

Master

LA-8095
UC-32
Issued: June 1980

SALE: A Simplified ALE Computer Program for Fluid Flow at All Speeds

A. A. Amsden
H. M. Ruppel
C. W. Hirt

DISCLAIMER

This document contains technical information which is the property of the University of California, Los Angeles. It is loaned to you for your personal use. It is not to be distributed, copied, or otherwise used in any way without the prior written consent of the University of California, Los Angeles. This document is not to be used for advertising or promotional purposes, for creating new collective works, or for resale.



CONTENTS

ABSTRACT	1
I. INTRODUCTION	3
II. THE SALE SOLUTION ALGORITHM	5
A. The Three Phase ICed-ALE Approach	5
B. The Computing Mesh	5
C. Initial Conditions and Preliminary Calculations	6
D. Phase 1 of the Calculation	6
1. Cycle Initialization	7
2. Artificial Viscous Forces	7
3. Stress Deviator Forces	9
4. Pressure Force Contributions	10
E. Phase 2 of the Calculation	10
F. The Energy Calculation	12
G. Phase 3 of the Calculation	13
1. Rezone	13
2. Regrid	13
3. Advective Flux of Mass, Energy, and Momentum	13
4. Updating the Vertex Quantities	16
H. Completion of the Cycle	16
I. Summary of Solution Algorithm	17
III. THE SALE FORTRAN PROGRAM	19
A. General Structure	19
B. The Indexing Notation	19
C. Boundary Conditions	19
D. Numerical Stability and Accuracy	22
IV. SAMPLE CALCULATIONS	25
A. Broken Dam	25
B. One-Dimensional Shock Tube	27
C. Supersonic Flow Through a Curved Duct	28
D. von Karman Vortex Street	30
E. Strong Shock Passing Over a Mercury Drop in Water	33
REFERENCES	38
APPENDIX A. FORTRAN LISTING OF THE SALE PROGRAM	41
APPENDIX B. SYSTEM SUBROUTINE CALLS IN SALE	89
APPENDIX C. SAMPLE OUTPUT FROM BROKEN DAM CALCULATION	91

**SALE: A SIMPLIFIED ALE COMPUTER PROGRAM
FOR FLUID FLOW AT ALL SPEEDS**

by

A. A. Amsden, H. M. Ruppel, and C. W. Hirt

ABSTRACT

A simplified numerical fluid-dynamics computing technique is presented for calculating two-dimensional fluid flows at all speeds. It combines an implicit treatment of the pressure equation similar to that in the Implicit Continuous-fluid Eulerian (ICE) technique with the grid rezoning philosophy of the Arbitrary Lagrangian-Eulerian (ALE) method. As a result, it can handle flow speeds from supersonic to the incompressible limit in a grid that may be moved with the fluid in typical Lagrangian fashion, or held fixed in an Eulerian manner, or moved in some arbitrary way to give a continuous rezoning capability. The report describes the combined (ICEd-ALE) technique in the framework of the SALE (Simplified ALE) computer program, for which a general flow diagram and complete FORTRAN listing are included. A set of sample problems show how to use or modify the basic code for a variety of applications. Numerical listings are provided for a sample problem run with the SALE program.

I. INTRODUCTION

Over the past decade, we have witnessed an increasing acceptance of and reliance upon numerical solutions for transient fluid flow problems. In many cases, experimental studies are prohibitively expensive, whereas high-speed computers are comparatively economical and allow a wide range of parameter variations to be examined in a short time. As a result, numerical solution techniques have become more sophisticated and the applications correspondingly more complex.

This report presents a simplified computer program to calculate two-dimensional fluid flows at all speeds, from the incompressible limit to highly supersonic. An implicit treatment of the pressure calculation similar to that in the Implicit Continuous-fluid Eulerian (ICE) technique¹ provides this flow-speed versatility. In addition, the computing mesh may move with the fluid in a typical Lagrangian fashion, be held fixed in an Eulerian manner, or move in some arbitrarily specified way to provide a continuous rezoning capability. This latitude results from the use of an Arbitrary Lagrangian-Eulerian (ALE) treatment² of the computing mesh. The program is named SALE, for Simplified ALE. The essential features of the ICed-ALE combination are presented here to make this report a self-contained guide. SALE bears a strong resemblance to YAQUI, the original but more complex ICed-ALE program.³

The partial differential equations solved by the SALE program are the Navier-Stokes equations,

$$\frac{\partial \rho u}{\partial t} + \frac{1}{r} \frac{\partial r \rho u^2}{\partial x} + \frac{\partial \rho u v}{\partial y} = - \frac{\partial (p+q)}{\partial x} + \frac{1}{r} \frac{\partial r \pi_{xx}}{\partial x} + \frac{\partial \pi_{xy}}{\partial y} - \frac{\pi_{\theta}}{r} + \rho g_x$$

$$\frac{\partial \rho v}{\partial t} + \frac{1}{r} \frac{\partial r \rho u v}{\partial x} + \frac{\partial \rho v^2}{\partial y} = - \frac{\partial (p+q)}{\partial y} + \frac{1}{r} \frac{\partial r \pi_{xy}}{\partial x} + \frac{\partial \pi_{yy}}{\partial y} + \rho g_y$$

and the mass and internal energy equations.

$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial r \rho u}{\partial x} + \frac{\partial \rho v}{\partial y} = 0$$

and

$$\frac{\partial \rho I}{\partial t} + \frac{1}{r} \frac{\partial r \rho I u}{\partial x} + \frac{\partial \rho I v}{\partial y} = - (p+q)D + \pi_{xx} \frac{\partial u}{\partial x} + \pi_{xy} \frac{\partial u}{\partial y} + \frac{u \pi_{\theta}}{r} + \pi_{xy} \frac{\partial v}{\partial x} + \pi_{yy} \frac{\partial v}{\partial y}$$

where D is the velocity divergence,

$$D = \frac{1}{r} \frac{\partial r u}{\partial x} + \frac{\partial v}{\partial y}$$

Velocity components (u,v) are in the Cartesian coordinate directions (x,y) or the cylindrical coordinate directions (r,z). When Cartesian coordinates are desired, all radii r, which appear in these equations, are set to unity. The fluid pressure p is determined from an equation of state $p = p(\rho, I)$ and supplemented with an artificial viscous pressure q for the computation of shock waves, where

$$q = \lambda_0 \rho \text{Area} D \min(0, D)$$

Artificial pressures are only used in regions of compression ($D < 0$) and are scaled proportional to the area (Area) of each computational cell, with the constant of proportionality λ_0 .

The stress deviator is defined according to

$$\pi_{xx} = 2\mu \frac{\partial u}{\partial x} + \lambda D$$

$$\pi_{yy} = 2\mu \frac{\partial v}{\partial y} + \lambda D$$

$$\pi_{\theta} = \text{Cyl} \left[2\mu \frac{u}{r} + \lambda D \right]$$

and

$$\pi_{xy} = \mu \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right),$$

in which μ is the coefficient of viscosity and λ is the coefficient of dilatational viscosity. The coefficient Cyl is zero for Cartesian coordinates and unity for cylindrical coordinates.

To facilitate its use by persons with modest experience in numerical fluid dynamics, the SALE program was written in modular form with extensive annotation and input options that provide a wide range of capabilities. In addition, SALE includes several improvements to the original YAQUI scheme that have been made since its publication. We intend that the SALE program serve not only as a useful tool for many applications, but also as a teaching aid and foundation

for the development of new programs with expanded capabilities.

The basic solution algorithm for SALE appears in Sec. II of this report. Section III describes the FORTRAN program. We include a general flow diagram showing the logical partitioning of the code into a set of subroutines, each responsible for a clearly definable task. Section IV presents the results of several SALE calculations chosen to illustrate the versatility of the program.

Appendix A contains a FORTRAN listing of SALE that has been liberally annotated with comment cards, beginning with a description of the input parameters, to make it as self-explanatory as possible. Appendix B describes the functions performed by operating system CALLs appearing in SALE. For users who wish to check their results with ours, App. C presents selected plots and prints from the first calculation described in Sec. IV.

II. THE SALE SOLUTION ALGORITHM

A. The Three-Phase ICed-ALE Approach

The basic hydrodynamic part of each cycle of SALE is divided into three phases:

- (1) Phase 1 is a typical, explicit Lagrangian calculation, in which the velocity field is updated by the effects of all forces.
- (2) Phase 2 is a Newton-Raphson iteration that provides time-advanced pressures and velocities. The purpose of Phase 2 is to allow calculations in the low-speed and even completely incompressible regimes. The implicit, iterative scheme makes this possible with greater efficiency than a purely explicit calculation with reduced time step, as it offers a numerically stable means by which pressure signals can traverse more than one cell in a time step.
- (3) Phase 3 performs all the advective flux calculations. This phase is required for runs that are Eulerian or contain some other form of mesh rezoning.

A powerful feature of SALE is the ease with which different phases can be combined in various ways to suit the requirements of individual problems. For example, in high-speed applications, an explicit calculation is acceptable, allowing the Phase 2 iteration to be bypassed. For an explicit Lagrangian calculation, only Phase 1 is required. For an implicit Lagrangian calculation, only the first two phases are used. In neither of these two cases are advective flux calculations necessary, and the Phase 1 or 2 results are final results for the cycle. All these options may be selected by appropriately defining the input data (see beginning of code in App. A).

B. The Computing Mesh

The computing mesh consists of a two-dimensional network of quadrilateral cells for either cylindrical or plane (Cartesian) coordinates. Calculations in cylindrical coordinates are scaled to unit azimuthal angle,

which allows the equations to be written without any π factors. The radial coordinate is denoted by r or x , and the axial coordinate by y , with the origin located at the lower left corner of the mesh. The coordinate names in the equations are x and y . The quantity r is used to determine the geometry: r is set equal to x for cylindrical coordinates, but the expressions automatically reduce to Cartesian form if all r 's are set to unity.

The vertices of the cells are labeled with the indices i and j , which increase in the radial and axial directions, respectively. Cell centers are denoted by half-integer indices $i+1/2$ and $j+1/2$. The mesh of cells is N_x cells wide by N_y cells high.

The mesh illustrated in Fig. 1 is in cylindrical coordinates, where the cells are sections of toroids of revolution about the cylindrical axis.

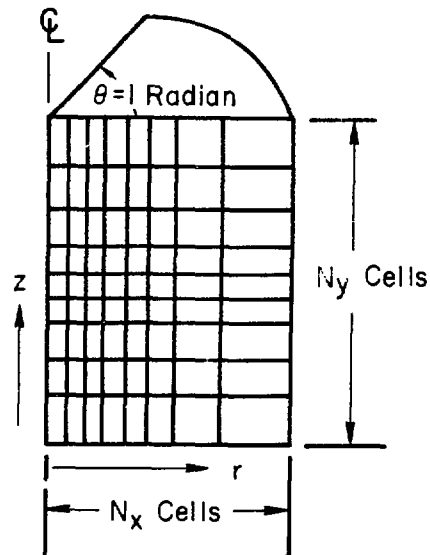


Fig. 1.

A typical SALE mesh in cylindrical coordinates.

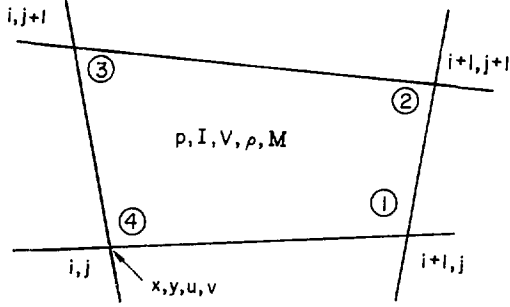


Fig. 2.

The assignment of variables about cell $(i+1/2, j+1/2)$.

The variables in an ICED-ALE grid are of two types: those defined at vertices and those defined at cell centers. The principal variables are shown in Fig. 2, where coordinates (x and y) and corresponding velocity components (u and v) are defined at vertices. Pressures (p), specific internal energies (I), cell volumes (V), densities (ρ), and masses (M) are all assigned at cell centers.

In the equations that follow, the superscript n refers to the beginning-of-cycle values. The advancement of the solution through a time step, of duration δt , provides values at the beginning of the next $(n+1)$ cycle. Intermediate values are typically labeled with a subscript L for the results of Phases 1 or 2.

C. Initial Conditions and Preliminary Calculations

The input data supply the initial values of x , y , u , and v at the vertices and ρ and I for the cells.

- (1) The radius r is calculated as $r = x$ in cylindrical coordinates, or $r = 1$ in plane coordinates. The coordinate system is determined by the input parameter CYL , which is equal to 1 for cylindrical coordinates and is equal to zero for plane coordinates. Thus, we write

$$r_1^j = \begin{pmatrix} x \\ 1 \end{pmatrix}^{j} CYL + 1 - CYL \quad .$$

- (2) Cell volumes per unit azimuthal angle are given by the exact expression

$$v_{1+1/2}^{j+1/2} = \frac{1}{3} \left[(r_1 + r_2 + r_3)_{ATR} + (r_3 + r_4 + r_1)_{ABL} \right], \quad (1)$$

where

$$ATR = \frac{1}{2} [(x_3 - x_2)(y_1 - y_2) - (x_1 - x_2)(y_3 - y_2)]$$

and

$$ABL = \frac{1}{2} [(x_1 - x_4)(y_3 - y_4) - (x_3 - x_4)(y_1 - y_4)] .$$

The numerical subscript notation for vertex quantities associated with a given cell is simplified to that shown in Fig. 2. It is used throughout this report and in the SALE code.

- (3) With the cell volumes defined, the masses at cell centers can be obtained from the product

$$M_{1+1/2}^{j+1/2} = \rho_{1+1/2}^{j+1/2} v_{1+1/2}^{j+1/2} \quad , \quad (2)$$

but it is also necessary to assign a mass to each vertex to obtain the time-advanced velocities. In SALE, we assume that the mass in each cell is shared equally between its four corner vertices, so vertex 4 in Fig. 2, for example, is given the mass

$$M_4 = \frac{1}{4} \left(M_{1+1/2}^{j+1/2} + M_{1-1/2}^{j+1/2} + M_{1-1/2}^{j-1/2} + M_{1+1/2}^{j-1/2} \right) . \quad (3)$$

D. Phase 1 of the Calculation

In this phase, velocities are advanced explicitly in time in a purely Lagrangian fashion. If viscous, elastic, or other stresses are desired, they are included in this phase as well. The updating of the specific internal energies is delayed until after the optional implicit pressure calculation of Phase 2. This delay permits time-advanced pressures to be used in computing the $p dV$ work and ensures consistency with the velocities coming out of Phase 2.

The velocities resulting from this Lagrangian calculation phase are denoted by (u_L, v_L) . Pressure, viscous, and other force contributions are computed in separate subroutines, so that in each case the (u_L, v_L) values are progressively updated with each contribution. This updating is started with the beginning-of-cycle values (u, v) .

In the actual code, the order of updating is performed in the following sequence.

1. Cycle Initialization. This routine initializes the (u_L, v_L) velocities with the beginning-of-cycle values (u, v) . In addition, cell densities ρ and ρ_L are calculated as the ratio of the cell mass to cell volume. Cell pressures (p) are calculated using an equation of state $p = f(\rho, I)$, although the equation of state is bypassed after the setup for implicit calculations, because the pressures resulting from the previous Phase 2 implicit solution generally prove to be a better initial guess for the next cycle iteration than the equation-of-state pressure. In the incompressible limit, we also bypass the equation of state in the setup and set zero pressures at time $t = 0$.

2. Artificial Viscous Forces. Here the (u_L, v_L) velocities are adjusted for contributions arising from a bulk artificial viscosity and from a coupling between alternate nodes.

a. Artificial Bulk Viscosity. For problems involving shock waves, an artificial pressure Q must be used to ensure mesh-resolvable shocks. This addition is required because mean kinetic energy is not conserved across a shock wave. Without dissipation, spurious velocity oscillations develop behind the shock to account for an excess of kinetic energy. We include the dissipation as a pressure addition, which models the fact that the pressure change across a shock is more than a simple adiabatic compression.

The viscous pressure used in SALE is quadratic in the velocity divergence, and is only added to cells undergoing compression,

$$Q_1^j = \min \left(0, D_1^j \right) \left[\lambda_0 \rho_1^j D_1^j (\text{Area}) \right] \quad (4)$$

In this expression, (Area) is the area of cell (i, j) , so that

$$\begin{aligned} (\text{Area}) = \frac{1}{2} & \left[(x_2 - x_4)(y_3 - y_1) \right. \\ & \left. - (x_1 - x_3)(y_4 - y_2) \right] \quad , \end{aligned}$$

and D_1^j is its velocity divergence $\nabla \cdot \vec{u}$ defined as

$$\begin{aligned} D_1^j = \frac{1}{2(\text{Area})} & \left[(u_2 - u_4)(y_3 - y_1) \right. \\ & - (u_1 - u_3)(y_4 - y_2) + (v_4 - v_2)(x_3 - x_1) \\ & \left. - (v_1 - v_3)(x_2 - x_4) \right] + \frac{u}{r} \quad , \end{aligned} \quad (5)$$

where

$$\frac{u}{r} = \text{CYL} \left(\frac{u_1 + u_2 + u_3 + u_4}{r_1 + r_2 + r_3 + r_4} \right) \quad (6)$$

The parameter λ_0 in the above expression for Q_1^j is denoted by ARTVIS in the input data list, and should be less than 0.25 to avoid excessive viscous damping. A value of ARTVIS = 0.1 has been satisfactory for many applications.

With Q_1^j calculated, the appropriate contributions to the four vertices of cell (i, j) are

$$\begin{aligned} (u_L)_1 &= u_1 + \frac{\delta t Q_1^j}{2M_1} r_1 (y_2 - y_4) \quad , \\ (u_L)_2 &= u_2 + \frac{\delta t Q_1^j}{2M_2} r_2 (y_3 - y_1) \quad , \\ (u_L)_3 &= u_3 - \frac{\delta t Q_1^j}{2M_3} r_3 (y_2 - y_4) \quad , \\ (u_L)_4 &= u_4 - \frac{\delta t Q_1^j}{2M_4} r_4 (y_3 - y_1) \quad , \\ (v_L)_1 &= v_1 - \frac{\delta t Q_1^j}{4M_1} (r_2 + r_4)(x_2 - x_4) \quad , \\ (v_L)_2 &= v_2 - \frac{\delta t Q_1^j}{4M_2} (r_1 + r_3)(x_3 - x_1) \quad , \\ (v_L)_3 &= v_3 + \frac{\delta t Q_1^j}{4M_3} (r_2 + r_4)(x_2 - x_4) \quad , \\ (v_L)_4 &= v_4 + \frac{\delta t Q_1^j}{4M_4} (r_1 + r_3)(x_3 - x_1) \quad . \end{aligned} \quad (7)$$

and

The asymmetry in the geometric factors in the above expressions, which also appears in other equations for pressure accelerations, arises from the difference in the effect of the boundary of the control volume on the two directions. Accelerations in the radial direction must include the forces on the ends of the one-radian section of the torus. These contributions do not enter in the axial direction.

b. Alternate Node Coupler. In a Lagrangian calculation using quadrilateral mesh cells, there are certain degenerate mesh deformations that do not result in net pressure or viscous forces. Typically, these deformations are associated with the shortest resolvable wavelengths ($2\delta x$) in the mesh. For example, Fig. 3 illustrates two such short-wavelength deformations. Figure 3a shows the bowtie pattern and Fig. 3b shows the herringbone pattern. In each case, the deforming cells undergo no change in volume so that no pressure variations are generated. Also, it is easily verified that no net viscous or elastic strain forces are generated at vertices embedded in the bowtie type of deformation.

Thus, to prevent such deformations from slowly degrading a solution, it is sometimes necessary to couple alternate mesh nodes with a small artificial restoring force. Ideally, this force should affect flows only at the $2\delta x$ wavelength level, but have no influence on the larger, better resolved flow variations. We introduce small accelerations at each vertex, which are based on the surrounding velocity field and tend to keep the vertex velocities from deviating too strongly from their neighbors.

A fourth-order coupling scheme is effective for the bowtie mode, but a more diffusive second-order scheme must be used for the herringbone pattern. The fourth-order form is given by

$$u_1^j = u_1^j + \frac{a_{nc}}{4} \left[2(u_{i+1}^j + u_1^{j+1} + u_{i-1}^j + u_1^{j-1}) - u_{i+1}^{j+1} - u_{i-1}^{j+1} - u_{i-1}^{j-1} - u_{i+1}^{j-1} - 4u_1^j \right],$$

in which a_{nc} is a coefficient that governs the amount of coupling and implies a relaxation time of a_{nc}^{-1} time steps.

The second-order form is given by

$$u_1^j = u_1^j + \frac{a_{nc}}{4} \left[(u_{i+1}^j + u_1^{j+1} + u_{i-1}^j + u_1^{j-1}) - 4u_1^j \right].$$

In SALE, we combine both of these forms in the following set of expressions, in which $\xi = 1$ results in the fourth-order form and $\xi = 0$ results in the second-order form. Also, rather than sweeping vertices to make the contributions, we may equivalently sweep over cells and adjust the four vertices of each cell, such that

$$(u_L)_1 = (u_L)_1 + \frac{a_{nc}}{4} \left[\left(\frac{1+\xi}{2} \right) (u_2 + u_4) - \xi u_3 - u_1 \right],$$

$$(u_L)_2 = (u_L)_2 + \frac{a_{nc}}{4} \left[\left(\frac{1+\xi}{2} \right) (u_3 + u_1) - \xi u_4 - u_2 \right],$$

$$(u_L)_3 = (u_L)_3 + \frac{a_{nc}}{4} \left[\left(\frac{1+\xi}{2} \right) (u_4 + u_2) - \xi u_1 - u_3 \right],$$

and

$$(u_L)_4 = (u_L)_4 + \frac{a_{nc}}{4} \left[\left(\frac{1+\xi}{2} \right) (u_1 + u_3) - \xi u_2 - u_4 \right]. \quad (8)$$

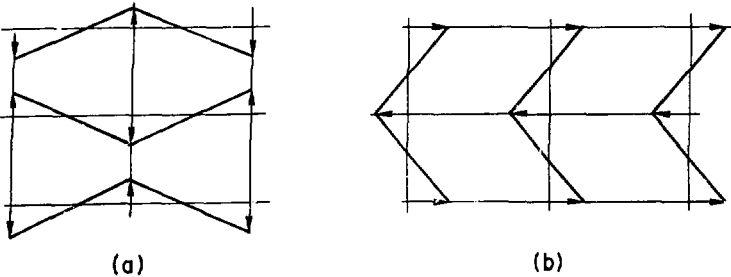


Fig. 3.
Two types of instabilities between adjacent nodes: (a) bowtie, (b) herringbone.

Corresponding expressions are used for the y direction, with every u or u_L replaced by v or v_L . Note that contributions at vertices on reflective boundaries must be doubled to obtain the correct value. This is necessary here because these artificial accelerations have been defined without reference to vertex masses. In the case of all other forces, no corrections are needed for boundary vertices, because the omission of force contributions from cells on the outside of a boundary is compensated for by a corresponding omission in vertex mass.

We emphasize that node coupling is diffusive and nonphysical and should be used with discretion. In a spherical expansion, for example, the smoothing effect of too much node coupling adversely affects the sphericity. To avoid its unintentional use, we require the SALE user to supply values for ξ and a_{nc} in the input data. Rarely should a_{nc} exceed 0.05.

3. Stress Deviator Forces. At this point, the shear viscosity (μ) and bulk viscosity (λ) contributions are added, if either is specified, in terms of a stress deviator force. (This would also be the appropriate place to add material strength effects. These effects, however, have not been included in this version of SALE.)

For each cell, we define the divergence $D = \nabla \cdot \vec{u}$ as in step 1 above, and the four components of the viscous stress tensor as

$$\Pi_{xx} = 2\mu \frac{\partial u}{\partial x} + \lambda \nabla \cdot \vec{u},$$

$$\Pi_{yy} = 2\mu \frac{\partial v}{\partial y} + \lambda \nabla \cdot \vec{u},$$

$$\Pi_{xy} = \mu \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right),$$

and

$$\Pi_{\theta} = c_{YL} \left[2\mu \left(\frac{u}{r} \right) + \lambda \nabla \cdot \vec{u} \right], \quad (9)$$

where u/r is defined as in Eq. (6). The finite difference expressions to compute these quantities are

$$\frac{\partial u}{\partial x} = \frac{1}{2(\text{Area})} [(u_2 - u_4)(y_3 - y_1)$$

$$- (u_3 - u_1)(y_2 - y_4)] ,$$

$$\frac{\partial v}{\partial x} = \frac{1}{2(\text{Area})} [(v_2 - v_4)(y_3 - y_1)$$

$$- (v_3 - v_1)(y_2 - y_4)] ,$$

$$\frac{\partial u}{\partial y} = \frac{1}{2(\text{Area})} [(u_3 - u_1)(x_2 - x_4)$$

$$- (u_2 - u_4)(x_3 - x_1)] ,$$

and

$$\frac{\partial v}{\partial y} = \frac{1}{2(\text{Area})} [(v_3 - v_1)(x_2 - x_4)$$

$$- (v_2 - v_4)(x_3 - x_1)] . \quad (10)$$

Stress deviator contributions to the vertex velocities are

$$(u_L)_1 = (u_L)_1 + \frac{\delta t}{4M_1} (r_2 + r_4) \left[\Pi_{xy} (x_2 - x_4) \right. \\ \left. - \Pi_{xx} (y_2 - y_4) - \frac{\text{Area}}{2} \Pi_{\theta} \right] ,$$

$$(u_L)_2 = (u_L)_2 + \frac{\delta t}{4M_2} (r_1 + r_3) \left[\Pi_{xy} (x_3 - x_1) \right. \\ \left. - \Pi_{xx} (y_3 - y_1) - \frac{\text{Area}}{2} \Pi_{\theta} \right] ,$$

$$(u_L)_3 = (u_L)_3 - \frac{\delta t}{4M_3} (r_2 + r_4) \left[\Pi_{xy} (x_2 - x_4) \right. \\ \left. - \Pi_{xx} (y_2 - y_4) + \frac{\text{Area}}{2} \Pi_{\theta} \right] ,$$

$$(u_L)_4 = (u_L)_4 - \frac{\delta t}{4M_4} (r_1 + r_3) \left[\Pi_{xy} (x_3 - x_1) \right. \\ \left. - \Pi_{xx} (y_3 - y_1) + \frac{\text{Area}}{2} \Pi_{\theta} \right] ,$$

$$(v_L)_1 = (v_L)_1 + \frac{\delta t}{4M_1} (r_2 + r_4) \left[\Pi_{yy} (x_2 - x_4) \right. \\ \left. - \Pi_{xy} (y_2 - y_4) \right] ,$$

$$\begin{aligned}
(v_L)_2 &= (v_L)_2 + \frac{\delta t}{4M_2} (r_1 + r_3) [\Pi_{yy} (x_3 - x_1) \\
&\quad - \Pi_{xy} (y_3 - y_1)] \quad , \\
(v_L)_3 &= (v_L)_3 - \frac{\delta t}{4M_3} (r_2 + r_4) [\Pi_{yy} (x_2 - x_4) \\
&\quad - \Pi_{xy} (y_2 - y_4)] \quad , \\
\text{and} \\
(v_L)_4 &= (v_L)_4 - \frac{\delta t}{4M_4} (r_1 + r_3) [\Pi_{yy} (x_3 - x_1) \\
&\quad - \Pi_{xy} (y_3 - y_1)] \quad . \tag{11}
\end{aligned}$$

The Π terms are stored for later inclusion in the internal energy.

4. Pressure Force Contributions. The principal contribution to the velocities in Phase 1 comes from the pressure forces and body forces acting on the vertices.

a. Pressure Accelerations. The difference approximations used for the pressure accelerations are

$$\begin{aligned}
(u_L)_1 &= (u_L)_1 + \frac{\delta t}{2M_1} p_i^j r_1 (y_2 - y_4) \quad , \\
(u_L)_2 &= (u_L)_2 + \frac{\delta t}{2M_2} p_i^j r_2 (y_3 - y_1) \quad , \\
(u_L)_3 &= (u_L)_3 - \frac{\delta t}{2M_3} p_i^j r_3 (y_2 - y_4) \quad , \\
(u_L)_4 &= (u_L)_4 - \frac{\delta t}{2M_4} p_i^j r_4 (y_3 - y_1) \quad , \\
(v_L)_1 &= (v_L)_1 - \frac{\delta t}{4M_1} p_i^j (r_2 + r_4) (x_2 - x_4) \quad , \\
(v_L)_2 &= (v_L)_2 - \frac{\delta t}{4M_2} p_i^j (r_1 + r_3) (x_3 - x_1) \quad , \\
(v_L)_3 &= (v_L)_3 + \frac{\delta t}{4M_3} p_i^j (r_2 + r_4) (x_2 - x_4) \quad ,
\end{aligned}$$

and

$$(v_L)_4 = (v_L)_4 + \frac{\delta t}{4M_4} p_i^j (r_1 + r_3) (x_3 - x_1) \quad . \tag{12}$$

b. Body Accelerations. Finally, any desired body accelerations, such as those arising from gravitational effects, are added to the velocities. For example,

$$(u_L)_1^j = (u_L)_1^j + \delta t g_x$$

and

$$(v_L)_1^j = (v_L)_1^j + \delta t g_y \quad . \tag{13}$$

E. Phase 2 of the Calculation

Phase 2 provides an implicit treatment required to eliminate Courant-like time step restrictions that would otherwise be required to ensure computational stability in low-speed or incompressible flows. This phase can be bypassed entirely when an explicit calculation will suffice. The purpose of the implicit treatment in Phase 2 is to obtain a velocity field that has been accelerated by time-advanced pressure gradients. The time-advanced pressures, in turn, depend upon the densities and energies obtained when vertices are moved with these new velocities, but because these are functions of the new pressures, the pressures are by definition implicit and are in general best determined by iteration. Our implicit approach is formulated as follows. With the subscript L again denoting time-advanced values, the desired pressure p_L of cell (i,j) will be the solution of

$$(p_L)_i^j = f \left[(c_L)_i^j, (I_L)_i^j \right] \quad , \tag{14}$$

where the new cell density and energy are approximated in terms of their initial values as

$$(\rho_L)_i^j = \rho_i^j (v/v^*)^j$$

and

$$(I_L)_i^j = I_i^j + (p_L)_i^j (1 - v^*/v) / (\rho_L)_i^j \quad . \tag{15}$$

V is the volume of the cell at time n, and V* is the volume the cell would have if its vertices were moved according to the current Lagrangian velocity field.

$$x_1^* = x_1 + (u_L)_1 \delta t, \quad y_1^* = y_1 + (v_L)_1 \delta t, \quad \dots \quad (16)$$

A solution for p_L is obtained by applying a Newton-Raphson iteration, for which the Phase I velocities (u_L, v_L) are used as initial guesses. The iteration consists of sweeping through the mesh and applying the following adjustments to each cell, once each sweep:

- (1) Compute V* using the most updated values for (u_L, v_L) ;
- (2) Compute new guesses for ρ_L , I_L , and p_L from the above equations; and
- (3) Compute a pressure change δp , according to

$$\delta p = - \frac{p_L - f(\rho_L, I_L)}{S}, \quad (17)$$

where the most updated values are used for p_L , ρ_L , and I_L , and S^{-1} is a relaxation factor to be described below.

- (4) Adjust the current guess for p_L by adding δp to it;
- (5) Adjust the velocities at the vertices of the cell to include this pressure change:

$$(u_L)_1 = (u_L)_1 + \frac{\delta t \delta p}{2M_1} r_1 (y_2 - y_4),$$

$$(u_L)_2 = (u_L)_2 + \frac{\delta t \delta p}{2M_2} r_2 (y_3 - y_1),$$

$$(u_L)_3 = (u_L)_3 - \frac{\delta t \delta p}{2M_3} r_3 (y_2 - y_4),$$

$$(u_L)_4 = (u_L)_4 - \frac{\delta t \delta p}{2M_4} r_4 (y_3 - y_1),$$

$$(v_L)_1 = (v_L)_1 - \frac{\delta t \delta p}{4M_1} (r_2 + r_4)(x_2 - x_4),$$

$$(v_L)_2 = (v_L)_2 - \frac{\delta t \delta p}{4M_2} (r_1 + r_3)(x_3 - x_1),$$

$$(v_L)_3 = (v_L)_3 + \frac{\delta t \delta p}{4M_3} (r_2 + r_4)(x_2 - x_4),$$

and

$$(v_L)_4 = (v_L)_4 + \frac{\delta t \delta p}{4M_4} (r_1 + r_3)(x_3 - x_1). \quad (18)$$

The mesh is repeatedly swept and steps (1) through (5) are performed once for each cell each sweep, until no cell exhibits a pressure change violating the inequality

$$\frac{|\delta p|}{|p_{\max}|} < \epsilon, \quad (19)$$

where p_{\max} is the actual or an estimated maximum pressure in the mesh and ϵ is an input number (EPS), typically of order 10^{-4} .

The quantity S used in step (3) must be chosen to keep the pressure changes bounded and progressing in the right direction. In the Newton-Raphson procedure, S is the derivative of the function whose root is sought with respect to p, the iteration variable. Here, S is the rate at which the quantity $p - f(\rho, I)$ changes as the variable p changes, and is computed numerically using the same relations outlined above. For this purpose, a small pressure change Δp is chosen, scaled to the calculation:

$$\Delta p = \frac{1}{\delta t^2} \left[\frac{p_L r}{2 \left(\frac{1}{\delta x^2} + \frac{1}{\delta y^2} \right)} \right].$$

Here, ρ is a typical fluid density at time $t = 0$, and p_L is an input quantity (PEPS), typically 10^{-4} . The velocity changes that would be induced by Δp are used to compute the corresponding volume, energy, and density changes, and from them a new pressure. Finally, S is determined from the difference between $p - f(\rho, I)$, evaluated before and after the small change in pressure, and divided by Δp . The resulting values for S^{-1} are multiplied by an optional over-relaxation coefficient, input as OM, and stored for each cell before the iteration is begun. These quantities are not recomputed during the iteration.

The above procedure works well across a broad range of low-speed flow applications, but in the incompressible limit, the procedure is modified. The reason for this is that the method is then excessively sensitive to volume changes. In this case, we replace $p = f(\rho, I)$ with

$$p = p_L + \frac{v_L}{\rho} - 1, \quad (20)$$

which effectively holds the densities constant and results in much faster iteration convergence. Corresponding expressions are used for the evaluation of S.

It should be noted that the densities and internal energies calculated in the pressure iteration are temporary quantities used only to update the pressure. To ensure exact mass conservation, the final new densities are computed in Phase 3 after the cell masses and volumes have been calculated. The internal energy is also recalculated with time-centered volume changes, which conserves internal energy, and viscous contributions are then included.

In some cases, when the pressure iteration does not converge within several hundred iterations, it is still possible to continue a calculation without serious error. Usually this only happens when the incompressible option is used. For example, a poor initial guess for velocities or pressures may require a high number of iterations to relax to an acceptable solution. In such cases, the code automatically terminates the iteration, continues the cycle, and then proceeds on to the next cycle and repeats this process up to 10 times. The code aborts if the pressure iteration still has not converged after 10 cycles.

The Phase 1 and 2 calculations as outlined above comprise an implicit Lagrangian method stable for any Courant number, and allow calculations at all values of sound speed vs fluid speed.

F. The Energy Calculation

The pressure work and viscous dissipation contributions to internal energy are calculated next. The pressures used in the work expression are those resulting from the Phase 2 iteration when the implicit option is used. In the case of explicit calculations, the pressures used are those coming from the equation of state at the beginning of each cycle.

The equation for the change in internal energy in a cycle is

$$I_i^j = I_i^j - \frac{\delta t}{2M_i^j} \left[(p_i^j + Q_i^j) \frac{dv}{dt} + \frac{dVIS}{dt} \right]. \quad (21)$$

Both the dV/dt and $dVIS/dt$ quantities are in time-centered form, using averages of beginning-of-cycle and current velocities, for example

$$(u_{TC})_1 = \frac{1}{2} [u_1 + (u_L)_1]$$

and

$$(v_{TC})_1 = \frac{1}{2} [v_1 + (v_L)_1], \dots$$

With this definition,

$$\begin{aligned} \frac{dV}{dt} = & (y_2 - y_4) [r_1 (u_{TC})_1 - r_3 (u_{TC})_3] \\ & + (y_3 - y_1) [r_2 (u_{TC})_2 - r_4 (u_{TC})_4] \\ & - \frac{1}{2} (r_2 + r_4) (x_2 - x_4) [(v_{TC})_1 - (v_{TC})_3] \\ & - \frac{1}{2} (r_1 + r_3) (x_3 - x_1) [(v_{TC})_2 - (v_{TC})_4], \end{aligned}$$

and

$$\begin{aligned} \frac{dVIS}{dt} = & \frac{1}{2} (r_2 + r_4) [\Pi_{xy} (x_2 - x_4) \\ & - \Gamma_{xx} (y_2 - y_4)] [(u_{TC})_1 - (u_{TC})_3] \\ & + \frac{1}{2} (r_1 + r_3) [\Pi_{xy} (x_3 - x_1) \\ & - \Pi_{xx} (y_3 - y_1)] [(u_{TC})_2 - (u_{TC})_4] \\ & - \frac{1}{2} (\Gamma_{\theta} \text{ Area}) [(u_{TC})_1 + (u_{TC})_2 + (u_{TC})_3 + (u_{TC})_4] \\ & + \frac{1}{2} (r_2 + r_4) [\Pi_{yy} (x_2 - x_4) \\ & - \Pi_{xy} (y_2 - y_4)] [(v_{TC})_1 - (v_{TC})_3] \\ & + \frac{1}{2} (r_1 + r_3) [\Pi_{yy} (x_3 - x_1) \\ & - \Pi_{xy} (y_3 - y_1)] [(v_{TC})_2 - (v_{TC})_4]. \end{aligned}$$

The four Π terms were evaluated in the Phase 1 stress deviator calculation using Eq. (9) and stored for each cell for use here. In addition, the artificial viscous pressure Q was saved from Phase 1, Eq. (4).

G. Phase 3 of the Calculation

1. Rezone. When large fluid distortions are not expected, a purely Lagrangian approach will suffice, allowing the computing grid to follow the fluid motion exactly. In many cases, however, large fluid motions would create devastating effects, contorting cells to extreme aspect ratios or even turning cells inside out. It is often possible to ameliorate these effects by moving the mesh vertices with respect to the fluid so as to maintain a reasonable mesh structure. Whenever a vertex is moved relative to the fluid, however, there must be an exchange of material among the cells surrounding the vertex. SALE allows a broad spectrum of rezoning possibilities by treating this material exchange as an advective flux. The simplest case is that of a purely Eulerian flow, in which the vertices are moved back to their original positions every cycle. Between this extreme and the Lagrangian extreme lies whatever form of continuous or discrete rezoning the user wishes.

This latitude is made possible by defining a set of grid vertex velocities (u_G, v_G) over the entire mesh. For a purely Lagrangian calculation, $u_G \equiv u_L$ and $v_G \equiv v_L$ everywhere. For a purely Eulerian calculation, $u_G \equiv 0$ and $v_G \equiv 0$. For a continuous rezone that approximates a Lagrangian calculation, but minimizes excessive grid distortions, grid velocities are chosen to lie somewhere between these two extremes. In particular, the vertices are moved according to some relaxation rate to place vertices at the average position of the neighboring vertices. This usually maintains cells of reasonable size and proportion throughout a run. Once a set of grid velocities u_G and v_G have been defined, it is a simple matter to construct the new grid and perform whatever advective flux calculations that may be required.

SALE could also be modified to have a discontinuous rezone capability in this Phase of a cycle. For example, grid quantities could be interpolated onto another grid whenever distortions are excessive.

2. Regrid. In this step, the vertices are moved to new locations as specified by (u_G, v_G) :

$$x_1^j = x_1^j + \delta t (u_G)_1^j \quad ,$$

$$y_1^j = y_1^j + \delta t (v_G)_1^j \quad ,$$

and

$$r_1^j = (x_1^j)_{CYL+1} - (x_1^j)_{CYL} \quad . \quad (22)$$

We next form a set of relative velocities (u_{REL}, v_{REL}) to simplify the later task of calculating advective fluxes. For this purpose, the vertex velocities with respect to the fluid are

$$(u_{REL})_1^j = (u_G)_1^j - (u_L)_1^j$$

and

$$(v_{REL})_1^j = (v_G)_1^j - (v_L)_1^j \quad . \quad (23)$$

New cell volumes ${}^{n+1}V$ are calculated from the new coordinates using Eq. (1), and replace the nV values in storage.

3. Advective Flux of Mass, Energy, and Momentum. This step is bypassed completely for a purely Lagrangian calculation. In all other cases the relative velocities are not zero, and we must calculate the flux of mass, energy, and momentum between cells.

The flux calculation is performed on a cell-by-cell basis. For every cell, we calculate the volume swept out by each of the four faces relative to their Lagrangian positions.

a. To calculate these volumes, it is necessary to first form the Lagrangian coordinates (x_p, x_p) given by

$$(x_p)_1 = x_1 - (u_{REL})_1 \delta t \quad ,$$

$$(y_p)_1 = y_1 - (v_{REL})_1 \delta t \quad ,$$

and

$$(r_p)_1 = (x_p)_1_{CYL+1} - (x_p)_1_{CYL}, \dots \quad (24)$$

b. Then the four volumes for the right, top, left, and bottom sides are proportional to

$$\begin{aligned}
FR = & \frac{1}{12} \left((r_1 + (r_p)_1 + (r_p)_2) \{x_1[(y_p)_2 - (y_p)_1] \right. & + (x_p)_1 [(y_p)_4 - y_1] \\
& + (x_p)_1 [y_1 - (y_p)_2] & + (x_p)_4 [y_1 - (y_p)_1] \\
& + (x_p)_2 [(y_p)_1 - y_1] & + [r_1 + r_4 + (r_p)_4] \{x_1 [(y_p)_4 - y_4] \\
& + [r_1 + r_2 + (r_p)_2] \{x_1 [y_2 - (y_p)_2] & + x_4 [y_1 - (y_p)_4] \\
& + x_2 [(y_p)_2 - y_1] & + (x_p)_4 [y_4 - y_1] \} \quad . \quad (25) \\
& + (x_p)_2 [y_1 - y_2] \} \quad ,
\end{aligned}$$

$$\begin{aligned}
FT = & \frac{1}{12} \left([(r_p)_2 + r_3 + (r_p)_3] \{ (x_p)_2 [y_3 - (y_p)_3] \right. \\
& + x_3 [(y_p)_3 - (y_p)_2] \\
& + (x_p)_3 [(y_p)_2 - y_3] \} \\
& + [r_2 + (r_p)_2 + r_3] \{ x_2 [y_3 - (y_p)_2] \\
& + (x_p)_2 [y_2 - y_3] \\
& + x_3 [(y_p)_2 - y_2] \} \quad ,
\end{aligned}$$

$$\begin{aligned}
FL = & \frac{1}{12} \left([(r_p)_3 + r_4 + (r_p)_4] \{ (x_p)_3 [y_4 - (y_p)_4] \right. \\
& + x_4 [(y_p)_4 - (y_p)_3] \\
& + (x_p)_4 [(y_p)_3 - y_4] \} \\
& + [r_3 + (r_p)_3 + r_4] \{ x_3 [y_4 - (y_p)_3] \\
& + (x_p)_3 [y_3 - y_4] \\
& + x_4 [(y_p)_3 - y_3] \} \quad ,
\end{aligned}$$

and

$$FB = \frac{1}{12} \left([r_1 + (r_p)_1 + (r_p)_4] \{ x_1 [(y_p)_1 - (y_p)_4] \right.$$

These represent *one-half* the volumes swept over by the sides moving from their Lagrangian positions to their rezoned positions, the factor of 1/2 being included for convenience. Note also that FR for cell (i+1/2, j+1/2) is equal to -FL for cell (i+3/2, j+1/2), and FT for cell (i+1/2, j+1/2) is equal to -FB for cell (i+1/2, j+3/2). This fact is used in the code to eliminate redundant calculations.

c. Associated with each fluid volume crossing a cell face there are corresponding values of mass, energy, and momentum. For example, the mass crossing the right face of cell (i+1/2, j+1/2) might be computed as the product of the fluxing volume 2(FR) times the average fluid density of the cells (i+1/2, j+1/2) and (i+3/2, j+1/2) located on either side of the boundary. Unfortunately, this so-called 'centered differencing' leads to numerical instabilities. One way to circumvent this instability is to weight the quantity being fluxed more in favor of the upstream value. In the above example, this means the density associated with FR should be more nearly equal to the density in cell (i+1/2, j+1/2) when the flux is leaving this cell (FR < 0), or more nearly equal to the density in cell (i+3/2, j+1/2) when the flux is leaving that cell (FR > 0). In SALE, we incorporate the flux coefficients FR, FT, FL, and FB within expressions that allow various differencing forms determined from input constants a_0 and b_0 :

$$a_R = a_0 \text{ sign FR} + 4b_0 \text{FR} \left/ \left(v_{i+3/2}^{j+1/2} + v_{i+1/2}^{j+1/2} \right) \right. ,$$

$$a_T = a_0 \text{ sign FT} + 4b_0 \text{FT} \left/ \left(v_{i+1/2}^{j+3/2} + v_{i+1/2}^{j+1/2} \right) \right. ,$$

$$a_L = a_0 \text{ sign FL} + 4b_0 \text{FL} \left/ \left(v_{i-1/2}^{j+1/2} + v_{i+1/2}^{j+1/2} \right) \right. ,$$

and

$$a_B = a_0 \text{ sign FR} + 4b_0 \text{FB} / \left(v_{i+\frac{1}{2}}^{j-\frac{1}{2}} + v_{i+\frac{1}{2}}^{j+\frac{1}{2}} \right), \quad (26)$$

where "sign FR," for example, equals +1 if $\text{FR} \geq 0$ and equals -1 if $\text{FR} < 0$. Both a_0 and b_0 lie in the range 0 to 1, and the limiting cases are

$a_0 = 0$ and $b_0 = 0 \rightarrow$ centered (unstable),

$a_0 = 1$ and $b_0 = 0 \rightarrow$ full donor cell or upstream differencing (stable, but diffusive),

$a_0 = 0$ and $b_0 = 1 \rightarrow$ interpolated donor cell (linearly stable, less diffusive),

and

$a_0 = 1$ and $b_0 = 1 \rightarrow$ (stable, but more diffusive).

Note that $(a_0 + b_0)$ must be sufficiently positive for numerical stability (see Sec. III.D).

d. In terms of these weighting fractions, the new mass and specific internal energy for a cell $(i+1/2, j+1/2)$ are then given by

$$\begin{aligned} n_{i+\frac{1}{2}}^{j+\frac{1}{2}} &= n_{i+\frac{1}{2}}^{j+\frac{1}{2}} + \text{FR}(1 + a_R) c_{L, i+\frac{1}{2}}^{j+\frac{1}{2}} \\ &+ \text{FT}(1 + a_T) c_{L, i+\frac{1}{2}}^{j+\frac{3}{2}} \\ &+ \text{FL}(1 + a_L) c_{L, i-\frac{1}{2}}^{j+\frac{1}{2}} + \text{FB}(1 + a_B) c_{L, i+\frac{1}{2}}^{j-\frac{1}{2}} \\ &+ [\text{FR}(1 - a_R) + \text{FT}(1 - a_T) + \text{FL}(1 - a_L) \\ &+ \text{FB}(1 - a_B)] c_{L, i+\frac{1}{2}}^{j+\frac{1}{2}} \end{aligned}$$

and

$$n_{i+\frac{1}{2}}^{j+1} = \frac{1}{n_{i+\frac{1}{2}}^{j+\frac{1}{2}}} \left\{ n(MI)_{i+\frac{1}{2}}^{j+\frac{1}{2}} + \text{FR}(1 + a_R) (n_{\tau, L})_{i+\frac{3}{2}}^{j+\frac{1}{2}} \right.$$

$$\begin{aligned} &+ \text{FT}(1 + a_T) (n_{\tau, L})_{i+\frac{3}{2}}^{j+\frac{3}{2}} \\ &+ \text{FL}(1 + a_L) (n_{\tau, L})_{i-\frac{1}{2}}^{j+\frac{1}{2}} + \text{FB}(1 + a_B) (n_{\tau, L})_{i-\frac{1}{2}}^{j-\frac{1}{2}} \\ &+ [\text{FR}(1 - a_R) + \text{FT}(1 - a_T) + \text{FL}(1 - a_L) \\ &+ \text{FB}(1 - a_B)] (n_{\tau, L})_{i+\frac{1}{2}}^{j+\frac{1}{2}} \left. \right\}. \end{aligned}$$

e. The advection of momentum requires an extra step, because cell momenta are not carried throughout the cycle as primary field variables. Here we use the concept of a cell-centered momentum flux, which is a departure from that of a vertex-centered form previously used.³ The cell-centered flux form has the advantage that momentum is fluxed consistently with mass and energy. The approach is to compute average cell-centered momenta based on the vertex velocities. Changes in these cell momenta resulting from advection are computed in the same way as the other cell-centered quantities. These changes are then apportioned back to the vertices. Although this scheme requires the additional calculation of cell-centered averages and their average effect back on the vertex velocities, the entire process is simpler than using another set of control volumes, because it can be easily included in the advection calculation for mass and energy. Tests with this method have shown it to be superior to all momentum advection methods based on vertex-centered control volumes. In particular, it better preserves cylindrical or spherical symmetry and does not introduce diffusion across streamlines.

The first step in the momentum flux calculation is to form the cell centered momenta. For every cell,

$$(u_{MOM})_{i+\frac{1}{2}}^{j+\frac{1}{2}} = \frac{(c_L)_i^j}{4} [(u_L)_1 + (u_L)_2 + (u_L)_3 + (u_L)_4]$$

and

$$(v_{MOM})_{i+\frac{1}{2}}^{j+\frac{1}{2}} = \frac{(c_L)_i^j}{4} [(v_L)_1 + (v_L)_2 + (v_L)_3 + (v_L)_4].$$

Then, using the flux coefficients formed in steps (b) and (c) above, the net advection changes in cell-centered momentum components are given by

$$\begin{aligned}
(\Delta UM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} &= FR(1 + a_R) \left(UM\emptyset_{M_L} \right)_{i+3/2}^{j+\frac{1}{2}} \\
&+ FT(1 + a_T) \left(UM\emptyset_{M_L} \right)_{i+\frac{1}{2}}^{j+3/2} \\
&+ FL(1 + a_L) \left(UM\emptyset_{M_L} \right)_{i-\frac{1}{2}}^{j+\frac{1}{2}} + FB(1 + a_B) \left(UM\emptyset_{M_L} \right)_{i+\frac{1}{2}}^{j-\frac{1}{2}} \\
&+ [FR(1 - a_R) + FT(1 - a_T) + FL(1 - a_L) \\
&+ FB(1 - a_B)] \left(UM\emptyset_{M_L} \right)_{i+\frac{1}{2}}^{j+\frac{1}{2}}
\end{aligned}$$

and

$$\begin{aligned}
(\Delta VM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} &= FR(1 + a_R) \left(VM\emptyset_{M_L} \right)_{i+3/2}^{j+\frac{1}{2}} \\
&+ FT(1 + a_T) \left(VM\emptyset_{M_L} \right)_{i+\frac{1}{2}}^{j+3/2} \\
&+ FL(1 + a_L) \left(VM\emptyset_{M_L} \right)_{i-\frac{1}{2}}^{j+\frac{1}{2}} + FR(1 + a_B) \left(VM\emptyset_{M_L} \right)_{i+\frac{1}{2}}^{j-\frac{1}{2}} \\
&+ [FR(1 - a_R) + FT(1 - a_T) + FL(1 - a_L) \\
&+ FB(1 - a_B)] \left(VM\emptyset_{M_L} \right)_{i+\frac{1}{2}}^{j+\frac{1}{2}} .
\end{aligned}$$

The momenta changes are finally converted to vertex velocity changes in the next step.

4. Updating the Vertex Quantities.

a. We first calculate new vertex masses from averages of the new cell masses, using Eq. (3).

b. To adjust the velocities, we set initial values at all vertices, where the $({}^n u, {}^n v)$ values in storage are replaced by

$${}^{n+1} u_i^j = \left(\frac{{}^n M}{n+1 M} \right)_i^j (u_L)_i^j ,$$

and

$${}^{n+1} v_i^j = \left(\frac{{}^n M}{n+1 M} \right)_i^j (v_L)_i^j .$$

Because both the ${}^{n+1} M$ and the ${}^n M$ values are required, the replacement of ${}^n M$ values by ${}^{n+1} M$ values is deferred until after completion of this step.

c. Finally, we distribute the cell-centered momentum changes to the four vertices of the cell, in the same manner that we calculate vertex masses, that is, giving equal fractions to each vertex,

$${}^{n+1} u_1 = {}^{n+1} u_1 + \left(\frac{0.25}{n+1 M_1} \right) (\Delta UM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} ,$$

$${}^{n+1} u_2 = {}^{n+1} u_2 + \left(\frac{0.25}{n+1 M_2} \right) (\Delta UM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} ,$$

$${}^{n+1} u_3 = {}^{n+1} u_3 + \left(\frac{0.25}{n+1 M_3} \right) (\Delta UM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} ,$$

$${}^{n+1} u_4 = {}^{n+1} u_4 + \left(\frac{0.25}{n+1 M_4} \right) (\Delta UM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} ,$$

$${}^{n+1} v_1 = {}^{n+1} v_1 + \left(\frac{0.25}{n+1 M_1} \right) (\Delta VM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} ,$$

$${}^{n+1} v_2 = {}^{n+1} v_2 + \left(\frac{0.25}{n+1 M_2} \right) (\Delta VM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} ,$$

$${}^{n+1} v_3 = {}^{n+1} v_3 + \left(\frac{0.25}{n+1 M_3} \right) (\Delta VM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} ,$$

and

$${}^{n+1} v_4 = {}^{n+1} v_4 + \left(\frac{0.25}{n+1 M_4} \right) (\Delta VM)_{i+\frac{1}{2}}^{j+\frac{1}{2}} .$$

H. Completion of the Cycle

In a purely Lagrangian calculation, the advective flux is bypassed entirely, and the end-of-cycle ${}^{n+1} u$ and ${}^{n+1} v$ remain to be set. In the case of an explicit Lagrangian calculation, the Phase I (u_L, v_L) values replace the $({}^n u, {}^n v)$ values. Similarly, for an implicit Lagrangian

case, the Phase 2 (u_1, v_1) values become the final values for the cycle.

i. Summary of Solution Algorithm

The above subsections complete the description of the basic finite difference approximations to the dif

ferential equations of motion. Alternative approximations may be easily substituted for any one of the these sections, because they reside in independent sub-routines. To complete the solution algorithm, it is necessary to specify suitable boundary conditions. SALE contains a variety of user options for boundary conditions, which are discussed in the next section, along with other code initialization and running instructions.

III. THE SALE FORTRAN PROGRAM

A. General Structure

The SALE computer program consists of a set of subroutines controlled by a short main program. The general structure is illustrated in Fig. 4, showing a top-to-bottom flow encompassing the three phases described in Sec. II. Beside each box in the flow diagram appears the name(s) of the primary subroutine(s) responsible for the associated task. An examination of the main program listing lines SALE.170 through SALE.193 (App. A) reveals that the program closely follows the logic path of Fig. 4.

In addition to the primary subroutines, Fig. 4 also identifies a number of supporting subroutines that perform tasks for the primaries. These are concerned with boundary conditions, equation of state, and program output. Comment cards at the beginning of every subroutine in the listing describe its purpose.

The listing in App. A is for the FORTRAN Extended (FTN) compiler in use at the Los Alamos Scientific Laboratory (LASL) on the CDC-7600 computer, which operates under the Livermore Time-Sharing System (LTSS). The code is close to ANSI standard and is generally compatible with other compilers. The principal incompatibility with other systems lies in the calls that communicate with the operating system. Most of these concern the film-plotting routines. WRITE(59,-) statements refer to the user's remote terminal at LASL. The functions of all calls to local routines in SALE are described in App. B to aid users at other installations.

The input quantities to set up a problem are described in the listing (lines SALE.11 through SALE.62), using the formats appearing in subroutine RINPUT. Provision is made for tape dump and subsequent restart. In this case, a modified input file is used, where $N_x \equiv 0$ and $N_y =$ the dump number.

B. The Indexing Notation

Figure 2 shows some variables centered at vertices and some at cell centers, typical of Lagrangian

methods. In FORTRAN, one can reference x_i^j simply as $X(I,J)$, but $p_{i+1/2}^{j+1/2}$ cannot be referenced by a "half-integer" index, so the convention is that $P(I,J)$ refers to this pressure. Thus, the indices I and J refer to a quantity lying at the lower left vertex of a cell, or at the cell center, depending upon where the quantity is defined. In SALE, (I,J) is replaced by (IJ), as only single subscripts are used for computer efficiency. In the SALE subscript notation, the letter P stands for + and M for -. Thus, we write

IMJ for $(i-1,j)$,
IPJ for $(i+1,j)$,
IJP for $(i,j+1)$,
IPJP for $(i+1, j+1)$, ...

This notation allows programmed equations in the listing to be quickly comprehended.

As the number of vertices in either direction is one greater than the number of cells, it is apparent that the grid in computer storage must be $(N_x + 1)$ by $(N_y + 1)$ in size. Because our indexing refers to cell centers and lower left vertices, we must allow one extra column of storage on the right and one extra row across the top of the mesh.

C. Boundary Conditions

Seven types of boundary conditions are provided in the SALE listing of App. A, identified on lines BC.6-BC.12. Except for special situations, as in the sample problem of Sec. IV.D, the user only needs to define the boundary types in the input data file and supply values for specified flow or applied pressure boundaries, and SALE will automatically do the rest. The input data flags indicating what conditions are to be applied along each edge of the mesh are WB, WL, WR, and WT, which correspond to the bottom, left, right, and top

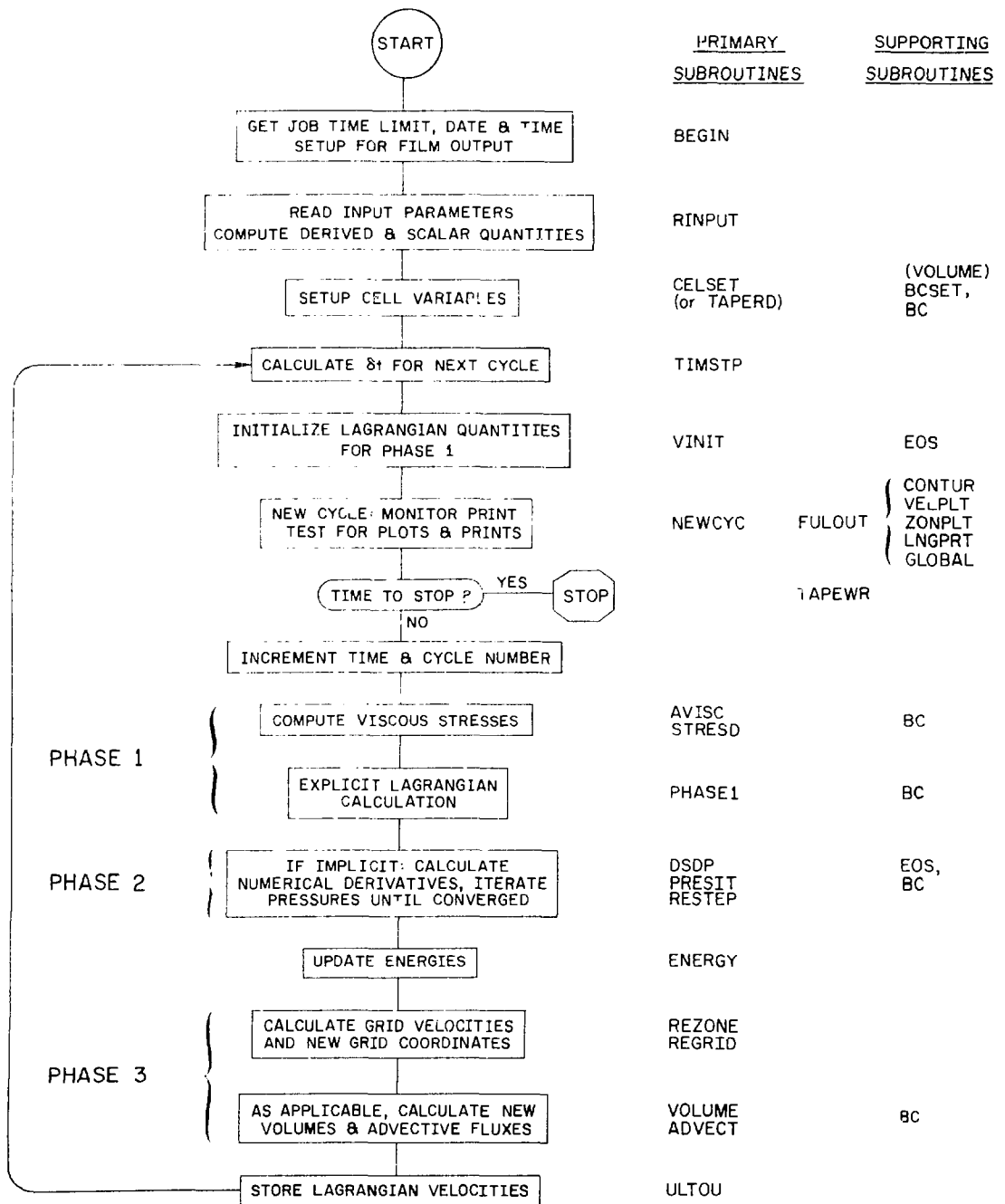


Fig. 4.
General flow diagram for the SALE program.

boundaries. Integer values assigned to these flags range from zero to six and have the following meanings.

- 0 = a free Lagrangian surface,
- 1 = a free-slip vertical or horizontal wall,
- 2 = a curved or tilted free-slip wall,
- 3 = a no-slip wall.
- 4 = a continuative outflow boundary,
- 5 = a specified inflow or outflow boundary, and
- 6 = a specified pressure boundary.

In general, application of a boundary condition implies some appropriate setting of the velocity components for boundary vertices. However, for a free Lagrangian surface, no adjustment is required, as the u_L and v_L from Phase 1 or 2 are the desired values, as in the sample calculation of Sec. IV.A.

For a symmetry boundary or a free-slip wall, the normal wall velocities must be kept at zero throughout the calculation. If such a boundary is parallel to the x or y axis, the u is set to zero on a left or right boundary, or the v is set to zero on a bottom or top boundary. If the wall is slanted or curved (as in the sample calculation of Sec. IV.C), both velocity components must be adjusted to make the flow tangent to the local slope. This is done by first computing an average tangent at a boundary vertex from the neighboring vertices. Then the vertex velocity is changed in such a way that its component along this tangent remains unchanged, but its normal component is zero.

Currently, the general free-slip condition calculates the tangential direction in terms of the fluid-mesh coordinates. For this reason, the boundary keeps its original shape only when the vertices lying along it are treated as Eulerian grid points. It would be straightforward to modify the code to specify a fixed boundary, not tied to the calculational mesh, in terms of which the boundary condition would be applied. This would allow a fixed, curved boundary to be used with fully Lagrangian fluid motion.

It should be noted that general free-slip curved boundaries can cause difficulties in the limit of incompressible flow. The reason is that tangential motion at the curved boundary will not precisely conserve volume. If ϵ , the convergence parameter, is such that it requires total volume changes less than the error committed at the curved boundary, the pressure iteration will not converge. It is necessary, then, to decrease δt , increase ϵ , or improve resolution along the curved boundary.

For a rigid no-slip wall, both velocity components are set to zero, regardless of wall orientation or curvature.

Inflow and outflow boundaries are more complex than those described above, as an inflow boundary requires not only specified velocity components (UIN, VIN), but also a density (ROIN) and energy (SIEIN). To have these cell quantities readily available for fluxing, SALE automatically makes the first column or row of cells at such a boundary into fictitious cells, and adjusts DO-loop limits accordingly so that the calculations bypass such cells.

The typical treatment of an outflow boundary is either to specify the outflow velocities or, if it is continuative, to set the velocity components equal to those located one vertex in. This generally works properly for high-speed flows, but for low-speed or incompressible flows, the prescription may require adjustment if it affects the upstream flow. Note also that an outflow boundary can only be used in a full-donor cell calculation ($a_0 = 1$, $b_0 = 0$), because the flux expressions will refer to outside quantities for any other a_0 and b_0 . SALE provides a warning message if the input specifies other than a full-donor cell treatment in combination with an outflow boundary. This can be dealt with, as we did in the sample calculation of Sec. IV.D, by storing the necessary values in outside cells. In such instances, it is simplest to choose the right or top boundaries for the outflow, as they provide true outside cells (N_x+1 and N_y+1), and inside fictitious cells are not provided for continuative outflow boundaries. One should also be aware that a continuative outflow boundary could become an inflow boundary if the velocity field unexpectedly reverses during the calculation. Should this happen, the flux calculations will be incorrect at the boundary. Continuative boundaries, therefore, must be used with caution.

The final type of boundary condition we offer is a specified pressure boundary. It too uses inside fictitious cells for the pressure definition. Again, DO-loop limits are automatically adjusted to bypass such cells in the calculation, except in Phase I, where these cells are included so that pressure accelerations are correctly calculated at the boundary. When a specified pressure boundary is used, the pressure must be defined in the input data list as the value of PAP.

The boundary conditions applied on the edges of the logical SALE mesh are set in the sequence of left, right, bottom, and top. A corner vertex, common to two edges, is therefore set to the condition of the edge that is treated second.

The boundary conditions of both edges meeting at a corner are considered when the general free-slip condition is applied to either edge. If both edges are general free-slip, we 'wrap around' and reference the neighboring points on each side when calculating the slope at the corner. This is especially helpful for meshes with connected curved edges, as it maintains tangential flow.

D. Numerical Stability and Accuracy

Numerical stability and accuracy are essential factors to consider when assessing the application of numerical simulation models. Time and experience have proven that first-order methods such as SALE are perfectly adequate for many problems of interest. The researcher, however, should realistically evaluate his needs when he considers the suitability of any computing technique or program. It is no wiser to pay the expense for an overly sophisticated technique than it is to struggle with trying to apply a technique to a situation for which it is not suited.

The useful accuracy of a given numerical solution may be difficult to determine analytically.⁴ In such cases, it is sometimes possible to use a spectrum of computer runs with different meshes, time steps, donor-cell coefficients, artificial viscosities, convergence criteria, etc., to determine if a calculated effect is physical or simply a numerical artifice. Aside from this type of 'brute force' approach, there are several general rules one should follow in using the SALE program. For example, if a solution exhibits large variations over distances comparable to a cell width or over times comparable to the time step, it is probably not very reliable. Thus, when computing time or memory limitations preclude the use of a cell size and time step that are fine enough to resolve all spatial and temporal variations of interest in the dependent variables, then the results must be interpreted with care. In spite of such limitations, the investigator often has some choices. For example, a thin boundary layer in a large region may be resolved by employing much finer zoning at the wall and a no-slip boundary condition. If, however, its resolution is unimportant, then coarser zoning and a free-slip condition at the wall may be a valid approximation.

Numerical methods may give solutions that develop large, high-frequency oscillations in space or time. If the physical problem being modeled is known not to exhibit such behavior, the source may be numerical instability,

caused by violation of one or more restrictions that should be used to limit the size of the time step.

Implicit methods have less stringent stability requirements than explicit methods, which typically require that the Courant condition on sound signal propagation,

$$\max\left(\frac{c \delta t}{\delta x}, \frac{c \delta t}{\delta y}\right) < 1 \quad ,$$

is not violated. When SALE is run implicitly, the Courant condition can be avoided because it uses time-advanced quantities, which are determined by iteration. The resulting increase in running time per cycle can be more than compensated for by the reduction in number of time steps, but the time step must always be chosen to ensure that important short time-scale phenomena are resolved. When the Mach number of the flow exceeds the 0.1 range, an explicit solution is often more efficient, but below this range, the restriction on sound signal propagation would require a large number of time steps to move the fluid even one cell width, and the implicit solution becomes preferable.

Whether run implicitly or explicitly, the time step in SALE is always restricted by the well-verified condition that fluid cannot be moved more than approximately one cell width per time step, that is,

$$\delta t < \min\left(\frac{\delta x}{|u|}, \frac{\delta y}{|v|}\right) \quad .$$

The minimum implies that every cell in the mesh must be considered to ensure that the δt satisfies the most restrictive case. Our general advice is to start by choosing δt equal to one-fifth of the minimum cell transit time (DTF = 0.2 in the code), being more liberal if experience allows it for the application at hand. Although Lagrangian calculations do not have as restrictive a stability limit due to advection, we still recommend that the time step satisfy this requirement, primarily for reasons of accuracy, and secondarily for efficiency by avoiding negative cell volumes at the end of Phase 1, as negative cell volumes automatically force the code to back up and restart the cycle with a smaller time step.

The donor cell or upstream component of the advection terms contributes numerical diffusion-like effects that influence the stability conditions. In particular, space-centered differencing ($a_0 = b_0 = 0$) leads to unstable results,² whereas full donor-cell differencing ($a_0 = 1, b_0 = 0$) may be too diffusive for some circumstances.

Our general recommendation is to use a_0 as small as possible without generating an instability.

Another numerical stability condition relates to the stress tensor. When viscous effects are included, the crucial condition to be satisfied is that

$$\delta t < \left[\frac{2(\lambda + 2\mu)}{\rho} \left(\frac{1}{\delta x^2} + \frac{1}{\delta y^2} \right) \right]^{-1}$$

is met in every cell, which roughly states that momentum must diffuse less than one cell width per time step. Also to be considered in Phase I is the related stability condition on the alternate node coupler, which can be shown to be $a_{nc} < 1$.

In SALE, we automatically choose a new time step every cycle (subroutine TIMSTP) that must satisfy four requirements: (1) advective flux, (2) viscous effects of λ and μ , (3) no more than 5% increase from the time step

of the previous cycle, for reasons of accuracy, and (4) no greater than the maximum time step for the calculation (*DTMAX* in the input file). We assume that the user has satisfied upstream (a_0, b_0) and node coupling (ANC) requirements in the input data.

A final comment regarding the selection of the time step is that we specifically do *not* recommend tailoring the time step to precisely fit a specified output time. Occasionally, this may result in suddenly having, for an output cycle, a time step several orders of magnitude smaller than the problem has been running with. Experience has shown that such a discontinuous drop can adversely affect the results and cause some computing methods to blow up. It is better to let the four requirements above determine the time step, and do the output when the problem time equals or first exceeds the specified output time.

IV. SAMPLE CALCULATIONS

SALE is written in a very general fashion and is not geared to any specific type of calculation, as many codes are. It has an unusually wide range of capabilities, but as a result, most problems will require at least some code modification. Typically, this is either in the setup, boundary conditions, or the rezone. Techniques for mesh generation, boundary treatment, and rezoning are explored in the examples that follow. These include input data and code modifications, from which it is apparent that the necessary code changes for most problems are quite straightforward. In these examples, code changes are written in CDC UPDATE format. A line of the form *I, *deckname.n* means the FORTRAN statement(s) that appear between the *I line and the next line beginning with a * are inserted following line *deckname.n*. The line *D, *deckname.m*, *deckname.n* means to delete statements *deckname.m* through *deckname.n* and replace them with any lines between the *D and the next * line.

The Central Processor Unit (CPU) times and the grind times are given for each example. The grind time, defined as the CPU time per cell per cycle, $\delta\text{CPU}/(N_x * N_y)$, is a useful indicator of the computing efficiency of the code. It should be noted that CPU usage is influenced by the dynamic load on the resources in a time-sharing environment.

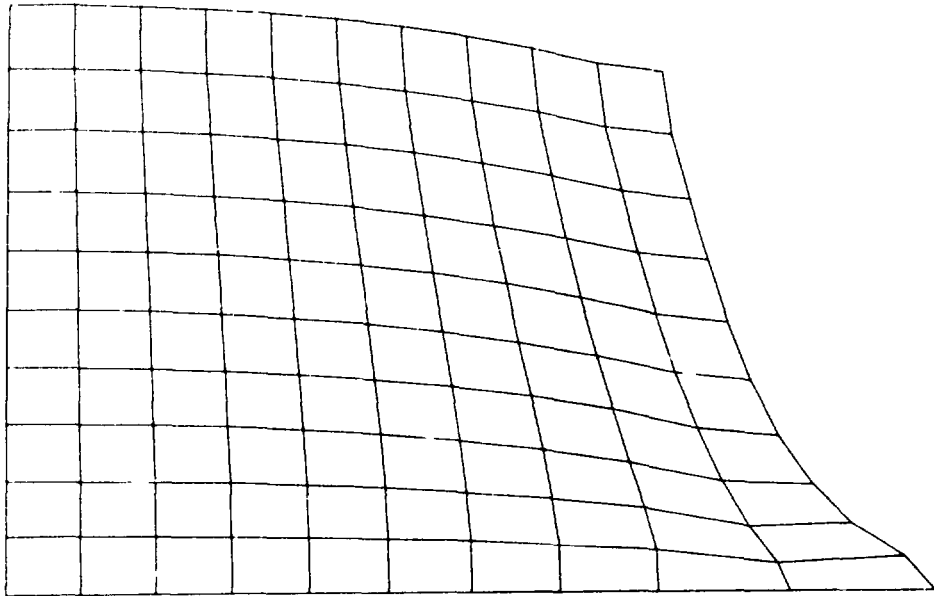
A. Broken Dam

This problem can be solved by the SALE program exactly as listed in App. A. Because no code modifications are required, it has been selected as the test problem in App. C, which presents several pages of numerical output for verification of results at other installations. The setup consists of a 10-cell by 10-cell uniform mesh, in plane geometry, resting on a rigid free-slip surface. The left boundary is a rigid free-slip wall, representing a plane of symmetry. At time $t = 0$, a dam at the right wall is removed, and the fluid is free to flow outward under the influence of gravity. The mesh is allowed to move in a purely Lagrangian fashion, and

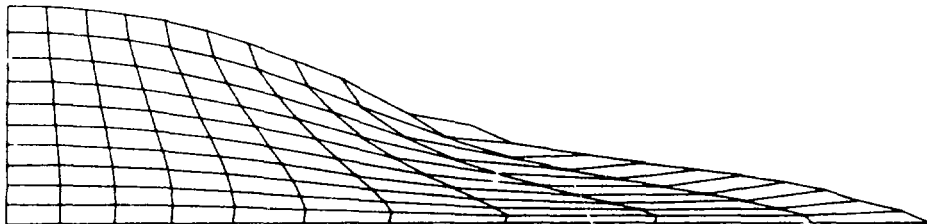
the top and right boundaries are treated as Lagrangian free surfaces. The calculation is run implicitly, in the incompressible limit (see Sec. II.E). Figure 5 shows the mesh configuration at three selected times: $t = 2.0$ (cycle 20), $t = 5.0$ (cycle 71), and at the specified finish time, $t = 10.0$ (cycle 207). The plots in the figure create the illusion of decreasing volume, solely because we scaled each plot to fit a specified maximum width on the film frame. The actual rightward progress of the flow can be determined from the numerical printout of cell data. The x coordinate of the lower right corner vertex (1,1), which was at position $x = 10.00$ at $t = 0$, is located at $x = 14.40$ at $t = 2.0$, at $x = 28.94$ at $t = 5.0$, and at $x = 58.10$ at $t = 10.0$. The y coordinate of the upper left corner vertex (1,1), which was at position $y = 10.00$ at $t = 0$, has dropped to $y = 9.127$ by $t = 2.0$, to $y = 6.782$ by $t = 5.0$, and down to $y = 3.379$ at $t = 10.0$.

The calculation required 42.5 s of CDC-7600 CPU time to run to completion, and created 110 frames of plots and printed information on microfiche. The input file had the following appearance.

```
T3AAA SLUMP, PURE LAGRANGIAN W/ INC=1.
  NX      10
  NY      10
  IMP     1
  INC     1
  IREZ    1
  LPR     1
  WB      1
  WL      1
  WR      0
  WT      0
  DX      1.0
  DY      1.0
  CYL     0.0
  DT      0.10
  DTMAX   0.10
  TLIMD   0.0
  TWFILM  1.0
  TWPRTR  200.0
  TWFIN   10.0
  OM      1.00
  PEPS    1.0E-4
```



EXPORT-SALE 04/06/79 14:28:13 T3AAA SLUPP. PURE LAGRANGIAN W/ INC=1. ASQ=100 040679-3
 T= 2.00000E+00 CYCLE 20



EXPORT-SALE 04/06/79 14:28:13 T3AAA SLUPP. PURE LAGRANGIAN W/ INC=1. ASQ=100 040679-3
 T= 5.02500E+00 CYCLE 71



EXPORT-SALE 04/06/79 14:28:13 T3AAA SLUPP. PURE LAGRANGIAN W/ INC=1. ASQ=100 040679-3
 T= 1.00075E+01 CYCLE 207

Fig. 5.

The broken dam calculation showing the configuration of the Lagrangian mesh at times $t = 2.0$, $t = 5.0$, and $t = 10.0$.

```

EPS      1.0E-4
RF       0.05
ARTVIS   0.1
LAMBDA   0.0
MU       0.0
ANC      0.05
X1       1.0
GX       0.0
GY       -1.0
AO       1.0
BO       0.0
ASQ      1.0E+2
RON      1.0
GM1      0.0
RO1      1.0
SIE1     0.0
UIN      0.0
VIN      0.0
ROIN     0.0
SIE1N    0.0
PAP      0.0

```

For further information on this calculation, refer to App. C.

B. One-Dimensional Shock Tube

The two graphs plotted in Fig. 6 illustrate density profiles from Lagrangian (upper profile) and Eulerian (lower profile) calculations of a 2:1 density-ratio shock tube. No attempt was made to obtain the best solutions that SALE can produce for this problem; rather, our intent is to illustrate that satisfactory solutions can be obtained in both limits. In Fig. 6, the SALE solutions are plotted with a heavy line and the theoretical solution⁵ is plotted with a light line.

The calculations were performed in a plane mesh 60 cells long by 1 cell high, allowing 30 cells for each fluid region. The initial density was 0.2 on the left and 0.1 on the right, and the initial specific internal energy was 0.18. The gas was polytropic with $\gamma = 5/3$. The initial cell size was $\delta x = \delta y = 1/3$. Both calculations were completely inviscid ($\lambda_0 = \lambda = \mu = a_{nc} = 0$), but were run with full donor-cell differencing ($a_0 = 1, b_0 = 0$). The only difference between the two calculations is that the first is Lagrangian implicit (Phases 1 and 2 only), and the second is Eulerian explicit (Phases 1 and 3 only).

At $t = 0$, the diaphragm separating the two fluid regions was instantaneously removed, causing a shock

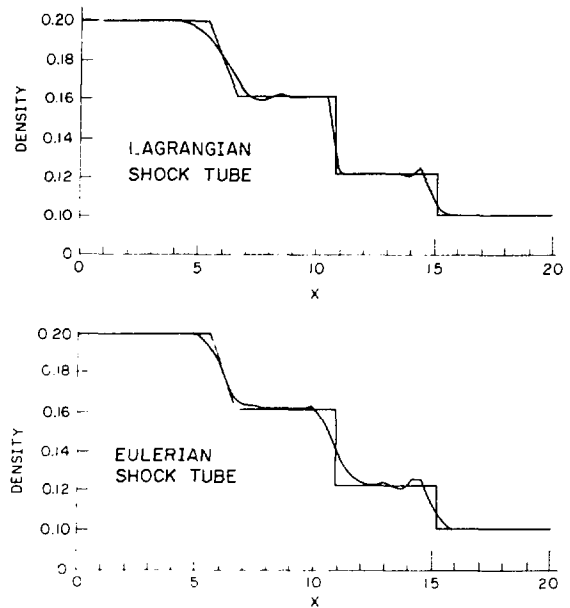


Fig. 6.

Density profiles at time $t = 10.0$ from an implicit Lagrangian (upper) and an explicit Eulerian (lower) calculation of a shock tube with a 2:1 density ratio.

to advance into the lower density region and a rarefaction to propagate back from the contact surface into the higher density region. In both calculations, δt was held constant at 0.1, and the profiles shown in Fig. 6 are at $t = 10.0$. The Lagrangian calculation required 8.6 s of CDC 7600 CPU time to run to $t = 15.0$, running at 3 iterations per cycle, with a grind time around 0.315 ms. The Eulerian calculation required 7.4 s, with a grind time around 0.210 ms. The one code modification required was to distinguish the two density regions in the setup:

```

*IDENT S020279
*1,CELSET,35
  IF(1.GT.30) RO(1J)=0.1

```

The input file for the Lagrangian shock tube appeared as follows.

T3AAA LAG ST, IMP=1, LAM=0 YAQUI

```

NX      60
NY      1
IMP     1
INC     0
IREZ    1
LPR     2
WB      1
WL      1
WR      1
WT      1
DX      .333333333
DY      .333333333
CYL     0.0
DT      0.1
DTMAX   0.1
TLIMD   0.0
THFILM  1.0
THPRTR  1.0
THFIN   15.0
OM      1.00
PEPS    1.0E-4
EPS     1.0E-4
RF      0.0
ARTVIS  0.0
LAMEDA  0.0
MU      0.0
ANC     0.0
XI      1.0
GX      0.0
GY      0.0
AO      1.0
BO      0.0
ASQ     0.0
RON     0.0
GM1     .66666667
ROI     0.2
SIEI    0.18
UIN     0.0
VIN     0.0
ROIN    0.0
SIEIN   0.0
PAP     0.0

```

C. Supersonic Flow Through a Curved Duct

In this example we illustrate supersonic flow through a curved two-dimensional duct. Of interest here is the procedure for creating the mesh, and the usefulness of the general free-slip boundary condition. The schematic for the mesh generation (Fig. 7) calls for a 35-cell-long by 6-cell-high Eulerian mesh, of which a 15-cell portion of the central region is to be deformed into a 90° curve, leaving a 10-cell straight section at

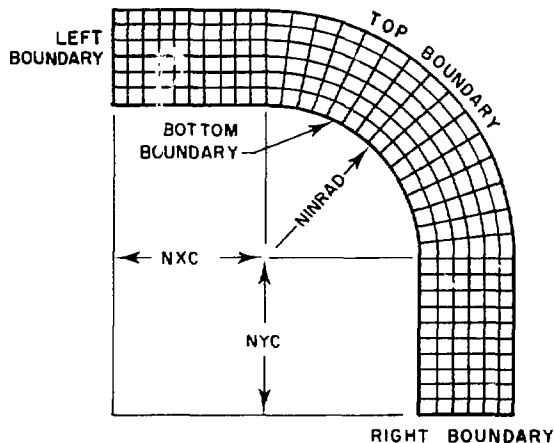


Fig. 7.

The curved-duct mesh. The three dimensions are defined in numbers of cells.

either end. The right mesh boundary, now visually appearing at the bottom, is the inflow boundary, and the left mesh boundary allows a continuative outflow. The top and bottom boundaries employ the general free-slip condition, which is intended for arbitrarily curved or straight regions.

The fluid is a polytropic gas with $\gamma = 1.4$. Initial conditions state that the fluid in the mesh is at rest, with density and specific internal energy both equal to unity, and that at time $t = 0$, a shock with a Mach number $M = 10$ enters at the right boundary. The shock relations for a polytropic gas⁵ allow the required conditions to be calculated as functions of M alone. In this case, the shock speed is 7.4833, while behind the shock, the fluid speed is 6.1737, the density is 5.7143, and the specific internal energy is 20.3874.

Figure 8 shows velocity vectors and isobars at three selected times in the calculation. The high and low contour values at the time of each contour plot are labeled with an H and L. At the first time, $t = 0.25$ (cycle 33), the shock is midway through the curved portion of the duct, and a high-pressure region has developed where it has encountered the wall. By time 0.50 (cycle 71), in the second set of plots, the shock front is approaching the outflow boundary and shows a strong deformation as a result of having been turned 90°. At the last time shown, $t = 3.00$ (cycle 445), well after the shock front has passed the outflow boundary, a nearly steady-state

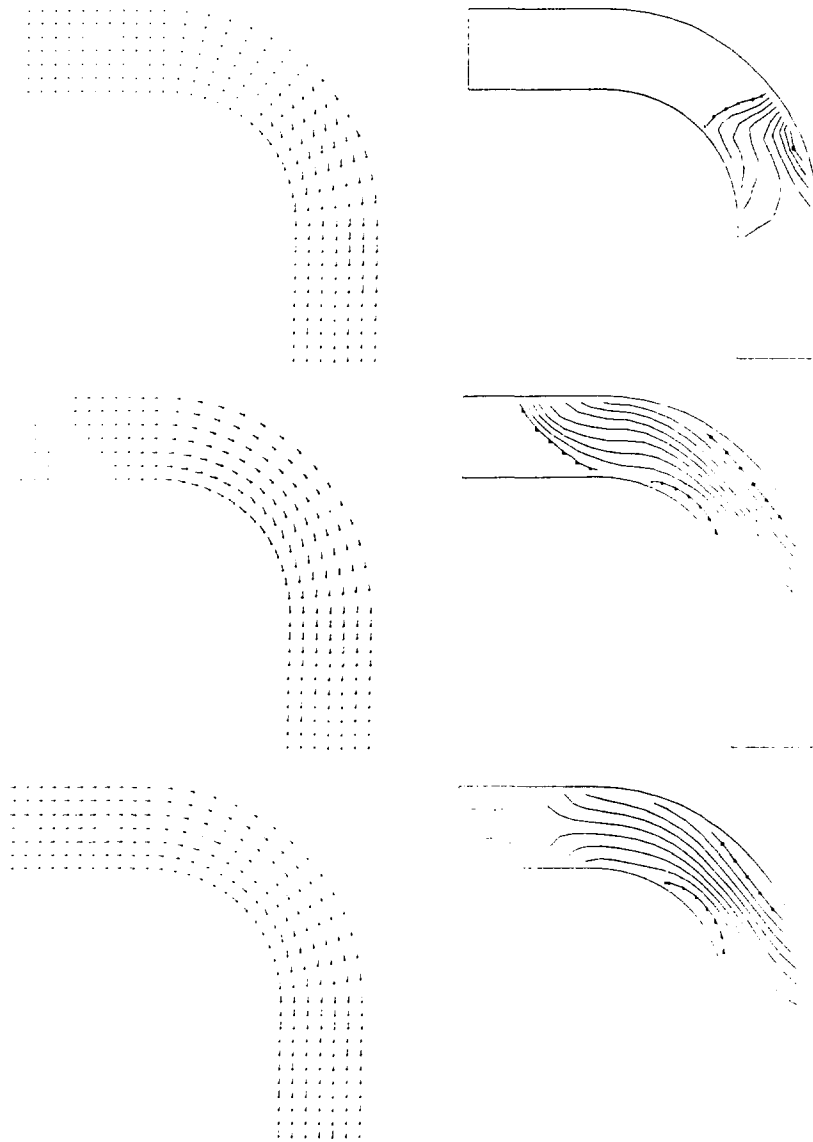


Fig. 8.

Velocity vectors (left) and isobars (right) for the supersonic duct calculation, at times $t = 0.25$ (top), $t = 0.50$ (middle), and $t = 3.00$ (bottom).

configuration has been established. The pressures (and similarly the densities and specific internal energies) are highest at the outer radius of the bend where the fluid reflects off the wall in the turning process.

This calculation required 28.0 s of CDC-7600 CPU time to run to time $t = 3.0$, with a grid time around 0.200 ms. The code modifications and input file for this problem are listed below. The first change, to DTF, allows the use of a larger time step than the standard conservative value in the code. Although this is not

possible for all problems, we did realize a substantial increase in computing efficiency for the duct problem. The remaining changes, in subroutine CELSET, create the mesh using the three dimensions NXC, NYC, and NINRAD identified in Fig. 7.

By simply varying the values of the five parameters (NX, NY, NXC, NYC, and NINRAD), one can alter the configuration considerably without having to revise the setup logic. In addition, it would be possible to create a mesh as shown here, then make another pass to

further modify it, for example, necking the outflow end to a nozzle. Iterative or direct schemes for grid generation⁶ are quite useful for such purposes.

```
*IDENT S041379
*J,RINPUT,58
    DTF=0.5
*I,CELSET,8
    NXC=NYC=10
    NINRAD=10
    R1=FLOAT(NINRAD)*DY
    CENX=FLOAT(NXC)*DX
    CENY=FLOAT(NYC)*DY
    NARC=(NXP-NYC)-(NXC+1)
    TH=90./FLOAT(NARC) * 0.0174532925
*D,CELSET,12,CELSET,13
    IF(1.LE.NXC+1) GO TO 2
    IF(1.GE.NXP-NYC) GO TO 3
    THFAC=FLOAT(1-(NXC+1))*TH
    SINFAC=SIN(THFAC)
    COSFAC=COS(THFAC)
    RADIUS=R1+FLOAT(J-1)*DY
    X(IJ)=CENX + RADIUS*SINFAC
    Y(IJ)=CENY + RADIUS*COSFAC
    GO TO 5
  2 X(IJ)=FLOAT(1-1)*DX
    Y(IJ)=FLOAT(J-1+NYC+NINRAD)*DY
    GO TO 5
  3 X(IJ)=FLOAT(J-1+NXC+NINRAD)*DX
    Y(IJ)=FLOAT(NXP-1)*DY
  5 CONTINUE
```

T3AAA 35X6 SUPERSONIC DUCT 122078. IMP=0. 050779

```
NX      35
NY       6
IMP      0
INC      0
IREZ     0
LPR      1
WB       2
WL       4
WR       5
WT       2
DX      0.1
DY      0.1
CYL     0.0
DT      0.01
DTMAX   1.0
TLIMD   0.0
TWFILM  0.25
THPRTR  100.0
TWFIN   3.0
OM       1.0
PEPS    1.0E-4
EPS     1.0E-4
RF      0.0
ARTVIS  0.2
LAMBDA  0.0
MU      0.0
ANC     0.05
XI      1.0
```

```
GX      0.0
GY      0.0
AO      1.0
BO      0.0
ASQ     0.0
RON     0.0
GMI     0.4
ROI     1.0
SIEI    1.0
UIN     0.0
VIN     6.1737
ROIN    5.7143
SIEIN   20.3874
PAP     0.0
```

D. von Karman Vortex Street

The sequence of velocity vector plots in Fig. 9 show the development of a von Karman vortex street. This fluid-flow phenomenon represents a true physical instability that is seldom seen because of fluid transparency, but is a common occurrence when air or water flows past an object. If the Reynolds number (Re) of the flow lies in a specific range,⁷ the wake will depart from uniform laminar flow, and vortices will be shed alternately from each corner of the object in a regular pattern.

In this example, the initial condition was a uniform upward flow of fluid past both sides of a rigid obstacle centered across the inflow boundary of a 16×46 cell mesh. The problem was run implicitly in the incompressible limit (see Sec. II.E).

After the laminar flow was well established, at time $t = 10$ (cycle 210, Fig. 9a), we perturbed the flow by decreasing the incoming velocity on one side of the obstacle by 5%, while increasing it by 5% on the other side. This perturbation was allowed to decay immediately as a function of time, and went to zero at $t = 30$. Its effect is evident by $t = 20$ (cycle 432, Fig. 9b), and by $t = 30$ (cycle 654, Fig. 9c) the flow is noticeably asymmetric. Figures 9d-9f show the appearance at $t = 40$ (cycle 925), $t = 65$ (cycle 1585), and $t = 70$ (cycle 1709). The frequency of shedding at each corner is about 10 units of time, thus the plots at $t = 50$ and $t = 60$ are similar to that at $t = 70$, and those at $t = 45$ and $t = 55$ to that at $t = 65$.

The mean flow velocity is about 0.5, the fluid density is 1.0, the effective obstacle width is 1.75, and the shear viscosity $\mu = 3.3 \times 10^{-3}$. This corresponds to $Re \approx 260$, but the effective viscosity in the system is probably closer to 10^{-2} , due to truncation error effects from donor-cell differencing. Although a truncation error

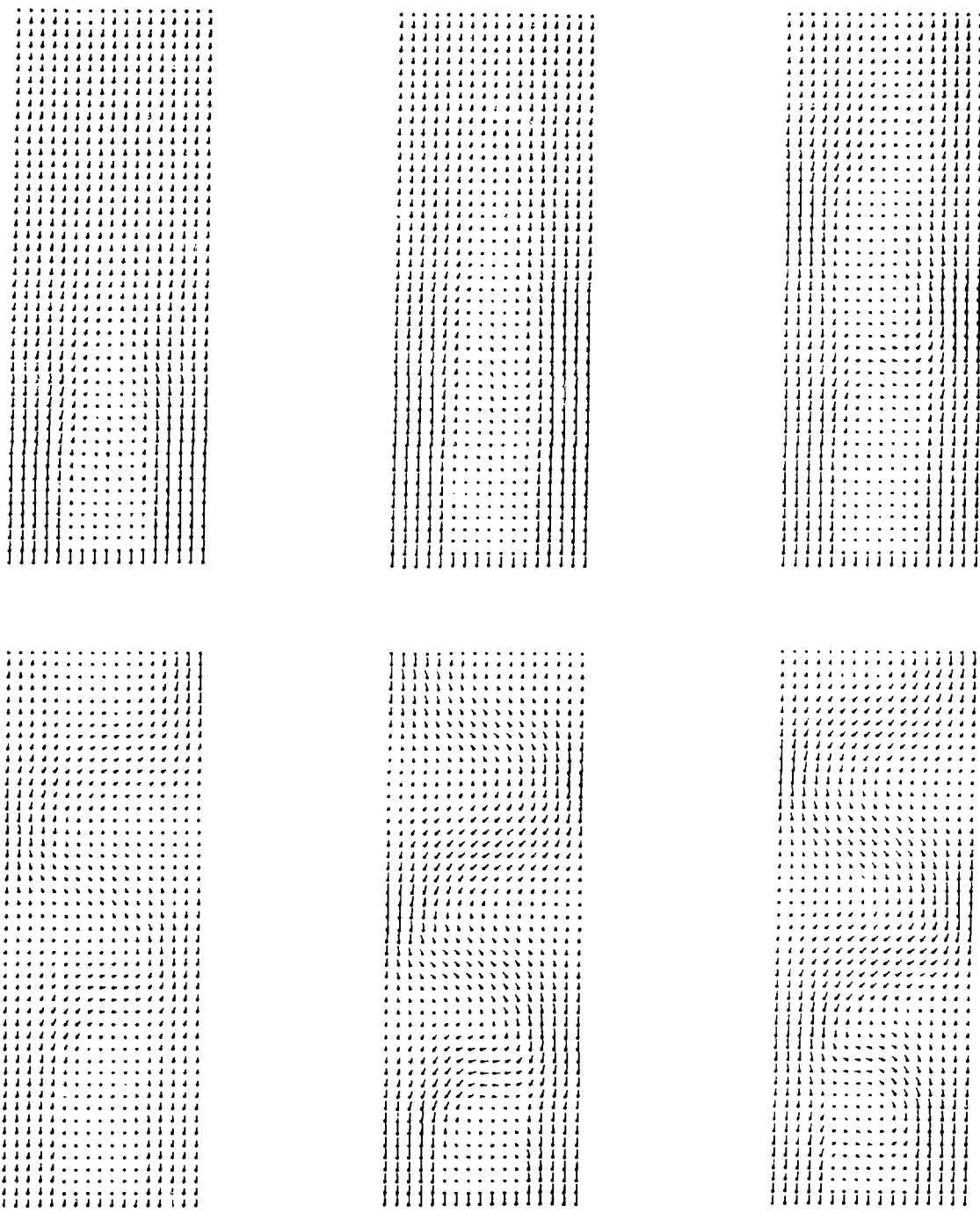


Fig. 9.
Velocity vectors for the von Karman vortex street calculation, at times $t = 10$, $t = 20$, $t = 30$, $t = 40$, $t = 65$, and $t = 70$.

analysis⁴ has not been performed for SALE, it is safe to say the actual Reynolds number of the flow is closer to 100. Our results are also influenced by the narrow channel width and the placement of the obstacle at the inflow boundary, rather than up in the mesh where the flow could pass completely around it.

Of importance are the modifications required at the continuative outflow boundary. Outflow boundaries always pose a problem for low speed flows, because whatever prescription is chosen has the potential to affect the entire flow field upstream. Our problem is compounded in the vortex street calculation, as the vortices significantly change the outflow velocity profile from one side of the channel to the other. The usual treatment for a continuative outflow boundary is to set both velocity components equal to those located one cell in from the boundary, except during the iteration, when they are allowed to vary with changes in pressure, as any interior velocity component. However, for the vortex street, the outflow velocities across the top must be continually scaled to the inflow to preserve the mass balance in the system. This must be repeated every iteration, because if the velocities are allowed to float, the number of iterations will double. Note also in this example that the open length across the inlet, required for the scaling, is $9\delta x$ rather than the $8\delta x$ it would appear to be, as two half cells are effectively available for mass flux at the obstacle corners.

A small amount of fourth order node coupling was required to prevent difficulty at the trailing edges of the obstacle.² To minimize diffusion, we ran with only a small amount of donor cell differencing, $a_0 = 0.1$, $b_0 = 0$. For any departure from full donor-cell ($a_0 = 1$, $b_0 = 0$), the density and energy *must* be set in the cells "outside" of the continuative boundary to prevent erroneous values from being computed in the flux calculation at the boundary.

The foregoing special considerations are dealt with in the UPDATE modifications listed below.

The calculation required 16.5 min of CDC-7600 CPU time to reach the completion time of $t = 70$. At early times, the iteration number was typically 5 per cycle with a grind time of 0.46 ms. By $t = 30$, as the flow became unsteady, the iteration number was around 10 (0.66-ms grind). By $t = 50$, 20 iterations (1.00-ms grind) were required. Thereafter, the iteration history oscillated, ranging as high as 27 (1.30-ms grinds), down to 13 (0.77-ms grind).

```

*IDENT KARMAN
*D,BC,13
  VAVG=0.
  DO 100 I=1,NX
    IJ=NY*NXP+I
    100 VAVG=VAVG+(VV(IJ-NXP)+VV(IJ-NXP+1))*0.5*DX
    CAPK=VIN*9.*DX/VAVG
*D,BC,103
  VEPS=AMAX1((30.-I)*2.5E-3,0.0)
  IF(T.LT.10.) VEPS=0.
  VEFF=1.-VEPS
  IF(I.GT.5) VEFF=0.
  IF(I.GT.12) VEFF=1.+VEPS
  VV(IJ+NXP)=VEFF
*D,BC,127
  540 CONTINUE
*I,BC,129
  RO(IJ)=RO(IJ-NXP)
  ROL(IJ)=ROL(IJ-NXP)
  SIE(IJ)=SIE(IJ-NXP)
  VV(IJ)=CAPK*VV(IJ)
*I,CELSET,24
  V(IJ)=1.
*D,CONTUR,137
  IF(I.EQ.1 .AND. (I.GT.4.AND.I.LT.13))
    1 CALL DRV(IX4,IY4,IX1,IY1)

```

```

T3AAA KVS 16X46 CELLCEN MOMFLX, A0=.10, 041379
  NX      16
  NY      46
  IMP     1
  INC     1
  IREZ    0
  LPR     1
  WB      5
  WL      1
  WR      1
  WT      4
  DX      0.25
  DY      0.25
  CYL     0.0
  DT      0.05
  DTMAX   1.0
  TLIMD   0.0
  THFILM  5.0
  THPRTR  200.0
  THFIN   70.0
  OM      1.80
  PEPS    1.0E-4
  EPS     1.0E-4
  RF      0.00
  ARTVIS  0.0
  LAMBDA  0.0
  MU      3.3333E-3
  ANC     0.05
  XI      1.0
  GX      0.0
  GY      0.0
  A0      0.1
  B0      0.0

```

ASQ	0.0
RON	0.0
GM1	0.4
ROI	1.0
SIEI	0.0
UIN	0.0
VIN	1.0
ROIN	1.0
SIEIN	0.0
PAP	0.0

E. Strong Shock Passing Over a Mercury Drop in Water

This final example concerns the calculation of a strong isothermal shock passing over a drop of mercury in water. It involves a more complex continuous rezone that illustrates what is sometimes required in order to obtain a solution, but it also illustrates the possibilities that can be realized in SALE with some imagination.

Figure 10 shows the initial configuration of the mesh. The drop has a 1-cm radius and all units are in the CGS system. The incident shock, input at the lower mesh boundary, has speed 3.62×10^5 , well into the supersonic regime, as the sound speed of water is 1.5×10^5 . The solution of the isothermal shock relations⁵ gives the inflow conditions behind the shock—a water velocity of 3×10^5 and density of 5.83. The mercury has density 13.5 and a slightly lower sound speed, 1.45×10^5 .

Mesh configuration, velocity vectors, and pressure contours at selected times are shown in Fig. 11. In Fig. 11a, at $t = 5 \times 10^{-6}$ (cycle 100), the shock has encountered the leading edge of the drop and a large pressure increase develops there because of the sudden increase in inertial resistance. By $t = 7.5 \times 10^{-6}$ (cycle 150, Fig. 11b), significant deformation of the drop has already occurred when the shock has reached its back side. By $t = 1 \times 10^{-5}$ (cycle 200, Fig. 11c) the shock is noticeably diffracting, and at $t = 1.25 \times 10^{-5}$ (cycle 250, Fig. 11d) it collapses on the symmetry axis behind the drop, and sends out a radial pressure wave evident in the $t = 1.5 \times 10^{-5}$ plot (cycle 300, Fig. 11e). A Rayleigh-Taylor type of instability is to be expected at the leading surface of the drop. The instability may be developing in the $t = 1.5 \times 10^{-5}$ plot, but the numerical resolution is too coarse and the time too short to show this.

The UPDATE modifications to set up and run this calculation are listed below. The modifications to subroutine CELSET principally concern the creation of the initial grid, which required 158 iterations.⁶ The input file now allows for the definition of one material in our two-

material problem. We defined the mercury in the input and supplied values for the water where needed (subroutines CELSET and VINIT). For efficiency, we bypassed the equation of state in the setup and the entire energy subroutine, taking advantage of the isothermal conditions.

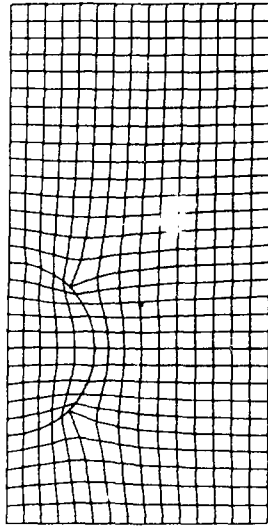
A major portion of the UPDATE concerns the continuous rezone. The DATA statement identifies the vertices along the surface of the mercury drop, in single-subscript code notation, where 81 and 241 are the vertices on the axis, at the leading and trailing edges, respectively. Except for the boundary of the mercury drop, continuous rezoning was employed to keep mesh distortions under control. A relaxation factor (RF) of 1.0 was required to keep the vertices sufficiently separated in the shock front. In an initial attempt, a value of $RF = 0.05$ resulted in cells going to zero height across several rows.

Initially, we ran with the boundary of the mercury drop treated as purely Lagrangian (that is, moving with the fluid), but by a time of 5×10^{-6} , as the shock was encountering the drop, vertices (6,6), (6,7), (6,8), and (6,9) pinched together and crossed over. To counter this, we added a DO loop at the end of the rezone to keep the interface vertices better distributed. Considering three vertices at a time, we passed a circular arc through them and rezoned the center vertex so that its new position would lie on the arc. The procedure involved determining the coordinates (x_0, y_0) and radius (r_0) of the circular arc for use in a quadratic equation, whose correct root may be either the positive or the negative one, depending upon the circumstances. Choice of the wrong root would place the new position of the vertex on the opposite side of the circle, so care must be taken to select the root that places the new position closer to the original position.

The additional loop completely eliminated all problems of interface vertex spacing. Eventually, however, the shock deformed the drop so severely that at time 1.71×10^{-5} (cycle 383), cell inversions took place in the folded region around vertex (16,6) and we ended the run. To proceed further would require a slide-line treatment and/or moving cells from one side of the interface to the other, but a project of this magnitude was beyond the scope of this study. The CPU time required for the run was 41.5 s on the CDC-7600, with a grind time of 0.174 ms.

It can be noted in Fig. 11 that our rezone allowed the vertices along the inflow boundary (the $j = 2$ line) to

7-0 CYCLE 0 TIME 0.00
NEW 0.1-0 01.0 00000



SPRT-BA. 01/10/70 10.20-15 13AM 150000 10.000 0.01000
CYCLE 0

SPRT-BA. 01/10/70 10.20

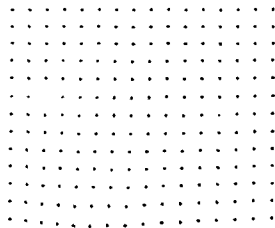


Fig. 10.
Initial mesh configuration for the mercury drop calculation.

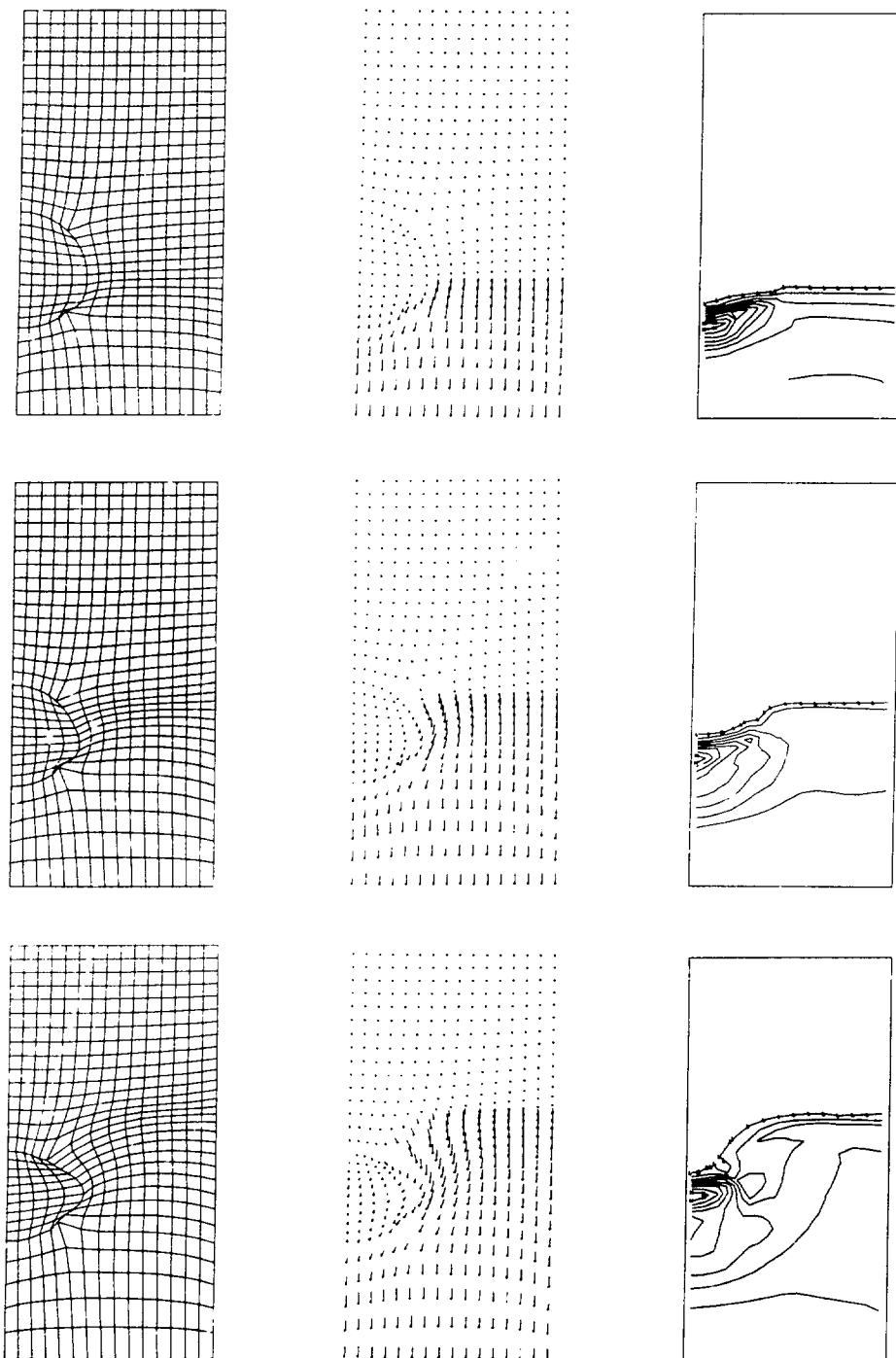


Fig. 11.

SALE calculation of a strong shock passing over a mercury drop in water. From left to right: the computing mesh, velocity vectors, and isobars. From top to bottom, the sequences are at times 5.0×10^{-6} , 7.5×10^{-6} , and 1.0×10^{-5} .

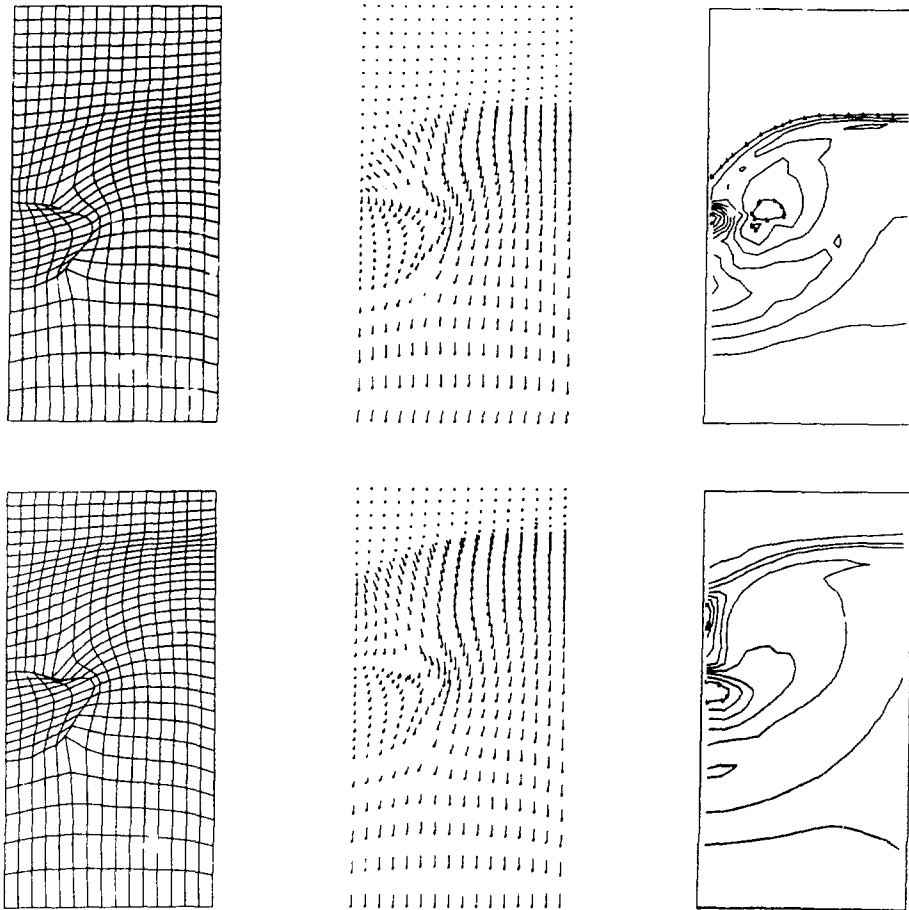


Fig. 11. (cont)
 The times are 1.25×10^{-5} and 1.50×10^{-5} .

move. As a result, the inflow conditions were not perfectly maintained. This particular calculation was not significantly affected, but as a general rule the vertices on a specified inflow boundary should not be allowed to move. A slight modification to the rezone logic to ensure zero grid velocities at these vertices can easily be made.

```

*IDENT S040679
*D,CELSET.9,CELSET.15
  ITER=0
  X0=0.0
  Y0=2.0
  RAD=1.0
  RDX=1./DX
  RDY=1./DY
5  IND=0
DO 19 J=1,NYP
  IJ=(J-1)*NXP+1
  IJP=IJ+NXP
  
```

```

      IJM=IJ-NXP
      DO 18 I=1,NXP
      IPJ=IJ+1
      IMJ=IJ-1
      IF(ITER.GT.0) GO TO 10
      X(IJ)=FLOAT(I-1)*DX
      Y(IJ)=FLOAT(J-1)*DY
      IND=I
      GO TO 17
10 IF(J.EQ.1 .OR. J.EQ.NYP) GO TO 12
      IF(I.EQ.1) GO TO 13
      IF(I.EQ.NXP) GO TO 14
      IF(I.LE.6 .AND. (J.EQ.6 .OR. J.EQ.16)) GO TO 15
      IF(I.EQ.6 .AND. (J.GE.6 .AND. J.LE.16)) GO TO 15
      XN=.25*(X(IPJ)+X(IJP)+X(IMJ)+X(IJM))
      YN=.25*(Y(IPJ)+Y(IJP)+Y(IMJ)+Y(IJM))
11 DELX=XN-X(IJ)
      DELY=YN-Y(IJ)
      X(IJ)=XN
      Y(IJ)=YN
      GO TO 16
12 IF(I.EQ.1 .OR. I.EQ.NXP) GO TO 17
      XN=.5*(X(IMJ)+X(IPJ))
      YN=Y(IJ)
      GO TO 11
13 IF(J.EQ.6 .OR. J.EQ.16) GO TO 17
14 XN=X(IJ)
      YN=.5*(Y(IJP)+Y(IJM))
      GO TO 11
15 BETA=.02*((X(IJ)-X0)**2+(Y(IJ)-Y0)**2-RAD**2)
      DELX=(X0-X(IJ))*BETA
      DELY=(Y0-Y(IJ))*BETA
      X(IJ)=X(IJ)+DELX
      Y(IJ)=Y(IJ)+DELY
16 XX=ABS(DELX)*RDX
      YY=ABS(DELY)*RDY
      IF(XX.GT.1.E-4 .OR. YY.GT.1.E-4) IND=1
17 IJ=IJ+1
      IJP=IJP+1
18 IJM=IJM+1
19 CONTINUE
      ITER=ITER+1
      IF(IND.GT.0) GO TO 5
      WRITE(59,20) ITER
20 FORMAT(110)
*1,CELSET.35
      IF(1.GT.5 .OR. J.LE.5 .OR. J.GE.16) R0(IJ)=1.0
*D,CELSET.41
      F(IJ)=0.0
*1,REZONE.8
      DIMENSION IHG(21)
      DATA IHG /81,82,83,84,85,86,102,118,134,150,166,182,
1          198,214,230,246,245,244,243,242,241/
*D,REZONE.45,REZONE.46
      UG(IJ)=VG(IJ)=0.
*1,REZONE.48
      IF(IJ.EQ.81 .OR. IJ.EQ.241) GO TO 71
*1,REZONE.53
      71 UG(IJ)=0.
          VG(IJ)=VL(IJ)

```

```

GO TO 78
*1,REZONE,60
  IF(I.EQ.1 .OR. J.EQ.NXP) UG(IJ)=0.
  IF(J.EQ.1 .OR. J.EQ.NYP) VG(IJ)=0.
*1,REZONE,64
  DO 95 K=2,20
    K1=IHG(K-1)
    K2=IHG(K)
    K3=IHG(K+1)
    X1=X(K1)+UL(K1)*DT
    X2=X(K2)+UL(K2)*DT
    X3=X(K3)+UL(K3)*DT
    Y1=Y(K1)+VL(K1)*DT
    Y2=Y(K2)+VL(K2)*DT
    Y3=Y(K3)+VL(K3)*DT
    XA=.5*(X1+X2)
    XB=.5*(X2+X3)
    YA=.5*(Y1+Y2)
    YB=.5*(Y2+Y3)
    X2MX1=X2-X1
    Y2MY1=Y2-Y1
    X3MX1=X3-X1
    Y3MY1=Y3-Y1
    RM1=X2MX1/Y2MY1
    RM2=(X3-X2)/(Y3-Y2)
    X0=(YB-YA-XA*RM1+XB*RM2)/(RM2-RM1)
    Y0=YA-RM1*(X0-XA)
    R0=SQRT((Y2-Y0)**2+(X2-X0)**2)
    AL=2.*Y3MY1
    BE=2.*X3MX1
    GA=X1**2+Y1**2-X3**2-Y3**2
    A=-GA/AL
    B=-BE/AL
    EMU=A-Y0
    ERO=X0**2-R0**2+EMU**2
    BTERM=B*EMU-X0
    ATERM=1.+B**2
    RADCL=SQRT(BTERM**2-ATERM*ERO)
    XN=XN1=(-BTERM+RADCL)/ATERM
    XN2=(-BTERM-RADCL)/ATERM
    YN=YN1=B*XN1+A
    YN2=B*XN2+A
    R1=SQRT((Y2-YN1)**2+(X2-XN1)**2)
    R2=SQRT((Y2-YN2)**2+(X2-XN2)**2)
    IF(R1.LT.R2) GO TO 94
    XN=XN2
    YN=YN2
  94 UG(K2)=UL(K2)+RFOOT*(XN-X2)
  95 VG(K2)=VL(K2)+RFOOT*(YN-Y2)
*D,VINIT,23
  P(IJ)=ASQ*(RO(IJ)-RON)
  IF(I.GT.5 .OR. J.LE.5 .OR. J.GE.16)
  1 P(IJ)=2.25E+10*(RO(IJ)-1.0)
*D,SALE,187
  30 IF(GM1.GT.0.) CALL ENERGY
T3AAA 15X30 HG IN H20, ROIN=5.83 VIN=3.0E5.

```

```

NX      15
NY      30
IMP     0
INC     0

```

```

IREZ    2
LPR     1
WB      5
WL      1
WR      1
WT      4
DX      0.2
DY      0.2
CYL     1.0
DT      5.0E-8
DTMAX   5.0E-8
TLIMD   0.0
TWFILM  5.0E-6
TWRPTR  100.0
TWFIN   4.0E-5
OM       0.0
PEPS    0.0
EPS      0.0
RF       1.0
ARTVIS  0.1
LAMBDA  0.0
MU       0.0
ANC      0.05
XI       1.0
GX       0.0
GY       0.0
AO       0.5
BO       0.0
ASQ     2.1025E+10
RON      13.5
GM1      0.0
ROI      13.5
SIEI    0.0
UIN      0.0
VIN      3.0E+5
ROIIN   5.83
SIEIN   0.0
PAP      0.0

```

REFERENCES

1. F. H. Harlow and A. A. Amsden, "A Numerical Fluid Dynamics Calculation Method for All Flow Speeds," J. Comput. Phys. 8, 197-213 (1971). Reprinted in AIAA Selected Reprints, Vol. XV, "Computer Fluid Dynamics—Recent Advances," 83-91 (1973).
2. C. W. Hirt, A. A. Amsden, and J. L. Cook, "An Arbitrary Lagrangian-Eulerian Computing Method for All Flow Speeds," J. Comput. Phys. 14, 227-253 (1974).
3. A. A. Amsden and C. W. Hirt, "YAQUI: An Arbitrary Lagrangian-Eulerian Computer Program for Fluid Flow at All Speeds," Los Alamos Scientific Laboratory report LA-5100 (March 1973).

4. C. W. Hirt, "Heuristic Stability Theory for Finite Difference Equations," J. Comput. Phys. 2, 339 (1968).
5. F. H. Harlow and A. A. Amsden, "Fluid Dynamics," Los Alamos Scientific Laboratory report LA-4700 (June 1971).
6. A. A. Amsden and C. W. Hirt, "A Simple Scheme for Generating General Curvilinear Grids," J. Comput. Phys. 11, 348-359 (1973).
7. H. Schlichting, *Boundary Layer Theory* (McGraw-Hill Book Co., New York, 1960), pp. 16, 18.

APPENDIX A

FORTRAN LISTING OF THE SALE PROGRAM

Note added in proof:

Line CELSET.53 should read: DO 180 J=JFIRST,JLAST
Line CELSET.54 should read: IJ=(J-1)*NXP+IFIRST
Line CELSET.56 should read: DO 170 I=IFIRST,ILAST
Line CELSET.67 should read: DO 200 J=JFIRST,JLASTV
Line CELSET.68 should read: IJ=(J-1)*NXP+IFIRST
Line CELSET.71 should read: DO 190 I=IFIRST,ILASTV
Line TIMSTP.9 should read: DO 40 J=JFIRST,JLAST
Line TIMSTP.10 should read: IJ=(J-1)*NXP+IFIRST
Line TIMSTP.12 should read: DO 30 I=IFIRST,ILAST

LASL Identification No. LP-2023

	PROGRAM SALE (1=TAPE, TAPE5=1=TAPE, TAPE6, TAPE7, TAPE8, TTY, TAPE59=TTY)	SALE	2
C	***	SALE	3
C	*** SALE 2D - A SIMPLIFIED ICED ALE PROGRAM IN 2 DIMENSIONS;	SALE	4
C	*** A.A.AMSDEN, LASL T-3. LA-8095 REPORT VERSION, 011780/1045	SALE	5
C	***	SALE	6
C	* * * * LIST OF VARIABLES- * * * *	SALE	7
C		SALE	8
C	(1) INPUT QUANTITIES-	SALE	9
C		SALE	10
C	NAME PROBLEM IDENTIFICATION LINE	SALE	11
C	NX NO. OF CELLS IN X-DIRECTION (OR 0 IF TAPE RESTART)	SALE	12
C	NY NO. OF CELLS IN Y-DIRECTION (OR DUMP NO. IF TAPE RESTART)	SALE	13
C	IMP =1 FOR IMPLICIT PRESSURE CALCULATION,	SALE	14
C	=0 FOR PURELY EXPLICIT CALCULATION	SALE	15
C	INC =1 FOR INCOMPRESSIBLE LIMIT VARIANT OF IMP=1 CALCULATION	SALE	16
C	IREZ REZONE FLAG- 0=EULERIAN, 1=LAGRANGIAN, 2 OR GREATER	SALE	17
C	FOR SOME SPECIFIED CONTINUOUS REZONE	SALE	18
C	LPR LONG PRINT CONTROL- 0=OMIT, 1=FILM, 2=FILM AND PRINTER,	SALE	19
C	3=PRINTER	SALE	20
C	WB, WL, WR, WT INDICATORS FOR BOUNDARY CONDITION TO BE USED	SALE	21
C	ALONG THE BOTTOM, LEFT, RIGHT, AND TOP EDGES	SALE	22
C	OF THE MESH (0=LAGRANGIAN SURFACE, 1=SIMPLE FREESLIP	SALE	23
C	2=GENERAL FREESLIP FOR CURVILINEAR BOUNDARIES, 3=	SALE	24
C	NOSLIP, 4=CONTINUATIVE OUTFLOW, 5=SPECIFIED INFLOW	SALE	25
C	OR OUTFLOW, 6=APPLIED PRESSURE)	SALE	26
C	DX CELL SIZE IN THE X-DIRECTION IF UNIFORMLY ZONED	SALE	27
C	DY CELL SIZE IN THE Y-DIRECTION IF UNIFORMLY ZONED	SALE	28
C	CYL =1.0 FOR CYLINDRICAL GEOMETRY, =0.0 FOR PLANE GEOMETRY	SALE	29
C	DT TIME STEP, SUBJECT TO AUTOMATIC RECALCULATION DURING RUN	SALE	30
C	DTMAX MAXIMUM DT ALLOWED	SALE	31
C	TLIMD =1.0 FORCES A TAPE DUMP EXIT BEFORE JOB TIME LIMIT	SALE	32
C	TWIFILM PROBLEM TIME INTERVAL BETWEEN FILM PLOTS	SALE	33
C	TWIPRTR PROBLEM TIME INTERVAL BETWEEN LONG PRINTS	SALE	34
C	TWIFIN PROBLEM TIME WHEN TO TERMINATE THE CALCULATION	SALE	35
C	GM RELAXATION COEFFICIENT USED IN PRESSURE ITERATION	SALE	36
C	PEPS PRESSURE FRACTION SCALING THE RELAXATION FACTOR RSDSP	SALE	37
C	EPS ALLOWED RELATIVE ERROR IN THE PRESSURE ITERATION	SALE	38
C	RF RELAXATION FACTOR FOR CONTINUOUS GRID REZONING	SALE	39
C	ARTVIS ARTIFICIAL (BULK) VISCOSITY COEFFICIENT	SALE	40
C	LAMBDA BULK VISCOSITY COEFFICIENT	SALE	41
C	MU SHEAR VISCOSITY COEFFICIENT	SALE	42
C	ANC ALTERNATE NODE-COUPLER COEFFICIENT	SALE	43
C	XI =1. FOR 4TH-ORDER NODE COUPLING,	SALE	44
C	=0. FOR 2ND-ORDER NODE-COUPLING	SALE	45
C	GX BODY ACCELERATION IN X-DIRECTION, + OR -	SALE	46
C	GY BODY ACCELERATION IN Y-DIRECTION, + OR -	SALE	47
C	A0, B0 FACTORS CONTROLLING CONVECTIVE FLUXING. LIMITING CASES-	SALE	48
C	0 0 CENTERED; UNSTABLE	SALE	49
C	1 0 FULL DONOR CELL; STABLE; DIFFUSIVE	SALE	50
C	0 1 INTERPOLATED DONOR CELL; LINEARLY STABLE; NON-DIFFUSIVE	SALE	51
C	1 1 STABLE; DIFFUSIVE	SALE	52
C	ASQ, RON, GM1 PARAMETERS FOR STIFFENED POLYTROPIC GAS EQUATION	SALE	53
C	OF STATE- ASQ IS THE SQUARE OF THE ZERO-TEMPERA-	SALE	54
C	TURE SOUND SPEED, RON IS THE FLUID NORMAL	SALE	55
C	DENSITY, AND GM1 IS GAMMA-1. IN WHICH GAMMA IS THE	SALE	56
C	RATIO OF SPECIFIC HEATS	SALE	57
C	ROI, SIE1 INITIAL FLUID DENSITY AND SPECIFIC INTERNAL ENERGY	SALE	58
C	UIN, VIN, ROIN, SIEIN DESCRIPTORS FOR A SPECIFIED FLOW BOUNDARY-	SALE	59
C	X-DIRECTION VELOCITY, Y-DIRECTION VELOCITY,	SALE	60
C	DENSITY, AND SPECIFIC INTERNAL ENERGY	SALE	61

C	PAP	APPLIED PRESSURE FOR PRESSURE BOUNDARY CONDITION	SALE 62
C			SALE 63
C	(2)	DERIVED QUANTITIES:	SALE 64
C			SALE 65
C	OMCYL	1-CYL	SALE 66
C	ANCO	ANC/4	SALE 67
C	XICOF	$(1+X1)/2$	SALE 68
C	COLAMU	LAMBDA*2* μ	SALE 69
C	DPCOF	$PEPS*RO1/(2(1/(DX*DX) + 1/(DY*DY)))$	SALE 70
C	GRFAC	$1/(NX*NY)$	SALE 71
C	TFILM	PROBLEM TIME INTERVAL BETWEEN FILM PLOTS	SALE 72
C	TPRTR	PROBLEM TIME INTERVAL BETWEEN LONG PRINTS	SALE 73
C	NYP	NY+1	SALE 74
C	NXP	NX+1	SALE 75
C		THE FOLLOWING 12 INDICES DEFINE DO-LOOP LIMITS, TO	SALE 76
C		PROVIDE FICTITIOUS CELLS FOR CERTAIN BOUNDARY TYPES:	SALE 77
C	IFIRST	=1 IF WL=1,2,3 OR 4; =2 IF WL=5 OR 6	SALE 78
C	JFIRST	=1 IF WB=1,2,3 OR 4; =2 IF WB=5 OR 6	SALE 79
C	ILAST	=NX IF WR=1,2,3 OR 4; =NX-1 IF WR=5 OR 6	SALE 80
C	JLAST	=NY IF WT=1,2,3 OR 4; =NY-1 IF WT=5 OR 6	SALE 81
C	IFPHI	=1 IF WL=1,2,3,4 OR 6; =2 IF WL=5	SALE 82
C	JFPHI	=1 IF WB=1,2,3,4 OR 6; =2 IF WB=5	SALE 83
C	ILPHI	=NX IF WR=1,2,3,4 OR 6; =NX-1 IF WR=5	SALE 84
C	JLPHI	=NY IF WT=1,2,3,4 OR 6; =NY-1 IF WT=5	SALE 85
C	ILASTV	ILAST+1	SALE 86
C	JLASTV	JLAST+1	SALE 87
C	ILASTM	ILAST-1	SALE 88
C	JLASTM	JLAST-1	SALE 89
C			SALE 90
C	(3)	SCALAR QUANTITIES:	SALE 91
C			SALE 92
C	T	PROBLEM TIME	SALE 93
C	NCYC	CYCLE COUNTER	SALE 94
C	IPRES	=1 DURING ITERATION TO LET CONTINUATIVE BDRY. UL,V. FLOAT	SALE 95
C	MAXIT	MAXIMUM NO. OF ITERATIONS ALLOWED BEFORE DT CUT IN HALF	SALE 96
C	NUMIT	NO. OF ITERATIONS REQD. FOR PRESSURE ITERATION CONVERGENCE	SALE 97
C	LOOPS	NO. OF DT CUTS FOR NON-CONVERGENCE PERFORMED	SALE 98
C		IN A GIVEN CYCLE	SALE 99
C	LOOPMX	LIMITS NO. OF TIMES BEFORE ERROR STOP THAT DT CAN BE	SALE 100
C		CUT DUE TO NON-CONVERGENCE IN A GIVEN CYCLE	SALE 101
C	THIRD	1/3	SALE 102
C	TWLFTH	1/12	SALE 103
C	PMAX	MAXIMUM PRESSURE IN THE SYSTEM	SALE 104
C	GRIND	CENTRAL PROCESSOR TIME PER CELL PER CYCLE, IN MSEC	SALE 105
C	NDUMP	TAPE DUMP COUNTER	SALE 106
C	DROU	SCALING FACTOR FOR THE VELOCITY VECTOR PLOT	SALE 107
C	VMAX	MAXIMUM VELOCITY IN THE SYSTEM	SALE 108
C	DTF	TIME-STEP FACTOR FOR CONVECTIVE STABILITY AND ACCURACY	SALE 109
C	C1	WALL CLOCK HRS/MIN/SEC WHEN THE JOB BEGAN	SALE 110
C	D1	MONTH/DAY/YEAR WHEN THE JOB BEGAN	SALE 111
C	XL	X-COORDINATE OF THE LEFTMOST VERTEX	SALE 112
C	YB	Y-COORDINATE OF THE BOTTOMMOST VERTEX	SALE 113
C	FIXL	FILM-FRAME COORDINATE ANALOG OF XL	SALE 114
C	FIYB	FILM-FRAME COORDINATE ANALOG OF YB	SALE 115
C	XCONV	FILM-FRAME CONVERSION COEFFICIENT IN X-DIRECTION	SALE 116
C	YCONV	FILM-FRAME CONVERSION COEFFICIENT IN Y-DIRECTION	SALE 117
C	TIMLMT	JOB TIME LIMIT, IN SECONDS	SALE 118
C	DTMIN	MINIMUM DT ALLOWED, = (DT OF CYCLE 1)*E-10	SALE 119
C	IDDT	SYMBOL IDENTIFYING THE RESTRICTION CONTROLLING THE	SALE 120
C		CURRENT TIME STEP, WHERE: G=105% OF PREVIOUS DT,	SALE 121

C	C=CONVECTION (DTF), V=SHEAR VISCOSITY, OR	SALE 122
C	M=MAXIMUM DT (DTMAX)	SALE 123
C	JNM OPTIONAL, IDENTIFIER FOR CODE	SALE 124
C	AA DUMMY WORD IDENTIFYING BEGINNING OF TAPE-DUMP DATA	SALE 125
C	ZZ DUMMY WORD IDENTIFYING END OF TAPE-DUMP DATA	SALE 126
C		SALE 127
C	(4) VECTOR QUANTITIES:	SALE 128
C		SALE 129
C	X CARTESIAN COORDINATE IN RADIAL DIRECTION	SALE 130
C	R RADIAL COORDINATE (R=1 FOR CARTESIAN GEOMETRY, R=X FOR CYLINDRICAL GEOMETRY)	SALE 131
C	Y CARTESIAN COORDINATE IN AXIAL DIRECTION	SALE 132
C	U X-DIRECTION VERTEX VELOCITY COMPONENT	SALE 134
C	V Y-DIRECTION VERTEX VELOCITY COMPONENT	SALE 135
C	MC CELL MASS	SALE 136
C	MV VERTEX MASS	SALE 137
C	RMV RECIPROCAL OF VERTEX MASS MV	SALE 138
C	RO CELL DENSITY	SALE 139
C	VOL CELL VOLUME	SALE 140
C	P CELL PRESSURE	SALE 141
C	SIE CELL SPECIFIC INTERNAL ENERGY	SALE 142
C	UL LAGRANGIAN U, CALCULATED IN PHASES 1 AND 2	SALE 143
C	VL LAGRANGIAN V, CALCULATED IN PHASES 1 AND 2	SALE 144
C	ROL LAGRANGIAN DENSITY, UPDATED IN PHASE 2	SALE 145
C	PL LAGRANGIAN PRESSURE, UPDATED IN PHASE 2	SALE 146
C	D VELOCITY DIVERGENCE	SALE 147
C	Q CELL ARTIFICIAL VISCOUS PRESSURE	SALE 148
C	RRSUM 1/(R1+R2+R3+R4) OF THE CELL	SALE 149
C	PIXX STRESS DEVIATOR TERM	SALE 150
C	PIXY STRESS DEVIATOR TERM	SALE 151
C	PIYY STRESS DEVIATOR TERM	SALE 152
C	PITH STRESS DEVIATOR TERM	SALE 153
C	RDSDP RECIPROCAL OF NUMERICAL DERIVATIVE FOR PHASE 2 ITERATION	SALE 154
C	UG GRID VELOCITY IN THE X-DIRECTION	SALE 155
C	VG GRID VELOCITY IN THE Y-DIRECTION	SALE 156
C	UREL RELATIVE VELOCITY BETWEEN GRID AND FLUID, =UG-UL	SALE 157
C	VREL RELATIVE VELOCITY BETWEEN GRID AND FLUID, =VG-VL	SALE 158
C	MP INTERMEDIATE STORAGE FOR NEW MC IN PHASE 3	SALE 159
C	MVP INTERMEDIATE STORAGE FOR NEW MV IN PHASE 3	SALE 160
C	SIEP INTERMEDIATE STORAGE FOR SIE IN PHASE 3	SALE 161
C	UMOM X-DIRECTION COMPONENT OF CELL MOMENTUM	SALE 162
C	VMOM Y-DIRECTION COMPONENT OF CELL MOMENTUM	SALE 163
C	UMOMP INTERMEDIATE STORAGE FOR NEW UMOM IN PHASE 3	SALE 164
C	VMOMP INTERMEDIATE STORAGE FOR NEW VMOM IN PHASE 3	SALE 165
C		SALE 166
C		SALE 167
C		SALE 168
C	COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
C	1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
C	2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
C	3 PIXY(800),PIYY(800),PITH(800),RDSDP(800),UG(800),VG(800),	COMD 5
C	4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
C	5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
C	COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
C	1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,DI,EPS,FIYL,FIYB,GMI,GRFAC,GRIND,	COMD 9
C	2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
C	3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
C	4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
C	5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD 13
C	6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPTR,	COMD 14

7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
CALL BEGIN	SALE 170
CALL RINPUT	SALE 171
IF(.<.GT.0) CALL CELSET	SALE 172
IF(NX.EQ.0) CALL TAPERD	SALE 173
10 CALL TIMSTP	SALE 174
20 CALL VINIT	SALE 175
CALL NEWCYC	SALE 176
IF(ARTVIS+ANC.GT.0.) CALL AVISC	SALE 177
IF(LAMBDA+MU.GT.0.) CALL STRESD	SALE 178
CALL PHASE1	SALE 179
IF(IMP.EQ.0) GO TO 30	SALE 180
CALL DSDP	SALE 181
CALL PRESIT	SALE 182
IF(NUMIT.EQ.MAXIT .AND. INC.EQ.1) CALL RESTEP	SALE 183
IF(NUMIT.EQ.MAXIT .AND. INC.EQ.1) GO TO 30	SALE 184
IF(NUMIT.GE.MAXIT) CALL RESTEP	SALE 185
IF(NUMIT.GE.MAXIT) GO TO 20	SALE 186
30 CALL ENERGY	SALE 187
CALL REZONE	SALE 188
CALL REGRID	SALE 189
IF(IRES.GT.0) CALL VOLUME	SALE 190
IF(IRES.NE.1) CALL ADVECT	SALE 191
IF(IRES.EQ.1) CALL ULTOU	SALE 192
GO TO 10	SALE 193
END	SALE 194

SUBROUTINE ADVECT	ADVECT 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZI	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,DI,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
DIMENSION AT(100),FT(100)	ADVECT 4
C ***	ADVECT 5
C *** PHASE 3. FLUXING OF CELL CENTERED QUANTITIES - MASS, ENERGY,	ADVECT 6
C *** AND MOMENTUM, THEN CONVERT MOMENTA TO VELOCITIES.	ADVECT 7
C *** CALLED ONLY IF EULERIAN (IREZ=0) OR OTHER REZONE (IREZ.GE.2)	ADVECT 8
C ***	ADVECT 9
C *** NOTE DO-LOOP LIMITS - INFLOW BOUNDARIES REQUIRE A MOMENTUM THAT	ADVECT10
C *** CAN BE FLUXED IN . . .	ADVECT11
C ***	ADVECT12
DO 20 J=1,NY	ADVECT13
[J=(J-1)*NXP+1	ADVECT14
IJP=1J+NXP	ADVECT15
DO 10 I=1,NX	ADVECT16
IPJ=1J+I	ADVECT17
IPJP=1JP+I	ADVECT18
UMOM(IJ)=.25*ROL(IJ)*(UL(IPJ)+UL(IPJP)+UL(IJP)+UL(IJ))	ADVECT19
VMOM(IJ)=.25*ROL(IJ)*(VL(IPJ)+VL(IPJP)+VL(IJP)+VL(IJ))	ADVECT20
IJ=IPJ	ADVECT21
10 IJP=IPJP	ADVECT22
20 CONTINUE	ADVECT23
DO 60 J=JFIRST,JLAST	ADVECT24
[J=(J-1)*NXP+JFIRST	ADVECT25
IJP=1J+NXP	ADVECT26
IJM=1J-NXP	ADVECT27
DO 50 I=IFIRST,ILAST	ADVECT28
IMJ=1J-I	ADVECT29
IPJ=1J+I	ADVECT30
IPJP=1JP+I	ADVECT31
X1=X(IPJ)	ADVECT32
Y1=Y(IPJ)	ADVECT33
R1=R(IPJ)	ADVECT34
X2=X(IPJP)	ADVECT35
Y2=Y(IPJP)	ADVECT36
R2=R(IPJP)	ADVECT37
X3=X(IJP)	ADVECT38
Y3=Y(IJP)	ADVECT39
R3=R(IJP)	ADVECT40
X4=X(IJ)	ADVECT41
Y4=Y(IJ)	ADVECT42
R4=R(IJ)	ADVECT43
XP1=X1-UREL(IPJ)*DT	ADVECT44
XP2=X2-UREL(IPJP)*DT	ADVECT45
XP3=X3-UREL(IJP)*DT	ADVECT46
XP4=X4-UREL(IJ)*DT	ADVECT47
YP1=Y1-VREL(IPJ)*DT	ADVECT48
YP2=Y2-VREL(IPJP)*DT	ADVECT49


```

YP3=Y3-VREL(IJ)*DT
YP4=Y4-VREL(IJ)*DT
RP1=XP1*CYL+OMCYL
RP2=XP2*CYL+OMCYL
RP3=XP3*CYL+OMCYL
RP4=XP4*CYL+OMCYL
VOLL=VOLB=VOLR=VOLT=VOLC=VOL(IJ)
IF(I.NE.1) VOLL=VOL(IMJ)
IF(J.NE.1) VOLB=VOL(IMJ)
IF(I.NE.NX) VOLR=VOL(IPJ)
IF(J.NE.NY) VOLT=VOL(IJP)
FL=-FR
AL=-AR
IF(I.EQ.1) FL=AL=0.
IF(WL.LT.4) GO TO 30
IF(L.GT.IFIRST) GO TO 30
FL=((RP3+RP4+RP4)*(XP3*(Y4-YP4)+X4*(YP4-YP3)+XP4*(YP3-Y4))
1 +(R3+RP3+R4)*(X3*(Y4-YP3)+XP3*(Y3-Y4)+X4*(YP3-Y3)))*TWLFTH
AL=A0*SIGN(1.,FL)+B0*4.*FL/(VOLL+VOLC)
30 FB=-FT(I)
AB=-AT(I)
IF(J.EQ.1) FB=AB=0.
IF(WB.LT.4) GO TO 40
IF(J.GT.JFIRST) GO TO 40
FB=((R1+RP1+RP4)*(X1*(YP1-YP4)+XP1*(YP4-Y1)+XP4*(Y1-YP1))
1 +(R1+R4+RP4)*(X1*(YP4-Y4)+X4*(Y1-YP4)+XP4*(Y4-Y1)))*TWLFTH
AB=A0*SIGN(1.,FB)+B0*4.*FB/(VOLB+VOLC)
40 FR=((R1+RP1+RP2)*(X1*(YP2-YP1)+XP1*(Y1-YP2)+XP2*(YP1-Y1))
1 +(R1+R2+RP2)*(X1*(Y2-YP2)+X2*(YP2-Y1)+XP2*(Y1-Y2)))*TWLFTH
AR=A0*SIGN(1.,FR)+B0*4.*FR/(VOLR+VOLC)
FT(I)=((RP2+R3+RP3)*(X2*(Y3-YP3)+X3*(YP3-YP2)+XP3*(YP2-Y3))
1 +(R2+RP2+R3)*(X2*(Y3-YP2)+XP2*(Y2-Y3)+X3*(YP2-Y2)))*TWLFTH
AT(I)=A0*SIGN(1.,FT(I))+B0*4.*FT(I)/(VOLT+VOLC)
S1=FR*(1.-AR)
S2=FR*(1.+AR)
S3=FT(I)*(1.-AT(I))
S4=FT(I)*(1.+AT(I))
S5=FL*(1.-AL)
S6=FL*(1.+AL)
S7=FB*(1.-AB)
S8=FB*(1.+AB)
S9=S1+S3+S5+S7
MP(IJ)=MC(IJ)+S9*ROL(IJ)+S2*ROL(IPJ)+S4*ROL(IJP)
1 +S6*ROL(IMJ)+S8*ROL(IJM)
SIEP(IJ)=(MC(IJ)+SIE(IJ)+S9*ROL(IJ)+S2*ROL(IPJ)+S4*ROL(IJP)+S6*ROL(IMJ)+S8*ROL(IJM)
1 +S4*ROL(IJP)+S6*ROL(IMJ)+S8*ROL(IJM))*SIE(IJ)
2 +S8*ROL(IJM)*SIE(IJM))/MP(IJ)
UMOMP(IJ)=S9*UMOM(IJ)+S2*UMOM(IPJ)+S4*UMOM(IJP)
1 +S6*UMOM(IMJ)+S8*UMOM(IJM)
VMOMP(IJ)=S9*VMOM(IJ)+S2*VMOM(IPJ)+S4*VMOM(IJP)
1 +S6*VMOM(IMJ)+S8*VMOM(IJM)
IJ=IPJ
IJP=IPJP
50 IJM=IJM+1
60 CONTINUE
C +++
C +++ COMPUTE NEW VERTEX MASSES
C +++
DO 80 J=JFIRST, JLAST
IJ=(J-1)*NX+IFIRST
IJP=IJ+NX
DO 70 I=IFIRST, ILAST
IPJ=IJ+1
ADVECT50
ADVECT51
ADVECT52
ADVECT53
ADVECT54
ADVECT55
ADVECT56
ADVECT57
ADVECT58
ADVECT59
ADVECT60
ADVECT61
ADVECT62
ADVECT63
ADVECT64
ADVECT65
ADVECT66
ADVECT67
ADVECT68
ADVECT69
ADVECT70
ADVECT71
ADVECT72
ADVECT73
ADVECT74
ADVECT75
ADVECT76
ADVECT77
ADVECT78
ADVECT79
ADVECT80
ADVECT81
ADVECT82
ADVECT83
ADVECT84
ADVECT85
ADVECT86
ADVECT87
ADVECT88
ADVECT89
ADVECT90
ADVECT91
ADVECT92
ADVECT93
ADVECT94
ADVECT95
ADVECT96
ADVECT97
ADVECT98
ADVECT99
ADVECT00
ADVECT01
ADVECT02
ADVECT03
ADVECT04
ADVECT05
ADVECT06
ADVECT07
ADVECT08
ADVECT09
ADVECT10
ADVECT11
ADVECT12

```

IPJP=IPJ+1	ADVEC113
MC(IJ)=MP(IJ)	ADVEC114
SIE(IJ)=SIEP(IJ)	ADVEC115
QM=0.25*MC(IJ)	ADVEC116
MVP(IPJ) =MVP(IPJ) +QM	ADVEC117
MVP(IPJP)=MVP(IPJP)+QM	ADVEC118
MVP(IJP) =MVP(IJP) +QM	ADVEC119
MVP(IJ) =MVP(IJ) +QM	ADVEC120
IJ=IPJ	ADVEC121
70 IJP=IPJP	ADVEC122
80 CONTINUE	ADVEC123
C ***	ADVEC124
C *** STORE VERTEX MASSES AND CALCULATE NEW VELOCITIES . . .	ADVEC125
C ***	ADVEC126
DO 100 J=JFIRST, JLAST	ADVEC127
IJ=(J-1)*NXP+IFIRST	ADVEC128
DO 90 I=IFIRST, ILAST	ADVEC129
RMV(IJ)=1./MVP(IJ)	ADVEC130
U(IJ)=UL(IJ)*MV(IJ)*RMV(IJ)	ADVEC131
V(IJ)=VL(IJ)*MV(IJ)*RMV(IJ)	ADVEC132
MV(IJ)=MVP(IJ)	ADVEC133
90 IJ=IJ+1	ADVEC134
100 CONTINUE	ADVEC135
DO 120 J=JFIRST, JLAST	ADVEC136
IJ=(J-1)*NXP+IFIRST	ADVEC137
IJP=IJ+NXP	ADVEC138
DO 110 I=IFIRST, ILAST	ADVEC139
IPJ=IJ+1	ADVEC140
IPJP=IPJ+1	ADVEC141
QMOMU=.25*UMOMP(IJ)	ADVEC142
U(IPJ) =U(IPJ) +QMOMU*RMV(IPJ)	ADVEC143
U(IPJP)=U(IPJP)+QMOMU*RMV(IPJP)	ADVEC144
U(IJP) =U(IJP) +QMOMU*RMV(IJP)	ADVEC145
U(IJ) =U(IJ) +QMOMU*RMV(IJ)	ADVEC146
QMOMV=.25*VMOMP(IJ)	ADVEC147
V(IPJ) =V(IPJ) +QMOMV*RMV(IPJ)	ADVEC148
V(IPJP)=V(IPJP)+QMOMV*RMV(IPJP)	ADVEC149
V(IJP) =V(IJP) +QMOMV*RMV(IJP)	ADVEC150
V(IJ) =V(IJ) +QMOMV*RMV(IJ)	ADVEC151
IJ=IPJ	ADVEC152
110 IJP=IPJP	ADVEC153
120 CONTINUE	ADVEC154
CALL BC(U,V)	ADVEC155
RETURN	ADVEC156
END	ADVEC157

SUBROUTINE AVISC	AVISC 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RSDOP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,AO,BO,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPH1,ILAST,ILASTM,ILASTV,ILPH1,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPH1,JLAST,JLASTM,JLASTV,JLPH1,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
IF(ARTVIS.EQ.0.) GO TO 50	AVISC 4
C +++	AVISC 5
C +++ CALCULATE ARTIFICIAL (BULK) VISCOUS CONTRIBUTIONS TO UL AND VL	AVISC 6
C +++	AVISC 7
DO 20 J=JFIRST,JLAST	AVISC 8
IJ=(J-1)*NXP+IFIRST	AVISC 9
IJP=IJ+NXP	AVISC 10
DO 10 I=IFIRST,ILAST	AVISC 11
IPJ=IJ+1	AVISC 12
IPJP=IJP+1	AVISC 13
X1=X(IPJ)	AVISC 14
Y1=Y(IPJ)	AVISC 15
U1=UL(IPJ)	AVISC 16
V1=VL(IPJ)	AVISC 17
X2=X(IPJP)	AVISC 18
Y2=Y(IPJP)	AVISC 19
U2=UL(IPJP)	AVISC 20
V2=VL(IPJP)	AVISC 21
X3=X(IJP)	AVISC 22
Y3=Y(IJP)	AVISC 23
U3=UL(IJP)	AVISC 24
V3=VL(IJP)	AVISC 25
X4=X(IJ)	AVISC 26
Y4=Y(IJ)	AVISC 27
U4=UL(IJ)	AVISC 28
V4=VL(IJ)	AVISC 29
AREA=0.5*((X2-X4)*(Y3-Y1)-(X1-X3)*(Y4-Y2))	AVISC 30
RAREA=1./AREA	AVISC 31
DUDX=0.5*RAREA*((U2-U4)*(Y3-Y1)-(U1-U3)*(Y4-Y2))	AVISC 32
DVDY=0.5*RAREA*((V4-V2)*(X3-X1)-(V1-V3)*(X2-X4))	AVISC 33
RRSUM(IJ)=1./(R(IPJ)+R(IPJP)+R(IJP)+R(IJ))	AVISC 34
UOR=(U1+U2+U3+U4)*RRSUM(IJ)	AVISC 35
D(IJ)=DUDX+DVDY*UOR*CYL	AVISC 36
Q(IJ)=ARTVIS*RO(IJ)*AREA*D(IJ)	AVISC 37
C +++	AVISC 38
C +++ Q IS AN ARTIFICIAL VISCOUS PRESSURE FOR USE WITH SHOCKS. THE	AVISC 39
C +++ FORM USED HERE IS QUADRATIC IN THE VELOCITY DIVERGENCE D=DEL DOT	UAVISC 40
C +++ Q IS ZERO IN EXPANDING CELLS (D POSITIVE).	AVISC 41
C +++	AVISC 42
IJP=IPJP	AVISC 43
10 IJ=IPJ	AVISC 44
20 CONTINUE	AVISC 45
DO 40 J=JFIRST,JLAST	AVISC 46
IJ=(J-1)*NXP+IFIRST	AVISC 47
IJP=IJ+NXP	AVISC 48
DO 30 I=IFIRST,ILAST	AVISC 49

IPJ=I J+1	AVISC 50
IPJP=I JP+1	AVISC 51
Q(IJ)=AM N1(0.,D(IJ))*Q(IJ)	AVISC 52
XX=0.5*DT*Q(IJ)	AVISC 53
R1=R(IPJ)	AVISC 54
R2=R(IPJP)	AVISC 55
R3=R(IJP)	AVISC 56
R4=R(IJ)	AVISC 57
RM1=RMV(IPJ)	AVISC 58
RM2=RMV(IPJP)	AVISC 59
RM3=RMV(IJP)	AVISC 60
RM4=RMV(IJ)	AVISC 61
Y24=Y(IPJP)-Y(IJ)	AVISC 62
Y31=Y(IJP)-Y(IPJ)	AVISC 63
XR24=(X(IPJP)-X(IJ))*.5*(R2+R4)	AVISC 64
XR31=(X(IJP)-X(IPJ))* .5*(R3+R1)	AVISC 65
UL(IPJP)=UL(IPJ)+XX*RM1*Y24*R1	AVISC 66
UL(IPJP)=UL(IPJP)+XX*RM2*Y31*R2	AVISC 67
UL(IJP)=UL(IJP)-XX*RM3*Y24*R3	AVISC 68
UL(IJ)=UL(IJ)-XX*RM4*Y31*R4	AVISC 69
VL(IPJP)=VL(IPJ)-XX*RM1*XR24	AVISC 70
VL(IPJP)=VL(IPJP)-XX*RM2*XR31	AVISC 71
VL(IJP)=VL(IJP)+XX*RM3*XR24	AVISC 72
VL(IJ)=VL(IJ)+XX*RM4*XR31	AVISC 73
IJP=IPJP	AVISC 74
30 IJ=IPJ	AVISC 75
40 CONTINUE	AVISC 76
CALL BC(UL,VL)	AVISC 77
50 IF(ANC.EQ.0.) RETURN	AVISC 78
C ***	AVISC 79
C *** OPTIONAL NODE COUPLER - A VELOCITY DIFFUSION TO SUPPRESS	AVISC 80
C *** VERTEX COASTING. USE X1=1.0 (4TH ORDER) TO COMBAT BOWTIES.	AVISC 81
C *** USE X1=0.0 (2ND ORDER) TO COMBAT HERRINGBONE PATTERN . . .	AVISC 82
C ***	AVISC 83
DO 70 J=JFIRST, JLAST	AVISC 84
IJ=(J-1)*NXP+IFIRST	AVISC 85
IJP=IJ+NXP	AVISC 86
DO 60 I=IFIRST, ILAST	AVISC 87
IPJ=IJ+1	AVISC 88
IPJP=I JP+1	AVISC 89
U1=U(IPJ)	AVISC 90
U2=U(IPJP)	AVISC 91
U3=U(IJP)	AVISC 92
U4=U(IJ)	AVISC 93
V1=V(IPJ)	AVISC 94
V2=V(IPJP)	AVISC 95
V3=V(IJP)	AVISC 96
V4=V(IJ)	AVISC 97
I VL=I UB=I VR=I UT=1.	AVISC 98
IF(I.EQ.1) I VL=2.	AVISC 99
IF(J.EQ.1) I UB=2.	AVISC100
IF(I.EQ.NX) I VR=2.	AVISC101
IF(J.EQ.NY) I UT=2.	AVISC102
UL(IPJ)=UL(IPJ)+ANCO*I UB*(X1COF*(U2+U4)-X1*U3-U1)	AVISC103
UL(IPJP)=UL(IPJP)+ANCO*I UT*(X1COF*(U1+U3)-X1*U4-U2)	AVISC104
UL(IJP)=UL(IJP)+ANCO*I UT*(X1COF*(U2+U4)-X1*U1-U3)	AVISC105
UL(IJ)=UL(IJ)+ANCO*I UB*(X1COF*(U1+U3)-X1*U2-U4)	AVISC106
VL(IPJ)=VL(IPJ)+ANCO*I VR*(X1COF*(V2+V4)-X1*V3-V1)	AVISC107
VL(IPJP)=VL(IPJP)+ANCO*I VR*(X1COF*(V1+V3)-X1*V4-V2)	AVISC108
VL(IJP)=VL(IJP)+ANCO*I VL*(X1COF*(V2+V4)-X1*V1-V3)	AVISC109
VL(IJ)=VL(IJ)+ANCO*I VL*(X1COF*(V1+V3)-X1*V2-V4)	AVISC110
IJP=IPJP	AVISC111
60 IJ=IPJ	AVISC112

```

70 CONTINUE
   CALL BC(UJ,VJ)
   RETURN
   END

```

```

AVISC113
AVISC114
AVISC115
AVISC116

```

```

SUBROUTINE BC(UJ,VJ)
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,AD,B0,COLAMU,CYL,C1,DPCOF,
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,DI,EPS,FXL,FIYB,GMI,GRFAC,GRIND,
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,
6 T,TFILM,THIRD,TIMLMT,TLIND,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ
REAL LAMBDA,MC,MP,MU,MV,MVP
INTEGER WB,WL,WR,WT
DIMENSION UJ(1),VJ(1)
C +++
C +++ SET VELOCITY BOUNDARY CONDITIONS FOR ALL 4 SIDES, WHERE
C +++ WL, WR, WB, AND WT ARE INPUT INTEGERS DEFINED AS FOLLOWS:
C +++ 0 = LAGRANGIAN SURFACE (NO VELOCITY ADJUSTMENT WHATSOEVER),
C +++ 1 = SIMPLE FREESLIP, 2 = GENERAL FREESLIP, 3 = NOSLIP,
C +++ 4 = CONTINUATIVE OUTFLOW, 5 = SPECIFIED INFLOW OR OUTFLOW,
C +++ 6 = SPECIFIED PRESSURE. (NOTE - THE CONTINUATIVE OUTFLOW BOUNDARY
C +++ APPROXIMATION GIVEN HERE MAY NOT WORK FOR ALL APPLICATIONS.)
C +++
      DO 400 J=1,NYP
      IJ=(J-1)*NXP+1
C +++
C +++ THE LEFT EDGE . . .
C +++
      IF (WL.EQ.0) GO TO 300
      GO TO (210,220,230,240,250,240),WL
210 UJ(IJ)=0.
      GO TO 300
220 IJM=IJP=IJ
      IF (J.GT.1) IJM=IJ-NXP
      IF (J.LT.NYP) IJP=IJ+NXP
      IF (J.EQ.1 .AND. WB.EQ.2) IJM=IJ+1
      IF (J.EQ.NYP .AND. WT.EQ.2) IJP=IJ+1
      EM=1.E+20
      XTE=X(IJP)-X(IJM)
      IF (XTE.NE.0.) EM=(Y(IJP)-Y(IJM))/XTE
      RDEN=1./(1.+EM*EM)
      UOLD=UU(IJ)
      UU(IJ)=(EM*VV(IJ)+UOLD)*RDEN
      VV(IJ)=(EM*EM*VV(IJ)+EM*UOLD)*RDEN
      GO TO 300
BC 2
COMD 2
COMD 3
COMD 4
COMD 5
COMD 6
COMD 7
COMD 8
COMD 9
COMD 10
COMD 11
COMD 12
COMD 13
COMD 14
COMD 15
COMD 16
COMD 17
BC 4
BC 5
BC 6
BC 7
BC 8
BC 9
BC 10
BC 11
BC 12
BC 13
BC 14
BC 15
BC 16
BC 17
BC 18
BC 19
BC 20
BC 21
BC 22
BC 23
BC 24
BC 25
BC 26
BC 27
BC 28
BC 29
BC 30
BC 31
BC 32
BC 33
BC 34
BC 35

```

230	UU(IJ)=VV(IJ)=0.	BC	36
	GO TO 300	BC	37
240	IF(IPRES.EQ.1) GO TO 300	BC	38
	UU(IJ)=UU(IJ+1)	BC	39
	VV(IJ)=VV(IJ+1)	BC	40
	GO TO 300	BC	41
250	UU(IJ+1)=UIN	BC	42
	VV(IJ+1)=VIN	BC	43
300	IJ=IJ+NX	BC	44
C	+++	BC	45
C	+++ THE RIGHT EDGE . . .	BC	46
C	+++	BC	47
	IF(WR.EQ.0) GO TO 400	BC	48
	GO TO (310,320,330,340,350,340),WR	BC	49
310	UU(IJ)=0.	BC	50
	GO TO 400	BC	51
320	IJP=IJ=IJ	BC	52
	IF(J.GT.1) IJM=IJ-NXP	BC	53
	IF(J.LT.NYP) IJP=IJ+NXP	BC	54
	IF(J.EQ.1 .AND. WB.EQ.2) IJM=IJ-1	BC	55
	IF(J.EQ.NYP .AND. WT.EQ.2) IJP=IJ-1	BC	56
	EM=1.E+20	BC	57
	XTE=X(IJP)-X(IJM)	BC	58
	IF(XTE.NE.0.) EM=(Y(IJP)-Y(IJM))/XTE	BC	59
	RDEN=1./(1.+EM*EM)	BC	60
	UOLD=UU(IJ)	BC	61
	UU(IJ)=(EM*VV(IJ)+UOLD)*RDEN	BC	62
	VV(IJ)=(EM*EM*VV(IJ)+EM*UOLD)*RDEN	BC	63
	GO TO 400	BC	64
330	UU(IJ)=VV(IJ)=0.	BC	65
	GO TO 400	BC	66
340	IF(IPRES.EQ.1) GO TO 400	BC	67
	UU(IJ)=UU(IJ-1)	BC	68
	VV(IJ)=VV(IJ-1)	BC	69
	GO TO 400	BC	70
350	UU(IJ-1)=UIN	BC	71
	VV(IJ-1)=VIN	BC	72
400	CONTINUE	BC	73
	DO 600 I=1,NXP	BC	74
	IJ=I	BC	75
C	+++	BC	76
C	+++ THE BOTTOM EDGE . . .	BC	77
C	+++	BC	78
	IF(WB.EQ.0) GO TO 500	BC	79
	GO TO (410,420,430,440,450,440),WB	BC	80
410	VV(IJ)=0.	BC	81
	GO TO 500	BC	82
420	IMJ=IPJ=IJ	BC	83
	IF(I.GT.1) IMJ=IJ-1	BC	84
	IF(I.LT.NXP) IPJ=IJ+1	BC	85
	IF(I.EQ.1 .AND. WL.EQ.2) IMJ=IJ+NXP	BC	86
	IF(I.EQ.NXP .AND. WR.EQ.2) IPJ=IJ+NXP	BC	87
	EM=1.E+20	BC	88
	XTE=X(IPJ)-X(IMJ)	BC	89
	IF(XTE.NE.0.) EM=(Y(IPJ)-Y(IMJ))/XTE	BC	90
	RDEN=1./(1.+EM*EM)	BC	91
	UOLD=UU(IJ)	BC	92
	UU(IJ)=(EM*VV(IJ)+UOLD)*RDEN	BC	93
	VV(IJ)=(EM*EM*VV(IJ)+EM*UOLD)*RDEN	BC	94
	GO TO 500	BC	95
430	UU(IJ)=VV(IJ)=0.	BC	96
	GO TO 500	BC	97
440	IF(IPRES.EQ.1) GO TO 500	BC	98

UU(IJ)=UU(IJ+NXP)	BC	99
VV(IJ)=VV(IJ+NXP)	BC	100
GO TO 500	BC	101
450 UU(IJ+NXP)=UIN	BC	102
VV(IJ+NXP)=VIN	BC	103
500 IJ=NY*NXP+i	BC	104
C ***	BC	105
C *** THE TOP EDGE . . .	BC	106
C ***	BC	107
IF(WT.EQ.0) GO TO 600	BC	108
GO TO (510,520,530,540,550,540),WT	BC	109
510 VV(IJ)=0.	BC	110
GO TO 600	BC	111
520 IMJ=IPJ=IJ	BC	112
IF(1.GT.1) IMJ=IJ-1	BC	113
IF(1.LT.NXP) IPJ=IJ+1	BC	114
IF(1.EQ.1 .AND. WL.EQ.2) IMJ=IJ-NXP	BC	115
IF(1.EQ.NXP .AND. WR.EQ.2) IPJ=IJ-NXP	BC	116
EM=1.E+20	BC	117
XTE=X(IPJ)-X(IMJ)	BC	118
IF(XTE.NE.0.) EM=(Y(IPJ)-Y(IMJ))/XTE	BC	119
RDEN=1./(.+.EM*EM)	BC	120
UOLD=UU(IJ)	BC	121
UU(IJ)=(EM*VV(IJ)+UOLD)*RDEN	BC	122
VV(IJ)=(EM*EM*VV(IJ)+EM*UOLD)*RDEN	BC	123
GO TO 600	BC	124
530 UU(IJ)=VV(IJ)-0.	BC	125
GO TO 600	BC	126
540 IF(IPRES.EQ.1) GO TO 600	BC	127
UU(IJ)=UU(IJ-NXP)	BC	128
VV(IJ)=VV(IJ-NXP)	BC	129
GO TO 600	BC	130
550 UU(IJ-NXP)=UIN	BC	131
VV(IJ-NXP)=VIN	BC	132
600 CONTINUE	BC	133
RETURN	BC	134
END	BC	135

SUBROUTINE BCSET	BCSET	2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),PC(800),	COMD	2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD	3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD	4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD	5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD	6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD	7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,AD,B0,COLAMU,CYL,C1,DPCOF,	COMD	8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,DI,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD	9
2 GX,GY,IDD1,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD	10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD	11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD	12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD	13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWFTH,TWPRTR,	COMD	14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD	15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD	16
INTEGER WB,WL,WR,WT	COMD	17
C ***	BCSET	4

C *** ADJUST U,V,RO,MC,SIE,P AS REQUIRED FOR INFLOW OR SPECIFIED	BCSET 5
C *** PRESSURE BOUNDARIES. (CALLED ONCE, BY SUBROUTINE CELSET). . .	BCSET 6
C ***	BCSET 7
DO 400 J=1,NYP	BCSET 8
IJ=(J-1)*NXP+1	BCSET 9
C ***	BCSET 10
C *** THE LEFT EDGE . . .	BCSET 11
C ***	BCSET 12
IF (WL.EQ.0) GO TO 300	BCSET 13
GO TO (300,300,300,300,250,260),WL	BCSET 14
250 U(IJ)=UIN	BCSET 15
V(IJ)=VIN	BCSET 16
RO(IJ)=ROIN	BCSET 17
MC(IJ)=VOL(IJ)*ROIN	BCSET 18
SIE(IJ)=SIEIN	BCSET 19
GO TO 300	BCSET 20
260 P(IJ)=PAP	BCSET 21
300 IJ=IJ+NX	BCSET 22
C ***	BCSET 23
C *** THE RIGHT EDGE . . .	BCSET 24
C ***	BCSET 25
IMJ=IJ-1	BCSET 26
IF (WR.EQ.0) GO TO 400	BCSET 27
GO TO (400,400,400,400,350,360),WR	BCSET 28
350 U(IMJ)=UIN	BCSET 29
V(IMJ)=VIN	BCSET 30
RO(IMJ)=ROIN	BCSET 31
MC(IMJ)=VOL(IMJ)*ROIN	BCSET 32
SIE(IMJ)=SIEIN	BCSET 33
GO TO 400	BCSET 34
360 P(IMJ)=PAP	BCSET 35
400 CONTINUE	BCSET 36
DO 600 I=1,NXP	BCSET 37
IJ=I	BCSET 38
C ***	BCSET 39
C *** THE BOTTOM EDGE . . .	BCSET 40
C ***	BCSET 41
IF (WB.EQ.0) GO TO 500	BCSET 42
GO TO (500,500,500,500,450,460),WB	BCSET 43
450 U(IJ)=UIN	BCSET 44
V(IJ)=VIN	BCSET 45
RO(IJ)=ROIN	BCSET 46
MC(IJ)=VOL(IJ)*ROIN	BCSET 47
SIE(IJ)=SIEIN	BCSET 48
GO TO 500	BCSET 49
460 P(IJ)=PAP	BCSET 50
500 IJ=NY*NXP+I	BCSET 51
C ***	BCSET 52
C *** THE TOP EDGE . . .	BCSET 53
C ***	BCSET 54
IJM=IJ-NXP	BCSET 55
IF (WT.EQ.0) GO TO 600	BCSET 56
GO TO (600,600,600,600,550,560),WT	BCSET 57
550 U(IJM)=UIN	BCSET 58
V(IJM)=VIN	BCSET 59
RO(IJM)=ROIN	BCSET 60
MC(IJM)=VOL(IJM)*ROIN	BCSET 61
SIE(IJM)=SIEIN	BCSET 62
GO TO 600	BCSET 63
560 P(IJM)=PAP	BCSET 64
600 CONTINUE	BCSET 65
RETURN	BCSET 66
END	BCSET 67

SUBROUTINE BEGIN	BEGIN	2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD	2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD	3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD	4
3 PIXY(800),PIYY(800),PITH(800),RSDSP(800),UG(800),VG(800),	COMD	5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD	6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZI	COMD	7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD	8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD	9
2 GX,GY,IDOT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD	10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD	11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD	12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD	13
6 T,TFILM,THIRD,TIMLMT,TLMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD	14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD	15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD	16
INTEGER WB,WL,WR,WT	COMD	17
C ***	BEGIN	4
C *** GET JOB IDENTIFICATION, RUN-TIME LIMIT, DATE AND TIME OF DAY.	BEGIN	5
C ***	BEGIN	6
READ(5,100) NAME	BEGIN	7
JNM=10HXPORT-SALE	BEGIN	8
CALL GETJTL(TIMLMT)	BEGIN	9
CALL DATEH(D1)	BEGIN	10
CALL TIMEH(C1)	BEGIN	11
C ***	BEGIN	12
C *** THE FOLLOWING 5 CALLS REFER STRICTLY TO LASL COM SOFTWARE.	BEGIN	13
C *** FILM CHOICES ARE: 3H105, 2H16, 3H16C, 2H35, 3H35C . . .	BEGIN	14
C ***	BEGIN	15
CALL GFR80 (1HU,NAME,60,3H105,5HT3AAA,4HKEEP)	BEGIN	16
CALL GRPHLUN(12)	BEGIN	17
CALL LIB4020	BEGIN	18
CALL GRPHFTN	BEGIN	19
CALL SETFLSH	BEGIN	20
C ***	BEGIN	21
C *** CLEAR SCM CELL STORAGE BLOCK . . .	BEGIN	22
C ***	BEGIN	23
NWSCI=LOC(ZZ1)-LOC(AA)+1	BEGIN	24
DO 10 N=1,NWSCI	BEGIN	25
10 AA(N)=0.	BEGIN	26
RETURN	BEGIN	27
100 FORMAT(8A10)	BEGIN	28
END	BEGIN	29

SUBROUTINE CELSET	CELSET 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C ***	CELSET 4
C *** INITIALIZE X AND Y IN THIS FIRST LOOP. THIS LOOP SHOULD BE	CELSET 5
C *** REPLACED BY THE USER WHEN DOING A SPECIAL GRID GENERATION. THE	CELSET 6
C *** REMAINING LOOPS OF CELSET ARE MORE GENERAL IN THEIR APPLICABILITY.	CELSET 7
C ***	CELSET 8
DO 20 J=1,NYP	CELSET 9
IJ=(J-1)*NXP+1	CELSET10
DO 10 I=1,NXP	CELSET11
X(IJ)=FLOAT(I-1)*DX	CELSET12
Y(IJ)=FLOAT(J-1)*DY	CELSET13
10 IJ=IJ+1	CELSET14
20 CONTINUE	CELSET15
C ***	CELSET16
C *** NEXT, INITIALIZE THE REMAINING VERTEX QUANTITIES	CELSET17
C *** (SPECIFIED INFLOW VELS. WILL BE SET IN SUBR. BC)	CELSET18
C ***	CELSET19
DO 140 J=1,NYP	CELSET20
IJ=(J-1)*NXP+1	CELSET21
DO 130 I=1,NXP	CELSET22
R(IJ)=X(IJ)*CYL+OMCYL	CELSET23
U(IJ)=V(IJ)=MV(IJ)=0.	CELSET24
130 IJ=IJ+1	CELSET25
140 CONTINUE	CELSET26
C ***	CELSET27
C *** INITIALIZE THE CELL CENTERED QUANTITIES	CELSET28
C *** FIRST, GET THE VOLUMES, REQUIRED FOR MC CALCULATION	CELSET29
C ***	CELSET30
CALL VOLUME	CELSET31
DO 160 J=1,NY	CELSET32
IJ=(J-1)*NXP+1	CELSET33
DO 150 I=1,NX	CELSET34
RO(IJ)=ROI	CELSET35
SIE(IJ)=SIE1	CELSET36
C ***	CELSET37
C *** INITIAL PRESSURE IS E.O.S. PRESSURE, EXCEPT FOR INCOMPRESSIBLE	CELSET38
C *** CASE (INC=1), FOR WHICH INITIAL PRESSURE IS ZERO...	CELSET39
C ***	CELSET40
CALL EOS(P(IJ),RO(IJ),SIE(IJ),0.,RO(IJ))	CELSET41
MC(IJ)=VOL(IJ)*RO(IJ)	CELSET42
150 IJ=IJ+1	CELSET43
160 CONTINUE	CELSET44
C ***	CELSET45
C *** BCSET WILL ADJUST BOUNDARY VALUES OF U,V,MC,RO,SIE,P AS REQD.	CELSET46
C *** IF INFLOW OR PRESSURE BOUNDARIES ARE SPECIFIED . . .	CELSET47
C ***	CELSET48
CALL BCSET	CELSET49

C ***		CELSET50
C ***	INITIALIZE VERTEX MASSES AND THEIR RECIPROALS	CELSET51
C ***		CELSET52
	DO 180 J=1,NY	CELSET53
	IJ=(J-1)*NXP+1	CELSET54
	IJP=IJ+NXP	CELSET55
	DO 170 I=1,NX	CELSET56
	IPJ=IJ+1	CELSET57
	IPJP=IJP+1	CELSET58
	QM=0.25*MC(IJ)	CELSET59
	MV(IPJ) =MV(IPJ) +QM	CELSET60
	MV(IPJP)=MV(IPJP)+QM	CELSET61
	MV(IJP) =MV(IJP) +QM	CELSET62
	MV(IJ) =MV(IJ) +QM	CELSET63
	IJ=IPJ	CELSET64
170	IJP=IPJP	CELSET65
180	CONTINUE	CELSET66
	DO 200 J=1,NYP	CELSET67
	IJ=(J-1)*NXP+1	CELSET68
	DO 190 I=1,NXP	CELSET69
	RMV(IJ)=1./MV(IJ)	CELSET70
190	IJ=IJ+1	CELSET71
200	CONTINUE	CELSET72
	CALL BC(U,V)	CELSET73
	RETURN	CELSET74
	END	CELSET75

SUBROUTINE CONTUR(L,CQ)	CONTUR 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),ROSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,AD,B0,COLAMJ,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
DIMENSION CQ(1),IX1(2),IY1(2),XCO(4),YCO(4),CON(11)	CONTUR 4
DIMENSION IDEN(3)	CONTUR 5
DATA (IDEN(1),1=1,3)/10HISOBARS ,10HISOPYCNICS,10HISOTHERMS /	CONTUR 6
C ***	CONTUR 7
C *** CONTOUR PLOT OF ARRAY CQ. (CALLED FROM SUBR. FULOUT)	CONTUR 8
C ***	CONTUR 9
IF(NX.EQ.1 .OR. NY.EQ.1) RETURN	CONTUR 10
C ***	CONTUR 11
C *** SET CONTOUR VALUES	CONTUR 12
C ***	CONTUR 13
QMN=1.E+200	CONTUR 14
QMX=-QMN	CONTUR 15
DO 20 J=JFIRST,JLAST	CONTUR 16
IJ=(J-1)*NXP+1	CONTUR 17
DO 10 I=IFIRST,ILAST	CONTUR 18
QMN=AMIN1(CQ(IJ),QMN)	CONTUR 19
QMX=AMAX1(CQ(IJ),QMX)	CONTUR 20
10 IJ=IJ+1	CONTUR 21
20 CONTINUE	CONTUR 22
XX=QMX-QMN	CONTUR 23
IF(XX.LE.0.001*AMAX1(ABS(QMX),ABS(QMN))) RETURN	CONTUR 24
DQ=0.1*(XX+1.E-50)	CONTUR 25
DO 30 K=1,11	CONTUR 26
30 CON(K)=QMN+(FLOAT(K-1))*DQ	CONTUR 27
C ***	CONTUR 28
C *** PRINT THE LABELS ON THE PLOT	CONTUR 29
C ***	CONTUR 30
CALL ADV (1)	CONTUR 31
CALL LINCNT(59)	CONTUR 32
WRITE(12,170) JNM,D1,C1,NAME,T,NCYC	CONTUR 33
WRITE(12,180) IDEN(L),QMN,QMX,CON(2),CON(10),DQ	CONTUR 34
C ***	CONTUR 35
C *** DRAW THE CONTOURS, CONSIDERING CELLS GROUPED IN QUADRANTS -	CONTUR 36
C *** IJ,IPJ,IJP,IPJP	CONTUR 37
C ***	CONTUR 38
DO 130 J=JFIRST,JLASTM	CONTUR 39
IJ=(J-1)*NX+FIRST	CONTUR 40
IJP=IJ+NXP	CONTUR 41
DO 120 I=IFIRST,ILASTM	CONTUR 42
IPJ=IJ+1	CONTUR 43
IPJP=IJP+1	CONTUR 44
N=0	CONTUR 45
C ***	CONTUR 46
C *** DRAW ALL CONTOUR SEGMENTS PASSING THRU THE AREA BOUNDED	CONTUR 47
C *** BY THE CENTERS OF THE FOUR CELLS . . .	CONTUR 48
C ***	CONTUR 49

DO 110 K=2,11	CONTUR50
K1=K2=K3=K4=0	CONTUR51
IF(CQ(IJ) .LE.CON(K)) K1=1	CONTUR52
IF(CQ(IPJ) .LE.CON(K)) K2=1	CONTUR53
IF(CQ(IJP) .LE.CON(K)) K3=1	CONTUR54
IF(CQ(IPJP) .LE.CON(K)) K4=1	CONTUR55
C ***	CONTUR56
C *** IF PRODUCT .NE. 0, THEN ALL 4 ARE = 1.	CONTUR57
C *** IF SUM. EQ. 0, THEN ALL 4 ARE = 0. FOR EITHER OF THESE,	CONTUR58
C *** THE CONTOUR DOES NOT PASS THRU, SO GO TO 110 TO TRY NEXT	CONTUR59
C *** VALUE ON K LOOP . . .	CONTUR60
C ***	CONTUR61
IF(K1*K2*K3*K4.NE.0.OR.K1+K2+K3+K4.EQ.0) GO TO 110	CONTUR62
IF(N.GT.0) GO TO 60	CONTUR63
IJB=IJ	CONTUR64
IJA=IJP	CONTUR65
DO 50 JJ=1,2	CONTUR66
DO 40 II=1,2	CONTUR67
IPJB=IJB+1	CONTUR68
IPJA=IJA+1	CONTUR69
N=N+1	CONTUR70
XCO(N)=.25*(X(IPJB)+X(IPJA)+X(IJA)+X(IJB))	CONTUR71
YCO(N)=.25*(Y(IPJB)+Y(IPJA)+Y(IJA)+Y(IJB))	CONTUR72
IJA=IPJA	CONTUR73
40 IJB=IPJB	CONTUR74
IJB=IJP	CONTUR75
50 IJA=IJP+NXP	CONTUR76
60 LL=0	CONTUR77
IF(K1+K3.NE.1) GO TO 70	CONTUR78
IC1=1	CONTUR79
IC2=3	CONTUR80
IJ1=IJ	CONTUR81
IJ2=IJP	CONTUR82
KR1=1	CONTUR83
GO TO 100	CONTUR84
70 IF(K1+K2.NE.1) GO TO 80	CONTUR85
IC1=1	CONTUR86
IC2=2	CONTUR87
IJ1=IJ	CONTUR88
IJ2=IPJ	CONTUR89
KR1=2	CONTUR90
GO TO 100	CONTUR91
80 IF(K2+K4.NE.1) GO TO 90	CONTUR92
IC1=2	CONTUR93
IC2=4	CONTUR94
IJ1=IPJ	CONTUR95
IJ2=IPJP	CONTUR96
KR1=3	CONTUR97
GO TO 100	CONTUR98
90 IF(K3+K4.NE.1) GO TO 110	CONTUR99
IC1=3	CONTU100
IC2=4	CONTU101
IJ1=IJP	CONTU102
IJ2=IPJP	CONTU103
KR1=4	CONTU104
100 LL=LL+1	CONTU105
XX=(CON(K)-CQ(IJ1))/(CQ(IJ2)-CQ(IJ1))	CONTU106
IX1(LL)=F1XL+(XCO(IC1)+XX*(XCO(IC2)-XCO(IC1))-XL)*XCONV	CONTU107
IY1(LL)=F1YB-(YCO(IC1)+XX*(YCO(IC2)-YCO(IC1))-YB)*YCONV	CONTU108
IF(LL.LT.2) GO TO (70,80,90,110),KR1	CONTU109
CALL DRV (IX1(1),IY1(1),IX1(2),IY1(2))	CONTU110
IF(K.EQ.2) CALL PLT (IX1(1),IY1(1),35)	CONTU111
IF(K.EQ.10) CALL PLT (IX1(1),IY1(1),24)	CONTU112

LL=0	CONTU113
IF (IJ2.EQ.1PJ) GO TO 80	CONTU114
110 CONTINUE	CONTU115
IJ=1PJ	CONTU116
120 IJP=1PJP	CONTU117
130 CONTINUE	CONTU118
C ***	CONTU119
C *** DRAW THE FRAME TO OUTLINE THE MESH PERIPHERY	CONTU120
C ***	CONTU121
DO 150 J=1,NY	CONTU122
IJ=(J-1)*NXP+1	CONTU123
IJP=IJ+NXP	CONTU124
DO 140 I=1,NX	CONTU125
1PJ=IJ+1	CONTU126
1PJP=1JP+1	CONTU127
IX1(1)=F1XL+(X(1PJ)-XL)*XCONV	CONTU128
IY1(1)=F1YB-(Y(1PJ)-YB)*YCONV	CONTU129
IX2=F1XL+(X(1PJP)-XL)*XCONV	CONTU130
IY2=F1YB-(Y(1PJP)-YB)*YCONV	CONTU131
IX3=F1XL+(X(1JP)-XL)*XCONV	CONTU132
IY3=F1YB-(Y(1JP)-YB)*YCONV	CONTU133
IX4=F1XL+(X(1J)-XL)*XCONV	CONTU134
IY4=F1YB-(Y(1J)-YB)*YCONV	CONTU135
IF (I.EQ.1) CALL DRV (IX3,IY3,IX4,IY4)	CONTU136
IF (J.EQ.1) CALL DRV (IX4,IY4,IX1(1),IY1(1))	CONTU137
IF (I.EQ.NX) CALL DRV (IX1(1),IY1(1),IX2,IY2)	CONTU138
IF (J.EQ.NY) CALL DRV (IX2,IY2,IX3,IY3)	CONTU139
IJ 1PJ	CONTU140
140 IJP=1PJP	CONTU141
150 CONTINUE	CONTU142
RETURN	CONTU143
170 FORMAT(2X,A10,2(2X,AB),2X,8A10/40X,3H T=,1PE12.5,6H CYCLE,15)	CONTU144
180 FORMAT(1X,A10,5H MIN=,1PE12.5,5H MAX=,E12.5,3H L=,E12.5,3H H=,	CONTU145
1 E12.5,4H DQ=,E12.5)	CONTU146
END	CONTU147

SUBROUTINE DSDP	DSDP	2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD	2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD	3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD	4
3 PIXY(800),PIYY(800),P1TH(800),RSDP(800),UG(800),VG(800),	COMD	5
4 UREL(800),VREL(800),MP(800),MVP(800),STEP(800),UMOM(800),	COMD	6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD	7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAM1,CYL,C1,DPCOF,	COMD	8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FYB,GMI,GRFAC,GRIND,	COMD	9
2 GX,GY,1DDT,1FIRST,1FPHI,1LAST,1LASTM,1LASTV,1LPHI,1MP,1NC,1PRES,	COMD	10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD	11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD	12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD	13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD	14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,XICOF,XL,YB,YCONV,ZZ	COMD	15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD	16
INTEGER WB,WL,WR,WT	COMD	17
C ***	DSDP	4
C *** PHASE 2. NUMERICAL EVALUATION OF RELAXATION FACTOR	DSDP	5
C *** TO BE USED IN THE PRESSURE ITERATION (SUBR. PRESIT) . . .	DSDP	6
C ***	DSDP	7
C ***	DSDP	8
DATA PTEMP,PSTAR /0.,0./	DSDP	9
DP=DPCOF/(DT*DT)	DSDP	10
DTP=0.5*DT*DP	DSDP	11
DO 20 J=JFIRST,JLAST	DSDP	12
IJ=(J-1)*NXP+1FIRST	DSDP	13
IJP=IJ+NXP	DSDP	14
DO 10 I=1FIRST,1LAST	DSDP	15
IPJ=IJ+1	DSDP	16
IPJP=IJP+1	DSDP	17
X1=X(IPJ)	DSDP	18
X2=X(IPJP)	DSDP	19
X3=X(IJP)	DSDP	20
X4=X(IJ)	DSDP	21
R1=R(IPJ)	DSDP	22
R2=R(IPJP)	DSDP	23
R3=R(IJP)	DSDP	24
R4=R(IJ)	DSDP	25
Y1=Y(IPJ)	DSDP	26
Y2=Y(IPJP)	DSDP	27
Y3=Y(IJP)	DSDP	28
Y4=Y(IJ)	DSDP	29
U1=UL(IPJ)	DSDP	30
U2=UL(IPJP)	DSDP	31
U3=UL(IJP)	DSDP	32
U4=UL(IJ)	DSDP	33
V1=VL(IPJ)	DSDP	34
V2=VL(IPJP)	DSDP	35
V3=VL(IJP)	DSDP	36
V4=VL(IJ)	DSDP	37
X1P=X1+U1*DT	DSDP	38
Y1P=Y1+V1*DT	DSDP	39
X2P=X2+U2*DT	DSDP	40
Y2P=Y2+V2*DT	DSDP	41
X3P=X3+U3*DT	DSDP	42
Y3P=Y3+V3*DT	DSDP	43
X4P=X4+U4*DT	DSDP	44
Y4P=Y4+V4*DT	DSDP	45
R1P=X1P*CYL+OMCYL	DSDP	46
R2P=X2P*CYL+OMCYL	DSDP	47
R3P=X3P*CYL+OMCYL	DSDP	48
R4P=X4P*CYL+OMCYL	DSDP	49

ATR=.5*((X3P-X2P)*(Y1P-Y2P)-(X1P-X2P)*(Y3P-Y2P))	DSOP	50
ABL=.5*((X1P-X4P)*(Y3P-Y4P)-(X3P-X4P)*(Y1P-Y4P))	DSOP	51
VOLLZ=THIRD*((R1P+R2P+R3P)*ATR+(R3P+R4P+R1P)*ABL)	DSOP	52
X1TEMP=SIE(IJ)+P(IJ)*(1.0-VOLLZ/VOL(IJ))/RO(IJ)	DSOP	53
ROTEMP=RO(IJ)*VOL(IJ)/VOLLZ	DSOP	54
CALL EOS(PTEMP,ROTEMP,X1TEMP,P(IJ),RO(IJ))	DSOP	55
RM1=RMV(IPJ)	DSOP	56
RM2=RMV(IPJP)	DSOP	57
RM3=RMV(IJP)	DSOP	58
RM4=RMV(IJ)	DSOP	59
Y24=Y2-Y4	DSOP	60
Y31=Y3-Y1	DSOP	61
XR24=0.5*(R2+R4)*(X2-X4)	DSOP	62
XR31=0.5*(R3+R1)*(X3-X1)	DSOP	63
U1P=U1+DTP*RM1*Y24*R1	DSOP	64
U2P=U2+DTP*RM2*Y31*R2	DSOP	65
U3P=U3-DTP*RM3*Y24*R3	DSOP	66
U4P=U4-DTP*RM4*Y31*R4	DSOP	67
V1P=V1-DTP*RM1*XR24	DSOP	68
V2P=V2-DTP*RM2*XR31	DSOP	69
V3P=V3+DTP*RM3*XR24	DSOP	70
V4P=V4+DTP*RM4*XR31	DSOP	71
X1P=X1+U1P*DT	DSOP	72
Y1P=Y1+V1P*DT	DSOP	73
X2P=X2+U2P*DT	DSOP	74
Y2P=Y2+V2P*DT	DSOP	75
X3P=X3+U3P*DT	DSOP	76
Y3P=Y3+V3P*DT	DSOP	77
X4P=X4+U4P*DT	DSOP	78
Y4P=Y4+V4P*DT	DSOP	79
R1P=X1P*CYL+OMCYL	DSOP	80
R2P=X2P*CYL+OMCYL	DSOP	81
R3P=X3P*CYL+OMCYL	DSOP	82
R4P=X4P*CYL+OMCYL	DSOP	83
ATR=.5*((X3P-X2P)*(Y1P-Y2P)-(X1P-X2P)*(Y3P-Y2P))	DSOP	84
ABL=.5*((X1P-X4P)*(Y3P-Y4P)-(X3P-X4P)*(Y1P-Y4P))	DSOP	85
VOLL=THIRD*((R1P+R2P+R3P)*ATR+(R3P+R4P+R1P)*ABL)	DSOP	86
X1STAR=X1TEMP+PTEMP*(1.0-VOLL/VOLLZ)/ROTEMP	DSOP	87
ROSTAR=RO(IJ)*VOL(IJ)/VOLL	DSOP	88
PPDP=P(IJ)+DP	DSOP	89
CALL EOS(PSTAR,ROSTAR,X1STAR,PPDP,RO(IJ))	DSOP	90
RDSOP(IJ)=DP/(PTEMP+DP-PSTAR)*OM	DSOP	91
IJ=IPJ	DSOP	92
10 IJP=IPJP	DSOP	93
20 CONTINUE	DSOP	94
RETURN	DSOP	95
END	DSOP	96

	SUBROUTINE ENERGY	ENERGY 2
	COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
	1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
	2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
	3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
	4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
	5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
	COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
	1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,F1YB,GMI,GRFAC,GRIND,	COMD 9
	2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
	3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
	4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
	5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD 13
	6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD 14
	7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,XICOF,XL,YB,YCONV,ZZ	COMD 15
	REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
	INTEGER WB,WL,WR,WT	COMD 17
C ***		ENERGY 4
C ***	CALCULATE ENERGY CHANGES DUE TO PDV WORK AND VISCOUS STRESSES	ENERGY 5
C ***		ENERGY 6
	DO 20 J=JFIRST,JLAST	ENERGY 7
	IJ=(J-1)*NXP+IFIRST	ENERGY 8
	IJP=IJ+NXP	ENERGY 9
	DO 10 I=IFIRST,ILAST	ENERGY10
	IPJ=I+I	ENERGY11
	IJPJ=IJP+I	ENERGY12
	X1=X(IPJ)	ENERGY13
	Y1=Y(IPJ)	ENERGY14
	R1=R(IPJ)	ENERGY15
	UTC1=U(IPJ)+UL(IPJ)	ENERGY16
	VTC1=V(IPJ)+VL(IPJ)	ENERGY17
	X2=X(IJPJ)	ENERGY18
	Y2=Y(IJPJ)	ENERGY19
	R2=R(IJPJ)	ENERGY20
	UTC2=U(IJPJ)+UL(IJPJ)	ENERGY21
	VTC2=V(IJPJ)+VL(IJPJ)	ENERGY22
	X3=X(IJP)	ENERGY23
	Y3=Y(IJP)	ENERGY24
	R3=R(IJP)	ENERGY25
	UTC3=U(IJP)+UL(IJP)	ENERGY26
	VTC3=V(IJP)+VL(IJP)	ENERGY27
	X4=X(IJ)	ENERGY28
	Y4=Y(IJ)	ENERGY29
	R4=R(IJ)	ENERGY30
	UTC4=U(IJ)+UL(IJ)	ENERGY31
	VTC4=V(IJ)+VL(IJ)	ENERGY32
	Y24=Y2-Y4	ENERGY33
	Y31=Y3-Y1	ENERGY34
	X24=X2-X4	ENERGY35
	X31=X3-X1	ENERGY36
	HR24=0.5*(R2+R4)	ENERGY37
	HR13=0.5*(R1+R3)	ENERGY38
	XX1=HR24*(PIXY(IJ)*X24-PIXX(IJ)*Y24)	ENERGY39
	XX2=HR13*(PIXY(IJ)*X31-PIXX(IJ)*Y31)	ENERGY40
	XX3=HR24*(PIYY(IJ)*X24-PIXY(IJ)*Y24)	ENERGY41
	XX4=HR13*(PIYY(IJ)*X31-PIXY(IJ)*Y31)	ENERGY42
	DV=Y24*(UTC1*R1-UTC3*R3) + Y31*(UTC2*R2-UTC4*R4)	ENERGY43
	1 -HR24*X24*(VTC1-VTC3) - HR13*X31*(VTC2-VTC4)	ENERGY44
	AREA=0.5*(X24*Y31-X31*Y24)	ENERGY45
	DVIS=XX1*(UTC1-UTC3)+XX2*(UTC2-UTC4)	ENERGY46
	1 -PITH(IJ)*(UTC1+UTC2+UTC3+UTC4)*0.5*AREA	ENERGY47
	2 +XX3*(VTC1-VTC3)+XX4*(VTC2-VTC4)	ENERGY48
	SIE(IJ)=SIE(IJ)-(P(IJ)+Q(IJ))*DV + DVIS)*0.25*DT/MC(IJ)	ENERGY49

IJP=IPJP	ENERGY50
10 IJ=IPJ	ENERGY51
20 CONTINUE	ENERGY52
RETURN	ENERGY53
END	ENERGY54

SUBROUTINE EOS(PTEMP,ROTEMP,S1ETMP,PLCUR,ROLCUR)	EOS	2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD	2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),S1E(800),UL(800),	COMD	3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD	4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD	5
4 UREL(800),VREL(800),MP(800),MVP(800),S1EP(800),UMOM(800),	COMD	6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD	7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD	8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD	9
2 GX,GY,DDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD	10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD	11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD	12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,S1E1,S1EIN,	COMD	13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD	14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD	15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD	16
INTEGER WB,WL,WR,WT	COMD	17
IF(INC.EQ.1) GO TO 100	EOS	4
C ***	EOS	5
C *** EQUATION OF STATE FOR REAL MATERIAL GOES HERE . . .	EOS	6
C *** (STIFFENED GAS + IDEAL GAS E.O.S. IS SHOWN HERE AS AN EXAMPLE)	EOS	7
C ***	EOS	8
PTEMP=ASQ*(ROTEMP-RON)+GMI*ROTEMP*S1ETMP	EOS	9
RETURN	EOS	10
C ***	EOS	11
C *** PSEUDO-PRESSURE CALCULATION FOR INCOMPRESSIBLE FLOWS (INC=1) . . .	EOS	12
C ***	EOS	13
100 IF(ROLCUR.EQ.0.) GO TO 110	EOS	14
PTEMP=PLCUR + ROTEMP/ROLCUR - 1.0	EOS	15
RETURN	EOS	16
110 PTEMP=0.	EOS	17
RETURN	EOS	18
END	EOS	19

SUBROUTINE FULOUT (LUN)	FULOUT	2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD	2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),S1E(800),UL(800),	COMD	3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD	4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD	5
4 UREL(800),VREL(800),MP(800),MVP(800),S1EP(800),UMOM(800),	COMD	6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD	7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD	8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD	9
2 GX,GY,DDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD	10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD	11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD	12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,S1E1,S1EIN,	COMD	13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD	14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD	15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD	16
INTEGER WB,WL,WR,WT	COMD	17

IF(LUN.EQ.0) GO TO 10	FULOUT 4
IF(LUN.EQ.6) GO TO 40	FULOUT 5
TWFILM=TWFILM+TFILM	FULOUT 6
C ***	FULOUT 7
C *** SETUP PLOT SCALING AND CALL THE VARIOUS PLOT AND PRINT SUBRS.	FULOUT 8
C ***	FULOUT 9
10 XL=YB=1.E+100	FULOUT10
XR=YT=VMAX=-XL	FULOUT11
DO 30 J=1,NYP	FULOUT12
IJ=(J-1)*NXP+1	FULOUT13
DO 20 I=1,NXP	FULOUT14
XL=AMINI(XL,X(IJ))	FULOUT15
XR=AMAXI(XR,X(IJ))	FULOUT16
YB=AMINI(YB,Y(IJ))	FULOUT17
YT=AMAXI(YT,Y(IJ))	FULOUT18
VMAX=AMAXI(VMAX,ABS(U(IJ)),ABS(V(IJ)))	FULOUT19
20 IJ=IJ+1	FULOUT20
30 CONTINUE	FULOUT21
IF(VMAX.NE.0.) DROU=0.9*XR/(FLOAT(NX)*VMAX)	FULOUT22
FIBY=900.	FULOUT23
C ***	FULOUT24
C *** MAKE PLOTS SLIGHTLY UNDERSIZE TO ENSURE VELOCITY VECTORS	FULOUT25
C *** WILL BE PLOTTED PROPERLY AT MESH BOUNDARIES . . .	FULOUT26
C ***	FULOUT27
XTE=0.025*(XR-XL)	FULOUT28
YTE=0.025*(YT-YB)	FULOUT29
XL=XL-XTE	FULOUT30
XR=XR+XTE	FULOUT31
YB=YB-YTE	FULOUT32
YT=YT+YTE	FULOUT33
XD=(XR-XL)/(YT-YB)	FULOUT34
YY=0.	FULOUT35
IF(XD.LT.1.13556) YY=1.	FULOUT36
FIXL=AMAXI(0.,(511.-450.*XD)*YY)	FULOUT37
FIXR=(511.+450.*XD)*YY + 1022.*(1.-YY)	FULOUT38
FITY=(900.-1022./XD)*(1.-YY)	FULOUT39
XCONV=(FIXR-FIXL)/(XR-XL)	FULOUT40
YCONV=(FITY-FITY)/(YT-YB)	FULOUT41
CALL ZONPLT	FULOUT42
CALL VELPLT	FULOUT43
CALL CONTUR(1,P)	FULOUT44
CALL CONTUR(2,R0)	FULOUT45
CALL CONTUR(3,SIE)	FULOUT46
IF(LPR.EQ.1 .OR. LPR.EQ.2) CALL LNGPRT(12)	FULOUT47
CALL GLOBAL(12)	FULOUT48
IF(LUN.EQ.0) GO TO 50	FULOUT49
RETURN	FULOUT50
40 TWPRTT=TWPRTT+TPRTT	FULOUT51
50 IF(LPR.GT.1) CALL LNGPRT(6)	FULOUT52
CALL GLOBAL(6)	FULOUT53
RETURN	FULOUT54
END	FULOUT55

SUBROUTINE GLOBAL (LUN)	GLOBAL 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),STEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,F1YB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IOOT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,I1PHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,X1COF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C ***	GLOBAL 4
C *** COMPUTE TOTAL MASS, MOMENTUM, AND ENERGY OF THE SYSTEM	GLOBAL 5
C ***	GLOBAL 6
TOTM=TOTI=TOTU=TOTV=TOTK=0.	GLOBAL 7
DO 20 J=1,NY	GLOBAL 8
IJ=(J-1)*NXP+1	GLOBAL 9
DO 10 I=1,NX	GLOBAL 10
TOTM=TOTM+MC(IJ)	GLOBAL 11
TOTI=TOTI+MC(IJ)*SIE(IJ)	GLOBAL 12
10 IJ=IJ+1	GLOBAL 13
20 CONTINUE	GLOBAL 14
DO 40 J=1,NYP	GLOBAL 15
IJ=(J-1)*NXP+1	GLOBAL 16
DO 30 I=1,NXP	GLOBAL 17
TOTU=TOTU+MV(IJ)*U(IJ)	GLOBAL 18
TOTV=TOTV+MV(IJ)*V(IJ)	GLOBAL 19
TOTK=TOTK+MV(IJ)*.5*(U(IJ)*U(IJ)+V(IJ)*V(IJ))	GLOBAL 20
30 IJ=IJ+1	GLOBAL 21
40 CONTINUE	GLOBAL 22
TOTE=TOTK+TOTI	GLOBAL 23
WRITE(LUN,50) T,NCYC,TOTE,TOTI,TOTM,TOTU,TOTV	GLOBAL 24
RETURN	GLOBAL 25
50 FORMAT(3H T=,1PE12.5,6H CYCLE,15,7H TOT E=,E15.8,5H SIE=,E15.8/	GLOBAL 26
1 26X,6H MASS=,E15.8,7H U MOM=,E15.8,7H V MOM=,E15.8)	GLOBAL 27
END	GLOBAL 28

```

SUBROUTINE LNGPRT (LUN)
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),
3 PIXY(800),PIYY(800),PITH(800),RDSOP(800),UG(800),VG(800),
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,DI,EPS,FXL,F1YB,GMI,GRFAC,GRIND,
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ
REAL LAMBDA,MC,MP,MU,MV,MVP
INTEGER WB,WL,WR,WT
LNGPRT 2
COMD 2
COMD 3
COMD 4
COMD 5
COMD 6
COMD 7
COMD 8
COMD 9
COMD 10
COMD 11
COMD 12
COMD 13
COMD 14
COMD 15
CCID 16
COMD 17
C ***
C *** LONG PRINT OF X,Y,U,V,SIE,RO,MC,VOL,F FOR ALL CELLS IN MESH.
C *** DESTINATION IS FICHE (LUN=12), AND/OR LINE PRINTER (LUN=6)
C ***
LPR1=LPR2=0
IF(LPR.GT.1 .AND. LUN.EQ.6) LPR1=1
IF(LPR.LT.3 .AND. LUN.EQ.12) LPR2=1
LINES=99
DO 50 J=1,NYP
  IJ=(J-1)*NXP+1
  DO 40 I=1,NXP
    IF(LINES.LT.56) GO TO 10
    LINES=0
    IF(LPR1.GT.0) WRITE(6,100) JNM,DI,C1,NAME,T,NCYC
    IF(LPR2.GT.0) WRITE(12,100) JNM,DI,C1,NAME,T,NCYC
  10 IF(LOOPS.LT.LOOPMX) GO TO 20
C ***
C *** SPECIAL PRINT FOR RUN-ABORT CASE . . .
C ***
IF(LPR1.GT.0) WRITE(6,110) I,J,X(IJ),Y(IJ),UL(IJ),VL(IJ),
1 SIE(IJ),ROL(IJ),MC(IJ),VOL(IJ),PL(IJ)
IF(LPR2.GT.0) WRITE(12,110) I,J,X(IJ),Y(IJ),UL(IJ),VL(IJ),
1 SIE(IJ),ROL(IJ),MC(IJ),VOL(IJ),PL(IJ)
GO TO 30
C ***
C *** NORMAL OUTPUT CASE . . .
C ***
20 IF(LPR1.GT.0) WRITE(6,110) I,J,X(IJ),Y(IJ),U(IJ),V(IJ),SIE(IJ),
1 RO(IJ),MC(IJ),VOL(IJ),P(IJ)
IF(LPR2.GT.0) WRITE(12,110) I,J,X(IJ),Y(IJ),U(IJ),V(IJ),SIE(IJ),
1 RO(IJ),MC(IJ),VOL(IJ),P(IJ)
30 LINES=LINES+1
40 IJ=IJ+1
50 CONTINUE
IF(LPR2.GT.0) CALL ADV(1)
RETURN
100 FORMAT(1H1,2X,A10,2(2X,A8),2X,8A10/40X,3H T=,1PE12.5,6H CYCLE,15/
1 1H0,7H 1 J,6X,1HX,10X,1HY,10X,1HU,10X,1HV,
2 10X,3HSIE,8X,3HROL,7X,4HMASS,8X,3HVOL,8X,1HP)
110 FORMAT(214,9(1PE11.3))
END
LNGPRT 4
LNGPRT 5
LNGPRT 6
LNGPRT 7
LNGPRT 8
LNGPRT 9
LNGPRT 10
LNGPRT 11
LNGPRT 12
LNGPRT 13
LNGPRT 14
LNGPRT 15
LNGPRT 16
LNGPRT 17
LNGPRT 18
LNGPRT 19
LNGPRT 20
LNGPRT 21
LNGPRT 22
LNGPRT 23
LNGPRT 24
LNGPRT 25
LNGPRT 26
LNGPRT 27
LNGPRT 28
LNGPRT 29
LNGPRT 30
LNGPRT 31
LNGPRT 32
LNGPRT 33
LNGPRT 34
LNGPRT 35
LNGPRT 36
LNGPRT 37
LNGPRT 38
LNGPRT 39
LNGPRT 40
LNGPRT 41
LNGPRT 42
LNGPRT 43
LNGPRT 44

```

SUBROUTINE NEWCYC	NEWCYC 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),Z71	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,OPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EFS,FXL,F1YB,GH1,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNH,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,RO1,ROIN,RON,SIE1,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,XICOF,X2,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
DATA TIME /0./	NEWCYC 4
C ***	NEWCYC 5
C *** BEGIN CYCLE - PROVIDE MONITOR PRINT, THEN TEST FOR	NEWCYC 6
C *** OUTPUT AND RUN TERMINATION. IF CONTINUING, INCREMENT	NEWCYC 7
C *** TIME AND CYCLE NUMBER . . .	NEWCYC 8
C ***	NEWCYC 9
IF(NCYC.LE.1) CALL FULOUT(0)	NEWCYC10
IF((MOD(NCYC,25).EQ.0).OR.(T.GE.TWFIN))	NEWCYC11
WRITE(59,100) NCYC,T,DT,NUMIT,GRIND,IDDT	NEWCYC12
WRITE(6,100) NCYC,T,DT,NUMIT,GRIND,IDDT	NEWCYC13
WRITE(12,100) NCYC,T,DT,NUMIT,GRIND,IDDT	NEWCYC14
IF(T.GE.TWFILM) CALL FULOUT(12)	NEWCYC15
IF(T.GE.TWPRTR) CALL FULOUT(6)	NEWCYC16
TOLD=TIME	NEWCYC17
CALL SECOND(TIME)	NEWCYC18
GRIND=(TIME-TOLD)*GRFAC	NEWCYC19
TLEFT=TIMLMT-TIME	NEWCYC20
IF(TLEFT.LT.180. .AND. TLIMD.EQ.1.) CALL TAPEWR	NEWCYC21
IF(T.GE.TWFIN) GO TO 10	NEWCYC22
T=T+DT	NEWCYC23
NCYC=NCYC+1	NEWCYC24
RETURN	NEWCYC25
10 WRITE(59,110)	NEWCYC26
WRITE(6,110)	NEWCYC27
WRITE(12,110)	NEWCYC28
IF(T.LT.TWFILM) CALL FULOUT(12)	NEWCYC29
IF(T.LT.TWPRTR) CALL FULOUT(6)	NEWCYC30
CALL EXITA(1)	NEWCYC31
100 FORMAT(5H NCYC,16,3H T=,1PE12.5,4H DT=,E12.5,7H NUMIT=,14,	NEWCYC32
1 7H GRIND=,OPF7.3,1X,A1)	NEWCYC33
110 FORMAT(19H NORMAL TERMINATION)	NEWCYC34
END	NEWCYC35

SUBROUTINE PHASE1	PHASE1 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),P1TH(800),RSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),VMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,AO,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,DI,EPS,FI XL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPH1,ILAST,ILASTM,ILASTV,ILPH1,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPH1,JLAST,JLASTM,JLASTV,JLPH1,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C +++	PHASE1 4
C +++ PHASE 1. EXPLICIT LAGRANGIAN CALCULATION, IN WHICH WE ADJUST	PHASE1 5
C +++ THE LAGRANGIAN VELOCITIES BY PRESSURE GRADIENTS AND BODY FORCES.	PHASE1 6
C +++	PHASE1 7
C +++ THE PRESSURE ACCELERATIONS . . .	PHASE1 6
C +++	PHASE1 9
DO 20 J=JFPH1,JLPH1	PHASE110
IJ=(J-1)*NXP+IFPH1	PHASE111
IJP=IJ+NXP	PHASE112
DO 10 I=IFPH1,ILPH1	PHASE113
IPJ=IJ+1	PHASE114
IPJP=IJP+1	PHASE115
DTP=0.5*DT*P(IJ)	PHASE116
RM1=RMV(IPJ)	PHASE117
RM2=RMV(IPJP)	PHASE118
RM3=RMV(IJP)	PHASE119
RM4=RMV(IJ)	PHASE120
R1=R(IPJ)	PHASE121
R2=R(IPJP)	PHASE122
R3=R(IJP)	PHASE123
R4=R(IJ)	PHASE124
XR24=(X(IPJP)-X(IJ))*0.5*(R2+R4)	PHASE125
XR31=(X(IJP)-X(IPJ))*0.5*(R3+R1)	PHASE126
Y24=Y(IPJP)-Y(IJ)	PHASE127
Y31=Y(IJP)-Y(IPJ)	PHASE128
UL(IPJ)=UL(IPJ)+DTP*RM1*Y24*R1	PHASE129
UL(IPJP)=UL(IPJP)+DTP*RM2*Y31*R2	PHASE130
UL(IJP)=UL(IJP)-DTP*RM3*Y24*R3	PHASE131
UL(IJ)=UL(IJ)-DTP*RM4*Y31*R4	PHASE132
VL(IPJ)=VL(IPJ)-DTP*RM1*XR24	PHASE133
VL(IPJP)=VL(IPJP)-DTP*RM2*XR31	PHASE134
VL(IJP)=VL(IJP)+DTP*RM3*XR24	PHASE135
VL(IJ)=VL(IJ)+DTP*RM4*XR31	PHASE136
IJ=IPJ	PHASE137
10 IJP=IPJP	PHASE138
20 CONTINUE	PHASE139
IF(GX.EQ.0..AND.GY.EQ.0.) GO TO 50	PHASE140
C +++	PHASE141
C +++ THE BODY ACCELERATIONS . . .	PHASE142
C +++	PHASE143
DTGX=DT*GX	PHASE144
DTGY=DT*GY	PHASE145
DO 40 J=JFIRST,JLASTV	PHASE146
IJ=NXP*(J-1)+IFIRST	PHASE147
DO 30 I=IFIRST,ILASTV	PHASE148
VL(IJ)=VL(IJ)+DTGY	PHASE149

```
      UL(IJ)=UL(IJ)+DTGX  
30  IJ=IJ+1  
40  CONTINUE  
50  CALL BC(UL,VL)  
      RETURN  
      END
```

```
PHASE150  
PHASE151  
PHASE152  
PHASE153  
PHASE154  
PHASE155
```


SUBROUTINE PRESIT	PRESIT 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),ROSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C +++	PRESIT 4
C +++ PHASE 2. THE NEWTON-RAPHSON PRESSURE ITERATION . . .	PRESIT 5
C +++	PRESIT 6
DATA PSTAR /0./	PRESIT 7
NUMIT=0	PRESIT 8
10 NUMIT=NUMIT+1	PRESIT 9
MUSTIT=0	PRESIT10
PMAXN=0.	PRESIT11
DO 30 J=JFIRST,JLAST	PRESIT12
IJ=(J-1)*NXP+IFIRST	PRESIT13
IJP=IJ+NXP	PRESIT14
DO 20 I=IFIRST,ILAST	PRESIT15
IPJ=IJ+I	PRESIT16
IPJP=IJP+1	PRESIT17
X1=X(IPJ)	PRESIT18
R1=R(IPJ)	PRESIT19
Y1=Y(IPJ)	PRESIT20
U1=UL(IPJ)	PRESIT21
V1=VL(IPJ)	PRESIT22
X2=X(IPJP)	PRESIT23
R2=R(IPJP)	PRESIT24
Y2=Y(IPJP)	PRESIT25
U2=UL(IPJP)	PRESIT26
V2=VL(IPJP)	PRESIT27
X3=X(IJP)	PRESIT28
R3=R(IJP)	PRESIT29
Y3=Y(IJP)	PRESIT30
U3=UL(IJP)	PRESIT31
V3=VL(IJP)	PRESIT32
X4=X(IJ)	PRESIT33
R4=R(IJ)	PRESIT34
Y4=Y(IJ)	PRESIT35
U4=UL(IJ)	PRESIT36
V4=VL(IJ)	PRESIT37
X1P=X1+UL(IPJ)*DT	PRESIT38
X2P=X2+UL(IPJP)*DT	PRESIT39
X3P=X3+UL(IJP)*DT	PRESIT40
X4P=X4+UL(IJ)*DT	PRESIT41
Y1P=Y1+VL(IPJ)*DT	PRESIT42
Y2P=Y2+VL(IPJP)*DT	PRESIT43
Y3P=Y3+VL(IJP)*DT	PRESIT44
Y4P=Y4+VL(IJ)*DT	PRESIT45
R1P=X1P*CYL+OMCYL	PRESIT46
R2P=X2P*CYL+OMCYL	PRESIT47
R3P=X3P*CYL+OMCYL	PRESIT48
R4P=X4P*CYL+OMCYL	PRESIT49

```

      ATR=.5*((X3P-X2P)*(Y1P-Y2P)-(X1P-X2P)*(Y3P-Y2P))
      ABL=.5*((X1P-X4P)*(Y3P-Y4P)-(X3P-X4P)*(Y1P-Y4P))
      VW=THIRD*((R1P+R2P+R3P)*ATR+(R3P+R4P+R1P)*ABL)
      IF (VW.LE.0.) GO TO 90
      ROL(IJ)=RO(IJ)*VOL(IJ)/VW
      X1STAR=SIE(IJ)+PL(IJ)*(1.-VW/VOL(IJ))/ROL(IJ)
      CALL EOS(PSTAR,ROL(IJ),X1STAR,PL(IJ),RO(IJ))
      S=PL(IJ)-PSTAR
      DP=-S*RSDP(IJ)
      PL(IJ)=PL(IJ)+DP
      PMAXN=AMAX1(PMAXN,ABS(PL(IJ)))
      Y24=Y2-Y4
      Y31=Y3-Y1
      XR24=(X2-X4)*.5*(R2+R4)
      XR31=(X3-X1)*.5*(R3+R1)
      XX=0.5*DT*DP
      RM1=RMV(1PJ)
      RM2=RMV(1PJP)
      RM3=RMV(1JP)
      RM4=RMV(IJ)
      UL(1PJ)=U1+XX*RM1*Y24*R1
      UL(1PJP)=U2+XX*RM2*Y31*R2
      UL(1JP)=U3-XX*RM3*Y24*R3
      UL(IJ)=U4-XX*RM4*Y31*R4
      VL(1PJ)=V1-XX*RM1*XR24
      VL(1PJP)=V2-XX*RM2*XR31
      VL(1JP)=V3+XX*RM3*XR24
      VL(IJ)=V4+XX*RM4*XR31
      IF (ABS(DP).GT.EPS*PMAX) MUSTIT=MUSTIT+1
      IJ=1PJ
20  IJP=1PJP
30  CONTINUE
C   +++
C   +++ IPRES=1 LETS CONTINUATIVE BOUNDARY UL,VL FLOAT DURING ITERATION.
C   +++
      IPRES=1
      CALL BC(UL,VL)
      IPRES=0
C   +++
C   +++ NUMIT=(MAXIT) IN PRESIT-PROBLEM COMMENT SIGNIFIES THAT
C   +++ CONVERGENCE FAILURE IS FORCING A DT CUT . . .
C   +++ BUT IF INC=1, SIMPLY EXIT ITERATION IF NUMIT=MAXIT.
C   +++
      PMAX=PMAXN
      IF (NUMIT.EQ.MAXIT .AND. INC.EQ.1) GO TO 60
      IF (NUMIT.EQ.MAXIT) RETURN
      IF ((MUSTIT.GT.0) .OR. (NCYC*NUMIT.EQ.1)) GO TO 10
60  DO 80 J=JFIRST,JLAST
      IJ=(J-1)*NXP+IFIRST
      DO 70 I=IFIRST,I LAST
      P(IJ)=PL(IJ)
70  IJ=IJ+1
80  CONTINUE
      IF (WB.EQ.4 .OR. WL.EQ.4 .OR. WR.EQ.4 .OR. WT.EQ.4) CALL BC(UL,VL)
      RETURN
C   +++
C   +++ NUMIT=9999 IN PRESIT-PROBLEM COMMENT SIGNIFIES THAT A
C   +++ NEGATIVE VOLUME IS FORCING A DT CUT . . .
C   +++
90  NUMIT=9999
      RETURN
      END
PRESIT50
PRESIT51
PRESIT52
PRESIT53
PRESIT54
PRESIT55
PRESIT56
PRESIT57
PRESIT58
PRESIT59
PRESIT60
PRESIT61
PRESIT62
PRESIT63
PRESIT64
PRESIT65
PRESIT66
PRESIT67
PRESIT68
PRESIT69
PRESIT70
PRESIT71
PRESIT72
PRESIT73
PRESIT74
PRESIT75
PRESIT76
PRESIT77
PRESIT78
PRESIT79
PRESIT80
PRESIT81
PRESIT82
PRESIT83
PRESIT84
PRESIT85
PRESIT86
PRESIT87
PRESIT88
PRESIT89
PRESIT90
PRESIT91
PRESIT92
PRESIT93
PRESIT94
PRESIT95
PRESIT96
PRESIT97
PRESIT98
PRESIT99
PRESI100
PRESI101
PRESI102
PRESI103
PRESI104
PRESI105
PRESI106
PRESI107
PRESI108
PRESI109
PRESI110
PRESI111

```

SUBROUTINE REGRID	REGRID 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RDSOP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),STEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,AD,BO,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,DI,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIND,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C +++	REGRID 4
C +++ MOVE VERTICES AND COMPUTE RELATIVE VELOCITY BETWEEN FLUID AND GRID	REGRID 5
C +++	REGRID 6
DO 20 J=1,NYP	REGRID 7
IJ=(J-1)*NXP+1	REGRID 8
DO 10 I=1,NXP	REGRID 9
X(IJ)=X(IJ)+DT*UG(IJ)	REGRID 10
Y(IJ)=Y(IJ)+DT*VG(IJ)	REGRID 11
R(IJ)=X(IJ)*CYL+OMCYL	REGRID 12
UREL(IJ)=UG(IJ)-UL(IJ)	REGRID 13
VREL(IJ)=VG(IJ)-VL(IJ)	REGRID 14
MVP(IJ)=0.	REGRID 15
10 IJ=IJ+1	REGRID 16
20 CONTINUE	REGRID 17
RETURN	REGRID 18
END	REGRID 19

SUBROUTINE RESTEP	RESTEP 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(S90),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,DI,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFILN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C +++	RESTEP 4
C +++ CALLED WHEN PRESSURE ITERATION EITHER FAILS TO CONVERGE OR	RESTEP 5
C +++ CALCULATES A NEGATIVE VOLUME. TREATMENT IS TO HALVE DT AND	RESTEP 6
C +++ RESTART THE CYCLE, ALLOWING UP TO (LOOPMX) ATTEMPTS PER CYCLE.	RESTEP 7
C +++	RESTEP 8
DATA LOOPS,NCYOLD /0,0/	RESTEP 9
IF(INC.EQ.1) GO TO 30	RESTEP10
IF(NCYC.NE.NCYOLD) LOOPS=0	RESTEP11
NCYOLD=NCYC	RESTEP12
LOOPS=LOOPS+1	RESTEP13
DTNEW=DT*0.5	RESTEP14
IF(NUMIT.EQ.9999) GO TO 10	RESTEP15
WRITE(59,100) T,NCYC,NUMIT,DT,DTNEW	RESTEP16
WRITE(6,100) T,NCYC,NUMIT,DT,DTNEW	RESTEP17
WRITE(12,100) T,NCYC,NUMIT,DT,DTNEW	RESTEP18
GO TO 20	RESTEP19
10 WRITE(59,110) T,NCYC,DT,DTNEW	RESTEP20
WRITE(6,110) T,NCYC,DT,DTNEW	RESTEP21
WRITE(12,110) T,NCYC,DT,DTNEW	RESTEP22
20 T=T-DT	RESTEP23
DT=DTNEW	RESTEP24
NCYC=NCYC-1	RESTEP25
IF(LOOPS.LT.LOOPMX) RETURN	RESTEP26
WRITE(59,120)	RESTEP27
WRITE(6,120)	RESTEP28
WRITE(12,120)	RESTEP29
GO TO 40	RESTEP30
30 LOOPS=LOOPS+1	RESTEP31
IF(LOOPS.LT.10) RETURN	RESTEP32
WRITE(59,130)	RESTEP33
WRITE(6,130)	RESTEP34
WRITE(12,130)	RESTEP35
40 CALL FULOUT(12)	RESTEP36
CALL FULOUT(6)	RESTEP37
CALL EXITA(2)	RESTEP38
100 FORMAT(26H CONVERGENCE FAILURE AT T=,1PE12.5,4H CYC,14,7H NUMIT=,	RESTEP39
1 14/19X,7HOLD DT=,E12.5,8H NEW DT=,E12.5)	RESTEP40
110 FORMAT(22H NEGATIVE VOLUME AT T=,1PE12.5,4H CYC,	RESTEP41
1 14/15X,7HOLD DT=,E12.5,8H NEW DT=,E12.5)	RESTEP42
120 FORMAT(34H JOB ABORTED - TIMESTEP TOO SMALL.)	RESTEP43
130 FORMAT(50H JOB ABORTED - INCOMPRESSIBLE FLOW NOT CONVERGING.)	RESTEP44
END	RESTEP45

SUBROUTINE REZONE	REZONE 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDOT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIE1,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C +++	REZONE 4
C +++ COMPUTE GRID VELOCITIES UG AND VG FOR USE IN REGRID	REZONE 5
C +++ IREZ=0 IS EULERIAN, IREZ=1 IS LAGRANGIAN, IREZ=2 IS AVERAGING RE-	REZONE 6
C +++ ZONE BY RELAXATION, IREZ=3 LEFT VACANT FOR SPECIFICATION BY USER.	REZONE 7
C +++	REZONE 8
JREZ=IREZ+1	REZONE 9
GO TO (10,40,70,100),JREZ	REZONE 10
C +++	REZONE 11
C +++ EULERIAN	REZONE 12
C +++	REZONE 13
10 DO 30 J=1,NYP	REZONE 14
IJ=(J-1)*NXP+1	REZONE 15
DO 20 I=1,NXP	REZONE 16
UG(IJ)=0.	REZONE 17
VG(IJ)=0.	REZONE 18
20 IJ=IJ+1	REZONE 19
30 CONTINUE	REZONE 20
RETURN	REZONE 21
C +++	REZONE 22
C +++ LAGRANGIAN	REZONE 23
C +++	REZONE 24
40 DO 60 J=1,NYP	REZONE 25
IJ=(J-1)*NXP+1	REZONE 26
DO 50 I=1,NXP	REZONE 27
UG(IJ)=UL(IJ)	REZONE 28
VG(IJ)=VL(IJ)	REZONE 29
50 IJ=IJ+1	REZONE 30
60 CONTINUE	REZONE 31
RETURN	REZONE 32
C +++	REZONE 33
C +++ SAMPLE CONTINUOUS REZONE - RELAX ALL VERTICES EXCEPT THE 4 CORNERS	REZONE 34
C +++ TOWARD THE AVERAGE POSITION OF THE 4 OR 2 CLOSEST NEIGHBORS...	REZONE 35
C +++	REZONE 36
70 RFOOT=RF/DT	REZONE 37
DO 90 J=1,NYP	REZONE 38
IJ=(J-1)*NXP+1	REZONE 39
IJP=IJ+NXP	REZONE 40
IJM=IJ-NXP	REZONE 41
DO 80 I=1,NXP	REZONE 42
IPI=IJ+1	REZONE 43
IMJ=IJ-1	REZONE 44
IG(IJ)=UL(IJ)	REZONE 45
VG(IJ)=VL(IJ)	REZONE 46
IF(IJ.EQ.1 .OR. IJ.EQ.NXP .OR. IJ.EQ.NXP*NY+1	REZONE 47
1 .OR. IJ.EQ.NXP*NYP) GO TO 78	REZONE 48
IF(I.EQ.1 .OR. I.EQ.NXP) GO TO 72	REZONE 49

IF(J.EQ.1 .OR. J.EQ.NYP) GO TO 74	REZONE50
XN=.25*(X(IPJ)+X(IJP)+X(IMJ)+X(IJM))	REZONE51
YN=.25*(Y(IPJ)+Y(IJP)+Y(IMJ)+Y(IJM))	REZONE52
GO TO 76	REZONE53
72 XN=.5*(X(IJP)+X(IJM))	REZONE54
YN=.5*(Y(IJP)+Y(IJM))	REZONE55
GO TO 76	REZONE56
74 XN=.5*(X(IPJ)+X(IMJ))	REZONE57
YN=.5*(Y(IPJ)+Y(IMJ))	REZONE58
76 UG(IJ)=UL(IJ)+RFODT*(XN-X(IJ))	REZONE59
VG(IJ)=VL(IJ)+RFODT*(YN-Y(IJ))	REZONE60
78 IJ=IJ+1	REZONE61
IJP=IJP+1	REZONE62
80 IJM=IJM+1	REZONE63
90 CONTINUE	REZONE64
RETURN	REZONE65
C +++	REZONE66
C +++ GENERAL REZONE - ROLL-YOUR-OWN HERE . . .	REZONE67
C +++	REZONE68
100 CONTINUE	REZONE69
RETURN	REZONE70
END	REZONE71

SUBROUTINE RINPUT	RINPUT 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,DI,EPS,FXL,F1YB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
DIMENSION HOUT(42)	RINPUT 4
C +++	RINPUT 5
C +++ READ DATA DECK, COMPUTE DERIVED AND SCALAR QUANTITIES	RINPUT 6
C +++	RINPUT 7
READ(5,210) HOUT(1),NX,HOUT(2),NY,HOUT(3),IMP,HOUT(4),INC	RINPUT 8
IF(NX.EQ.0) RETURN	RINPUT 9
READ(5,210) HOUT(5),IREZ,HOUT(6),LPR	RINPUT10
READ(5,210) HOUT(7),WB,HOUT(8),WL,HOUT(9),WR,HOUT(10),WT	RINPUT11
READ(5,220) HOUT(11),DX,HOUT(12),DY,HOUT(13),CYL	RINPUT12
READ(5,220) HOUT(14),DT,HOUT(15),DTMAX,HOUT(16),TLIMD	RINPUT13
READ(5,220) HOUT(17),TWFILM,HOUT(18),TWPRTR,HOUT(19),TWFIN	RINPUT14
READ(5,220) HOUT(20),OM,HOUT(21),PEPS,HOUT(22),EPS,HOUT(23),RF	RINPUT15
READ(5,220) HOUT(24),ARTVIS,HOUT(25),LAMBDA,HOUT(26),MU	RINPUT16
READ(5,220) HOUT(27),ANC,HOUT(28),XI,HOUT(29),GX	RINPUT17
READ(5,220) HOUT(30),GY,HOUT(31),A0,HOUT(32),B0	RINPUT18
READ(5,220) HOUT(33),ASQ,HOUT(34),RON,HOUT(35),GMI	RINPUT19
READ(5,220) HOUT(36),ROI,HOUT(37),SIEI	RINPUT20
READ(5,220) HOUT(38),UIN,HOUT(39),VIN	RINPUT21
READ(5,220) HOUT(40),ROIN,HOUT(41),SIEIN,HOUT(42),PAP	RINPUT22
WRITE(12,210) HOUT(1),NX,HOUT(2),NY,HOUT(3),IMP,HOUT(4),INC	RINPUT23
WRITE(12,210) HOUT(5),IREZ,HOUT(6),LPR	RINPUT24
WRITE(12,210) HOUT(7),WB,HOUT(8),WL,HOUT(9),WR,HOUT(10),WT	RINPUT25
WRITE(12,230) HOUT(11),DX,HOUT(12),DY,HOUT(13),CYL	RINPUT26
WRITE(12,230) HOUT(14),DT,HOUT(15),DTMAX,HOUT(16),TLIMD	RINPUT27
WRITE(12,230) HOUT(17),TWFILM,HOUT(18),TWPRTR,HOUT(19),TWFIN	RINPUT28
WRITE(12,230) HOUT(20),OM,HOUT(21),PEPS,HOUT(22),EPS,HOUT(23),RF	RINPUT29
WRITE(12,230) HOUT(24),ARTVIS,HOUT(25),LAMBDA,HOUT(26),MU	RINPUT30
WRITE(12,230) HOUT(27),ANC,HOUT(28),XI,HOUT(29),GX	RINPUT31
WRITE(12,230) HOUT(30),GY,HOUT(31),A0,HOUT(32),B0	RINPUT32
WRITE(12,230) HOUT(33),ASQ,HOUT(34),RON,HOUT(35),GMI	RINPUT33
WRITE(12,230) HOUT(36),ROI,HOUT(37),SIEI	RINPUT34
WRITE(12,230) HOUT(38),UIN,HOUT(39),VIN	RINPUT35
WRITE(12,230) HOUT(40),ROIN,HOUT(41),SIEIN,HOUT(42),PAP	RINPUT36
WRITE(6,210) HOUT(1),NX,HOUT(2),NY,HOUT(3),IMP,HOUT(4),INC	RINPUT37
WRITE(6,210) HOUT(5),IREZ,HOUT(6),LPR	RINPUT38
WRITE(6,210) HOUT(7),WB,HOUT(8),WL,HOUT(9),WR,HOUT(10),WT	RINPUT39
WRITE(6,230) HOUT(11),DX,HOUT(12),DY,HOUT(13),CYL	RINPUT40
WRITE(6,230) HOUT(14),DT,HOUT(15),DTMAX,HOUT(16),TLIMD	RINPUT41
WRITE(6,230) HOUT(17),TWFILM,HOUT(18),TWPRTR,HOUT(19),TWFIN	RINPUT42
WRITE(6,230) HOUT(20),OM,HOUT(21),PEPS,HOUT(22),EPS,HOUT(23),RF	RINPUT43
WRITE(6,230) HOUT(24),ARTVIS,HOUT(25),LAMBDA,HOUT(26),MU	RINPUT44
WRITE(6,230) HOUT(27),ANC,HOUT(28),XI,HOUT(29),GX	RINPUT45
WRITE(6,230) HOUT(30),GY,HOUT(31),A0,HOUT(32),B0	RINPUT46
WRITE(6,230) HOUT(33),ASQ,HOUT(34),RON,HOUT(35),GMI	RINPUT47
WRITE(6,230) HOUT(36),ROI,HOUT(37),SIEI	RINPUT48
WRITE(6,230) HOUT(38),UIN,HOUT(39),VIN	RINPUT49

```

WRITE(6,230) HOUT(40),ROIN,HOUT(41),SIEIN,HOUT(42),PAP
OMCYL=1.-CYL
T=GRIND=DTMIN=0.
NCYC=NUMIT=IPRES=NDUMP=0
C ***
C *** ENSURE E.O.S. WILL BE CALCULATED PROPERLY FOR EXPLICIT RUNS...
C ***
      IF(IMP.EQ.0) INC=0
      DTF=0.2
      MAXIT=1000 + INC*500
      LOOPMX=6
      THIRD=1./3.
      TWLFTH=.25*THIRD
      ANCO=.25*ANC
      XICOF=.5*(1.+X1)
      COLAMU=LAMBDA+2.*MU
      DPCOF=PEPS*RO1/(2.*(1./(DX*DX)+1./(DY*DY)))
      GRFAC=1000./FLOAT(NX*NY)
      TFILM=TWFILM
      TPRTR=TWPRTR
      NYP=NY+1
      NXP=NX+1
C ***
C *** ADJUST LIMITS OF CALCULATIONAL DO-LOOPS FOR SPECIFIED INFLOW (5)
C *** OR APPLIED PRESSURE (6) BOUNDARY CONDITIONS
C ***
      IFIRST=JFIRST=IFPHI=JFPHI=1
      ILAST=ILPHI=NX
      JLAST=JLPHI=NY
      IF(WL.GE.5) IFIRST=2
      IF(WB.GE.5) JFIRST=2
      IF(WR.GE.5) ILAST=NX-1
      IF(WT.GE.5) JLAST=NY-1
C ***
C *** PHASE 1 PRESSURE GRADIENTS INCLUDE APPLIED PRESSURE BOUNDARY
C *** BUT EXCLUDE A SPECIFIED INFLOW BOUNDARY . . .
C ***
      IF(WL.EQ.5) IFPHI=2
      IF(WB.EQ.5) JFPHI=2
      IF(WR.EQ.5) ILPHI=NX-1
      IF(WT.EQ.5) JLPHI=NY-1
      ILASTV=ILAST+1
      JLASTV=JLAST+1
      ILASTM=ILAST-1
      JLASTM=JLAST-1
      IF(A0.EQ.1.0 .AND. B0.EQ.0.0) GO TO 100
      IF(WL.EQ.4 .OR. (WL.EQ.5.AND.UIN.LT.0.)) WRITE(59,240)
      IF(WB.EQ.4 .OR. (WB.EQ.5.AND.VIN.LT.0.)) WRITE(59,240)
      IF(WR.EQ.4 .OR. (WR.EQ.5.AND.UIN.GT.0.)) WRITE(59,240)
      IF(WT.EQ.4 .OR. (WT.EQ.5.AND.VIN.GT.0.)) WRITE(59,240)
100 RETURN
210 FORMAT(A10,I5)
220 FORMAT(A10,F10.5)
230 FORMAT(A10,2X,IPE12.5)
240 FORMAT(52H WARNING - OUTFLOW BOUNDARY BUT NOT FULL DONOR CELL./
1 42H ARE OUTSIDE DENSITY AND ENERGY SPECIFIED?)
      END
RINPUT50
RINPUT51
RINPUT52
RINPUT53
RINPUT54
RINPUT55
RINPUT56
RINPUT57
RINPUT58
RINPUT59
RINPUT60
RINPUT61
RINPUT62
RINPUT63
RINPUT64
RINPUT65
RINPUT66
RINPUT67
RINPUT68
RINPUT69
RINPUT70
RINPUT71
RINPUT72
RINPUT73
RINPUT74
RINPUT75
RINPUT76
RINPUT77
RINPUT78
RINPUT79
RINPUT80
RINPUT81
RINPUT82
RINPUT83
RINPUT84
RINPUT85
RINPUT86
RINPUT87
RINPUT88
RINPUT89
RINPUT90
RINPUT91
RINPUT92
RINPUT93
RINPUT94
RINPUT95
RINPUT96
RINPUT97
RINPUT98
RINPUT99
RINPUT100
RINPUT101
RINPUT102
RINPUT103
RINPUT104
RINPUT105
RINPUT106

```



```

SUBROUTINE STRESSD                                STRESSD 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800), COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800), COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800), COMD 4
3 PIYY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800), COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800), COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1 COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,80,COLAMU,CYL,C1,DPCOF, COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND, COMD 9
2 GX,GY,1DDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES, COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS, COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP, COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN, COMD 13
6 T,TFILM,THIRD,TIMLMT,TLMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR, COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP COMD 16
INTEGER WB,WL,WR,WT COMD 17
REAL LAMD STRESSD 4
C +++ STRESSD 5
C +++ THE STRESS DEVIATOR SUBROUTINE, IN WHICH WE CALCULATE THE STRESSD 6
C +++ SHEAR (MU) AND BULK (LAMBDA) VISCOSITY CONTRIBUTIONS TO UL AND VL. STRESSD 7
C +++ THE 4 STRESS TERMS ARE SAVED FOR LATER USE IN SUBR. ENERGY . . . STRESSD 8
C +++ (MATERIAL STRENGTH EFFECTS COULD BE ADDED TO SUBR. STRESSD.) STRESSD 9
C +++ STRESSD10
DT02=.5*DT STRESSD11
DO 20 J=JFIRST,JLAST STRESSD12
IJ=(J-1)*NXP+IFIRST STRESSD13
IJP=IJP+NXP STRESSD14
DO 10 I=IFIRST,ILAST STRESSD15
IPJ=IJP+1 STRESSD16
IPJP=IJP+1 STRESSD17
X1=X(IPJ) STRESSD18
R1=R(IPJ) STRESSD19
Y1=Y(IPJ) STRESSD20
U1=U(IPJ) STRESSD21
V1=V(IPJ) STRESSD22
X2=X(IPJP) STRESSD23
R2=R(IPJP) STRESSD24
Y2=Y(IPJP) STRESSD25
U2=U(IPJP) STRESSD26
V2=V(IPJP) STRESSD27
X3=X(IJP) STRESSD28
R3=R(IJP) STRESSD29
Y3=Y(IJP) STRESSD30
U3=U(IJP) STRESSD31
V3=V(IJP) STRESSD32
X4=X(IJ) STRESSD33
R4=R(IJ) STRESSD34
Y4=Y(IJ) STRESSD35
U4=U(IJ) STRESSD36
V4=V(IJ) STRESSD37
X24=X2-X4 STRESSD38
Y24=Y2-Y4 STRESSD39
X31=X3-X1 STRESSD40
Y31=Y3-Y1 STRESSD41
UOR=(U1+U2+U3+U4)*RRSUM(IJ)*CYL STRESSD42
HR13=.5*(R1+R3) STRESSD43
HR24=.5*(R2+R4) STRESSD44
DT02M1=DT02*RMV(IPJ) STRESSD45
DT02M2=DT02*RMV(IPJP) STRESSD46
DT02M3=DT02*RMV(IJP) STRESSD47
DT02M4=DT02*RMV(IJ) STRESSD48
AREA=0.5*(X24*Y31-X31*Y24) STRESSD49

```

```

AREA2=AREA*2.0
RAREA2=1./AREA2
U24=U2-U4
U31=U3-U1
V24=V2-V4
V31=V3-V1
DUDX=RAREA2*(U24*Y31-U31*Y24)
DUDY=RAREA2*(U31*X24-U24*X31)
DVDX=RAREA2*(V24*Y31-V31*Y24)
DVDY=RAREA2*(V31*X24-V24*X31)
LAMD=LAMBDA*(DUDX+DVDY+UOR)
PIXX(IJ)=2.*MU*DUDX+LAMD
PIYY(IJ)=2.*MU*DVDY+LAMD
PIXY(IJ)=MU*(DUDY+DVDX)
PITH(IJ)=CYL*(2.0*MU*UOR+LAMD)
ZZ=0.5*AREA*PITH(IJ)
XX=HR24*(PIXY(IJ)*X24-PIXX(IJ)*Y24)
UL(IPJ)=UL(IPJ)+DT02M1*(XX-ZZ)
UL(IJP)=UL(IJP)-DT02M3*(XX+ZZ)
XX=HR13*(PIXY(IJ)*X31-PIXX(IJ)*Y31)
UL(IPJP)=UL(IPJP)+DT02M2*(XX-ZZ)
UL(IJ)=UL(IJ)-DT02M4*(XX+ZZ)
XX=HR24*(PIYY(IJ)*X24-PIXY(IJ)*Y24)
VL(IPJ)=VL(IPJ)+DT02M1*XX
VL(IJP)=VL(IJP)-DT02M3*XX
XX=HR13*(PIYY(IJ)*X31-PIXY(IJ)*Y31)
VL(IPJP)=VL(IPJP)+DT02M2*XX
VL(IJ)=VL(IJ)-DT02M4*XX
IJ=IPJ
10 IJP=IPJP
20 CONTINUE
CALL BC(UL,VL)
RETURN
END

```

```

STRESS050
STRESS051
STRESS052
STRESS053
STRESS054
STRESS055
STRESS056
STRESS057
STRESS058
STRESS059
STRESS060
STRESS061
STRESS062
STRESS063
STRESS064
STRESS065
STRESS066
STRESS067
STRESS068
STRESS069
STRESS070
STRESS071
STRESS072
STRESS073
STRESS074
STRESS075
STRESS076
STRESS077
STRESS078
STRESS079
STRESS080
STRESS081
STRESS082
STRESS083

```

	SUBROUTINE TAPERD	TAPERD 2
	COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
	1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
	2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
	3 PIXY(800),PIYY(800),PITH(800),ROSDP(800),UG(800),VG(800),	COMD 5
	4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
	5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
	COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,AD,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
	1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
	2 GX,GY,IOOT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
	3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
	4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
	5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
	6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
	7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,XICOF,XL,YB,YCONV,ZZ	COMD 15
	REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
	INTEGER WB,WL,WR,WT	COMD 17
C ***		TAPERD 4
C ***	RESTART PROBLEM FROM A TAPE DUMP	TAPERD 5
C ***		TAPERD 6
	NTD=NY	TAPERD 7
	NWCOMD=LOC(ZZ)-LOC(AA)+1	TAPERD 8
	READ(7) (AA(N),N=1,NWCOMD)	TAPERD 9
	IF(NTD.NE.NDUMP) GO TO 10	TAPERD10
	WRITE(6,100) NDUMP,T,NCYC	TAPERD11
	WRITE(59,100) NDUMP,T,NCYC	TAPERD12
	WRITE(12,100) NDUMP,T,NCYC	TAPERD13
	NDUMP=NDUMP+1	TAPERD14
	CALL GETJTL(TIMLMT)	TAPERD15
	RETURN	TAPERD16
10	WRITE(6,110) NDUMP,NTD	TAPERD17
	WRITE(59,110) NDUMP,NTD	TAPERD18
	WRITE(12,110) NDUMP,NTD	TAPERD19
	CALL EXITA(4)	TAPERD20
100	FORMAT(20H RESTARTING FROM TD,13,3H T=,1PE12.5,6H CYCLE,15)	TAPERD21
110	FORMAT(20H WRONG DUMP NUMBER -,216)	TAPERD22
	END	TAPERD23

SUBROUTINE TAPEWR	TAPEWR 2
COMMON /SC1/ .A(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),ROSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZI	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FIXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
DATA NDUMP/0/	TAPEWR 4
C ***	TAPEWR 5
C *** WRITE A DUMP TAPE AND EXIT	TAPEWR 6
C ***	TAPEWR 7
NWCMD=LOC(ZZ)-LOC(AA)+1	TAPEWR 8
WRITE(8) (AA(N), N=1, NWCMD)	TAPEWR 9
WRITE(6, 100) NDUMP, T, NCYC	TAPEWR 10
WRITE(59, 100) NDUMP, T, NCYC	TAPEWR 11
WRITE(12, 100) NDUMP, T, NCYC	TAPEWR 12
CALL EXITA(3)	TAPEWR 13
100 FORMAT(11H TAPE DUMP, 13, 6H AT T=, 1PE12.5, 6H CYCLE, 15)	TAPEWR 14
END	TAPEWR 15

	SUBROUTINE TIMSTP	TIMSTP 2
	COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
	1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
	2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
	3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
	4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
	5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
	COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,AO,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
	1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
	2 GX,GY,IDDT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
	3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,UNM,LAMBDA,LOOPS,	COMD 11
	4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
	5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
	6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD 14
	7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
	REAL LAMBDA,MC,MP,MU,MVP	COMD 16
	INTEGER WB,WL,WR,WT	COMD 17
C ***		TIMSTP 4
C ***	COMPUTE THE NEW TIME STEP, DT	TIMSTP 5
C ***		TIMSTP 6
	DTCON=DTVIS=1.E+20	TIMSTP 7
	UTMAX=-1.E+20	TIMSTP 8
	DO 40 J=1,NY	TIMSTP 9
	IJ=(J-1)*NXP+1	TIMSTP10
	IJP=IJ+NXP	TIMSTP11
	DO 30 I=1,NX	TIMSTP12
	IPI=IJ+I	TIMSTP13
	DX1=(X(IPI)-X(IJ))**2	TIMSTP14
	DY1=(Y(IPI)-Y(IJ))**2	TIMSTP15
	DX3=(X(IPI)-X(IJ))**2	TIMSTP16
	DY3=(Y(IPI)-Y(IJ))**2	TIMSTP17
	RD1=1./(DX1+DY1)	TIMSTP18
	RD3=1./(DX3+DY3)	TIMSTP19
C ***		TIMSTP20
C ***	IF SALE IS RUN IN THE LAGRANGIAN MODE (IREZ=1), THERE IS NO	TIMSTP21
C ***	STABILITY LIMIT DUE TO CONVECTION. NONETHELESS, DT SHOULD BE	TIMSTP22
C ***	LIMITED AS FOLLOWS FOR REASONS OF ACCURACY AND TO ENSURE	TIMSTP23
C ***	POSITIVE CELL VOLUMES AT THE END OF PHASE 1 . . .	TIMSTP24
C ***		TIMSTP25
	UV14=(U(IPI)-U(IJ))**2+(V(IPI)-V(IJ))**2	TIMSTP26
	CMAX=SQRT(AMAX1(UV14*RD1,UV14*RD3))	TIMSTP27
	UTMAX=AMAX1(UTMAX,CMAX)	TIMSTP28
	IF (IREZ.EQ.1) GO TO 10	TIMSTP29
	UVR4=UREL(IJ)**2+VREL(IJ)**2	TIMSTP30
	CMAX=SQRT(AMAX1(UVR4*RD1,UVR4*RD3))	TIMSTP31
	UTMAX=AMAX1(UTMAX,CMAX)	TIMSTP32
	10 IF (COLAMU.EQ.0.) GO TO 20	TIMSTP33
	XY1=DX1+DY1	TIMSTP34
	XY3=DX3+DY3	TIMSTP35
C ***		TIMSTP36
C ***	BYPASS CELLS W/ RO=0, E.G. SPECIAL BOUNDARIES OR OBSTACLES . . .	TIMSTP37
C ***		TIMSTP38
	IF (RO(IJ).EQ.0.) GO TO 20	TIMSTP39
	DTVIS=AMIN (DTVIS,RO(IJ)*XY1*XY3/(XY1+XY3))	TIMSTP40
	20 IJ=IPI	TIMSTP41
	30 IJP=IPI+1	TIMSTP42
	40 CONTINUE	TIMSTP43
	DTGROW=.05*DT	TIMSTP44
	IF (NCYC.EQ.0) DTGROW=DT	TIMSTP45
	IF (UTMAX.NE.0.) DTCON=DTF/UTMAX	TIMSTP46
	IF (COLAMU.NE.0.) DTVIS=.5*DTVIS/COLAMU	TIMSTP47
	DT=AMINI (DTGROW,DTCON,DTVIS,DTMAX)	TIMSTP48
	IF (DT.EQ.DTGROW) IDDT=1HG	TIMSTP49

IF (DT.EQ.DTCON) IDOT=IHC	TIMSTP50
IF (DT.EQ.DTVIS) IDOT=IHW	TIMSTP51
IF (DT.EQ.DTMAX) IDOT=IHM	TIMSTP52
IF (NCYC.EQ.1) DTMIN=DT*1.E-10	TIMSTP53
IF (DT.GT.DTMIN) RETURN	TIMSTP54
WRITE (6,100) DT,NCYC,IDOT	TIMSTP55
WRITE (59,100) DT,NCYC,IDOT	TIMSTP56
WRITE (12,100) DT,NCYC,IDOT	TIMSTP57
CALL EXITA(6)	TIMSTP58
100 FORMAT(4H DT=,1PE12.5,9H AT CYCLE,15,11H, CAUSE IS ,A1)	TIMSTP59
END	TIMSTP60

SUBROUTINE ULTOU	ULTOU 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXY(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RSDP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),IMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GM1,GRFAC,GRIND,	CCMD 9
2 GX,GY,IDOT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFFH1,JLAST,JLASTM,JLASTV,JLPH1,JNM,LAMBDA,LOOPS,	COMD 11
4 LOGPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C ***	ULTOU 4
C *** LAGRANGIAN CALCULATIONS BYPASS ALL CONVECTIVE FLUXING, THUS THE	ULTOU 5
C *** LAGRANGIAN VELOCITIES ARE THE FINAL VELOCITIES FOR THE CYCLE	ULTOU 6
C *** AND NEED TO BE TRANSFERRED TO THE N-TIME ARRAY.	ULTOU 7
C ***	ULTOU 8
DO 20 J=JFIRST,JLASTV	ULTOU 9
IJ=(J-1)*NXP+IFIRST	ULTOU 10
DO 10 I=IFIRST,ILASTV	ULTOU 11
U(IJ)=UL(IJ)	ULTOU 12
V(IJ)=VL(IJ)	ULTOU 13
10 IJ=IJ+1	ULTOU 14
20 CONTINUE	ULTOU 15
RETURN	ULTOU 16
END	ULTOU 17

SUBROUTINE VELPLT	VELPLT 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RDSOP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIID,	COMD 9
2 GX,GY,I0DT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLIMD,TPRTR,TWFLM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,X1COF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVF	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C ***	VELPLT 4
C *** THE VELOCITY VECTOR PLOT. (CALLED FROM SUBR. FUELOUT)	VELPLT 5
C ***	VELPLT 6
IF(VMAX.EQ.0) GO TO 30	VELPLT 7
CALL ADV(1)	VELPLT 8
DO 20 J=1,NYP	VELPLT 9
IJ=(J-1)*NXP+1	VELPLT 10
DO 10 I=1,NXP	VELPLT 11
IX1=FXL+(X(IJ)-XL)*XCONV	VELPLT 12
IY1=FIYB-(Y(IJ)-YB)*YCONV	VELPLT 13
IX2=FXL+(X(IJ)+U(IJ)*DROU-XL)*YCONV	VELPLT 14
IY2=FIYB-(Y(IJ)+V(IJ)*DROU-YB)*YCONV	VELPLT 15
IF(IY2.GE.1) GO TO 5	VELPLT 16
IF(IY1.EQ.IY2) GO TO 5	VELPLT 17
IX2=IX1+(IX2-IX1)*(IY1-1)/(IY1-IY2)	VELPLT 18
IY2=1	VELPLT 19
5 CALL DRV(IX1,IY1,IX2,IY2)	VELPLT 20
CALL PLT(IX1,IY1,16)	VELPLT 21
10 IJ=IJ+1	VELPLT 22
20 CONTINUE	VELPLT 23
CALL LINCNT(60)	VELPLT 24
WRITE(12,100) JNM,D1,C1,NAME,T,NCYC,VMAX	VELPLT 25
30 CONTINUE	VELPLT 26
RETURN	VELPLT 27
100 FORMAT(2X,A10,2(2X,A8),2X,8A10/40X,3H T=,1PE12.5,6H CYCLE,15,	VELPLT 28
1 6H VMAX=,E12.5)	VELPLT 29
END	VELPLT 30

SUBROUTINE VINIT	VINIT 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),O(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIXY(800),PIYY(800),PITH(800),RDSOP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZI	COMD 7
COMMON /SC2/ ANG,ANCO,ARTVIS,ASQ,A0,RO,COLAMU,CYL,C1,OPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IOOT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPMX,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,ROI,ROIN,RON,SIEI,SIEIN,	COMD 13
6 T,TEILM,THIRD,TIMLMT,TLIND,TPRTR,TWILM,TWIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,XI,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C ***	VINIT 4
C *** INITIALIZE RO, P, PL, U, V, X AND Y TO BEGIN THE CYCLE.	VINIT 5
C *** MAINTAIN PAP AT APPROPRIATE PRESSURE BOUND, IF USED	VINIT 6
C ***	VINIT 7
11 J=1	VINIT 8
12 NX	VINIT 9
13 NY	VINIT 10
IF (WB.EQ.0) 11,2	VINIT 11
IF (WR.EQ.0) 11,2	VINIT 12
IF (WL.EQ.0) 12,12,1	VINIT 13
IF (WT.EQ.0) 12,12,1	VINIT 14
DO 20 J=1,NP	VINIT 15
IJ=(J-1)*NXP+1	VINIT 16
DO 10 I=1,12	VINIT 17
RO(IJ)=MC(IJ)/VOL(IJ)	VINIT 18
C ***	VINIT 19
C *** E.O.S. IS BYPASSED FOR IMPLICIT CALCULATIONS, BECAUSE PL FROM THE	VINIT 20
C *** PREVIOUS CYCLE IS PROBABLY THE BEST GUESS FOR THE NEXT CYCLE.	VINIT 21
C ***	VINIT 22
IF (IMP.EQ.0) CALL EOSIP(IJ),RO(IJ),SIE(IJ),0.,0.)	VINIT 23
10 IJ=IJ+1	VINIT 24
20 CONTINUE	VINIT 25
PMAX=0.	VINIT 26
DO 40 J=1,NYP	VINIT 27
IJ=(J-1)*NXP+1	VINIT 28
DO 30 I=1,NXP	VINIT 29
ROL(IJ)=RO(IJ)	VINIT 30
PL(IJ)=P(IJ)	VINIT 31
PMAX=AMAX1(PMAX,ABS(P(IJ)))	VINIT 32
UL(IJ)=U(IJ)	VINIT 33
VL(IJ)=V(IJ)	VINIT 34
30 IJ=IJ+1	VINIT 35
40 CONTINUE	VINIT 36
RETURN	VINIT 37
END	VINIT 38

SUBROUTINE VOLUME	VOLUME 2
COMMON /SC1/ AA(1),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MV(800),RMV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 VL(800),ROL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIYY(800),PIYY(800),PITH(800),RDSOP(800),UG(800),VG(800),	COMD 5
4 UREL(800),VREL(800),MP(800),MVP(800),SIEP(800),UMOM(800),	COMD 6
5 VMOM(800),UMOMP(800),VMOMP(800),ZZ1	COMD 7
COMMON /SC2/ ANC,ANCO,ARTVIS,ASQ,A0,B0,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DROU,DT,DTF,DTMAX,DTMIN,DX,DY,D1,EPS,FIXL,FIYB,GMI,GRFAC,GRIND,	COMD 9
2 GX,GY,IDOT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IREZ,JFIRST,JFPHI,JLAST,JLASTM,JLASTV,JLPHI,JNM,LAMBDA,LOOPS,	COMD 11
4 LOOPM,LPR,MAXIT,MU,NAME(8),NCYC,NDUMP,NUMIT,NX,NXP,	COMD 12
5 NY,NYP,OM,OMCYL,PAP,PEPS,PMAX,RF,RO',ROIN,RON,SIE1,SIE1N,	COMD 13
6 T,TFILM,THIRD,TIMLMT,TLMD,TPRTR,TWFILM,TWFIN,TWLFTH,TWPRTR,	COMD 14
7 UIN,VIN,VMAX,WB,WL,WR,WT,XCONV,X1,XICOF,XL,YB,YCONV,ZZ	COMD 15
REAL LAMBDA,MC,MP,MU,MV,MVP	COMD 16
INTEGER WB,WL,WR,WT	COMD 17
C ***	VOLUME 4
C *** CALCULATE VOLUMES OF ALL CELLS IN THE MESH, USING PAPPAS THEOREM	VOLUME 5
C ***	VOLUME 6
DO 20 J=1,NY	VOLUME 7
IJ=(J-1)*NXP+1	VOLUME 8
IJP=IJ+NXP	VOLUME 9
DO 10 I=1,NX	VOLUME 10
IPJ=IJ+1	VOLUME 11
IPJP=IPJ+1	VOLUME 12
X1=X(IPJ)	VOLUME 13
Y1=Y(IPJ)	VOLUME 14
R1=R(IPJ)	VOLUME 15
X2=X(IPJP)	VOLUME 16
Y2=Y(IPJP)	VOLUME 17
R2=R(IPJP)	VOLUME 18
X3=X(IJP)	VOLUME 19
Y3=Y(IJP)	VOLUME 20
R3=R(IJP)	VOLUME 21
X4=X(IJ)	VOLUME 22
Y4=Y(IJ)	VOLUME 23
R4=R(IJ)	VOLUME 24
ATR=.5*((X3-X2)*(Y1-Y2)-(X1-X2)*(Y3-Y2))	VOLUME 25
ABL=.5*((X1-X4)*(Y3-Y4)-(X3-X4)*(Y1-Y4))	VOLUME 26
VOL(IJ)=THIRD*((R1+R2+R3)*ATR+(R3+R4+R1)*ABL)	VOLUME 27
IJ=IPJ	VOLUME 28
10 IJP=IPJP	VOLUME 29
20 CONTINUE	VOLUME 30
RETURN	VOLUME 31
END	VOLUME 32

SUBROUTINE ZONPLT	ZONPLT 2
COMMON /ZSC1/ AA(11),X(800),R(800),Y(800),U(800),V(800),MC(800),	COMD 2
1 MZ(800),RPTV(800),RO(800),VOL(800),P(800),SIE(800),UL(800),	COMD 3
2 X(800),POL(800),PL(800),D(800),Q(800),RRSUM(800),PIXX(800),	COMD 4
3 PIYY(800),PIYI(800),PITH(800),RDSOP(800),UG(800),VG(800),	COMD 5
4 UPEL(800),VPEL(800),MPE(800),MVP(800),STEP(800),UMDM(800),	COMD 6
5 VMUM(800),VMUMP(800),VMOMP(800),ZZI	COMD 7
COMMON /ZSC2/ ANIC,ANCO,ARTVIS,ASQ,AO,BO,COLAMU,CYL,C1,DPCOF,	COMD 8
1 DPROU,DT,DTE,DTMAX,DTMIN,DX,DY,DI,EPS,FXL,FIYB,GM,GRFAC,GRIND,	COMD 9
2 GX,GY,IGOUT,IFIRST,IFPHI,ILAST,ILASTM,ILASTV,ILPHI,IMP,INC,IPRES,	COMD 10
3 IPEZ, JFIRST, JEPHI, JLAST, JLASTM, JLASTV, JLPHI, JNM, LAMBDA, LLOOPS,	COMD 11
4 LOPMAX, LPR, MAXIT, MU, NAME(8), NCYC, NDUMP, NUMIT, NX, NXP,	COMD 12
5 NY, NYP, OM, OMCYL, PAP, PEPS, PMAX, RE, ROI, ROIN, RON, SIEI, SIEIN,	COMD 13
6 T, TFLM, THIRD, TIMEMT, TIMEO, TPRTR, TWFLM, TWFIN, TWLTH, TWPTR,	COMD 14
7 UIN, VIN, VMAX, WB, WL, WR, WT, XCONV, XI, XICOF, XL, YB, YCONV, ZZ	COMD 15
REAL LAMBDA, MC, MP, MU, MV, MVP	COMD 16
INTEGER WB, WL, WR, WT	COMD 17
C ***	ZONPLT 4
C *** THE ZONE PLOT (CALLED) FROM SUBR FULOUT)	ZONPLT 5
C ***	ZONPLT 6
IF (IPEZ.EQ.0) .AND. NCYC.GT.0) RETURN	ZONPLT 7
CALL ADV(1)	ZONPLT 8
DO 20 J=1,NY	ZONPLT 9
IJ=(J-1)*NXP+1	ZONPLT 10
IJP=IJ+NXP	ZONPLT 11
DO 10 I=1,NX	ZONPLT 12
IPJ=IJ+I	ZONPLT 13
IPJP=IJP+I	ZONPLT 14
IX1=FXL*(X(IPJ)-XL)*XCONV	ZONPLT 15
IX2=FXL*(X(IPJP)-XL)*XCONV	ZONPLT 16
IX3=FXL*(X(IJ)-XL)*XCONV	ZONPLT 17
IX4=FXL*(X(IJ)-XL)*XCONV	ZONPLT 18
IY1=FIYB*(Y(IPJ)-YB)*YCONV	ZONPLT 19
IY2=FIYB*(Y(IPJP)-YB)*YCONV	ZONPLT 20
IY3=FIYB*(Y(IJ)-YB)*YCONV	ZONPLT 21
IY4=FIYB*(Y(IJ)-YB)*YCONV	ZONPLT 22
CALL DRV(IX4,IY4,IX3,IY3)	ZONPLT 23
CALL DRV(IX4,IY4,IX1,IY1)	ZONPLT 24
IF (I.EQ.NX) CALL DRV(IX1,IY1,IX2,IY2)	ZONPLT 25
IF (J.EQ.NY) CALL DRV(IX2,IY2,IX3,IY3)	ZONPLT 26
IJP=IPJP	ZONPLT 27
10 IJ=IPJ	ZONPLT 28
20 CONTINUE	ZONPLT 29
CALL LINCNT(60)	ZONPLT 30
WRITE(12,100) JNM,D1,C1,NAME,T,MCYC	ZONPLT 31
RETURN	ZONPLT 32
100 FORMAT(2X,A10,2(2X,A8),2X,8A10/40X,3H T=,1PE12.5,6H CYCLE,15)	ZONPLT 33
END	ZONPLT 34

APPENDIX B

SYSTEM SUBROUTINE CALLS IN SALE

SALE calls a number of system subroutines to display graphic or numeric information on microfiche. The original microfilm recording CRT device at LASL was the SC 4020, and although it has been supplanted, the coordinate system in the particular software system we are using is that of the SC 4020. The CRT face has a matrix of 1024×1024 raster points, where (0,0) is the coordinate of the upper left corner and (1023,1023) that of the lower right corner. Because this coordinate system is different from that of **SALE**, our code must convert physical mesh coordinates to locate their positions on the 4020 frame. This scaling process is performed in **SALE** subroutine **FULOUT**. Numerical information is displayed in the typing mode, in which the film frame consists of 64 lines of 128 characters each. The system subroutines called by **SALE** are:

CALL ADV (nf) advances the film by nf frames.

CALL PLOT (IX,IY,ch) plots the 4020 character identified by ch at frame coordinates (IX,IY).

CALL DRV (IX1,IY1,IX2,IY2) draws a straight line vector segment connecting the 4020 points (IX1,IY1) and (IX2,IY2).

CALL LINCNT (LN) locates the first column of line LN. Accessible lines range between 2 and 61. Frame advancement is automatic.

In addition to the above calls that are used continuously during program execution, initialization of the film file at the beginning of the run is handled by calls to **GFR80**, **GRPHLUN**, **LIB4020**, **GRPHFTN** and **SETFLSH**. These communicate with the graphics system at LASL and need not concern the outside user.

Other system calls not related to film usage appear in **SALE**:

CALL GETJTL (TL) returns the job CPU time limit in seconds.

CALL DATEH(D1) returns the date as a Hollerith constant of the form MM/DD/YY.

CALL TIMEH(T1) returns the wall clock time as a Hollerith constant of the form HH:MM:SS.

CALL SECOND(time) returns the CPU time used by the job up to this point.

CALL EXITA(n) terminates the code. Each call to **EXITA** in **SALE** has a different value for n, which is retained by the operating system and available for determining the cause of the exit, if necessary.

APPENDIX C

SAMPLE OUTPUT FROM BROKEN DAM CALCULATION

The broken dam calculation described in Sec. IV.A is chosen as a sample calculation for aiding in code verification at other installations. It is solved using the SALE program exactly as listed in App. A and the input file listed in Sec. IV.A.

The frames on the following pages provide the cell data as created at time $t = 0$, again after one cycle ($t = 0.1$), and again much later at cycle 71 ($t = 5.0$). Also

provided are two neighboring frames showing system totals of mass, momentum, and energy, and a sampling of cycle-by-cycle monitor prints of iteration number, grind time, and time step history.

Exact agreement with our calculated values may be impossible to attain because of different word lengths on other computers and differences in various FORTRAN compilers.

REPORT SALE 04/06/79 14 28 13 T3AAA SLUMP, PURE LAGRANDIAN W/ INC=1. ASQ=100 040879-3
 T= 0 CYCLE 0

I	J	#	Y	U	V	SIE	RHO	MASS	VOL	P
1	0	0	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
2	1	1.000E+00	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
3	1	2.000E+00	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
4	1	3.000E+00	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
5	1	4.000E+00	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
6	1	5.000E+00	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
7	1	6.000E+00	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
8	1	7.000E+00	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
9	1	8.000E+00	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
10	1	9.000E+00	0	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
11	1	1.000E+01	0	0	0	0	0	0	0	0
1	2	0	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
2	2	1.000E+00	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
3	2	2.000E+00	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
4	2	3.000E+00	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
5	2	4.000E+00	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
6	2	5.000E+00	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
7	2	6.000E+00	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
8	2	7.000E+00	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
9	2	8.000E+00	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
10	2	9.000E+00	1.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
11	2	1.000E+01	1.000E+00	0	0	0	0	0	0	0
1	3	0	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
2	3	1.000E+00	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
3	3	2.000E+00	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
4	3	3.000E+00	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
5	3	4.000E+00	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
6	3	5.000E+00	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
7	3	6.000E+00	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
8	3	7.000E+00	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
9	3	8.000E+00	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
10	3	9.000E+00	2.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
11	3	1.000E+01	2.000E+00	0	0	0	0	0	0	0
1	4	0	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
2	4	1.000E+00	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
3	4	2.000E+00	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
4	4	3.000E+00	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
5	4	4.000E+00	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
6	4	5.000E+00	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
7	4	6.000E+00	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
8	4	7.000E+00	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
9	4	8.000E+00	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
10	4	9.000E+00	3.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
11	4	1.000E+01	3.000E+00	0	0	0	0	0	0	0
1	5	0	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
2	5	1.000E+00	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
3	5	2.000E+00	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
4	5	3.000E+00	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
5	5	4.000E+00	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
6	5	5.000E+00	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
7	5	6.000E+00	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
8	5	7.000E+00	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
9	5	8.000E+00	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
10	5	9.000E+00	4.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0
11	5	1.000E+01	4.000E+00	0	0	0	0	0	0	0
1	6	0	5.000E+00	0	0	0	1.000E+00	1.000E+00	1.000E+00	0

EXPORT SALE ON 06-79 IN PB 13 T3AAA SLUMP, PURE LAGRANDIAN M/ INC-1, ASD-100 040679 3
 T= 0 CYCLE 0

I	J	K	Y	U	V	SIE	RHO	MASS	VOL	P
2	6	1	0.000E+00	5.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
3	6	2	0.000E+00	5.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
4	6	3	0.000E+00	5.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
5	6	4	0.000E+00	5.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
6	6	5	0.000E+00	5.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
7	6	6	0.000E+00	5.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
8	6	7	0.000E+00	5.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
9	6	8	0.000E+00	5.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
10	6	9	0.000E+00	5.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
11	6	1	0.000E+01	5.000E+00	0	0	0.	0.	0.	0.
1	7	0	6.000E+00	0.	0	0	1.000E+00	1.000E+00	1.000E+00	0
2	7	1	0.000E+00	6.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
3	7	2	0.000E+00	6.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
4	7	3	0.000E+00	6.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
5	7	4	0.000E+00	6.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
6	7	5	0.000E+00	6.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
7	7	6	0.000E+00	6.000E+00	0	0	1.000E+00	1.000E+00	1.000E+00	0
8	7	7	0.000E+00	6.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
9	7	8	0.000E+00	6.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
10	7	9	0.000E+00	6.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
11	7	1	0.000E+01	6.000E+00	0.	0.	0.	0.	0.	0.
1	8	0	7.000E+00	0.	0	0	1.000E+00	1.000E+00	1.000E+00	0
2	8	1	0.000E+00	7.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
3	8	2	0.000E+00	7.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
4	8	3	0.000E+00	7.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
5	8	4	0.000E+00	7.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
6	8	5	0.000E+00	7.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
7	8	6	0.000E+00	7.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
8	8	7	0.000E+00	7.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
9	8	8	0.000E+00	7.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
10	8	9	0.000E+00	7.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
11	8	1	0.000E+01	7.000E+00	0.	0.	0.	0.	0.	0.
1	9	0	8.000E+00	0.	0	0	1.000E+00	1.000E+00	1.000E+00	0
2	9	1	0.000E+00	8.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
3	9	2	0.000E+00	8.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
4	9	3	0.000E+00	8.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
5	9	4	0.000E+00	8.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
6	9	5	0.000E+00	8.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
7	9	6	0.000E+00	8.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
8	9	7	0.000E+00	8.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
9	9	8	0.000E+00	8.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
10	9	9	0.000E+00	8.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
11	9	1	0.000E+01	8.000E+00	0.	0.	0.	0.	0.	0.
1	10	0	9.000E+00	0.	0	0	1.000E+00	1.000E+00	1.000E+00	0
2	10	1	0.000E+00	9.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
3	10	2	0.000E+00	9.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
4	10	3	0.000E+00	9.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
5	10	4	0.000E+00	9.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
6	10	5	0.000E+00	9.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
7	10	6	0.000E+00	9.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
8	10	7	0.000E+00	9.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
9	10	8	0.000E+00	9.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
10	10	9	0.000E+00	9.000E+00	0.	0.	1.000E+00	1.000E+00	1.000E+00	0
11	10	1	0.000E+01	9.000E+00	0.	0.	0.	0.	0.	0.
1	11	0	1.000E+01	0.	0	0	0.	0.	0.	0.
2	11	1	0.000E+00	1.000E+01	0.	0.	0.	0.	0.	0.

KPORT-SALE 04/06/79 14:28:13 T3AAA SLUMP, PURE LAGRANGIAN W/ INC=1, ASO=100 D=0579-3
T= 0. CYCLE 0

I	J	X	Y	U	V	SIE	RHO	MASS	VOL	F
3	11	2.000E+00	1.000E+01	0.	0.	0.	0.	0.	0.	0.
4	11	3.000E+00	1.000E+01	0.	0.	0.	0.	0.	0.	0.
5	11	4.000E+00	1.000E+01	0.	0.	0.	0.	0.	0.	0.
6	11	5.000E+00	1.000E+01	0.	0.	0.	0.	0.	0.	0.
7	11	6.000E+00	1.000E+01	0.	0.	0.	0.	0.	0.	0.
8	11	7.000E+00	1.000E+01	0.	0.	0.	0.	0.	0.	0.
9	11	8.000E+00	1.000E+01	0.	0.	0.	0.	0.	0.	0.
10	11	9.000E+00	1.000E+01	0.	0.	0.	0.	0.	0.	0.
11	11	1.000E+01	1.000E+01	0.	0.	0.	0.	0.	0.	0.

XPORT-SALE 04/08/79 14:28.13 T3AAA SLUMP, PURE LAORANGIAN W/ INC=1, ASQ=100 040879-3
 T= 1.00000E-01 CYCLE I

I	J	X	Y	U	V	SIE	RHO	MASS	VOL	P
1	1	0.	0.	0.	0.	8.303E-05	1.000E+00	1.000E+00	1.000E+00	6.268E+00
2	1	1.001E+00	0.	8.178E-03	0.	5.038E-05	1.000E+00	1.000E+00	1.000E+00	6.188E+00
3	1	2.002E+00	0.	1.673E-02	0.	4.463E-05	1.000E+00	1.000E+00	1.000E+00	6.020E+00
4	1	3.003E+00	0.	2.569E-02	0.	3.761E-05	1.000E+00	1.000E+00	1.000E+00	5.761E+00
5	1	4.004E+00	0.	3.603E-02	0.	2.958E-05	1.000E+00	1.000E+00	1.000E+00	5.401E+00
6	1	5.005E+00	0.	4.769E-02	0.	2.072E-05	1.000E+00	1.000E+00	1.000E+00	4.924E+00
7	1	6.006E+00	0.	6.160E-02	0.	1.122E-05	1.000E+00	1.000E+00	1.000E+00	4.308E+00
8	1	7.007E+00	0.	7.926E-02	0.	1.033E-06	1.000E+00	1.000E+00	1.000E+00	3.515E+00
9	1	8.010E+00	0.	1.030E-01	0.	-1.295E-05	1.000E+00	1.000E+00	1.000E+00	2.485E+00
10	1	9.014E+00	0.	1.438E-01	0.	-1.441E-05	1.000E+00	1.000E+00	1.000E+00	1.074E+00
11	1	1.002E+01	0.	2.095E-01	0.	0.	0.	0.	0.	0.
1	2	0.	9.992E-01	0.	-8.311E-03	3.502E-05	1.000E+00	1.000E+00	1.000E+00	5.352E+00
2	2	1.001E+00	9.992E-01	8.048E-03	-8.442E-03	1.088E-05	1.000E+00	1.000E+00	1.000E+00	5.273E+00
3	2	2.002E+00	9.991E-01	1.844E-02	-8.850E-03	9.257E-06	1.000E+00	1.000E+00	1.000E+00	5.111E+00
4	2	3.003E+00	9.990E-01	2.944E-02	-9.985E-03	7.338E-06	1.000E+00	1.000E+00	1.000E+00	4.862E+00
5	2	4.004E+00	9.989E-01	3.935E-02	-1.073E-02	5.022E-06	1.000E+00	1.000E+00	1.000E+00	4.519E+00
6	2	5.005E+00	9.988E-01	4.809E-02	-1.242E-02	2.304E-06	1.000E+00	1.000E+00	1.000E+00	4.086E+00
7	2	6.006E+00	9.985E-01	6.008E-02	-1.504E-02	-5.988E-07	1.000E+00	1.000E+00	1.000E+00	3.474E+00
8	2	7.007E+00	9.981E-01	7.899E-02	-1.927E-02	-4.089E-06	1.000E+00	1.000E+00	1.000E+00	2.739E+00
9	2	8.010E+00	9.974E-01	9.894E-02	-2.844E-02	-7.588E-06	1.000E+00	1.000E+00	1.000E+00	1.794E+00
10	2	9.013E+00	9.975E-01	1.298E-01	-4.511E-02	-3.848E-06	1.000E+00	1.000E+00	1.000E+00	6.404E-01
11	2	1.002E+01	9.974E-01	1.888E-01	-5.930E-02	0.	0.	0.	0.	0.
1	3	0.	1.998E+00	0.	-1.823E-02	2.674E-05	1.000E+00	1.000E+00	1.000E+00	4.519E+00
2	3	1.001E+00	1.998E+00	7.862E-03	-1.849E-02	8.114E-06	1.000E+00	1.000E+00	1.000E+00	4.441E+00
3	3	2.002E+00	1.998E+00	1.504E-02	-1.728E-02	6.823E-06	1.000E+00	1.000E+00	1.000E+00	4.290E+00
4	3	3.002E+00	1.998E+00	2.411E-02	-1.888E-02	5.438E-06	1.000E+00	1.000E+00	1.000E+00	4.057E+00
5	3	4.003E+00	1.998E+00	3.338E-02	-2.089E-02	3.710E-06	1.000E+00	1.000E+00	1.000E+00	3.737E+00
6	3	5.004E+00	1.998E+00	4.373E-02	-2.404E-02	1.808E-06	1.000E+00	1.000E+00	1.000E+00	3.318E+00
7	3	6.005E+00	1.997E+00	5.564E-02	-2.880E-02	-1.818E-07	1.000E+00	1.000E+00	1.000E+00	2.791E+00
8	3	7.007E+00	1.995E+00	6.958E-02	-3.588E-02	-2.079E-06	1.000E+00	1.000E+00	1.000E+00	2.138E+00
9	3	8.009E+00	1.995E+00	8.818E-02	-4.820E-02	-2.888E-06	1.000E+00	1.000E+00	1.000E+00	1.393E+00
10	3	9.010E+00	1.993E+00	1.017E-01	-6.978E-02	-7.244E-07	1.000E+00	1.000E+00	1.000E+00	4.747E-01
11	3	1.001E+01	1.992E+00	1.119E-01	-8.343E-02	0.	0.	0.	0.	0.
1	4	0.	2.998E+00	0.	-2.384E-02	1.887E-05	1.000E+00	1.000E+00	1.000E+00	3.751E+00
2	4	1.001E+00	2.998E+00	7.050E-03	-2.401E-02	5.838E-06	1.000E+00	1.000E+00	1.000E+00	3.684E+00
3	4	2.001E+00	2.997E+00	1.438E-02	-2.512E-02	4.967E-06	1.000E+00	1.000E+00	1.000E+00	3.548E+00
4	4	3.002E+00	2.997E+00	2.205E-02	-2.708E-02	3.892E-06	1.000E+00	1.000E+00	1.000E+00	3.394E+00
5	4	4.003E+00	2.997E+00	3.030E-02	-3.002E-02	2.888E-06	1.000E+00	1.000E+00	1.000E+00	3.094E+00
6	4	5.004E+00	2.997E+00	3.932E-02	-3.429E-02	1.388E-06	1.000E+00	1.000E+00	1.000E+00	2.688E+00
7	4	6.005E+00	2.996E+00	4.921E-02	-4.037E-02	1.083E-07	1.000E+00	1.000E+00	1.000E+00	2.230E+00
8	4	7.006E+00	2.995E+00	6.001E-02	-4.917E-02	-8.343E-07	1.000E+00	1.000E+00	1.000E+00	1.682E+00
9	4	8.007E+00	2.994E+00	7.058E-02	-6.212E-02	-1.058E-06	1.000E+00	1.000E+00	1.000E+00	1.053E+00
10	4	9.008E+00	2.992E+00	7.858E-02	-7.929E-02	-2.408E-07	1.000E+00	1.000E+00	1.000E+00	3.624E-01
11	4	1.001E+01	2.991E+00	8.371E-02	-8.877E-02	0.	0.	0.	0.	0.
1	5	0.	3.997E+00	0.	-3.038E-02	1.377E-05	1.000E+00	1.000E+00	1.000E+00	3.059E+00
2	5	1.001E+00	3.997E+00	6.258E-03	-3.081E-02	3.879E-06	1.000E+00	1.000E+00	1.000E+00	2.987E+00
3	5	2.001E+00	3.997E+00	1.271E-02	-3.219E-02	3.374E-06	1.000E+00	1.000E+00	1.000E+00	2.879E+00
4	5	3.002E+00	3.997E+00	1.942E-02	-3.448E-02	2.837E-06	1.000E+00	1.000E+00	1.000E+00	2.688E+00
5	5	4.003E+00	3.996E+00	2.848E-02	-3.797E-02	1.813E-06	1.000E+00	1.000E+00	1.000E+00	2.459E+00
6	5	5.003E+00	3.996E+00	3.398E-02	-4.288E-02	9.688E-07	1.000E+00	1.000E+00	1.000E+00	2.143E+00
7	5	6.004E+00	3.995E+00	4.181E-02	-4.958E-02	2.079E-07	1.000E+00	1.000E+00	1.000E+00	1.784E+00
8	5	7.005E+00	3.994E+00	4.958E-02	-5.898E-02	-3.198E-07	1.000E+00	1.000E+00	1.000E+00	1.320E+00
9	5	8.006E+00	3.993E+00	5.848E-02	-7.015E-02	-4.814E-07	1.000E+00	1.000E+00	1.000E+00	8.188E-01
10	5	9.006E+00	3.992E+00	6.147E-02	-8.418E-02	-1.011E-07	1.000E+00	1.000E+00	1.000E+00	2.803E-01
11	5	1.001E+01	3.991E+00	6.427E-02	-9.179E-02	0.	0.	0.	0.	0.
1	6	0.	4.996E+00	0.	-3.623E-02	9.800E-06	1.000E+00	1.000E+00	1.000E+00	2.417E+00

I	J	X	Y	U	V	SIE	RHO	MASS	VOL	P
1	2	1.001E+00	4.998E+00	5.331E-03	-3.872E-02	2.492E-08	1.000E+00	1.000E+00	1.000E+00	2.399E+00
3	6	2.001E+00	4.998E+00	1.064E-02	-3.822E-02	2.107E-08	1.000E+00	1.000E+00	1.000E+00	2.271E+00
4	6	3.002E+00	4.998E+00	1.842E-02	-4.073E-02	1.837E-08	1.000E+00	1.000E+00	1.000E+00	2.123E+00
5	6	4.002E+00	4.998E+00	2.222E-02	-4.497E-02	1.118E-08	1.000E+00	1.000E+00	1.000E+00	1.822E+00
6	6	5.003E+00	4.998E+00	2.818E-02	-4.973E-02	8.021E-07	1.000E+00	1.000E+00	1.000E+00	1.670E+00
7	6	6.003E+00	4.994E+00	3.413E-02	-5.849E-02	1.557E-07	1.000E+00	1.000E+00	1.000E+00	1.387E+00
8	6	7.004E+00	4.993E+00	3.972E-02	-6.501E-02	-1.488E-07	1.000E+00	1.000E+00	1.000E+00	1.017E+00
9	6	8.004E+00	4.992E+00	4.445E-02	-7.533E-02	-2.498E-07	1.000E+00	1.000E+00	1.000E+00	6.284E-01
10	6	9.005E+00	4.991E+00	4.765E-02	-8.718E-02	-4.804E-08	1.000E+00	1.000E+00	1.000E+00	2.140E-01
11	6	1.000E+01	4.991E+00	4.943E-02	-9.338E-02	0.	0.	0.	0.	0.
1	7	0.	5.998E+00	0.	-4.112E-02	5.298E-08	1.000E+00	1.000E+00	1.000E+00	1.828E+00
2	7	1.000E+00	5.998E+00	4.320E-03	-4.184E-02	1.384E-08	1.000E+00	1.000E+00	1.000E+00	1.791E+00
3	7	2.001E+00	5.998E+00	8.731E-03	-4.322E-02	1.142E-08	1.000E+00	1.000E+00	1.000E+00	1.714E+00
4	7	3.001E+00	5.998E+00	1.321E-02	-4.593E-02	8.728E-07	1.000E+00	1.000E+00	1.000E+00	1.598E+00
5	7	4.002E+00	5.998E+00	1.778E-02	-4.982E-02	5.784E-07	1.000E+00	1.000E+00	1.000E+00	1.443E+00
6	7	5.002E+00	5.994E+00	2.230E-02	-5.501E-02	2.938E-07	1.000E+00	1.000E+00	1.000E+00	1.249E+00
7	7	6.003E+00	5.994E+00	2.868E-02	-6.158E-02	5.381E-08	1.000E+00	1.000E+00	1.000E+00	1.018E+00
8	7	7.003E+00	5.993E+00	3.688E-02	-6.952E-02	-1.019E-07	1.000E+00	1.000E+00	1.000E+00	7.953E-01
9	7	8.003E+00	5.992E+00	3.362E-02	-7.878E-02	-1.458E-07	1.000E+00	1.000E+00	1.000E+00	4.853E-01
10	7	9.004E+00	5.991E+00	3.807E-02	-8.908E-02	-2.788E-08	1.000E+00	1.000E+00	1.000E+00	1.982E-01
11	7	1.000E+01	5.991E+00	3.723E-02	-9.442E-02	0.	0.	0.	0.	0.
1	8	0.	8.998E+00	0.	-4.498E-02	2.808E-08	1.000E+00	1.000E+00	1.000E+00	1.278E+00
2	8	1.000E+00	8.998E+00	3.261E-03	-4.549E-02	5.717E-07	1.000E+00	1.000E+00	1.000E+00	1.291E+00
3	8	2.001E+00	8.998E+00	8.578E-03	-4.712E-02	4.889E-07	1.000E+00	1.000E+00	1.000E+00	1.198E+00
4	8	3.001E+00	8.998E+00	9.914E-03	-4.987E-02	3.391E-07	1.000E+00	1.000E+00	1.000E+00	1.113E+00
5	8	4.001E+00	8.998E+00	1.329E-02	-5.378E-02	2.617E-07	1.000E+00	1.000E+00	1.000E+00	1.003E+00
6	8	5.002E+00	8.994E+00	1.852E-02	-5.888E-02	7.147E-08	1.000E+00	1.000E+00	1.000E+00	8.887E-01
7	8	6.002E+00	8.993E+00	1.982E-02	-6.518E-02	-3.207E-08	1.000E+00	1.000E+00	1.000E+00	7.051E-01
8	8	7.002E+00	8.993E+00	2.239E-02	-7.283E-02	-9.098E-08	1.000E+00	1.000E+00	1.000E+00	5.219E-01
9	8	8.002E+00	8.992E+00	2.453E-02	-8.109E-02	-9.428E-08	1.000E+00	1.000E+00	1.000E+00	3.208E-01
10	8	9.003E+00	8.991E+00	2.595E-02	-9.031E-02	-1.758E-08	1.000E+00	1.000E+00	1.000E+00	1.088E-01
11	8	1.003E+01	8.990E+00	2.671E-02	-9.507E-02	0.	0.	0.	0.	0.
1	9	0.	7.998E+00	0.	-4.771E-02	8.801E-07	1.000E+00	1.000E+00	1.000E+00	7.953E-01
2	9	1.000E+00	7.998E+00	2.179E-03	-4.828E-02	1.048E-07	1.000E+00	1.000E+00	1.000E+00	7.388E-01
3	9	2.000E+00	7.998E+00	4.389E-03	-4.988E-02	7.278E-08	1.000E+00	1.000E+00	1.000E+00	7.088E-01
4	9	3.001E+00	7.998E+00	6.587E-03	-5.288E-02	3.328E-08	1.000E+00	1.000E+00	1.000E+00	6.588E-01
5	9	4.001E+00	7.994E+00	8.783E-03	-5.653E-02	-8.482E-08	1.000E+00	1.000E+00	1.000E+00	5.918E-01
6	9	5.001E+00	7.994E+00	1.098E-02	-6.153E-02	-4.594E-08	1.000E+00	1.000E+00	1.000E+00	5.097E-01
7	9	6.001E+00	7.993E+00	1.287E-02	-6.788E-02	-7.011E-08	1.000E+00	1.000E+00	1.000E+00	4.148E-01
8	9	7.001E+00	7.993E+00	1.459E-02	-7.487E-02	-7.594E-08	1.000E+00	1.000E+00	1.000E+00	3.099E-01
9	9	8.002E+00	7.992E+00	1.593E-02	-8.257E-02	-5.895E-08	1.000E+00	1.000E+00	1.000E+00	1.878E-01
10	9	9.002E+00	7.991E+00	1.681E-02	-9.118E-02	-1.074E-08	1.000E+00	1.000E+00	1.000E+00	8.379E-02
11	9	1.000E+01	7.990E+00	1.728E-02	-9.549E-02	0.	0.	0.	0.	0.
1	10	0.	6.998E+00	0.	-4.937E-02	1.352E-07	1.000E+00	1.000E+00	1.000E+00	2.488E-01
2	10	1.000E+00	6.998E+00	1.098E-03	-4.982E-02	-2.488E-08	1.000E+00	1.000E+00	1.000E+00	2.438E-01
3	10	2.000E+00	6.998E+00	2.193E-03	-5.158E-02	-5.174E-08	1.000E+00	1.000E+00	1.000E+00	2.328E-01
4	10	3.000E+00	6.998E+00	3.291E-03	-5.431E-02	-8.888E-08	1.000E+00	1.000E+00	1.000E+00	2.182E-01
5	10	4.000E+00	6.994E+00	4.371E-03	-5.813E-02	-1.228E-08	1.000E+00	1.000E+00	1.000E+00	1.944E-01
6	10	5.001E+00	6.994E+00	5.408E-03	-6.308E-02	-1.503E-08	1.000E+00	1.000E+00	1.000E+00	1.679E-01
7	10	6.001E+00	6.993E+00	6.383E-03	-6.898E-02	-1.988E-08	1.000E+00	1.000E+00	1.000E+00	1.398E-01
8	10	7.001E+00	6.992E+00	7.188E-03	-7.582E-02	-1.441E-08	1.000E+00	1.000E+00	1.000E+00	1.003E-01
9	10	8.001E+00	6.992E+00	7.834E-03	-8.341E-02	-1.018E-08	1.000E+00	1.000E+00	1.000E+00	6.182E-02
10	10	9.001E+00	6.991E+00	8.248E-03	-9.194E-02	-1.824E-08	1.000E+00	1.000E+00	1.000E+00	2.888E-02
11	10	1.000E+01	6.990E+00	8.484E-03	-9.571E-02	0.	0.	0.	0.	0.
1	11	0.	9.998E+00	0.	-5.028E-02	0.	0.	0.	0.	0.
2	11	1.000E+00	9.998E+00	5.448E-04	-5.079E-02	0.	0.	0.	0.	0.

1	J	X	Y	U	V	SITE	RHO	MASS	VOL	P
3	11	2.000E+00	9.99E+00	1.09E-03	-5.23E-02	0.	0.	0.	0.	0.
4	11	3.000E+00	9.99E+00	1.64E-03	-5.91E-02	0.	0.	0.	0.	0.
5	11	4.000E+00	9.99E+00	2.17E-03	-5.89E-02	0.	0.	0.	0.	0.
6	11	5.000E+00	9.99E+00	2.68E-03	-6.381E-02	0.	0.	0.	0.	0.
7	11	6.000E+00	9.99E+00	3.15E-03	-6.96E-02	0.	0.	0.	0.	0.
8	11	7.000E+00	9.99E+00	3.561E-03	-7.637E-02	0.	0.	0.	0.	0.
9	11	8.000E+00	9.99E+00	3.87E-03	-8.380E-02	0.	0.	0.	0.	0.
10	11	9.000E+00	9.99E+00	4.07E-03	-9.17E-02	0.	0.	0.	0.	0.
11	11	1.000E+01	9.99E+00	4.17E-03	-9.98E-02	0.	0.	0.	0.	0.

EXPORT SALE 04/06/79 14:28:13 T3AA SUPP. PURE LABRANJAN W/ INC=1, ASO=100 0+0679-3
 1 - 1.0000E-01 CYCLE 1

1 T= 1.0000E-01 DT= 1.0000E-01 NUMIT= 193 GRIND= 11.855 M
 2 T= 2.0000E-01 DT= 1.0000E-01 NUMIT= 39 GRIND= 4.878 M
 3 T= 3.0000E-01 DT= 1.0000E-01 NUMIT= 11 GRIND= 1.808 M
 4 T= 4.0000E-01 DT= 1.0000E-01 NUMIT= 51 GRIND= 2.510 M
 5 T= 5.0000E-01 DT= 1.0000E-01 NUMIT= 59 GRIND= 2.506 M
 6 T= 6.0000E-01 DT= 1.0000E-01 NUMIT= 64 GRIND= 2.703 M
 7 T= 7.0000E-01 DT= 1.0000E-01 NUMIT= 68 GRIND= 2.860 M
 8 T= 8.0000E-01 DT= 1.0000E-01 NUMIT= 72 GRIND= 3.034 M
 9 T= 9.0000E-01 DT= 1.0000E-01 NUMIT= 74 GRIND= 3.110 M
 MASS= 1.00000000E+02 U MOM= 2.94712745E+00 V MOM= 4.9081083E+00
 T= 1.0000E-01 CYCLE 1 TOT E= 2.45405442E-01 SITE= 4.45181099E-04

KPORT SALE 04/06/79 14:28:13 T3AAA SLUMP, PURE LAORANGIAN W/ INC=1, ASQ=100 040879-3
 T= 5.02599E+00 CYCLE 71

I	J	X	Y	U	V	SIE	RHO	MASS	VOL	P	
1	1	0	0	0.	0.	2.787E-03	1.000E+00	1.000E+00	0.990E-01	6.530E+00	
2	1	1	672E+00	0	2.169E-01	0.	1.347E-03	1.000E+00	1.000E+00	9.990E-01	6.451E+00
3	1	3	378E+00	0	4.440E-01	0	1.059E-03	1.000E+00	1.000E+00	9.990E-01	6.292E+00
4	1	5	168E+00	0	7.030E-01	0.	6.189E-04	1.000E+00	1.000E+00	9.990E-01	6.007E+00
5	1	7	099E+00	0	1.003E+00	0.	-1.211E-04	1.000E+00	1.000E+00	9.990E-01	5.507E+00
6	1	9	300E+00	0	1.418E+00	0.	-1.288E-03	9.990E-01	1.000E+00	1.000E+00	4.939E+00
7	1	1	197E+01	0	2.043E+00	0.	-3.820E-03	9.990E-01	1.000E+00	1.000E+00	3.896E+00
8	1	1	560E+01	0	3.082E+00	0.	-5.824E-03	9.990E-01	1.000E+00	1.001E+00	2.372E+00
9	1	2	032E+01	0	4.220E+00	0.	-3.820E-03	9.990E-01	1.000E+00	1.001E+00	1.488E+00
10	1	2	524E+01	0	4.969E+00	0.	-5.824E-04	9.990E-01	1.000E+00	1.000E+00	4.387E-01
11	1	2	894E+01	0	5.956E+00	0.	0.	0.	0.	0.	0.
1	2	0	5.990E-01	0.	-7.841E-02	1.309E-03	1.000E+00	1.000E+00	9.990E-01	5.930E+00	
2	2	1	584E+00	5.824E-01	2.269E-01	-7.980E-02	1.018E-04	1.000E+00	1.000E+00	9.990E-01	5.880E+00
3	2	3	409E+00	5.740E-01	4.668E-01	-8.024E-02	9.393E-05	1.000E+00	1.000E+00	9.990E-01	5.720E+00
4	2	5	208E+00	5.387E-01	7.958E-01	-8.483E-02	-6.543E-05	1.000E+00	1.000E+00	9.990E-01	5.498E+00
5	2	7	194E+00	4.926E-01	1.052E+00	-8.113E-02	-3.033E-04	1.000E+00	1.000E+00	1.000E+00	5.131E+00
6	2	9	366E+00	4.108E-01	1.471E+00	-9.289E-02	-7.087E-04	1.000E+00	1.000E+00	1.000E+00	4.588E+00
7	2	1	206E+01	3.316E-01	2.103E+00	-8.378E-02	-1.394E-03	1.000E+00	1.000E+00	1.000E+00	3.810E+00
8	2	1	567E+01	2.187E-01	3.131E+00	-7.830E-02	-2.198E-03	9.990E-01	1.000E+00	1.000E+00	2.233E+00
9	2	2	034E+01	2.078E-01	4.234E+00	-2.580E-02	-1.434E-03	9.997E-01	1.000E+00	1.000E+00	1.293E+00
10	2	2	503E+01	2.091E-01	4.990E+00	-3.792E-02	-1.298E-05	9.990E-01	1.000E+00	1.000E+00	4.109E-01
11	2	2	808E+01	3.982E-01	5.284E+00	-2.672E-02	0.	0.	0.	0.	0.
1	3	0	1.198E+00	0.	-1.967E-01	1.019E-03	1.000E+00	1.000E+00	9.990E-01	5.321E+00	
2	3	1	682E+00	1.187E+00	2.221E-01	-1.998E-01	1.352E-04	1.000E+00	1.000E+00	9.990E-01	5.270E+00
3	3	3	360E+00	1.150E+00	4.973E-01	-1.839E-01	5.197E-05	1.000E+00	1.000E+00	9.990E-01	5.181E+00
4	3	5	133E+00	1.069E+00	7.191E-01	-1.881E-01	-7.148E-05	1.000E+00	1.000E+00	9.990E-01	4.977E+00
5	3	7	049E+00	9.900E-01	1.031E+00	-1.877E-01	-2.580E-04	1.000E+00	1.000E+00	1.000E+00	4.877E+00
6	3	9	193E+00	8.453E-01	1.428E+00	-1.772E-01	-5.977E-04	1.000E+00	1.000E+00	1.000E+00	4.298E+00
7	3	1	182E+01	8.674E-01	2.044E+00	-1.779E-01	-1.140E-03	1.000E+00	1.000E+00	1.000E+00	3.411E+00
8	3	1	529E+01	4.747E-01	3.042E+00	-1.502E-01	-1.849E-03	9.990E-01	1.000E+00	1.000E+00	2.163E+00
9	3	1	978E+01	3.982E-01	4.129E+00	-7.097E-02	-1.272E-03	9.990E-01	1.000E+00	1.000E+00	1.183E+00
10	3	2	417E+01	4.511E-01	4.841E+00	-8.174E-02	-2.707E-05	1.000E+00	1.000E+00	1.000E+00	4.089E-01
11	3	2	671E+01	6.810E-01	5.134E+00	-8.082E-02	0.	0.	0.	0.	0.
1	4	0	1.810E+00	0.	-2.408E-01	7.828E-04	1.000E+00	1.000E+00	9.990E-01	4.898E+00	
2	4	1	627E+00	1.793E+00	2.154E-01	-2.412E-01	8.886E-05	1.000E+00	1.000E+00	9.990E-01	4.898E+00
3	4	3	288E+00	1.739E+00	4.412E-01	-2.482E-01	2.210E-05	1.000E+00	1.000E+00	9.990E-01	4.588E+00
4	4	5	018E+00	1.644E+00	6.953E-01	-2.533E-01	-7.531E-05	1.000E+00	1.000E+00	1.000E+00	4.433E+00
5	4	6	888E+00	1.509E+00	9.957E-01	-2.598E-01	-2.087E-04	1.000E+00	1.000E+00	1.000E+00	4.201E+00
6	4	8	933E+00	1.312E+00	1.388E+00	-2.813E-01	-4.770E-04	1.000E+00	1.000E+00	1.000E+00	3.884E+00
7	4	1	143E+01	1.038E+00	1.943E+00	-2.798E-01	-9.330E-04	1.000E+00	1.000E+00	1.000E+00	3.220E+00
8	4	1	471E+01	7.636E-01	2.887E+00	-2.374E-01	-1.479E-03	9.990E-01	1.000E+00	1.000E+00	2.118E+00
9	4	1	894E+01	6.070E-01	3.969E+00	-1.311E-01	-1.042E-03	9.990E-01	1.000E+00	1.000E+00	1.153E+00
10	4	2	311E+01	6.810E-01	4.701E+00	-9.129E-02	-2.249E-07	1.000E+00	1.000E+00	1.000E+00	3.787E-01
11	4	2	566E+01	1.008E+00	4.989E+00	-1.250E-01	0.	0.	0.	0.	0.
1	5	0	2.438E+00	0.	-3.222E-01	5.390E-04	1.000E+00	1.000E+00	9.990E-01	4.094E+00	
2	5	1	581E+00	2.414E+00	2.058E-01	-3.243E-01	4.899E-05	1.000E+00	1.000E+00	9.990E-01	4.029E+00
3	5	3	188E+00	2.348E+00	4.213E-01	-3.287E-01	1.101E-06	1.000E+00	1.000E+00	1.000E+00	3.887E+00
4	5	4	860E+00	2.228E+00	6.613E-01	-3.400E-01	-7.483E-05	1.000E+00	1.000E+00	1.000E+00	3.878E+00
5	5	6	641E+00	2.060E+00	9.489E-01	-3.457E-01	-1.688E-04	1.000E+00	1.000E+00	1.000E+00	3.887E+00
6	5	8	599E+00	1.818E+00	1.293E+00	-3.488E-01	-3.489E-04	1.000E+00	1.000E+00	1.000E+00	3.448E+00
7	5	1	092E+01	1.471E+00	1.804E+00	-3.678E-01	-7.293E-04	1.000E+00	1.000E+00	1.000E+00	2.988E+00
8	5	1	396E+01	1.094E+00	2.688E+00	-3.397E-01	-1.142E-03	9.990E-01	1.000E+00	1.000E+00	2.089E+00
9	5	1	786E+01	8.577E-01	3.729E+00	-2.134E-01	-8.697E-04	9.990E-01	1.000E+00	1.000E+00	1.138E+00
10	5	2	187E+01	8.888E-01	4.501E+00	-1.335E-01	-3.382E-05	1.000E+00	1.000E+00	1.000E+00	3.818E-01
11	5	2	437E+01	1.249E+00	4.748E+00	-1.568E-01	0.	0.	0.	0.	0.
1	6	0	3.083E+00	0.	-4.048E-01	3.510E-04	1.000E+00	1.000E+00	9.990E-01	3.384E+00	

XPORT SALE 04/06/79 14 28:13 T3AAA SLUMP, PURE LAORANGIAN W/ INC=1, ASQ=100 040679-3
 T= 5.02599E+00 CYCLE 71

	J	X	Y	U	V	SIE	RHO	MASS	VOL	P
1	6	1.524E+00	3.056E+00	1.936E-01	-4.081E-01	1.545E-05	1.000E+00	1.000E+00	1.000E+00	3.372E+00
3	5	3.073E+00	2.980E+00	3.986E-01	-4.134E-01	-1.411E-05	1.000E+00	1.000E+00	1.000E+00	3.322E+00
4	6	4.670E+00	2.843E+00	6.196E-01	-4.250E-01	-6.562E-05	1.000E+00	1.000E+00	1.000E+00	3.276E+00
5	6	6.370E+00	2.643E+00	8.894E-01	-4.403E-01	-1.343E-04	1.000E+00	1.000E+00	1.000E+00	3.151E+00
6	6	8.205E+00	2.379E+00	1.212E+00	-4.364E-01	-2.299E-04	1.000E+00	1.000E+00	1.000E+00	2.955E+00
7	6	1.032E+01	1.979E+00	1.646E+00	-4.578E-01	-5.156E-04	1.000E+00	1.000E+00	1.000E+00	2.698E+00
8	6	1.308E+01	1.496E+00	2.410E+00	-4.539E-01	-8.406E-04	1.000E+00	1.000E+00	1.000E+00	2.020E+00
9	6	1.666E+01	1.152E+00	3.423E+00	-3.220E-01	-7.173E-04	9.999E-01	1.000E+00	1.000E+00	1.134E+00
10	6	2.055E+01	1.105E+00	4.271E+00	-1.994E-01	-3.339E-05	1.000E+00	1.000E+00	1.000E+00	3.473E-01
11	6	2.305E+01	1.457E+00	4.537E+00	-1.916E-01	0.	0.	0.	0.	0.
1	7	0.	3.753E+00	0.	4.906E-01	2.006E-04	1.000E+00	1.000E+00	9.999E-01	2.691E+00
2	7	1.461E+00	3.727E+00	1.809E-01	-4.912E-01	-4.569E-06	1.000E+00	1.000E+00	1.000E+00	2.675E+00
3	7	2.941E+00	3.640E+00	3.693E-01	-5.010E-01	-2.468E-05	1.000E+00	1.000E+00	1.000E+00	2.669E+00
4	7	4.464E+00	3.496E+00	5.777E-01	-5.101E-01	-5.176E-05	1.000E+00	1.000E+00	1.000E+00	2.650E+00
5	7	6.056E+00	3.272E+00	8.151E-01	-5.328E-01	-1.023E-04	1.000E+00	1.000E+00	1.000E+00	2.584E+00
6	7	7.787E+00	2.989E+00	1.122E+00	-5.360E-01	-1.481E-04	1.000E+00	1.000E+00	1.000E+00	2.406E+00
7	7	9.664E+00	2.581E+00	1.489E+00	-5.429E-01	-3.012E-04	1.000E+00	1.000E+00	1.000E+00	2.269E+00
8	7	1.210E+01	1.993E+00	2.120E+00	-5.693E-01	-5.672E-04	1.000E+00	1.000E+00	1.000E+00	1.851E+00
9	7	1.535E+01	1.513E+00	3.062E+00	-4.578E-01	-5.547E-04	1.000E+00	1.000E+00	1.000E+00	1.123E+00
10	7	1.911E+01	1.344E+00	3.978E+00	-2.871E-01	-1.895E-05	1.000E+00	1.000E+00	1.000E+00	3.409E-01
11	7	2.159E+01	1.643E+00	4.283E+00	-2.463E-01	0.	0.	0.	0.	0.
1	8	0.	4.457E+00	0.	-5.746E-01	9.153E-05	1.000E+00	1.000E+00	9.999E-01	1.962E+00
2	8	1.393E+00	4.426E+00	1.666E-01	-5.784E-01	-1.569E-05	1.000E+00	1.000E+00	1.000E+00	1.956E+00
3	8	2.801E+00	4.339E+00	3.393E-01	-5.896E-01	-2.602E-05	1.000E+00	1.000E+00	1.000E+00	1.944E+00
4	8	4.242E+00	4.183E+00	5.263E-01	-6.013E-01	4.063E-05	1.000E+00	1.000E+00	1.000E+00	1.933E+00
5	8	5.736E+00	3.993E+00	7.419E-01	-6.184E-01	-6.414E-05	1.000E+00	1.000E+00	1.000E+00	1.892E+00
6	8	7.331E+00	3.642E+00	1.010E+00	-6.494E-01	-9.660E-05	1.000E+00	1.000E+00	1.000E+00	1.867E+00
7	8	9.071E+00	3.256E+00	1.347E+00	-6.396E-01	-1.488E-04	1.000E+00	1.000E+00	1.000E+00	1.804E+00
8	8	1.109E+01	2.695E+00	1.828E+00	-6.708E-01	-3.095E-04	1.000E+00	1.000E+00	1.000E+00	1.595E+00
9	8	1.393E+01	1.978E+00	2.648E+00	-6.151E-01	-3.956E-04	1.000E+00	1.000E+00	1.000E+00	1.097E+00
10	8	1.752E+01	1.633E+00	3.602E+00	-4.181E-01	-5.819E-06	1.000E+00	1.000E+00	1.000E+00	3.245E-01
11	8	1.997E+01	1.838E+00	3.847E+00	-3.338E-01	0.	0.	0.	0.	0.
1	9	0.	5.193E+00	0.	-6.815E-01	2.422E-05	1.000E+00	1.000E+00	1.000E+00	1.201E+00
2	9	1.322E+00	5.164E+00	1.510E-01	-6.842E-01	-1.679E-05	1.000E+00	1.000E+00	1.000E+00	1.196E+00
3	9	2.657E+00	5.073E+00	3.084E-01	-6.738E-01	-2.041E-05	1.000E+00	1.000E+00	1.000E+00	1.195E+00
4	9	4.013E+00	4.918E+00	4.771E-01	-6.896E-01	-2.625E-05	1.000E+00	1.000E+00	1.000E+00	1.191E+00
5	9	5.413E+00	4.692E+00	6.697E-01	-7.102E-01	-3.392E-05	1.000E+00	1.000E+00	1.000E+00	1.177E+00
6	9	6.871E+00	4.381E+00	8.940E-01	-7.392E-01	-4.689E-05	1.000E+00	1.000E+00	1.000E+00	1.171E+00
7	9	8.459E+00	3.977E+00	1.193E+00	-7.569E-01	-6.595E-05	1.000E+00	1.000E+00	1.000E+00	1.123E+00
8	9	1.020E+01	3.448E+00	1.587E+00	-7.701E-01	-9.130E-05	1.000E+00	1.000E+00	1.000E+00	1.005E+00
9	9	1.244E+01	2.660E+00	2.205E+00	-7.872E-01	-1.8950E-04	1.000E+00	1.000E+00	1.000E+00	9.369E-01
10	9	1.577E+01	1.999E+00	3.171E+00	-6.015E-01	5.473E-05	1.000E+00	1.000E+00	1.000E+00	3.687E-01
11	9	1.818E+01	2.084E+00	3.543E+00	-4.571E-01	0.	0.	0.	0.	0.
1	10	0.	5.971E+00	0.	-7.478E-01	8.703E-07	1.000E+00	1.000E+00	1.000E+00	4.048E-01
2	10	1.252E+00	5.942E+00	1.351E-01	-7.510E-01	-6.486E-06	1.000E+00	1.000E+00	1.000E+00	4.042E-01
3	10	2.511E+00	5.893E+00	2.748E-01	-7.611E-01	-7.310E-06	1.000E+00	1.000E+00	1.000E+00	4.045E-01
4	10	3.787E+00	5.702E+00	4.245E-01	-7.776E-01	-8.569E-06	1.000E+00	1.000E+00	1.000E+00	4.021E-01
5	10	5.088E+00	5.481E+00	5.903E-01	-8.011E-01	-1.089E-05	1.000E+00	1.000E+00	1.000E+00	4.085E-01
6	10	6.432E+00	5.184E+00	7.836E-01	-8.286E-01	-1.323E-05	1.000E+00	1.000E+00	1.000E+00	3.899E-01
7	10	7.837E+00	4.793E+00	1.014E+00	-8.612E-01	-2.314E-05	1.000E+00	1.000E+00	1.000E+00	4.238E-01
8	10	9.381E+00	4.297E+00	1.346E+00	-8.882E-01	-2.177E-05	1.000E+00	1.000E+00	1.000E+00	3.297E-01
9	10	1.106E+01	3.643E+00	1.738E+00	-8.731E-01	-8.968E-05	1.000E+00	1.000E+00	1.000E+00	3.896E-01
10	10	1.369E+01	2.649E+00	2.580E+00	-8.243E-01	9.239E-06	1.000E+00	1.000E+00	1.000E+00	2.511E-01
11	10	1.579E+01	2.442E+00	2.895E+00	-6.602E 01	0.	0.	0.	0.	0.
1	11	0.	6.782E+00	0.	-8.332E-01	0.	0.	0.	0.	0.
2	11	1.216E+00	6.753E+00	1.270E-01	-8.378E 01	0.	0.	0.	0.	0.

EXPORT SALE 04/06/79 14:28:13 T3AAA SLUMP, PURE LAORANGIAN W/ INC=1, ASO=100 040679-3
 T= 5.02599E+00 CYCLE 71

I	J	X	Y	U	V	SIE	RHO	MASS	VOL	P
3	11	2.437E+00	6.663E+00	2.579E-01	-8.493E-01	0.	0.	0.	0.	0.
4	11	3.671E+00	6.510E+00	3.976E-01	-8.669E-01	0.	0.	0.	0.	0.
5	11	4.923E+00	6.289E+00	5.501E-01	-8.951E-01	0.	0.	0.	0.	0.
6	11	6.207E+00	5.988E+00	7.287E-01	-9.335E-01	0.	0.	0.	0.	0.
7	11	7.530E+00	5.606E+00	8.298E-01	-9.634E-01	0.	0.	0.	0.	0.
8	11	8.961E+00	5.079E+00	1.230E+00	-1.035E+00	0.	0.	0.	0.	0.
9	11	1.044E+01	4.526E+00	1.553E+00	-1.007E+00	0.	0.	0.	0.	0.
10	11	1.259E+01	3.373E+00	2.322E+00	-1.042E+00	0.	0.	0.	0.	0.
11	11	1.450E+01	3.039E+00	2.636E+00	-8.142E-01	0.	0.	0.	0.	0.

T= 5.02599E+00 CYCLE 71 TOT F= 2.57784527E+02 SIE=-2.93271763E-02
 MASS= 1.00000000E+02 U MOM= 1.85024287E+02 V MOM=-4.1376603+E+01

NCYC	71	T= 5.02599E+00	DT= 4.05062E-02	NUMIT= 47	GRIND= 5.397 C
NCYC	72	T= 5.06549E+00	DT= 4.03490E-02	NUMIT= 47	GRIND= 2.063 C
NCYC	73	T= 5.10684E+00	DT= 4.02058E-02	NUMIT= 47	GRIND= 2.068 C
NCYC	74	T= 5.14705E+00	DT= 4.00764E-02	NUMIT= 46	GRIND= 2.016 C
NCYC	75	T= 5.18713E+00	DT= 3.99601E-02	NUMIT= 47	GRIND= 2.054 C
NCYC	76	T= 5.22709E+00	DT= 3.98569E-02	NUMIT= 46	GRIND= 2.026 C
NCYC	77	T= 5.26694E+00	DT= 3.97652E-02	NUMIT= 46	GRIND= 1.998 C
NCYC	78	T= 5.30671E+00	DT= 3.96857E-02	NUMIT= 46	GRIND= 2.006 C
NCYC	79	T= 5.34639E+00	DT= 3.96178E-02	NUMIT= 45	GRIND= 1.960 C
NCYC	80	T= 5.38601E+00	DT= 3.95611E-02	NUMIT= 45	GRIND= 1.995 C
NCYC	81	T= 5.42557E+00	DT= 3.95152E-02	NUMIT= 45	GRIND= 1.977 C
NCYC	82	T= 5.46509E+00	DT= 3.94800E-02	NUMIT= 44	GRIND= 1.928 C
NCYC	83	T= 5.50457E+00	DT= 3.94455E-02	NUMIT= 44	GRIND= 1.922 C
NCYC	84	T= 5.54402E+00	DT= 3.94102E-02	NUMIT= 43	GRIND= 1.878 C
NCYC	85	T= 5.58346E+00	DT= 3.93751E-02	NUMIT= 43	GRIND= 1.877 C
NCYC	86	T= 5.62290E+00	DT= 3.93400E-02	NUMIT= 42	GRIND= 1.843 C
NCYC	87	T= 5.66234E+00	DT= 3.93054E-02	NUMIT= 42	GRIND= 1.853 C
NCYC	88	T= 5.70178E+00	DT= 3.92704E-02	NUMIT= 42	GRIND= 1.856 C
NCYC	89	T= 5.74127E+00	DT= 3.92353E-02	NUMIT= 41	GRIND= 1.813 C
NCYC	90	T= 5.78077E+00	DT= 3.92000E-02	NUMIT= 40	GRIND= 1.770 C
NCYC	91	T= 5.82032E+00	DT= 3.91642E-02	NUMIT= 41	GRIND= 1.819 C
NCYC	92	T= 5.85982E+00	DT= 3.91286E-02	NUMIT= 39	GRIND= 1.723 C
NCYC	93	T= 5.89938E+00	DT= 3.90932E-02	NUMIT= 39	GRIND= 1.724 C
NCYC	94	T= 5.93890E+00	DT= 3.90579E-02	NUMIT= 39	GRIND= 1.728 C
NCYC	95	T= 5.97910E+00	DT= 3.90227E-02	NUMIT= 37	GRIND= 1.650 C