in water and aqueaous solution of HCl were made. The approximate results are shown in Fig. 3.

From these it is clear that the effect of a 20 minute attack by water or by weak solution of hydrochloric acid (to prevent the hydrolysis of uranium compounds) at 10 $^{\circ}$ C on the UC was practically negligible. The flow sheet used in the present work is shown in fig. 4.

3. Kinetics: results and discussion

The first stage in the investigation of equilibrium is of course the kinetic measurement. For this purpose the vranium carbide reaction with a series of the above mentioned metal chlorides was investigated.

The chlorination by $HgCl_2$ (Hg_2Cl_2) and $CdCl_2$ goes very rapidly. For a sample of solid uranium carbide of approx 0.5 g of irregular shape in an arbitary choosen ratio of uranium carbide to the metal chloride;

$$UC : \frac{3}{x} Q MeCl_{x}$$

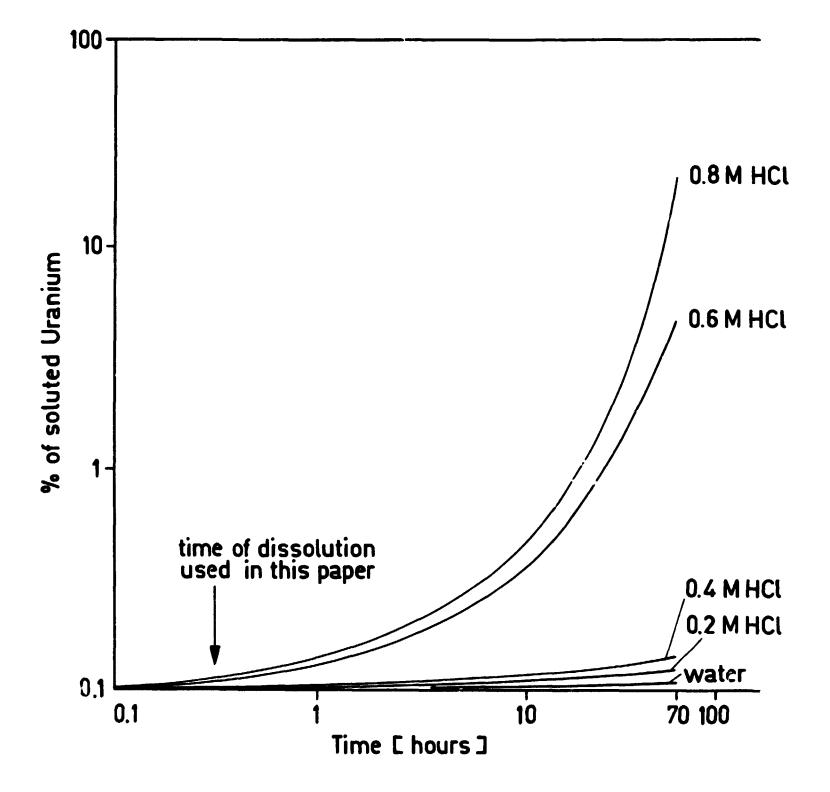


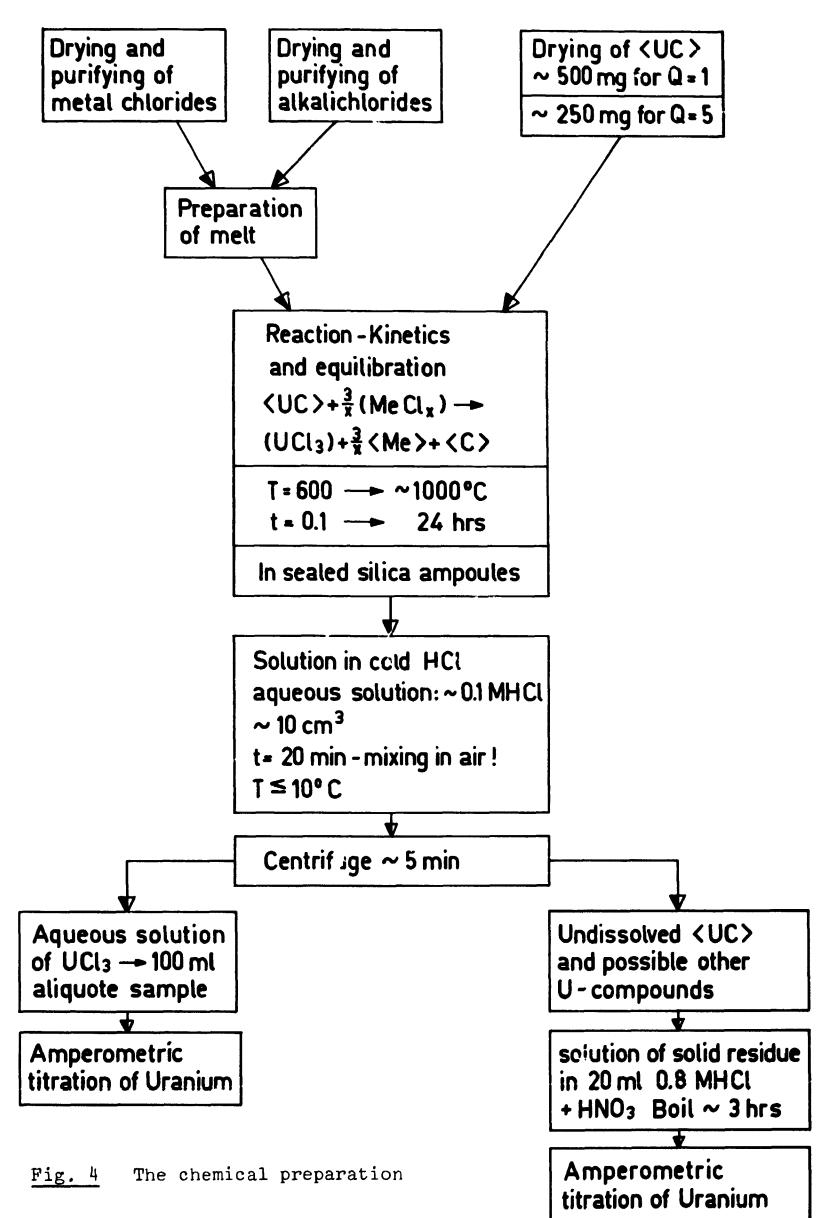
Fig. 3 The roughly estimated kinetics of solution of uranium carbides in water and low concentration aqueous HCl solutions

```
Specimen 0.5 g UC + 5 ml aqueous solution

T \cong 1)^{\circ}C \pm 5^{\circ}C

t \leq 70 hours

Numbers given represent the molarity of HCl
```



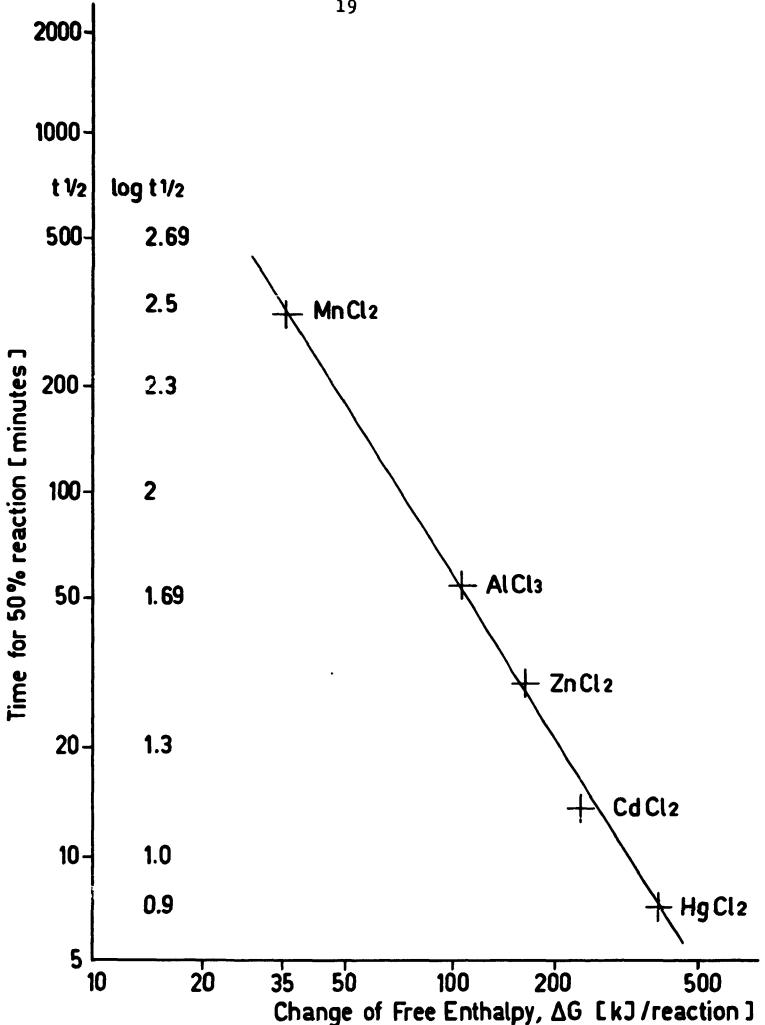
Where Q = 1 (simply stoichiometry) or Q = 1.5, in the temperature range 700 $^{\circ}$ C - 900 $^{\circ}$ C, the dissolution of approximately half of the tranium carbide occured in 10-30 minutes.

All the data cited - in fig. 5 - here are roughly interpolated from the series of experiments due to the volatility of some of the chlorides, and in sealed silica ampules they are not very reproducible.

Fig. 5 gives the results for a temperature of approximately 800 $^{\circ}$ C against the free enthalpy change of the reaction 1). The time of half dissolution t 1/2 (in minutes) is a rather simple function of the free enthalpy change of the appropriate reaction Δ G reaction (see fig. 5). For NaCl/CaCl₂ the time of dissolution was too short to be measured.

Fig. 6 shows the kinetics of the chlorination by aluminium trichloride. The approx. increase of temperature from 1000 K up to 1170 K that is the inverse temperature from 1×10^{-3} to $0.85 \times 10^{-3} \text{ K}^{-1}$ results in the half dissolution time t 1/2 for UC falling from 4.5 hours to approx 0.6 hours, that is 7.5 times faster. It must be stressed that the AlCl₃ acts in a different manner than the other metal chlorides and the reaction 4). and probably 5). may also occur, influencing the effective kinetics.

The manganese chloride (fig. 7) shows a considerable lower reaction rate, and what is of importance achieves equilibrium in a reasonable time of ~ 18 hours at 730 $^{\circ}$ C, ~ 2 hours at 900 $^{\circ}$ C, equivalent to an 9 fold increase of reaction rate in the same



Kinetics of 50 % dissolution of UC in molten chlorides media Fig. 5 at 800 °C as a function of free enthalpy changes in the investigated reaction. Q ≅ 1

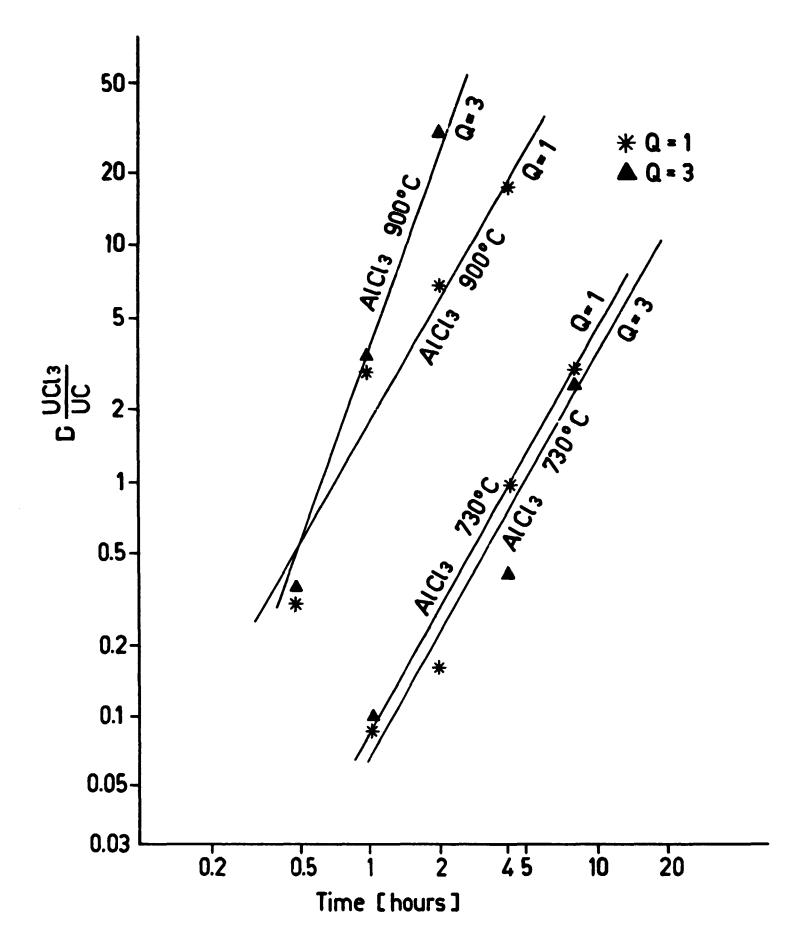
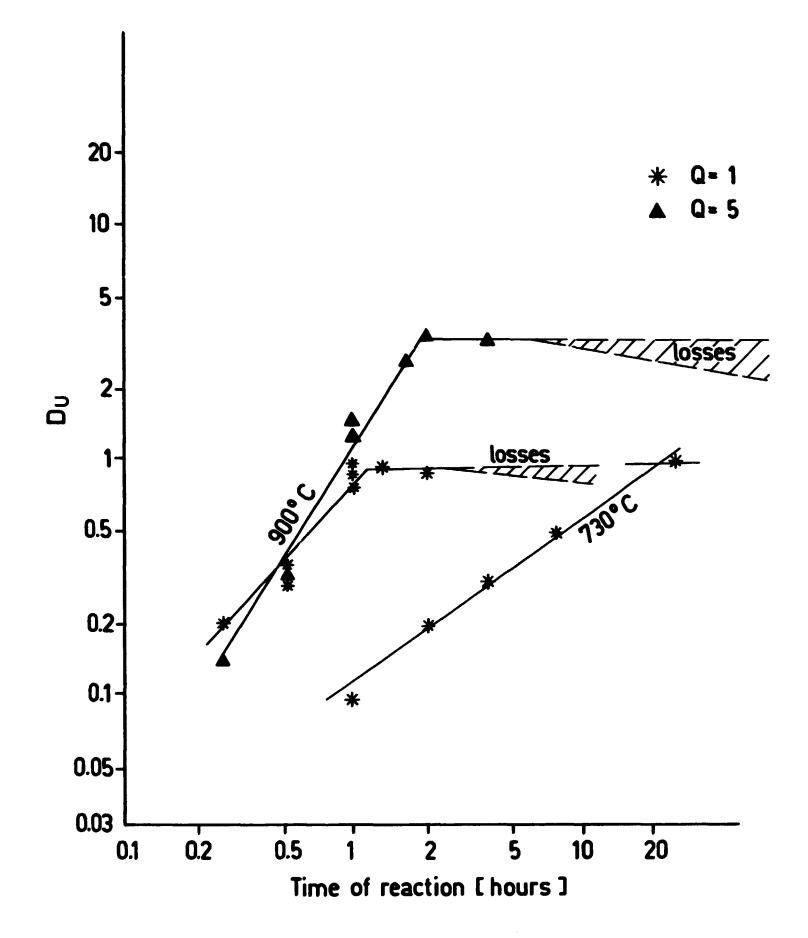
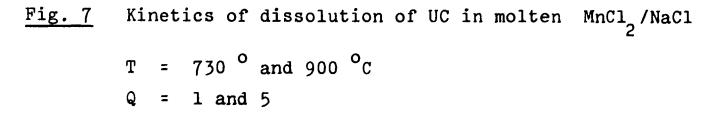


Fig. 6 Kinetics of dissolution of UC in molten $AlCl_3/NaCl$ Q = 1,3 T = 730, 900 °C





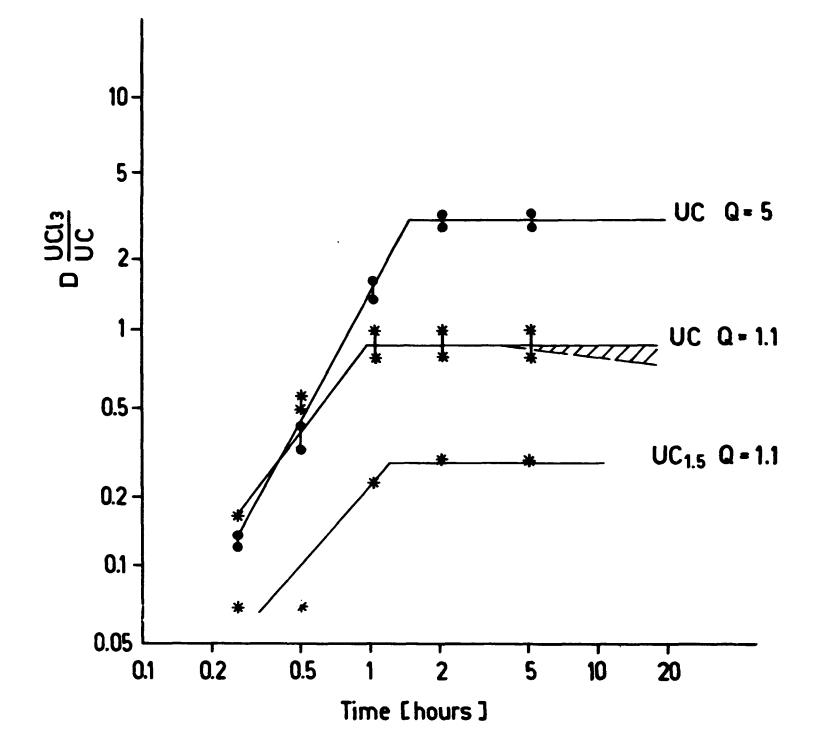


Fig. 8Kinetics of dissolution of UC and UCin molten $MnCl_2/NaCl$ 1:4T = 900 °C

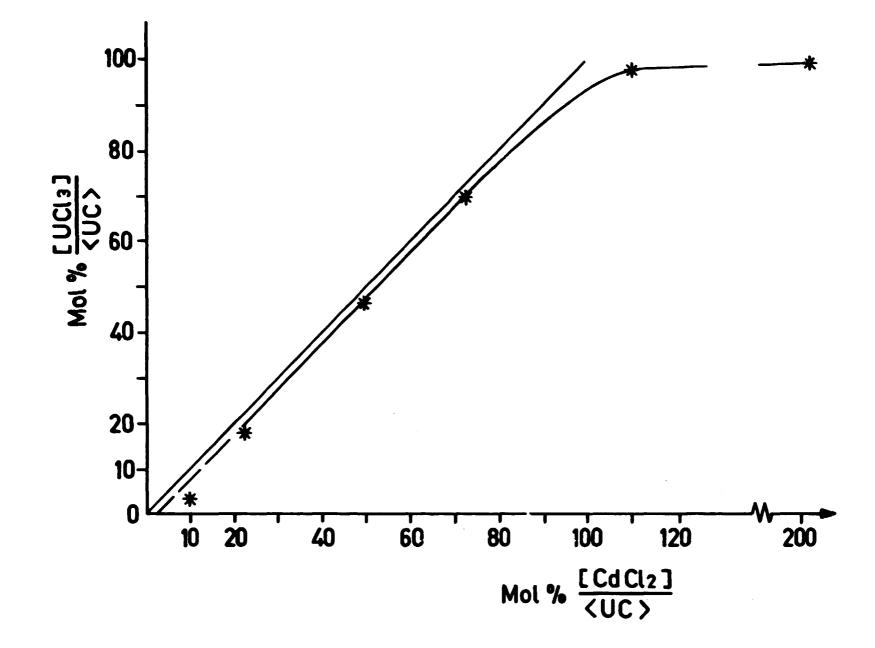


Fig. 9 The "stoichiometry" of dissolution of UC in molten CdCl₂/NaCl

T = 800 °C; t = 1/2 hour

temperature range. The clear achievement of an equilibrium state is shown in fig. 7 where the manganese dichloride was used as the chlorinating agent. Note that the kinetic slopes differ for different temperatures.

The kinetics of dissolution of uranium sesquicarbide seem to give the value of t 1/2 a factor 2.5 lower than for uranium mono-carbide when the chlorination using MnCl₂ was measured (fig. 8).

From this it is clear that for manganese dichloride the equilibrium may be achieved in a reasonable time at 1000 K after ~ 20 hours at 1170 K after ~ 2 hours. The larger reaction time is not appreciable due to loss of uranium trichloride probably from the reaction with silica.

The correctness of postulated stoichiometry of reaction 1). was measured in the case of $CdCl_{2}$ which is shown in fig. 9.

4. Equilibrium: results and discussion

The simplified reaction represented by (1) must be modified by the assessment of the impact of the metal carbides formation: reaction 2). The metals used in this work as a carrier for chlorine have a relatively small value of carbide formation.

In the case of manganese chloride the possible reaction as represented by:

 $\langle UC \rangle + \frac{3}{2}$ (MnCl₂) \gtrsim (UCl₃) + $\langle Mn_{3/2}.C \rangle$ *

* for a formal stoichiometry, not for chemical individuum.

The manganese / carbon system includes numerous compounds (Pascal 1960), the most probable in our case is the formation of Mn_3C : the stoichiometry of the reaction given above suggests such a possibility

$$\langle Mn_{3/2} \rangle + 1/2 Mn_{3} + 1/2 \rangle$$

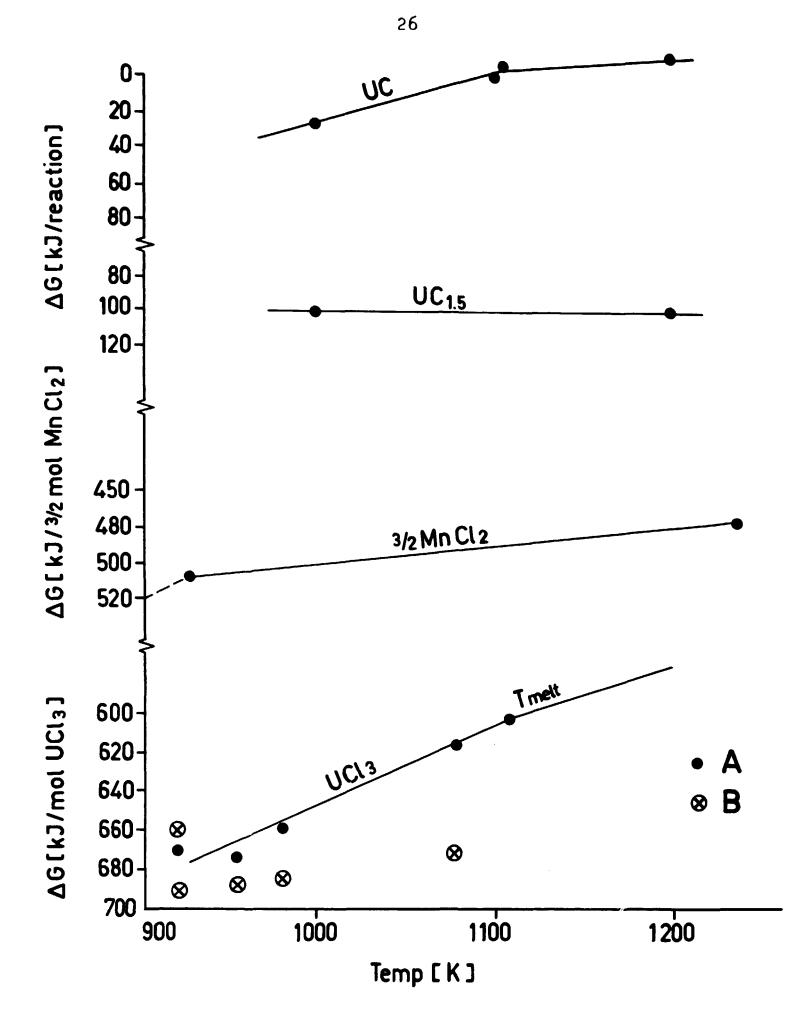
For the temperature 1000 K the free enthalpy of formation (Zefirov, 1965) equals

$$\Delta G^{f (1000 K)}_{\langle Mn_{3}C \rangle} = ~ -14 KJ. mole ^{-1} C$$

In our case the change of the full free enthalpy of reaction 2). may be assessed as approx - 7 KJ/reaction. This value is rather small and does not strongly influence the calculated equilibrium state.

This is additionally influenced by the relatively large constraints in the formation of Mn_3^C because in the system under study the metallic manganese and the free carbon are in two separated phases: the carbon (graphite) with a density ~ 2 g.cm⁻³ is floating on the surface of the molten salt (density ~ 3 g.cm⁻³). and the metallic manganese is at the bottom (density ~ 6 g.cm⁻³).

We must stress here that the change of free enthalpy for reaction 1) is rather independet of the temperature in the investigated region (900 - 1200 K). The data for the calculated values of ΔG for reaction 1) are given in fig. 10.



<u>Fig. 10</u> Calculated data of the influence of temperature on the dissolution UC and $UC_{1.5}$ in molten MnCl₂/NaCl

- A) Ferris 1972
- B) others (see Ferris 1972)

Table 1 gives the values of the distribution ratio for the equilibrium state at 900 $^{\circ}$ C in NaCl - medium. From equation (9) and (10) one can assess the activity co-efficient quotient π_{γ}

$$\pi_{\gamma} = \frac{\gamma(UCl_3)}{\frac{3}{x}} = K_{eq} / (D_U \times D_{Me}^{3/x} \cdot N_C)$$

For stoichiometric ratio 3/x MeCl_x/UC approx 1:1 we obtain

Now we arbitrarly postulate $\gamma_{(UCl_3)NaCl} \cong 1$ (for a more detailed discussion of the activity co-efficient of UCl₃ in molten chlorides media see section V) in this case we obtain

$$\gamma(MnCl_2)_{NaCl} \cong 0.63$$

But for the hypostoichiometric ratio: $\frac{3}{x}$ MeCl_x/UC \cong 5

we obtain:
$$\pi_{\gamma} = 0.74 \text{ and } \gamma_{(UCl_3)NaCl} \cong 1$$

The activity co-efficient for manganese chloride equals

<u>Table 1</u>	Value	of	dist	ributi	ion	ratio	f	or	equilibrium	state
		Т	= 9	00 °C	in	NaCl	-	eut	ectic	

Carbide UC _y (nominal)	Molar ratio: $Q = \frac{MeCl_2}{UC_y}$	Distribution ratio (precision is roughly estimated).				
UC	~ 1.1	0.95 ± 0.05				
	~ 5	3.5 ± 0.3				
^{UC} 1.5	~ 1.1	0.25 ± 0.2				

Experimental results: T = 1100 K; ΔG calcul. \cong 0; K calcul \cong 1

ୡ	D U measured	W calc.	D _{me} calc.	D _{me} ^{3/2}	N _c assessed	^π γ calc.
1	~1 (0.95± ±0.005)	~0.5	1	1	0.5	2
5	3.5 ± 0.3	~0.78	0.305	0.5	0.78	0.74

The validity of this calculation and appropriate assumptions is shown also for the reaction of manganese chloride with uranium sesquicarbide $UC_{1.5}$.

According to Potter:

$$\Delta G^{f} (UC_{1.5}) = -22240 - 1.96 T[Kcal.mol-1] (1100 - 1400)K$$

For 1100 K $\Delta G_{f}^{1100K} (UC_{1.5}) = -98 KJ.mol-1 UC_{1.5}$

The possible reaction is represented by:

$$\langle UC_{1.5} \rangle + \frac{3}{2} (MnCl_2) \gtrsim (UCl_3) + \frac{3}{2} \langle Mn \rangle + \frac{3}{2} \langle C \rangle$$

The calculated free enthalpy change of this reaction

$$\Delta G^{1100 K} = + 9 KJ$$

For all other unchanged parameters (activity coefficient etc.)

```
R Tln K = \Delta G = + 9 KJ
K <sup>1100K</sup> \cong 2.6
```

The calculated distribution ratio is

$$D_{U} (UC_{1.5}) \cong 0.37$$

The experimentely measured distribution ratio D_U (UC_{1.5}) = 0.25 ±0.2

The discrepancy between the calculated and measured results is probably due to the oxygen content in the nominal uranium sesquicarbide in the form of uranium oxycarbide (see below). The problem of oxycarbides

An important problem arises due to the occurrence of bound oxygen in so called uranium carbide which is in fact uranium oxycarbide.

In this case the reaction is as given in equation (4).

In the MnCl₂ system investigated here the reaction is probably as for equation 4 with x = 0.017 which for the sake of simplicity is taken for stoichiometry and which approximately corresponds with our substrate (see list of substrates) - and y = 0.05 which is here more or less arbitrarily choosen on the basis of the data of Anselm (see Potter 1972) concerning the U-C-O system at 1400 °C. (See also the criticism of the U-C-O system (Potter 1972.)

Our substrate is thus an oxycarbide with x = 0.017(1-x) = 0.983 and the product according to Anselm may be choosen as an oxycarbide with y = 0.05 (1-y) = 0.095 (see reaction 4) which gives

$$\frac{3}{2} \text{ UC}_{\sim 0.983} \circ_{\sim 0.017} + \frac{3}{2} \text{ MeCl}_2 \rightarrow \text{UCl}_3 + \frac{1}{2} \text{ UC}_{0.95} \circ_{0.05} + \frac{3}{2} \text{ Me} + 1 \text{ C}$$

For the sake of explanation the following ideal solution is postulated

$$UC_{0.983} O_{0.017} \ge \frac{3}{2} UC + \frac{1}{3} UC_{0.95} O_{0.05}$$

According to Potter (1972) the free enthalpy of formation of hypothetical uranium monoxide can be calculated from the reaction

$$\Delta G_{\langle UO \rangle}^{f} = \frac{1}{2} \Delta G_{\langle UO_{2} \rangle}^{f} - RTln x - (1-x)^{2}E$$

E = interaction parameter or heat therm for a regular solution;<math>E = 0 for an ideal solution x = mole fraction of UO in monoxycarbide phase.

Here we calculate for simplicity using E = 0 a value of

$$G_{UO}^{f(1100 K)} \cong 120 KJ. mol^{-1}$$

The shift of the equilibrium constant may be estimated from

RTIN K =
$$-\Delta G_{UO}^{f} - \Delta G_{UC}^{f}$$

 $\ln K^{(1100 \text{ K})} = -\frac{1}{8.3 \times 1100} (120 - 107) = \frac{-13}{9.2} = -1.4$ K = 25

which for otherwise unchanged parameters results in decreasing the distribution ratio for uranium oxycarbide to 0.04 versus approx 1 for hypothetical uranium monocarbide. Robinson (1964) observed a non scluble residue in the system UC in $Zn_{(molten)}/ZnCl_2$ (molten salt) in the form of a black uranium carbide phase in a zinc matrix without any uranium - zinc phase present but with 1.5 % ox/gen. The product of this reaction is uranium oxycarbide (equilibrium time some hours, temperature ~600 °C). The maximum fraction of the uranium in uranium carbide which could have been oxidized was 0.91. A high concentration of $ZnCl_2$ in the salt was necessary to accomplish this 91 % oxidation. So the present experiments agree with the general results of Robinson.

Some explanation for the case discussed above can be found in the short discussion of the U-C-O system by Anselm (see Potter 1972) (fig. 11).

The chlorination of UC 0 may be represented by two reactions

$$UC_{0.983}O_{0.017} \rightarrow \frac{2}{3}UC + \frac{1}{3}UC_{0.95}O_{0.05}$$

A) UC + $\frac{2}{3}$ MnCl₂ \rightarrow (UCl₃) + ...; ΔG^{1100} K \cong 0

B) $UC_{0.95}O_{0.05} + \frac{2}{3}MnCl_2 \rightarrow 0.95(UCl_3) + 0.05 \langle UO \rangle + ...;$ $\Delta G = + 13 \text{ KJ mol}$

According to our kinetics investigation the reaction A has a higher rate and of course, also a greater equilibrium constant. This results in a faster and more complete chlorination of the hypothetical uranium monocarbide than that of the monoxycarbide $UC_{0.95} = 0.05$ (Fig. 11).

The reaction between uranium oxycarbide and aluminium chloride may follow the reaction (5) because of the much higher free enthalpy formation of aluminium oxide than that for the chlorides (according to Zefirov 1965)

$$\Delta G_{A1_2O_3}^{f(1100 \text{ K})} = 450 \text{ x } 1.5 = -675 \text{ KJ mol}^{-1} \text{ Al}$$

$$\Delta G_{A1C1_3}^{f(1100 \text{ K})} = 185 \text{ x } 3 = -555 \text{ KJ mol}^{-1} \text{ Al}$$

$$\Delta G_{A1}^{1000 \text{ K}} = \Delta G_{A1_2O_3}^{f} - \Delta G_{A1C1_3}^{f} = -120 \text{ KJ mol}^{-1} \text{ Al}$$

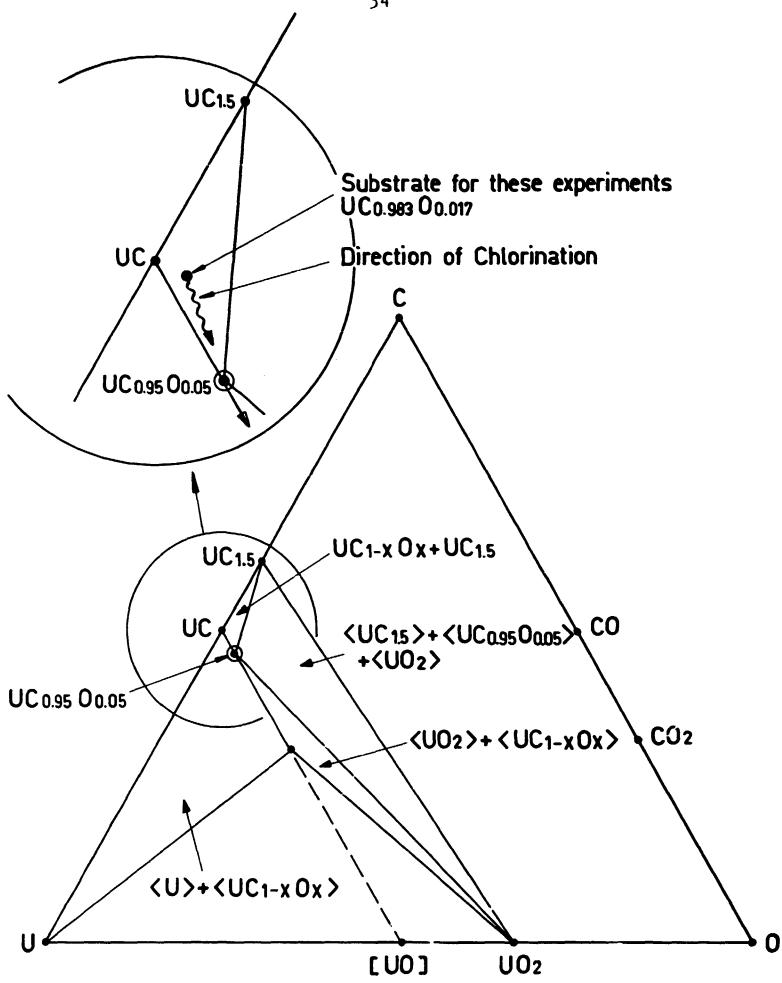
and the same values for uranium (simplified without oxidation).

$$\Delta G_{UO}^{f(1000 K)} \cong 475 \times 1.5 = 710 \text{ KJ mol}^{-1} \text{ U}$$

$$\Delta G_{UC1_3}^{f(1000 K)} \cong 155 \times 4.18 = 650 \text{ KJ mol}^{-1} \text{ U}$$

$$\Delta G_{UC1_3}^{1000} = \Delta G_{UC1_3}^{f(1000 K)} - \Delta G_{UO_{1.5}}^{f(1000 K)} = -60 \text{ KJ mol}^{-1} \text{ U}$$

Following equations 5) and then 6)



<u>Fig. 11</u> Phase diagram U-C-0 Anseln ~1400 ^OC (According to Potter 1972)

$$\frac{2}{2-0.017} \quad \langle UO_{0.017} \quad C_{0.983} \rangle + (A1C1_3 \ge (UC1_3) + \frac{0.017}{2-0.017} \langle UO_2 \rangle \\ + \langle Me \rangle + \frac{2-2x \ 0.017}{2 \ x \ 0.017} \quad \langle C \rangle$$

without stoichiometric coefficient for the sake of simplicity

$$\langle u0_2 \rangle + (A1C1_3) \ge (UC1_3) + \langle A1_20_3 \rangle$$

5. The Impact of the 'inert' metal chlorides

The reactions governing the chlorination of uranium carbide discussed above is of course, influenced by the properties of the molten salt medium. In this investigation the following 'inactive' alkali metal and alkali earth metal chlorides were used. NaCl, NaCl/KCl eutectic, KCl, RbCl, CsCl and NaCl/CaCl₂ eutectic.

The influence of these metal chlorides arises from two mechanisms:

- 1) interaction with the UCl₃ which is the product
- 2) interaction with the MnCl₂ the substrate.

The UCl₃ - MeCl_x system was rather intensely investigated but most of the published experiments have been carried out in LiCl/KCl eutectic, which because of the peculiar properties of the small cations of lithium is rather irrelevant to the studies made for this paper. We need only say that UCl₃ in this eutectic at ~500 $^{\circ}$ C has a positive deviation from ideal, the activity coefficient being of the order of 10 for low concentrations of UCl₃ (for literature see Hardy 1966). The activity of UCl₃ in NaCl/KCl eutectic (Flenglas 1962) is reasonably close to that above.

The more exact measurements (Hardy 1966) of the system UCl₃/NaCl shows a positive deviation from ideal: the activity coefficient is essentially greater that 1. The deviation from the ideal is lower, if the temperature is higher and is extremely sensitive to temperature changes. The deviation is lower at lower concentrations but according to Kertes (1971) in all system studied (UCl₃, UCl₄..) the activity coefficients are reasonably constant over the concentration range - usually below 0.01 mol fraction. Also the results of Krahe (1965) show a positive deviation for the UCl₃ solid /LiCl - KCl system. Harder, Long and Steinaway in their recent publication (1969) estimate the activity coefficient for UCl₃ in NaCl as excess partial molar free enthalpy

RT ln γ (UCl₃) [Kcal mol⁻¹]:

from UCl₃ liquidus data: - 1.9 from the U/UCl₃ potential: - 3.0

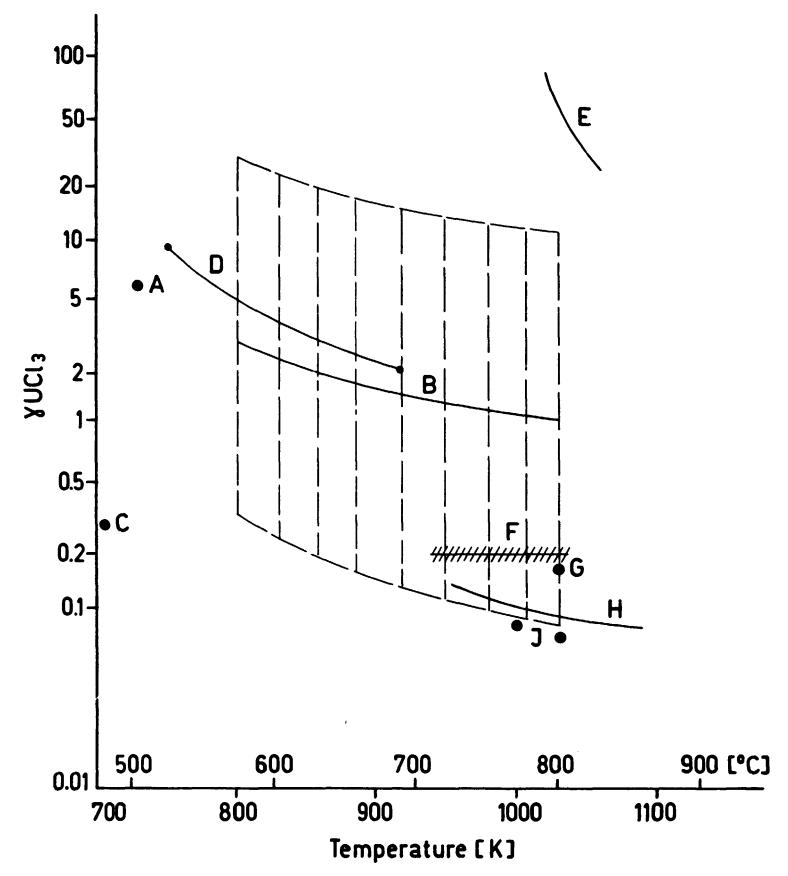
average for UCl₃ in relation to PuCl₃, CeCl₃ and the above data: -2.7 ± 0.6

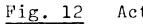
for 0.3 mol fraction UCl₃ in NaCl/UCl₃. Over the temperature range 600 - 800 $^{\circ}$ C the average value for the activity coefficient of UCl₃ is therefore 0.25 ± 0.10. Some additional information may be obtained from the phase diagrams of UCl₃/ MeCl_x, but it must be stressed that such derivations are not sufficiently conclusive to prove the existence of complex compounds and, therefore, the excess enthalpy. A sharp maximum at the melting point is highly indicative of the formation of a complex compound, a less pronounced maximum simply means a complex of lower thermodynamic stability (Kertes, 1971).

From the point of view of complex formation the $PuCl_3$ systems are similar to those of UCl_3 as far as the composition of the double salts and their melting characteristics re concerned.

Usually there is no intermediate compound with NaCl. The UCl₃/NaCl system gives an eutectic.

For the UCl₃ system it seems that a cautious examination of the phase diagrams points to the existence of two compounds, K_2 UCl₅ and K_3 UCl₆ (see Bagnall, 1969). From this it can be concluded that the activity coefficient for UCl₃ is essentially lower than 1. In addition PuCl₃ has an activity coefficient in the KCl medium lower than that for the NaCl system (Pascal 1960, p. 390) (Fig. 12).





Activity coefficient of UCl₃ in molten chlorides

- A) Partridge 1961 UC1/KC1
- B) Ferris LiCl ∞ dilution $\lg \gamma_{UCl_3} = 2.18 + 2190_4 \pm 1$
- C) Inman 1961 UC1/KC1
- D) Knoch, Krahe LiCl/KCl dilute

- E) Hardy 1966 in NaCl
- F) Harder, Long 1969 NaCl
- G) Knoch 1967 MgCl₂
- H) Flenglas 1961 KC1/NaC1
- J) Knoch 1967 MgCl₂/NaCl/KCl

The impact of MnCl₂ activity

The system under investigation at equilibrium is a tertiary system (e.g. $UCl_3/MnCl_2$ / MeCl where Me is an alkali metal) which may also be described as quasi-binary system Me_xUCl_{3+x} Me_yMnCl_{2+y}. The case for Mn_zUCl_{3+2z} seems much less likely because the Mn⁺² with a half filled d-electron shell and with a radius of 9 nm has the relation $R_{MnCl_2}/R_{Cl} = 0.50$ which results in the octahedral co-ordination $MnCl_6^{-3}$. U⁺³ in a chloride medium has the same tendency for octahedral coordination: UCl_6^{-3} . The cation partner is probably MeCl in both cases. The systems of MnCl₂/NaCl, MnCl₂/KCl and MnCl₂/ CsCl are investigated by Seifert (1966). Among others the following melting compounds were found KMnCl₃, NaMnCl₃.

Of course one must treat these assumptions made from the phase diagrams concerning complexion in the liquid phase with some caution. But according to Sandannini (see Lumsden 1966) the NaCl₃/MnCl₂ molten system was investigated and the deviations from ideality in this system found

R T ln $\gamma = -14000 (1-N_{Na}^{+})^2 / (2 - Na^{+})^2$ cal

and for NaCl : MnCl₂ 1:1

R T ln $\gamma \cong 1000$ cal $\cong 4180$ J

which for T \cong 1100 ° results in $\gamma \cong 0.2$

Lumsden (1966) believes that the interaction here is so strong that it cannot be assumed that the equation given above for γ applies over the whole range of compositions.

For the system NaCL/MnCl₂ our calculation of the activity coefficient according to the Bogacz and Trzebiatowski (1956) methods (see also Ferris, 1972)

$$\log_{1} = \ln N_{1} + \ln \gamma_{1} = -\frac{\Delta H_{fi}}{R} \left(\frac{1}{TO} - \frac{1}{T}\right) + -\frac{\Delta C_{pi}}{R} \left(\frac{TO}{T} - 1 + \ln \frac{T}{TO}\right)$$

where To = melting point of component i
T = melting point of the eutectic here =
$$428 \, ^{\circ}C$$

R = Gas constant
 ΔC_{pi} = difference of the molar heat of the crystaline
component i on melting
 ΔH_{fi} = heat of fusion of component i

- gives for the excess free enthalpy

 $\Delta G_{T}^{excess} = RTln \Upsilon \cong 5420 \text{ KJ mol}^{-1}$

which is in good agreement with the above data.

From this it seems that the activity coefficient of MnCl₂ in molten chlorides is close to 1 since as stated by Ferris (1972) the activity coefficient for the uranium trichlorides which must be taken into account is about

 $lg\gamma_{UC1_{3}} = 0 \pm 1$ that is $10^{-1} < \gamma < 10$ The experimental results of the impact of the metal chlorides investigated here are given below (Fig. 13).

In the series of alkali/metal chlorides: Na, (Na-K), K, Cs, the decrease of distribution ratio is clearly seen which could be interpreted that the activity coefficient quotient:

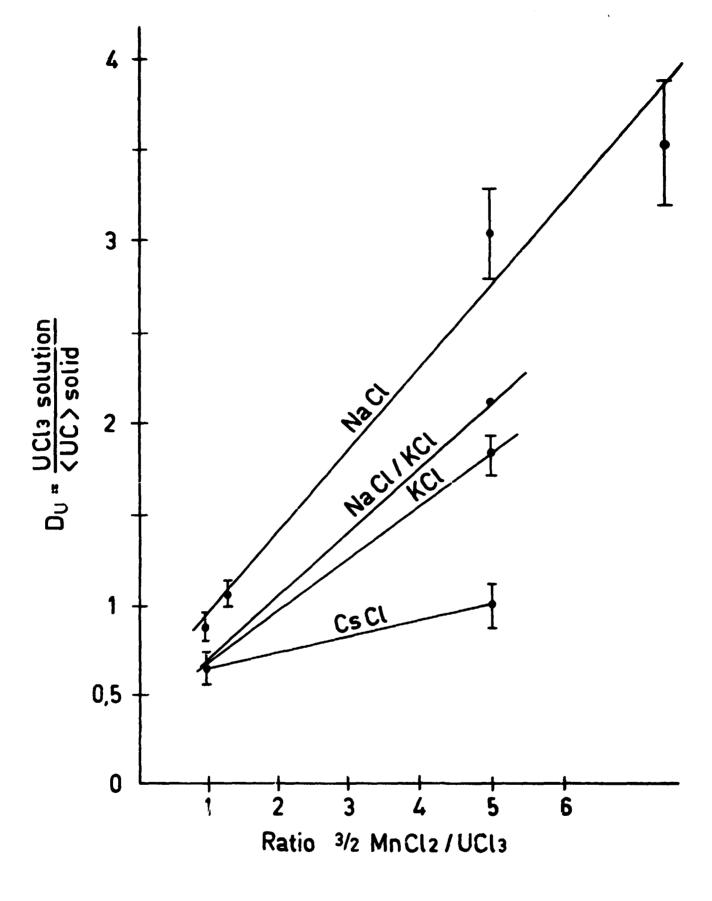
$$\pi_{\gamma} = \frac{UCl_3}{MnCl_2}$$

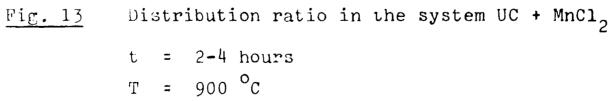
is relatively strongly influenced by the alkali metal component. If the ionic radius increase the distribution ratio decrease and the activity coefficient quotient increases. This is possible when $\gamma_{\rm UCl_3}$ increases and/or $\gamma_{\rm MnCl_2}$ decreases.

6. General remarks

The chlorination of nominal uranium monocarbide in molten chlorides media is influenced by several parameters

- the rate of chlorination increases a bout 100 times (from 500 min to 5 min at 800 $^{\circ}$ for half dissclved UC) if the value of the free enthalpy change for the given metal chlorides changes from 25 KJ per reaction to more than 400 KJ per reaction - that is 16 times.
- the equilibrium state with K ≅ 1 is for T = 1100 K
 achieved for the system UC/MnCl₂ in molten NaCl.





- the thermodynamic data for UCl₃ from Ferris (1972) and UC, UC_{1.5} UO_xC_{1-x} from Potter (1972) are in good agreement with our results, if the appropriate activity coefficient of UCl₃ and MnCl₂ in molten alkali metal chlorides are between 0.1 and 10.
- the presence of uranium monoxycarbide strongly influences the equilibrium obtained for these chlorination reagents which have relatively low free enthalpy of formation e.g. MnCl₂ but not for strong chlorination agents; e.g. Al Cl₃

Acknowledgements

The authors gratefully acknowledge the assistance of Dr. S. Huwyler in carrying out the analyses; Mr R. Stratton for preparation of the text; and they would also like to thank Dr. H. Schumacher and Dr. P. Tempus for their support in the performance of these studies.

Literature

K.W. Bagnall The Halogen Chemistry of the Actinides in "Halogen Chemistry" in V. Gutmann (ed) "Halogen Chemistry", Vol. 3. p. 304 Academic Press, London (1967) P. Beucherie, M. Payrissat, J.G. Wurm Preparation des carbures d'uranium et de carbures mixtes par conversion directe des halogenures en carbures Comm. Europ de l'Energie Atomique, Euratom. EUR 3170 f. Isp**ra** 1966 J. Besson, P. Blum, J. Sputs A Study of Hydrolysis of Uranium Carbides in Proceed. Symposium "Carbides in Nuclear Energy" Harwell, 1963 M.J. Bradley, L.M. Ferris Hydrolysis of u.anium carbide between 25 and 100 $^{\circ}$ C. I. Uranium Monocarbide, Inorg. Chemistry, 1, 3, 683 (1962)D. Brown, J. Edwards Preparation and Crystallographic Properties of the Trichlorides Tribromides and Tri-Iodides of U, Np, Pu. J. Chem. Soc. Dalton, Trans 16, 1757 (1972) P. Chiotti, W.C. Robinson, M. Kanno Thermodynamic Properties of Uranium Oxycarbides J. of Less Common Metals, 10, 273 (1966) L.M. Ferris, J.C. Mailen, F.J. Smith Estimated free Energies of Formation of some Lanthanide and Actinide Halides at 600 ° - 800 °C using Molten Salt - Liquid Metal Distribution Coefficient Data. J Inorg. Nucl. Chem. 34, 491 (1972) W.N. Hansen Reprocessing of Uranium Carbide by Molten Salt Electrolysis, NAA - SR - 7660 (1963)

B.R. Harder, G. Long, W.P. Stanaway Compatibility and Processing Problems in the Use of Molten Uranium Chloride - Alkali Chloride Mixtures as Reactor Fuels. Nuclear Metallurgy 15, 405 (1969) C. Hardy-Grena Etude thermodynamique sur le trichlorure d'uranium disscus dans les chlorures alcalins fondus. Comm. Europ de l'Energie Atomique, Euratom, Ispra EUR 3153 f (1966)T. Ishihara, K. Hiraua Chlorination Distillation Processing of Irradiated UO2 an UC2 Third Internat. Conf. Peaceful Uses of Atomic Energy, Geneva 1964, Volume 10, 8/798. p. 520 C.P. Kempter Hydrolysis Properties of Uranium Monocarbide and Dicarbide, J. of Less-Common Metals, 4, 419 (1962) A.S. Kertes Complexes of Actinides in Molten Salts Actinides Reviews, 1, 371 (1971) J. Krahe Aktivität von UCl, und anodische Polarisation von UC in der Schmelze LiCl-KCl Technische Hochschule, Aachen, Dissertation, 1965 J. Lumsden Thermodynamics of Molten Salt Mixtures Academic Press, London N.York, 1966 D.L. Maride, D.N. Hume A New Method for Preparing OH-free Alkali Chloride Melts, Electroch. Soc. J. 107, 354 (1960) E.J. McIver A Galvanic Cell for Measuring the Uranium Activity in Carbides at High Temperature, Harwell, A.E.R.E. - R. 4983 (1966) B.A. Partridge The Thermodynamic Properties of Dilute Solutions of UC1, in UC1 - KC1 Eutectic, Harwell, A.E.R.E. - R 3683 (1960)

P. Pascal "Nouveau traite de chimie minerale" Tome XVI, Masson Cie, Paris, 1960 P.E. Potter Ther Uranium-Plutonium-Carbon-Oxygen System, J. Nucl. Met. 42, 1, (1972) W.C. Robinson, P. Chiotti Reactions of Uranium Carbide in Fused KCl - LiCl/Zinc System, J. Less-Common Metals, 10, 190 (1966) H. Schumacher Plutonium-Brennstoffprogramm Jahresbericht 1972 EIR-Report 230, Würenlingen (1973) R.K. Steuerenberg, R.D. Pierce, L. Burris Pyrometallurgical and Pyrochemical Fuel Processing . Process Chemistry, 1970 CM 56 : PC U M. Taube et al. New Boiling Salt Fast Breeder Reactor Concept Nucl. Eng. Design 5, 109, (1967) M. Taube, H. Schumacher A Carbide Fuelled Fast Breeder Reactor with Molten Chlorides as Fuel Bonding Material and Chloride Vapour as Coolant. EIR-Report 167, Würenlingen (1969) M. Taube, J. Ligou Molten Chlorides Fast Breeder EIR-Report 215, Würenlingen (1972) M. Taube, J. Strejcek Reaction of Uranium Carbides with Transient Metals Chlorides in Molten Salt Media (to be published) R.C. Vogel, M. Levensa, F.R. Masten Argonne National Laboratory, Chemical Eng. Div. Research Highlights, April 1965 ANL - 7020 A.P. Zefirov "Thermodynamic Properties of Some Inorganic Substances" Atomizdat, Moscow, 1965 (in Russian)