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IAEA-SPE-1: PRE-TEST CALCULATIONS FOR THE
PMK-NVH STANDARD PROBLEM EXERCISE

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IAEA-SPE-1: PRE-TEST CALCULATIONS FOR THE
PMK-NVH STANDARD PROBLEM EXERCISE

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ABSTRACT

Pre-test calculations of the IAEA-PMK-NVH Standard Problem Exercise (IAEA-SPE-1) are presented. The analysis was carried out by the KFK version of RELAP4/mod6 code. Requirements of the Specification Report are strictly followed in presenting the results.

АННОТАЦИЯ

Данный отчет содержит предварительные расчеты эксперимента IAEA-PMK-NVH Standard Problem Exercise. Для анализа был использован вариант вычислительной программы RELAP4/mod6, имеющейся в МАГАТЭ. Результаты расчетов представлены в виде, соответствующем требованиям спецификационного отчета.

KIVONAT

A riport az IAEA-PMK-NVH Standard Problem Exercise (IAEA-SPE-1) kísérletet megelőző számításait tartalmazza. Az elemzéshez a RELAP4/mod6 nukleáris biztonsági rendszerkód Kfk változatát használtuk. Az eredményeket a Specifikációs Riport követelményeinek megfelelően közöljük.

1. Introduction

Standard Problem Exercises /SPE/ offer unique possibilities for computer code assessment of participating organizations and for the exchange of informations in a strictly defined field of nuclear safety research.

Therefore, IAEA has deemed it necessary to organize an SPE which is open for all the Member States interested in.

The experimental basis of the SPE is the PMK-NVH integral-type experimental facility located at the Central Research Institute for Physics of the Hungarian Academy of Sciences.

The PMK-NVH facility is a full-pressure 1:2070 scaled model of the Paks Nuclear Power Plant and designed mainly to investigate processes following a small and medium size break in the primary circuit and to study the natural circulation behaviour, but it was conceived in a way that allows simulation of a variety of plant dynamic processes of WWER-type PWRs. [1, 2, 3]

The transient chosen by a Working Group of the IAEA is a 7.4 % break in the cold leg of the Paks Nuclear Power Plant.

The pre-test calculations have been performed by the RELAP4/mod6 code /KfK version/ on the IBM 3081 computer at the IAEA Headquarters in the framework of the Regional Programme on the Computer Aided Safety Analysis.

2. Data for the pre-test analysis

Data for the pre-test analysis are given in [1, 4, 5]. The measured actual initial conditions are slightly different of the nominal initial conditions given in Ref.[1] and they are used as listed below.

2.1 Initial conditions at 0 second

The initial conditions at 0. s for the Standard Problem Test /SPT/ are characterized by the data as follows:

o Primary circuit

- pressure in upper plenum	12.65 MPa
- loop flow	4.73 kg/s
- core inlet temperature	538 K
- core power	654 kW
- coolant level above bottom of pressurizer /collapsed/	1.46 m

o Secondary circuit

- pressure in SG	4.67 MPa
- coolant level above bottom of SG secondary side /collapsed/	2.25 m
- feed water flow	0.353 kg/s

o Position of valves

- MV11, PV12, PV23, MV31, PV31 are closed
- PV11 is throttled, closing current is 11.514 mA
- MV12 is open
- PV21 and PV22 are throttled.

2.2 Transient initiation

The SPT, a 7.4 % cold leg break starting from the above defined conditions was performed with the sequence of events as listed below:

- break valve MV31 starts opening 0.0 s
- PV21, PV22 starts to close 0.0 s
/closing time 4 s/
- break valve open 0.1 s
- transient for power is initiated at 11.6 MPa
/power v time, see Table 1./
- modelling of the pump coast down is initiated at 9.47 MPa
/closing current v. time of valve PV11, see Table 2./
- HPIS flow initiated at 11.6 MPa
/flow rate v. time see Table 3./
- SG secondary side relief valve PV23
 - opening pressure 5.4 MPa
 - closing pressure 5.0 MPa
 - the flow rate was limited by an orifice, with a diameter of 6.0 mm

2.3 End of the test

The test was terminated at 997 s

2.4 Other data

The pressure distribution applied to the calculation is given in Table 4.

The flow diagram of the facility and the measurement locations are given in 2.1 and 2.2 respectively.

3. Code information and physical models used

3.1 Problems of nodalization

The nodalization scheme applied to the calculations is given in Fig. 3.1.

The number of nodalization elements applied to the scheme is presented in Table 5. Several schemes of higher number of elements were investigated to obtain the right values for them.

In order to get, however, an acceptable computer time and for the neglitation of numerical oscillations, the number of volumes and heat slabs were reduced to 19 and 16, respectively.

The nodalization scheme applied to the calculations is given in Fig. 3.1 and further informations are presented in Table 6.

Slabs S1 - S5 are core heat slabs, while the heat capacity of the steatit is represented by slabs S12 - S14.

3.2 Physical models and options used

For the calculations the standard RELAP4 program option with minimal controls /ISPROG = 0/ was used. For the heat transfer coefficients the HTS2, the new MOD6 blowdown correlation package was chosen.

At the break junction the Henry-Fauske/HEM explicit critical flow model /JCHOKE=5/ with critical flow model dial:

flow rate multipliers: 0.95
transition quality: 0.02

was selected.

The enthalpy transport model was used for the steady state calculation only /until 10 s/.

Vertical slip model was applied for junctions:

J13, J5, J6, J8, J9, J19, J20, J10, J11

In the bubble rise model for volumes /see Table 6./ the used values of bubble density gradient /Alph/ and bubble velocity /Vbub/ are shown in Table 7.

3.3 Computer type and main characteristics of the calculations

The characteristics of calculation and code performance are given in Table 8.

3.4 Remarks on the steady-state calculation

RELAP4/mod6 has no ability to calculate the initial steady-state conditions. Several trial runs have been performed in order to set up the input for the final run, especially the correct amount of heat transferred in the steam generator was difficult to achieve. In the final calculation the break was opened at 10 s that allowed disturbances provoked by incoherent input data to smooth out. /E.g. SG power changed from 718 to 647 kW in this period/. All data were within the error band of measured parameters at break initiation.

4. Results of the calculation

The results of the calculation are presented in Figs. 4.1 to 4.46. Figure numbers correspond to plot numbers as required by the Specification Report [1]. Note that Figs. 4.2 and 4.4 are missing since the heated part of the fuel rod simulators was modelled by three heat slabs only. /Figs. 4.1, 4.3 and 4.5/.

Figs. 4.34 to 4.46 present additional information supposed to be important in the assessment.

Section 7 gives a complete list of figures along with the units used for additional plots.

Results of the calculation are discussed in the next section, while major occurrences, as required by the Specification Report, are summarized in Table 9.

5. Discussion

The transient process initiated by the break on top of the downcomer is characterized by fast initial depressurization /Figs. 4.14, 4.15/. However, until the pressurizer runs empty it pushes sufficient water to the system to avoid flashing in any other part of the loop. Afterwards, steam appears in the hot leg, hot collector of the steam generator and the vessel head resulting in continuously sinking mixture levels in these volumes /Figs. 4.40, 4.41 and 4.34, respectively/.

In this period primary pressure is dictated by secondary pressure, but the hot leg loop seal plays an important role as well. The loop seal starts to vent steam at 61.5 s, at the same time, when the vessel mixture level drops to the elevation of the hot leg and this results in steam condensation on the steam generator primary side with a subsequent pressure decrease.

Until the pump is stopped there isn't much change in the situation described above, only at about 85 s the level in the SG cold collector /Fig. 4.39/ starts to decrease. Thus it can be stated that pump operation results in high mixture level in the reactor vessel, while most of the hot leg and the part of the cold leg from SG to pump is voided. Also the neighbourhood of the break remains single phase.

The asymmetric levels brought about by the pump have a great influence on system behaviour after the pump is stopped. There is an immediate flow reversal in the core and the downcomer /Fig. 4.26/ that leads to a fast drop of the mixture level in the vessel. At 185 s the core starts to uncover and this first uncovering is quite violent as it can be seen from Figs. 4.35 to 4.37. This is why dryout occurs practically at the same time, /Figs. 4.3 and 4.5/ due to stagnating flow conditions, steam in the upper part of the core becomes superheated, Fig. 4.7.

At 200 s the cold leg loop seal starts to vent steam that leads to severe oscillation in the downcomer and cold leg flow rates, Figs. 4.26 and 4.27. Soon it also results in two-phase coolant conditions at the break, Fig. 4.28. However, it is only after break uncovering that mixture level in the core increases significantly and this also results in heater rod rewet.

According to the calculation the core level soon starts to decrease again and a second dryout occurs that lasts several hundred seconds. The rest of the transient is characterized by little change in the parameters, only the system pressure decreases continuously. After 600 s the HPIS compensates the slowly decreasing break flow and the core level increases again /Fig..4.37/. This finally leads to a decrease of the heater rod temperatures.

6. References

- [1] L. Szabados et al.: Specification for the PMK-NVH Standard Problem Exercise. Budapest, 1985.
- [2] L. Szabados: Scaling and Instrumentation of the PMK-NVH Facility. Specialists Meeting on Small Break LOCA Analyses in LWRs. Pisa /1985/ Vol.1.p.527.
- [3] L.Szabados, C.Almeida, L.Maróti: The PMK-NVH Facility and Ist Use for an IAEA Standard Problem Exrcise.SPM on SBLOCA Analyses in LWRs. Pisa /1986/
- [4] PMK-NVH Standard Problem Exercise. Additional Information to Participants. February 1st, 1986.
/Distributed by C.Almeida, 1986/
- [5] Measured Initial Conditions for the IAEA - PMK-NVH Standard Problem Test. Budapest-Vienna. May 1986.
/Distributed by C.Almeida, 1986./

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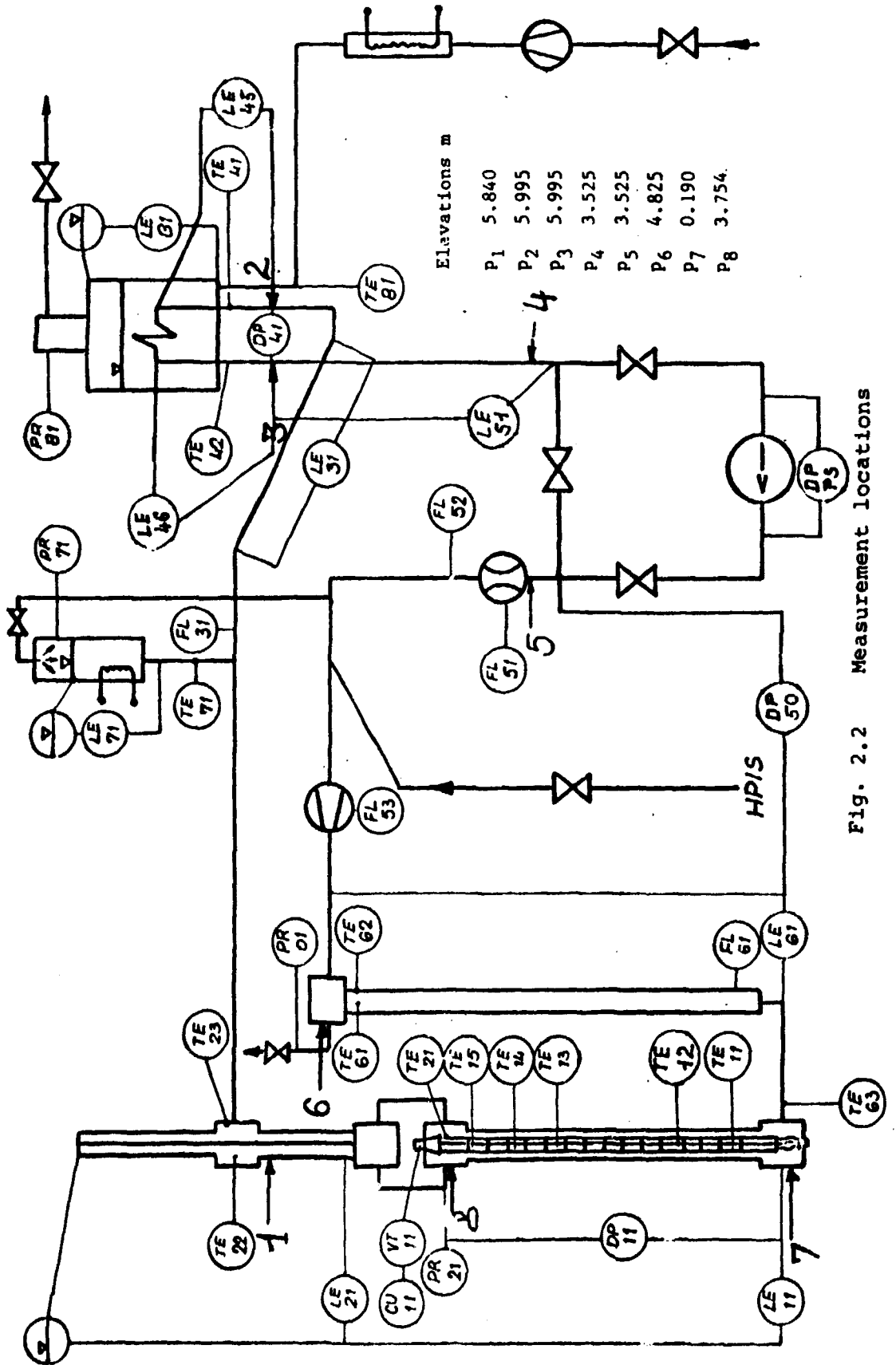


Fig. 2.2 Measurement locations

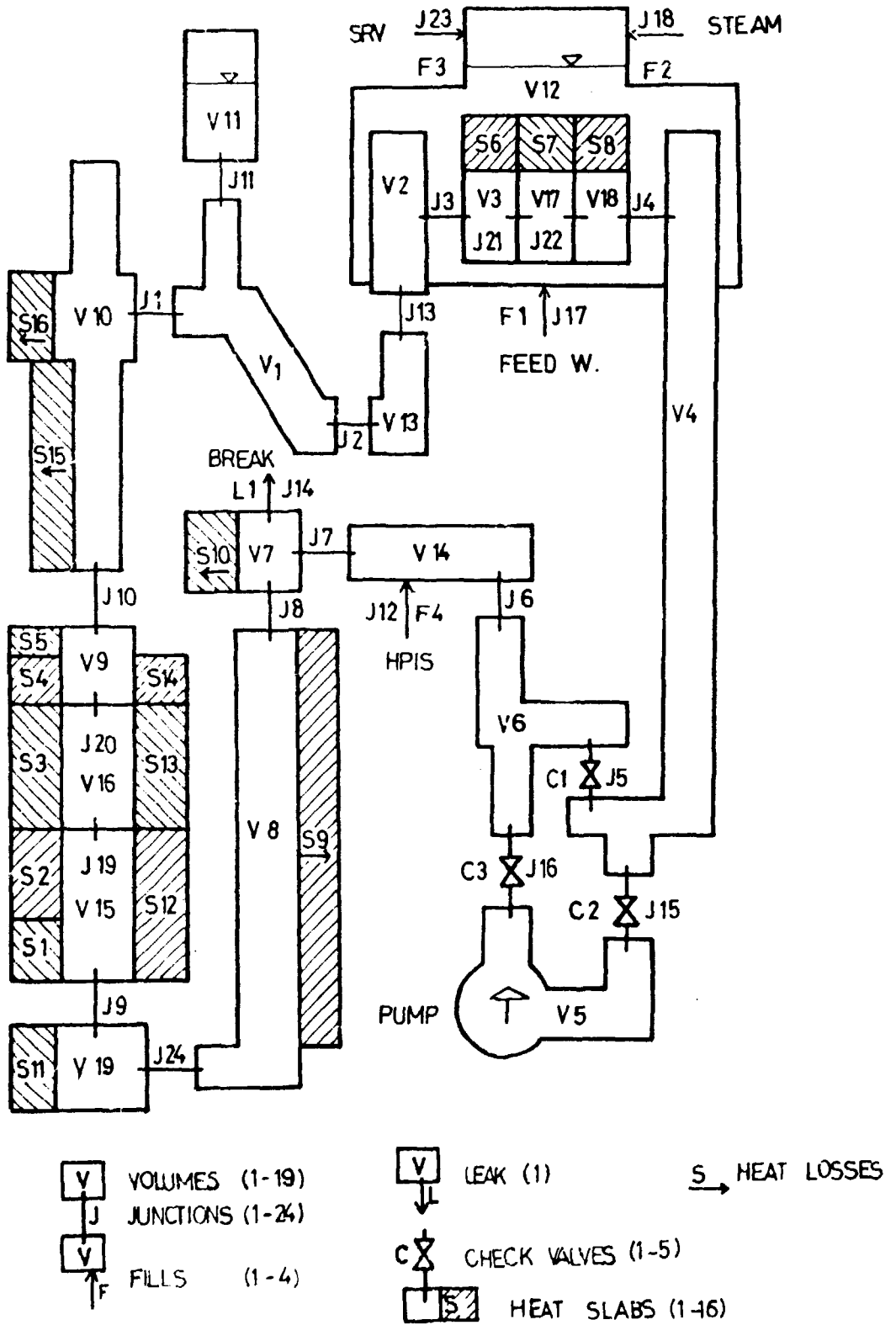


Fig. 3.1

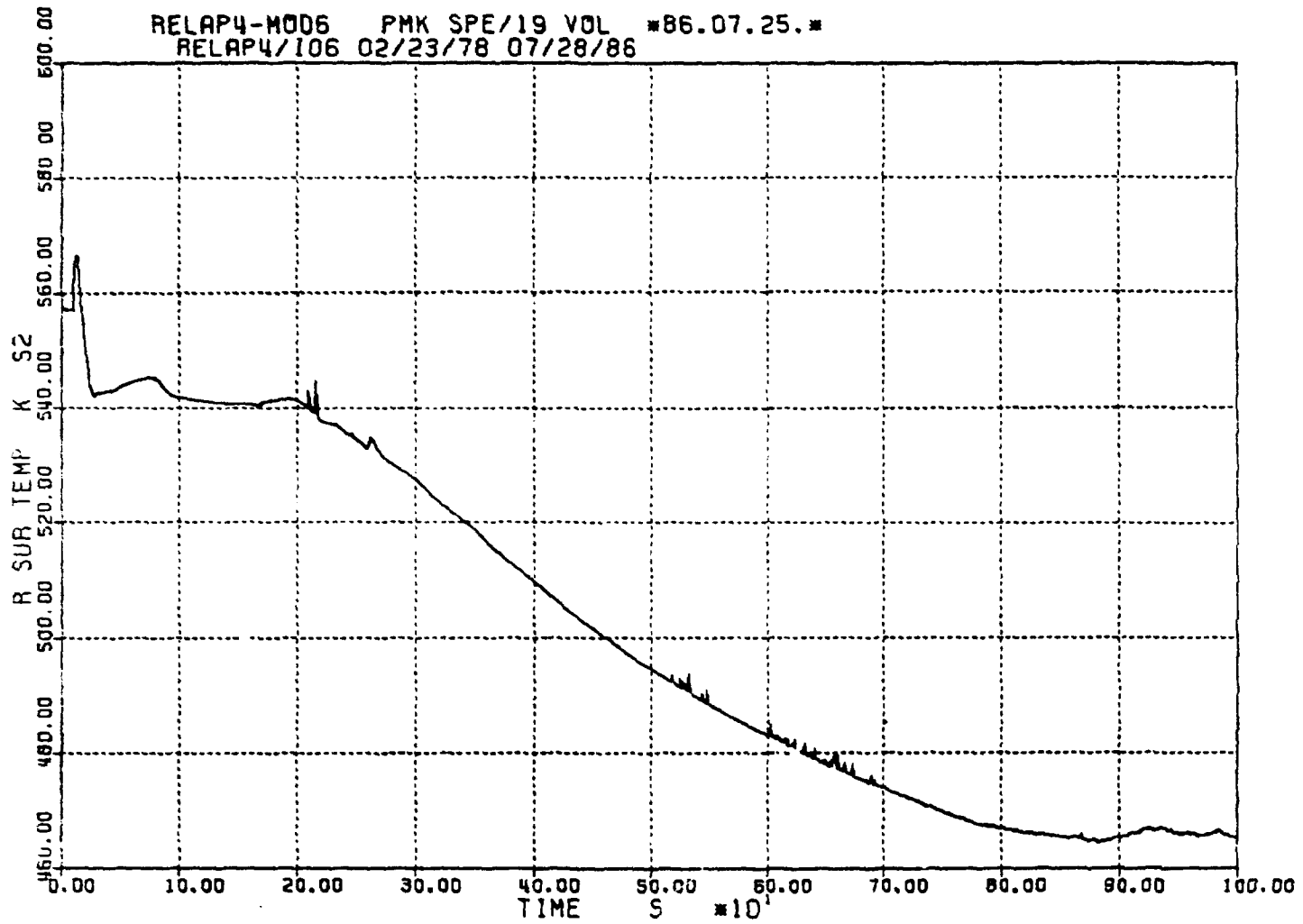


Fig. 4.1

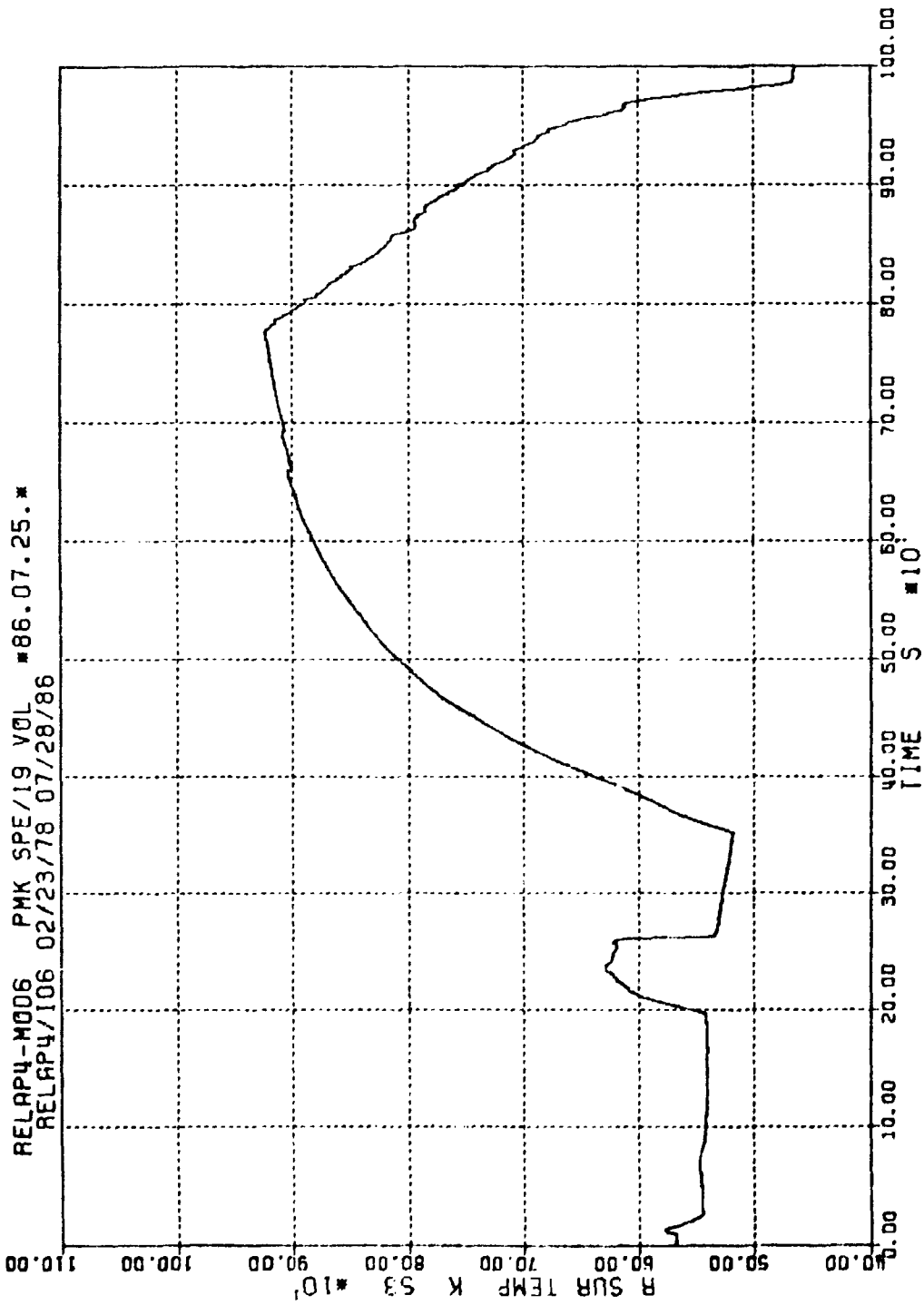


Fig. 4.3

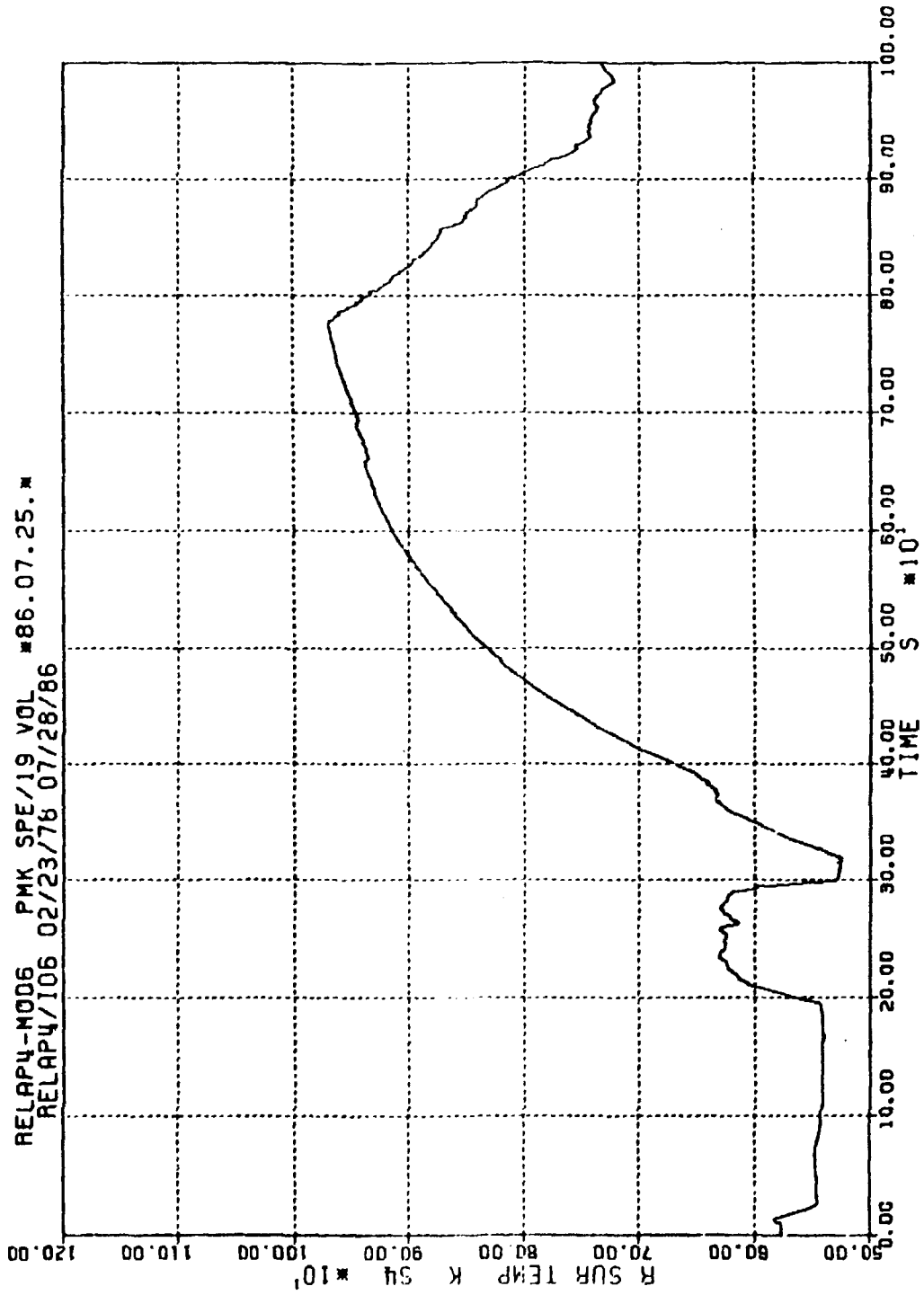


Fig. 4.5

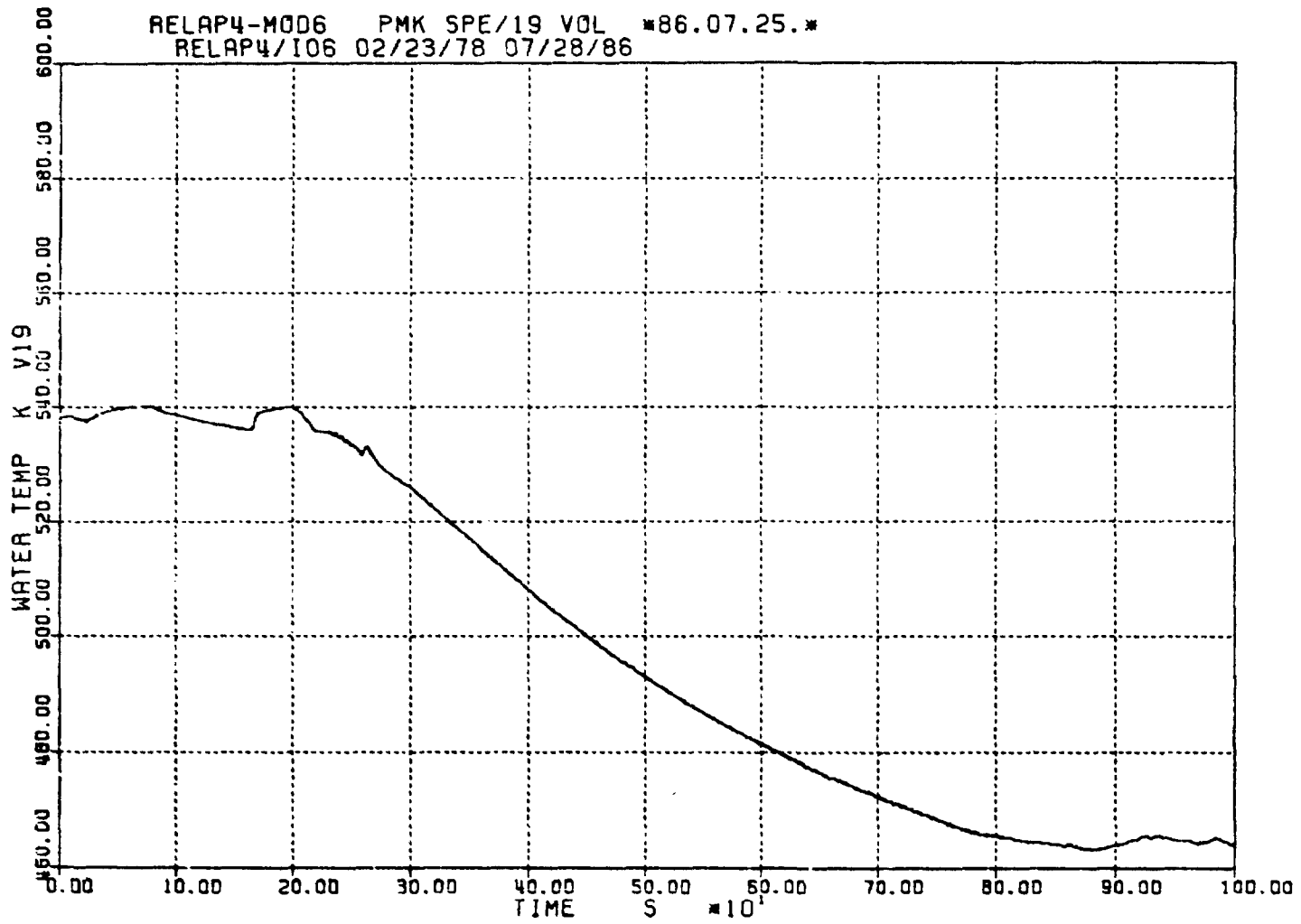


Fig. 4.6

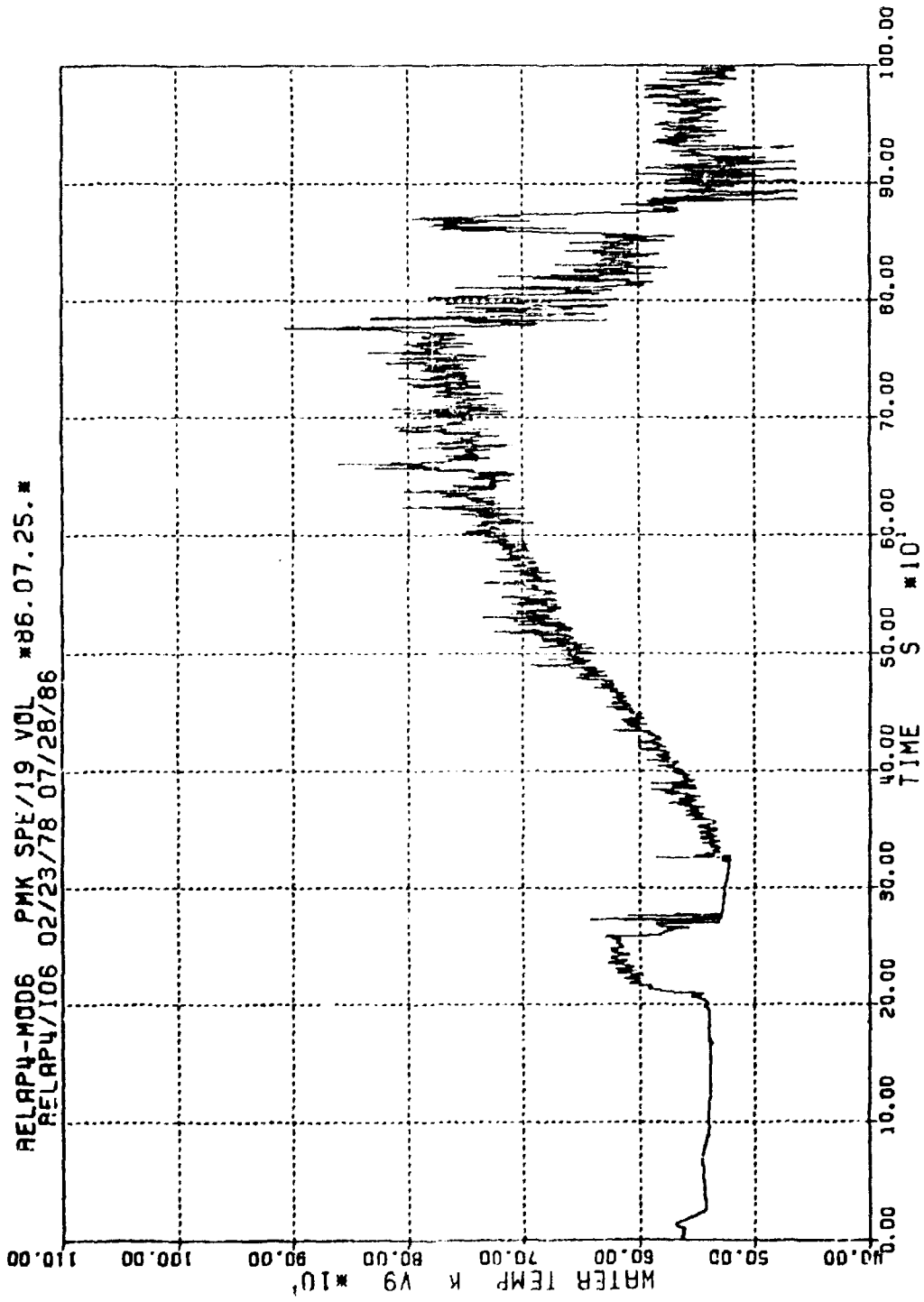


Fig. 4.7

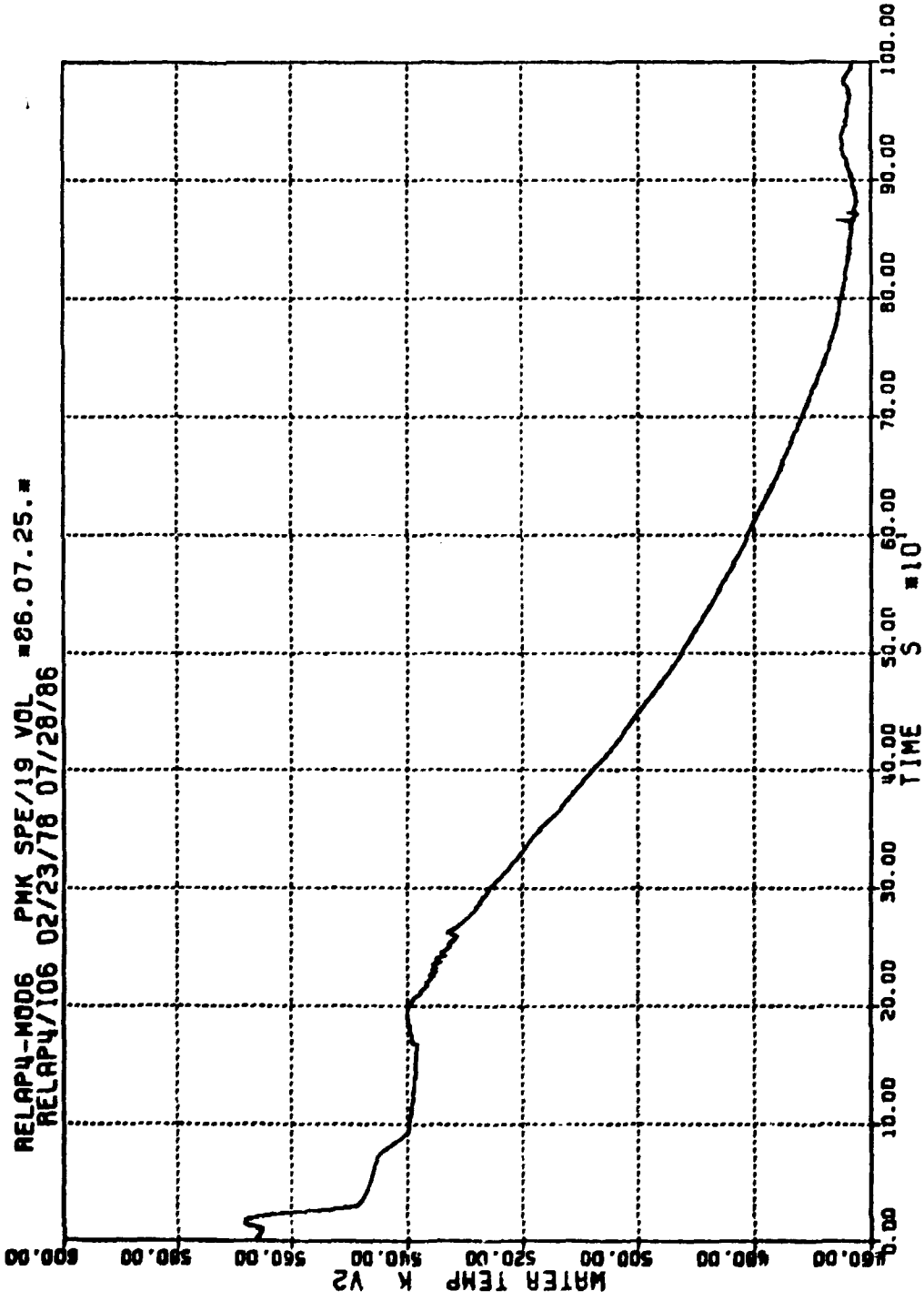


Fig. 4.8

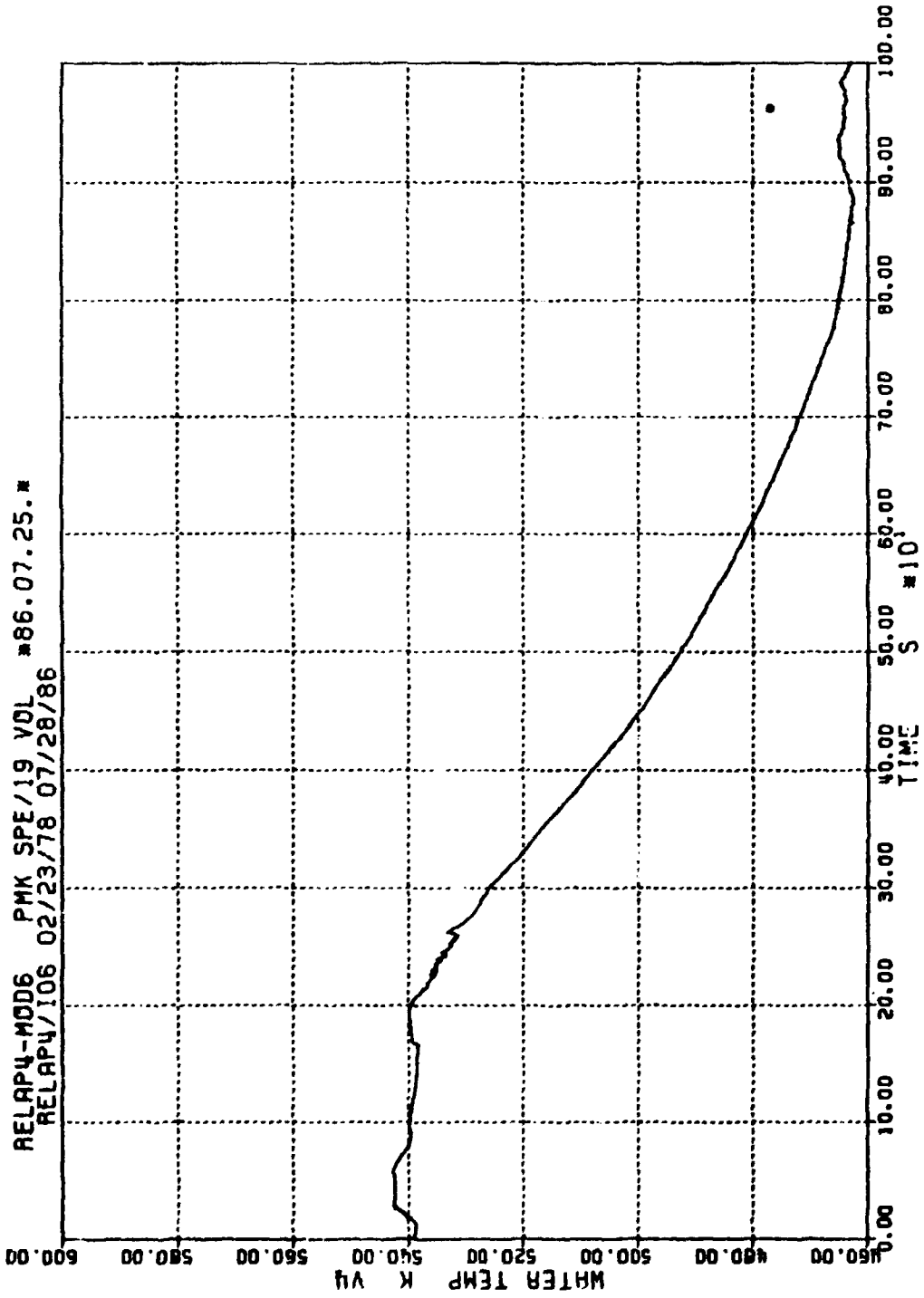


Fig. 4.9

RELAP4-MOD6 PMK SPE/19 VOL #86.07.25.*
RELAP4/I06 02/23/78 07/28/86

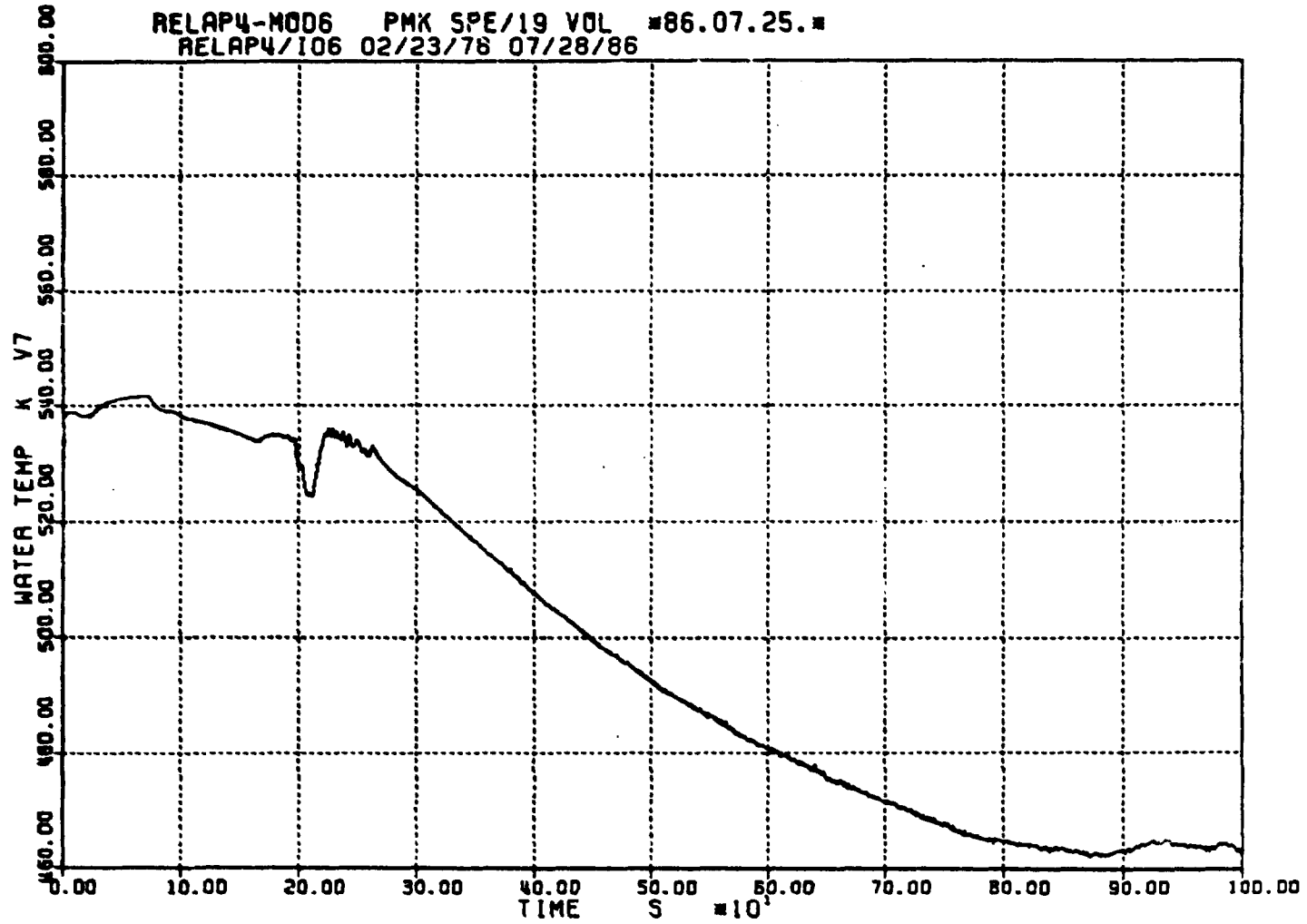


Fig. 4.10

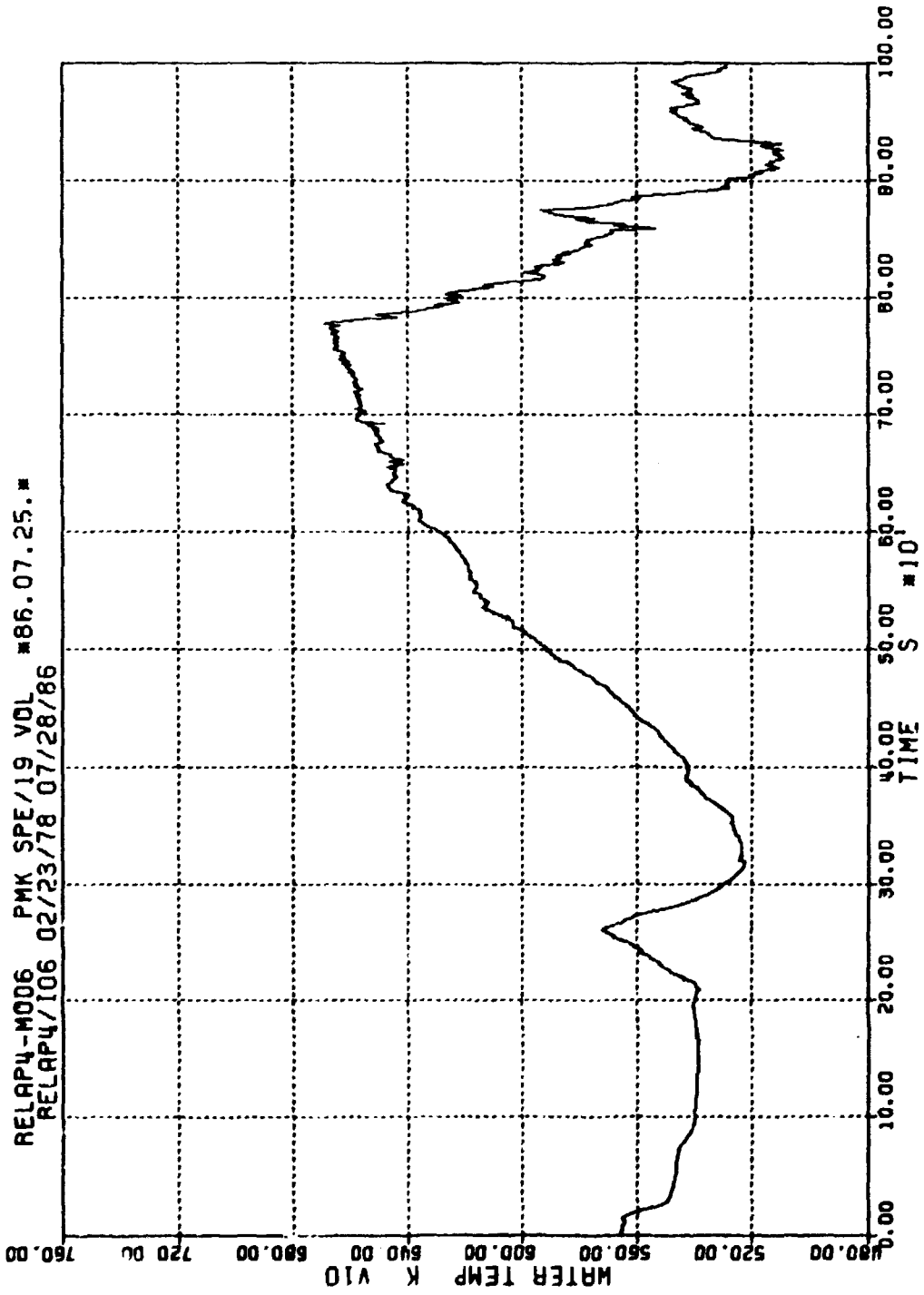


Fig. 4.11

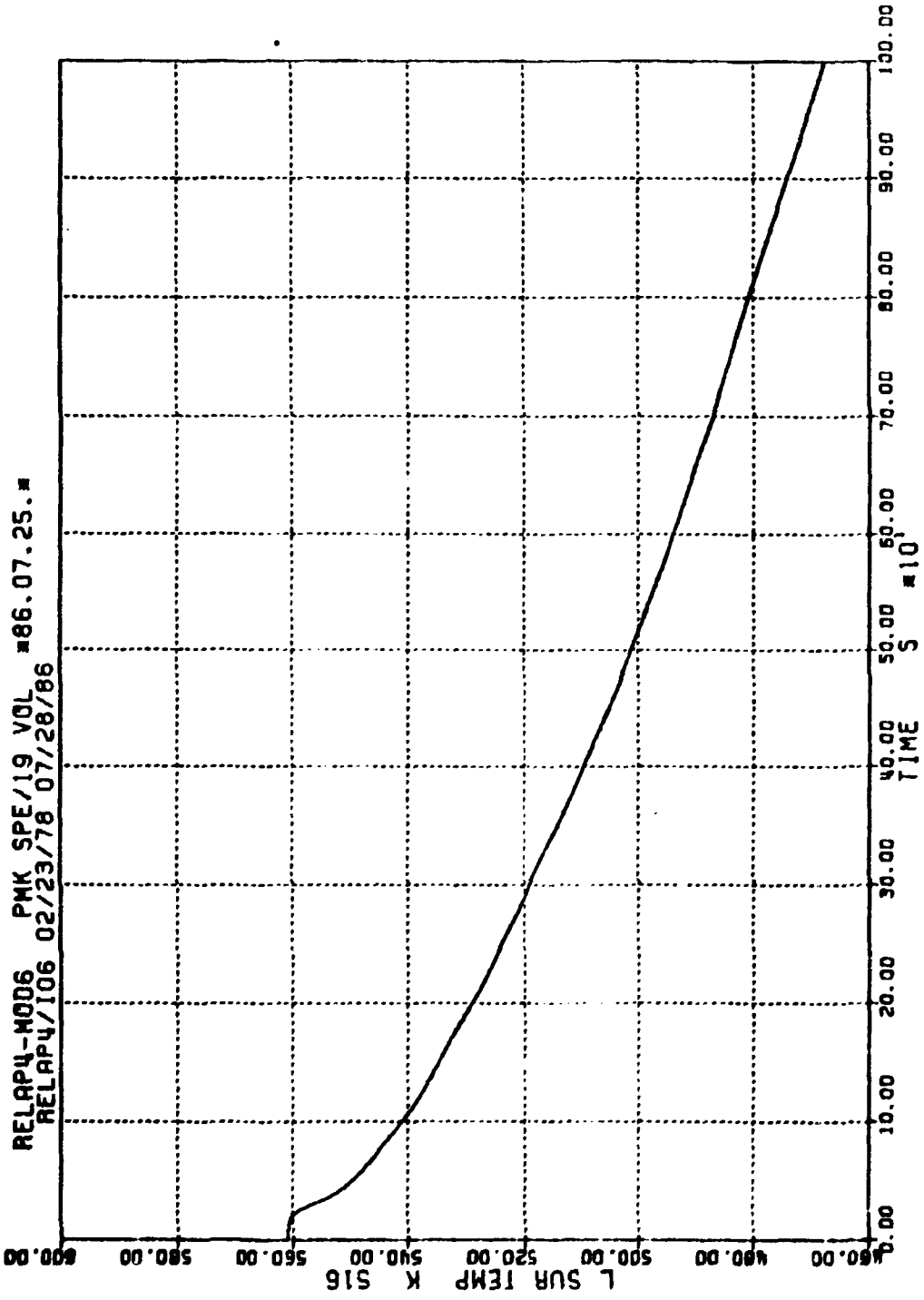


Fig. 4.12

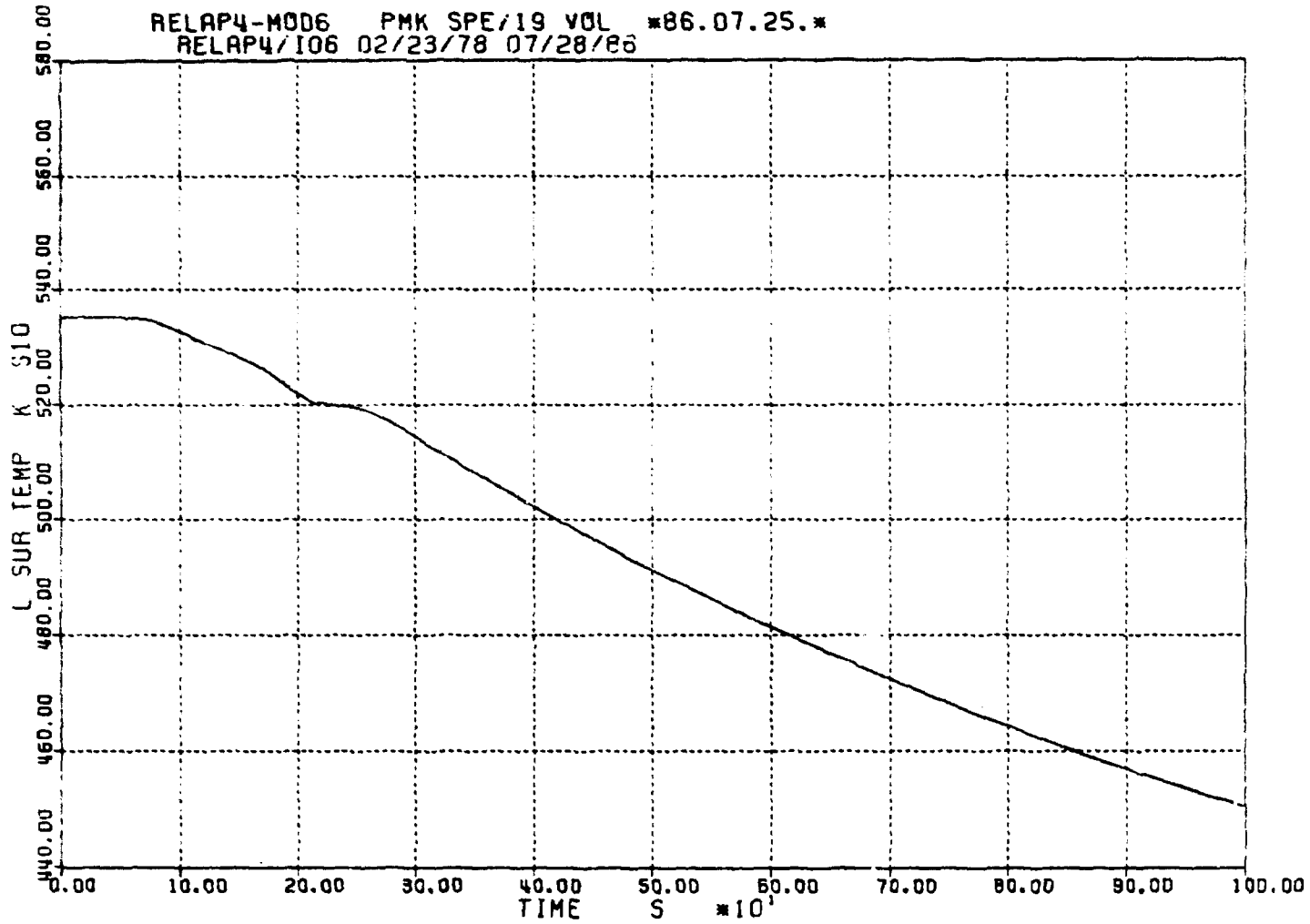


Fig. 4.13

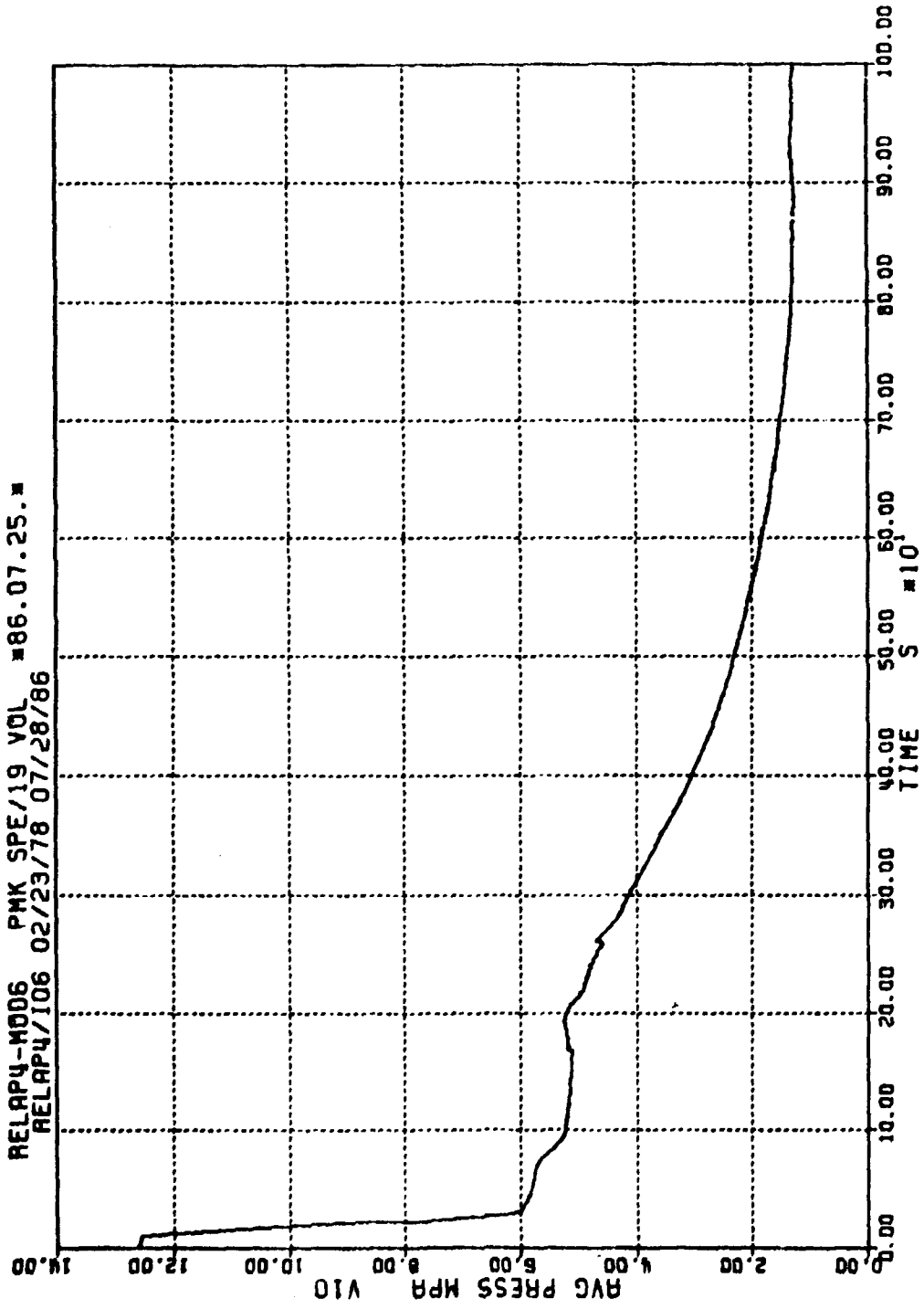


FIG. 4.14

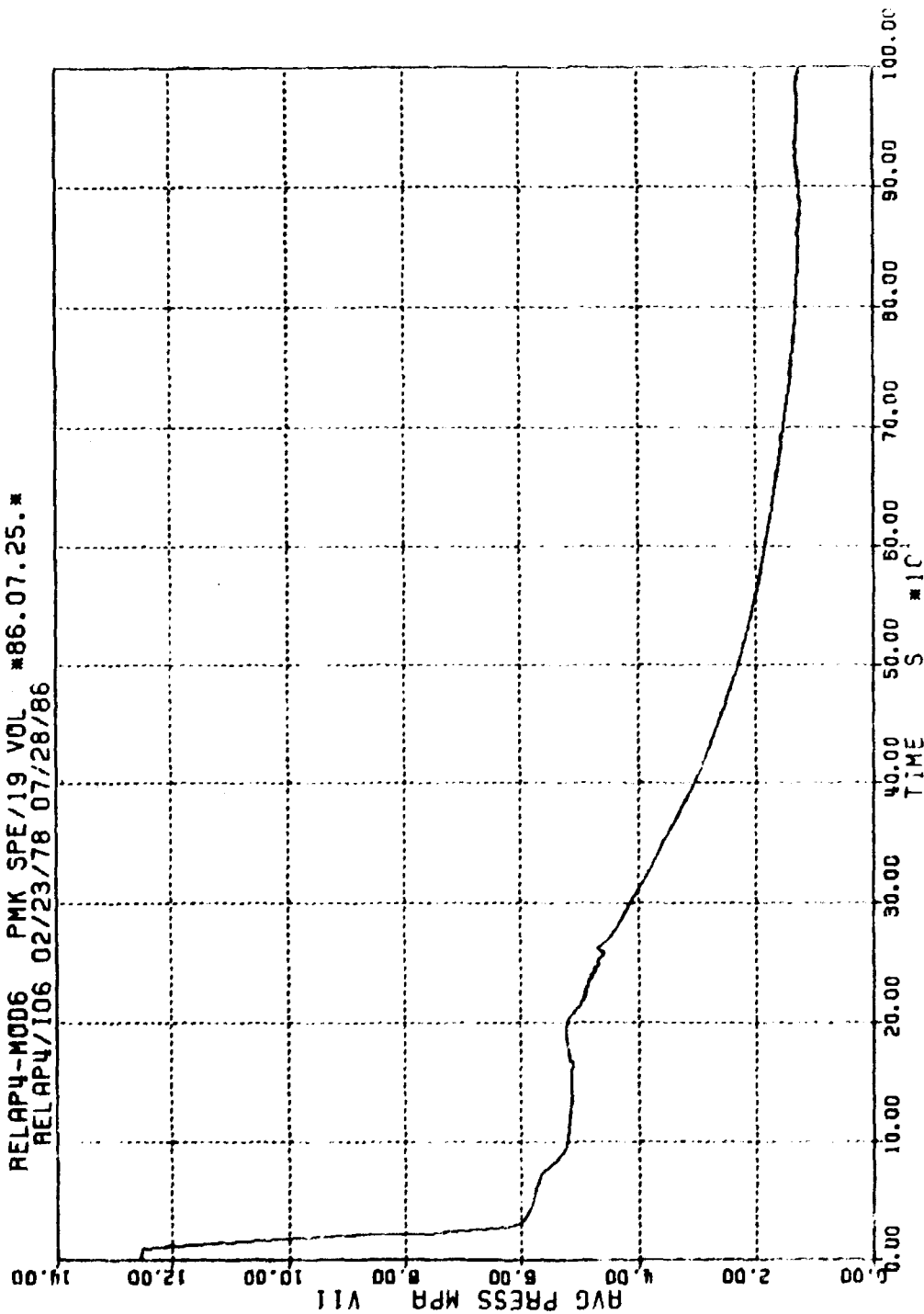


Fig. 4.15

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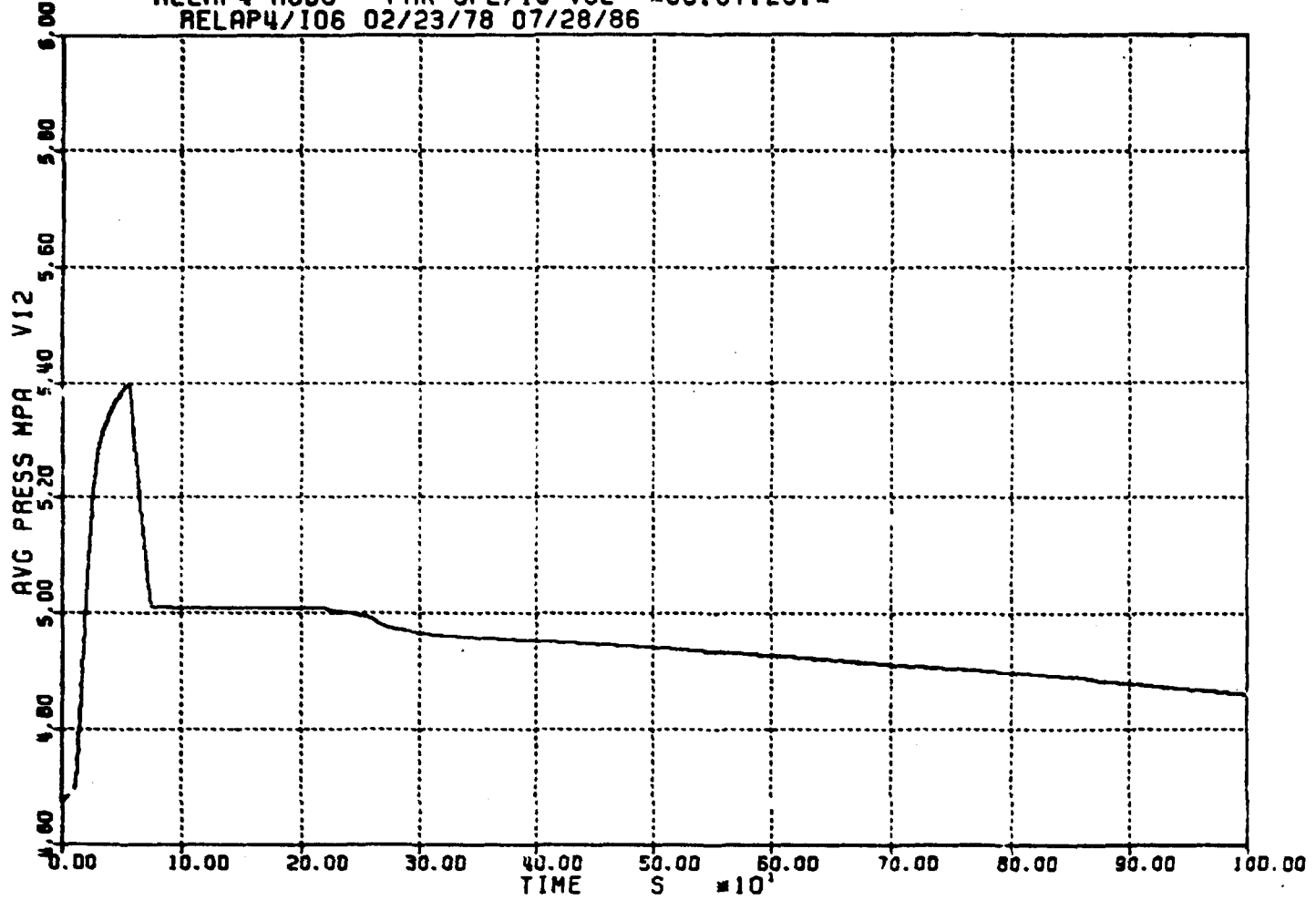


Fig. 4.16

RELAP4-M006 PMK SPE/19 VOL *86.07.25.*
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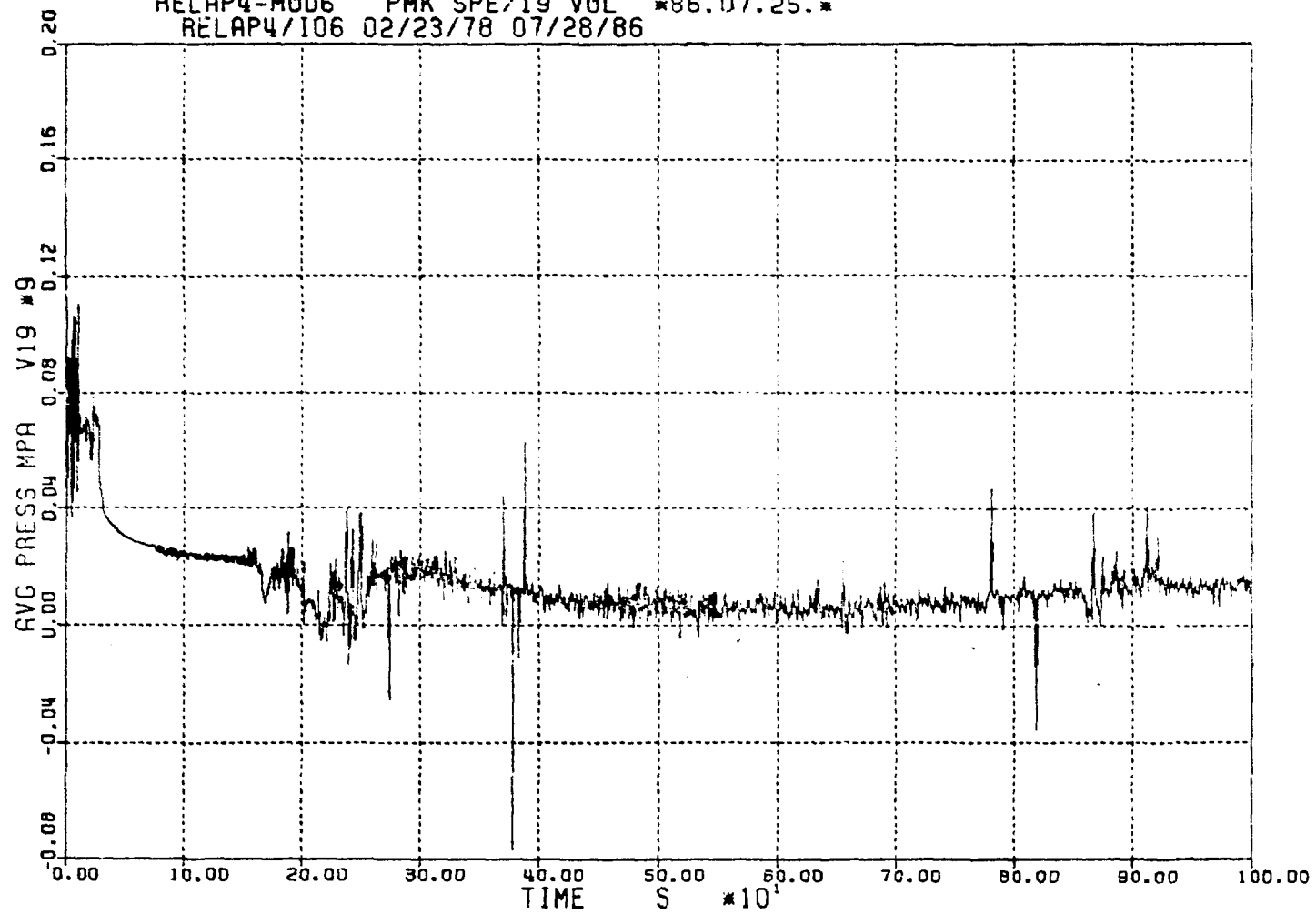


Fig. 4.17

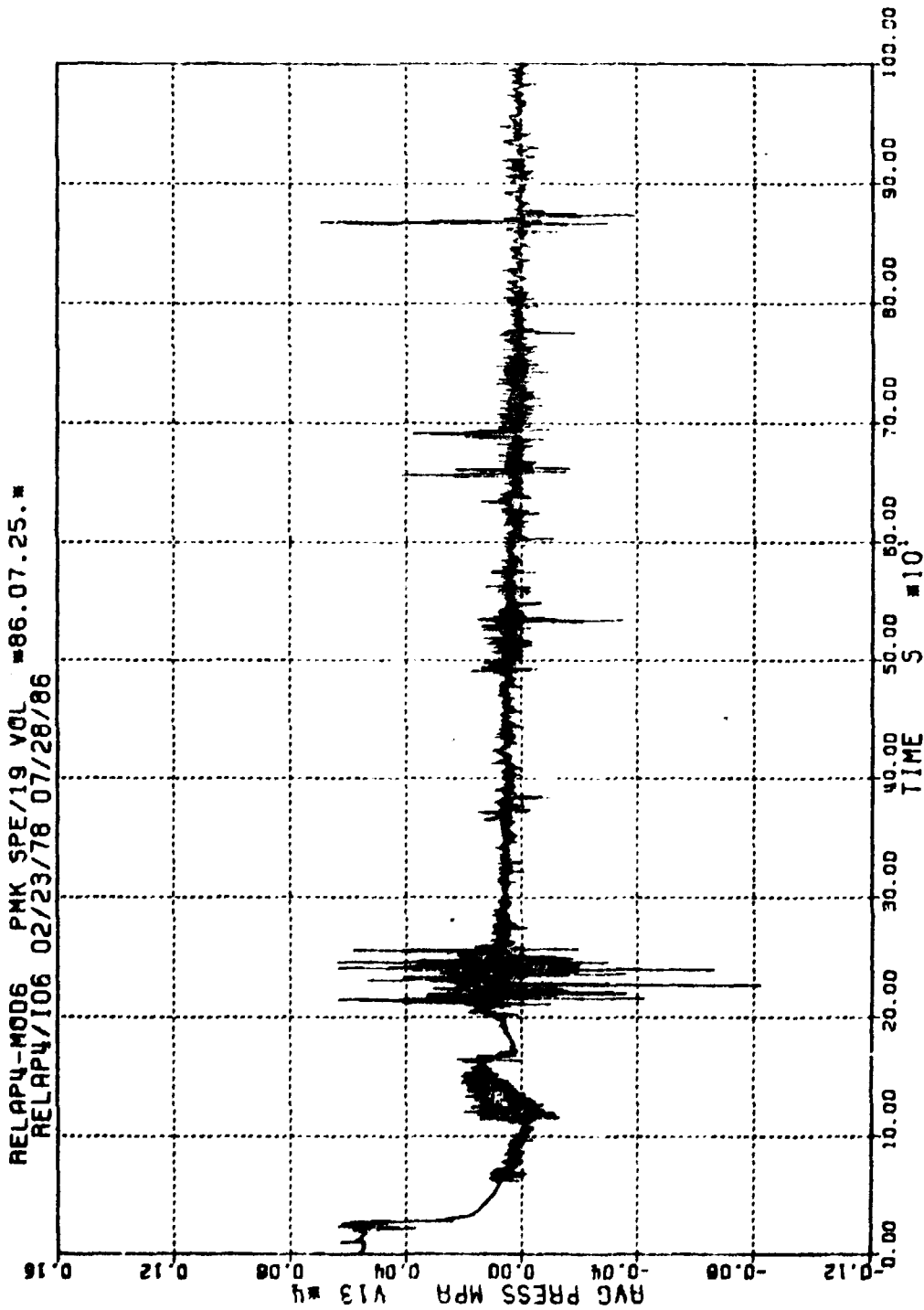


Fig. 4.18

IAEA--SPE 7.4% SBLOCA ON PMK--NVII

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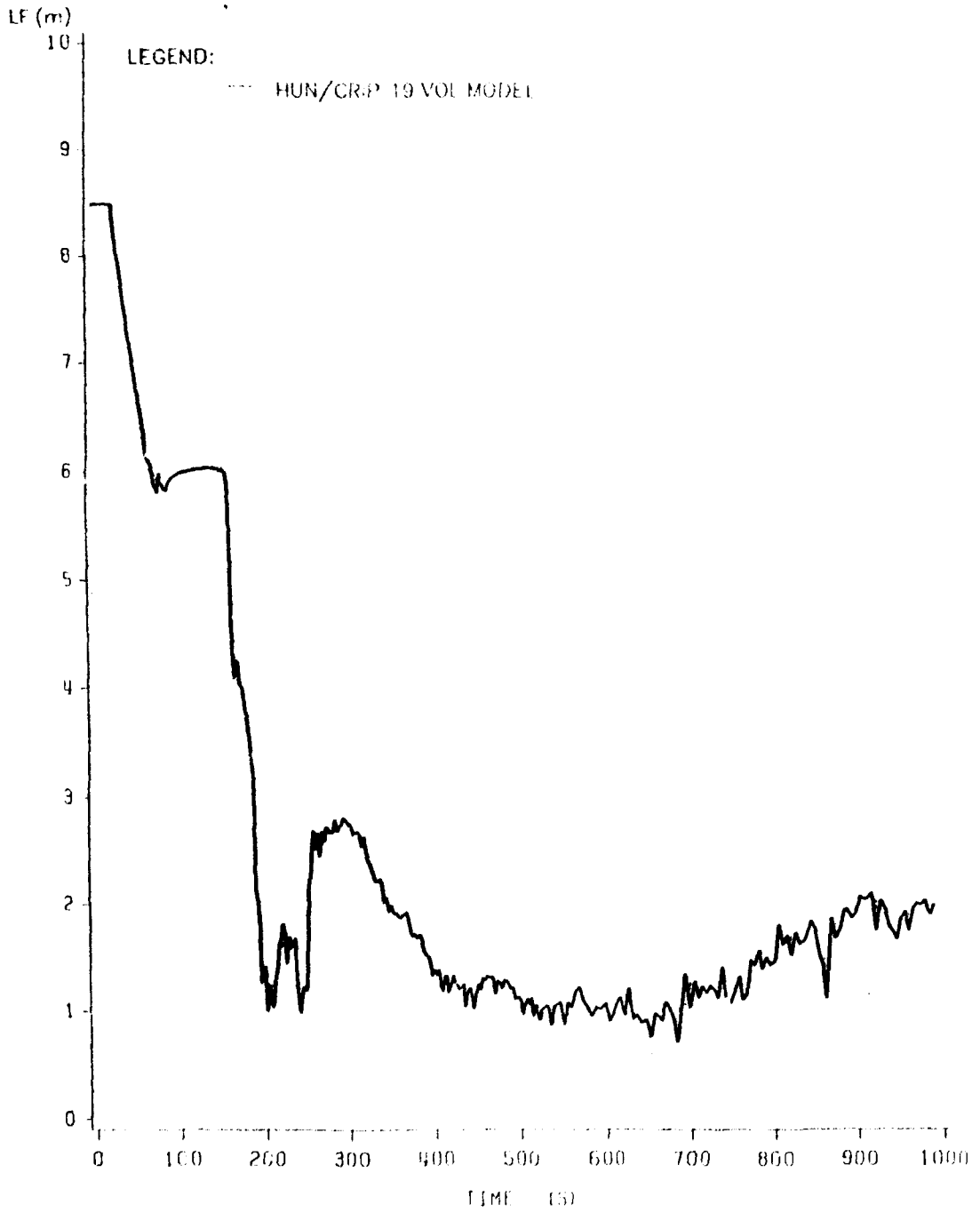


Fig. 4.19

IAEA -SPE 7.4% SBLOCA ON PMK-NVH
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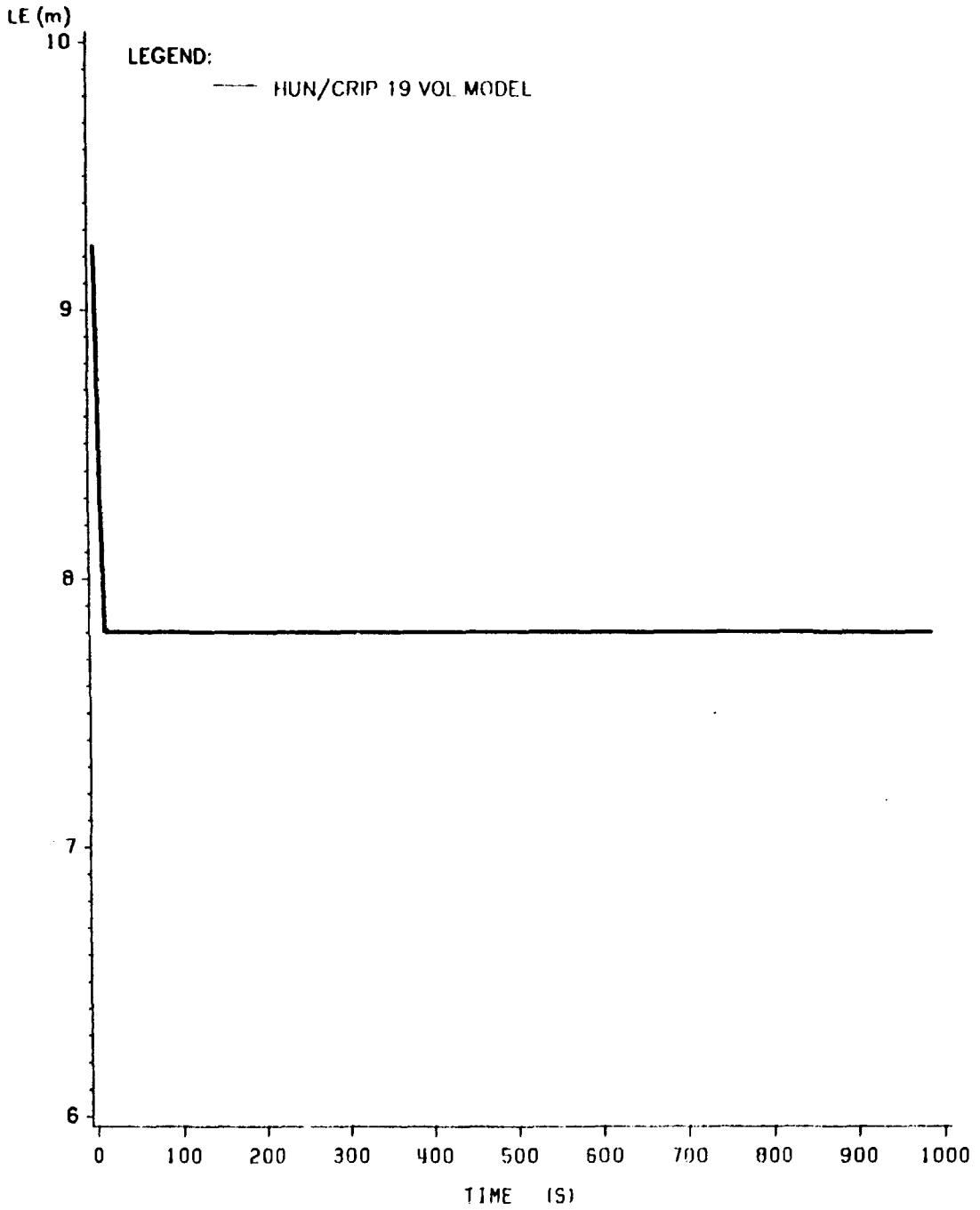


Fig. 4.20

IAEA-SPE 7.4% SBLOCA ON PMK-NVII
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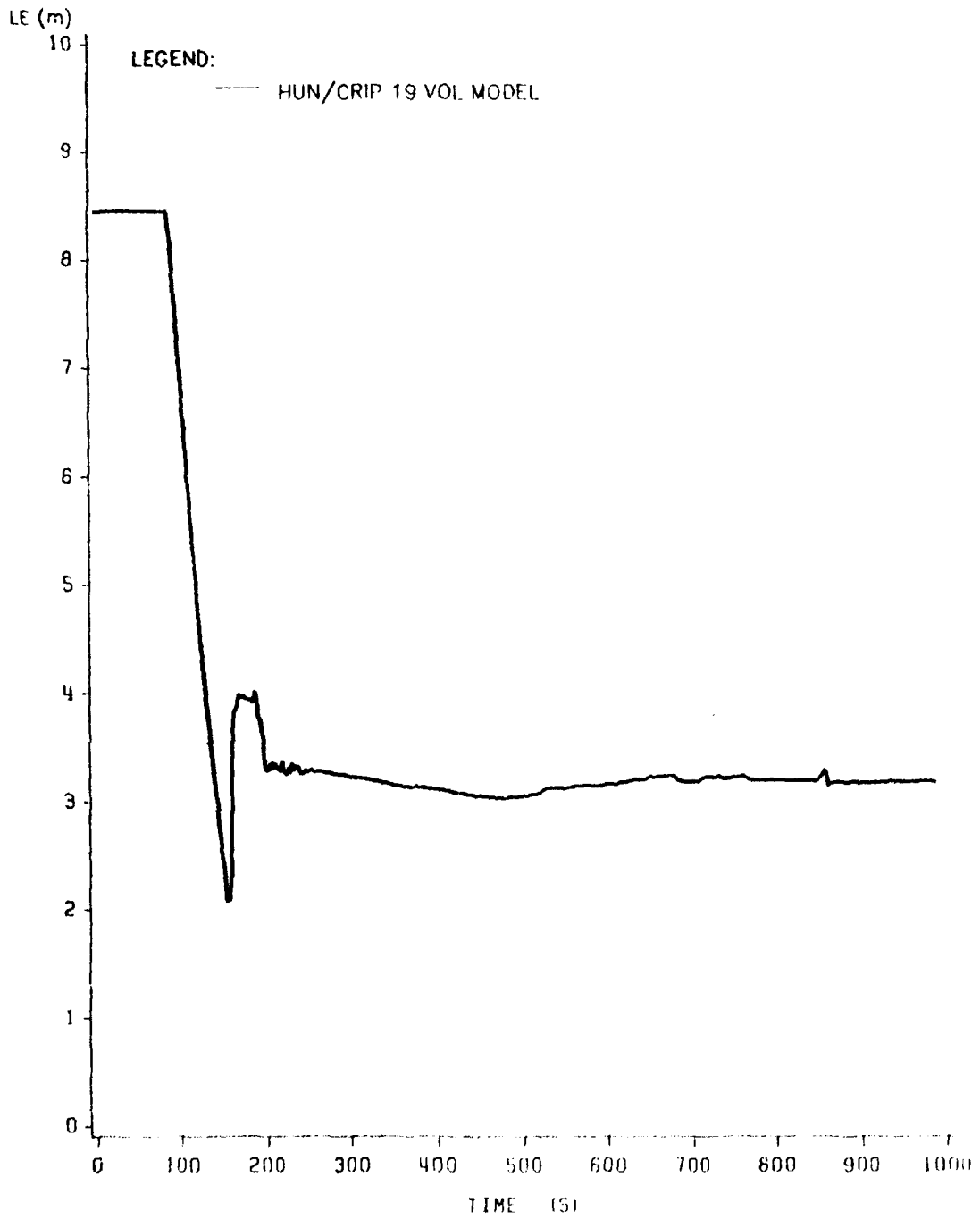


Fig. 4.21

IAEA-SPE 7.4% SBLOCA ON PMK-NVH
PLOTNO-22

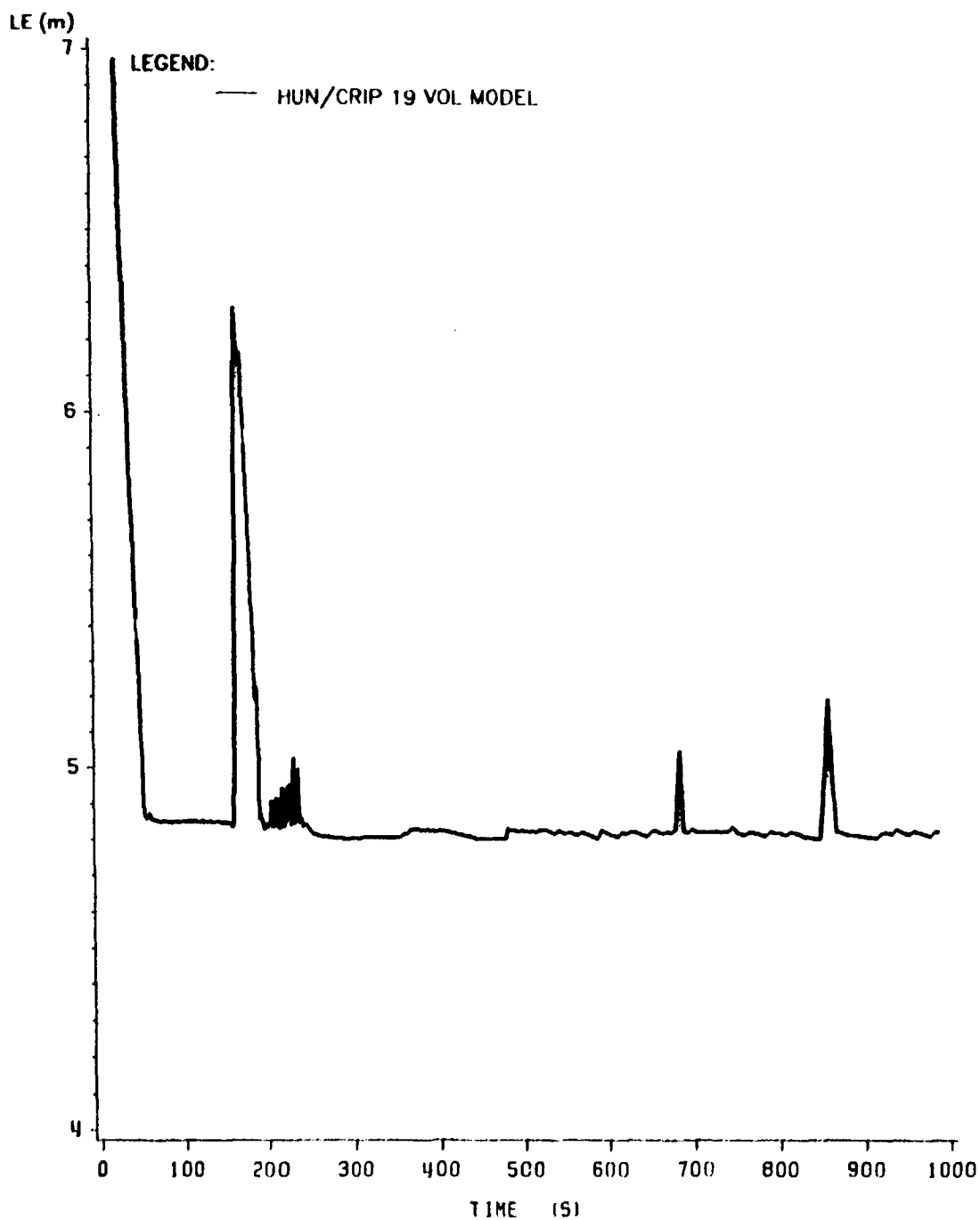


Fig. 4.22

IAEA- SPE 7.4% SBLOCA ON PMK--NVH
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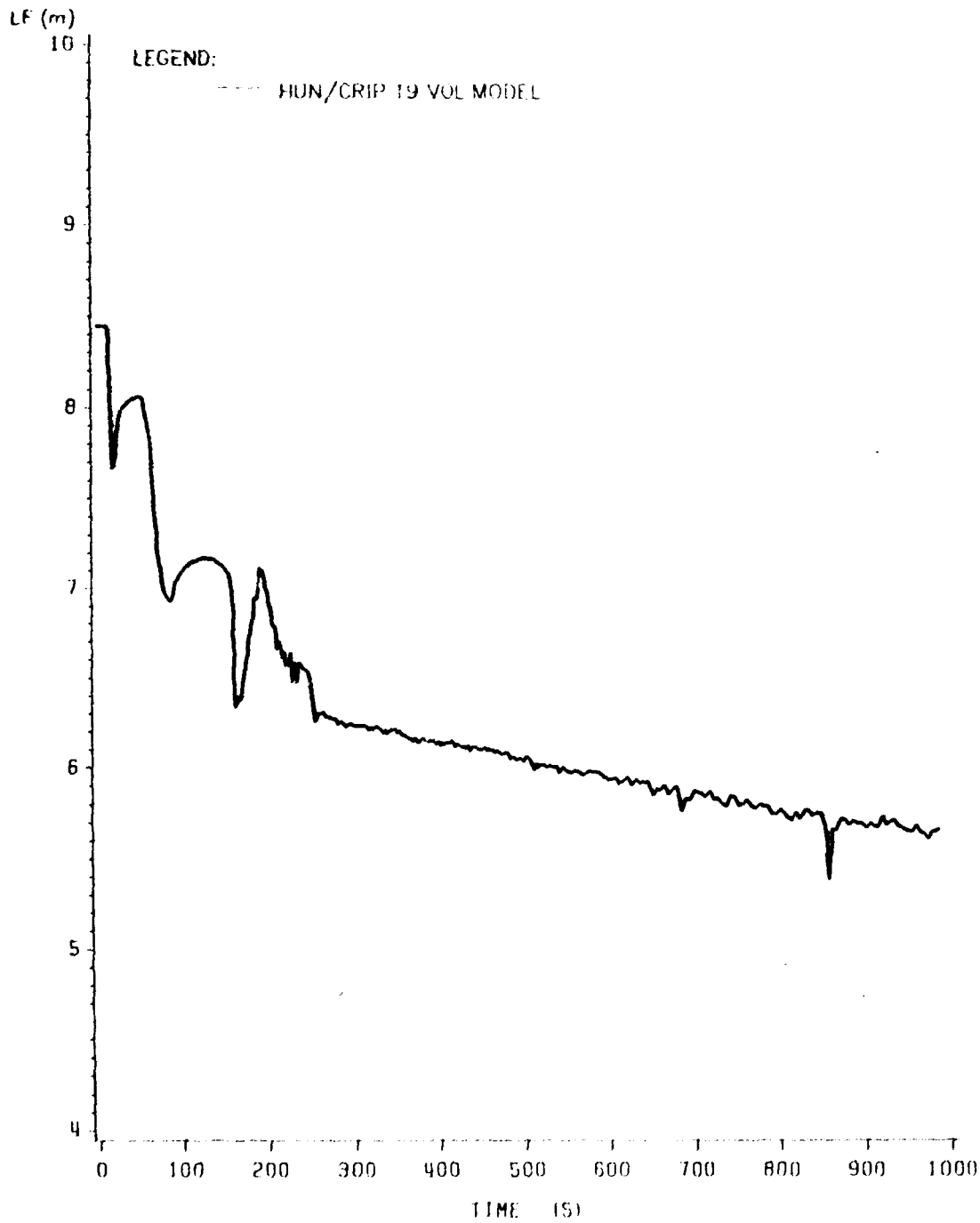


Fig. 4.23

IAEA-SPE 7.4% SBLOCA ON PMK-NVH

PLOTNO=24

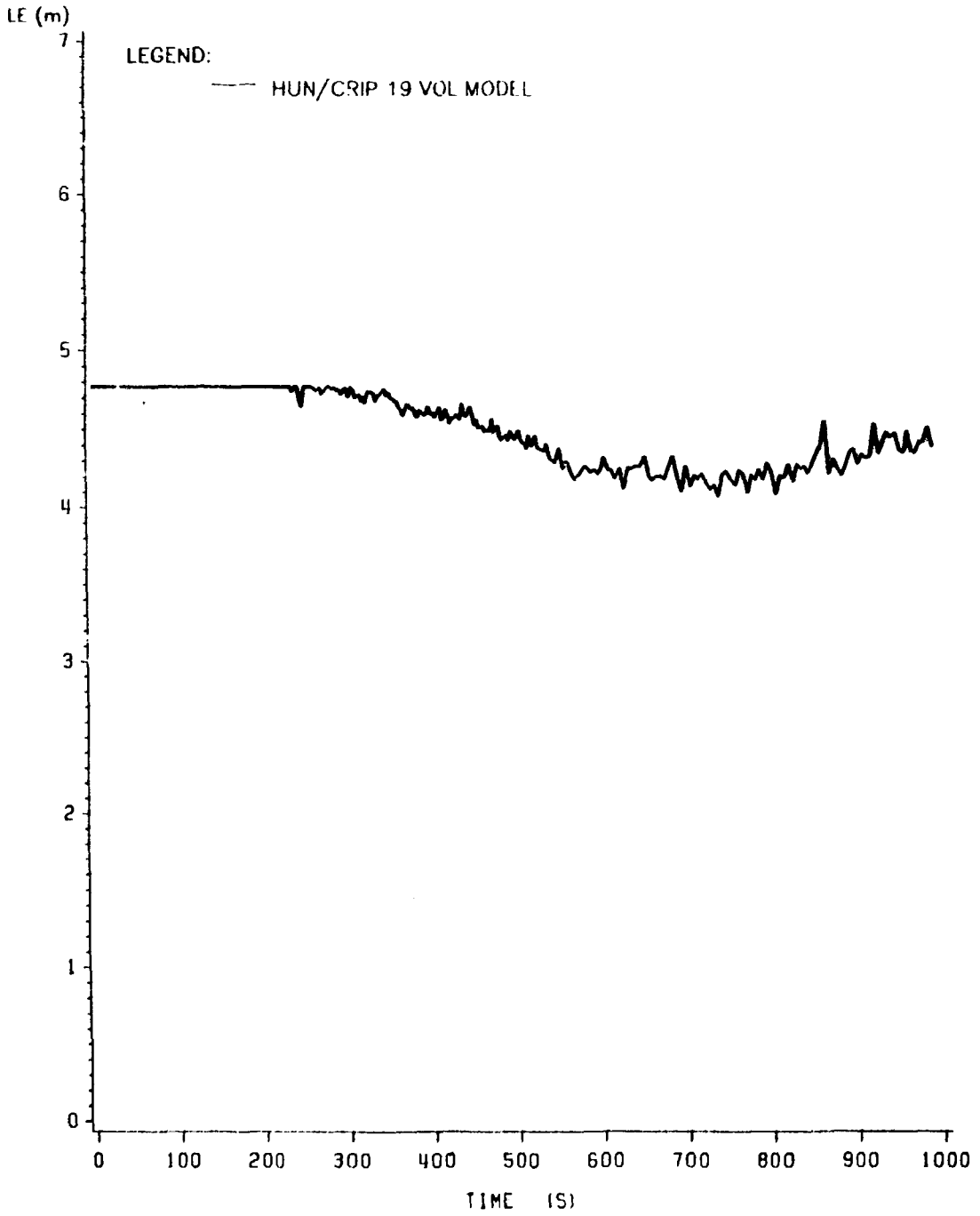


Fig. 4.24

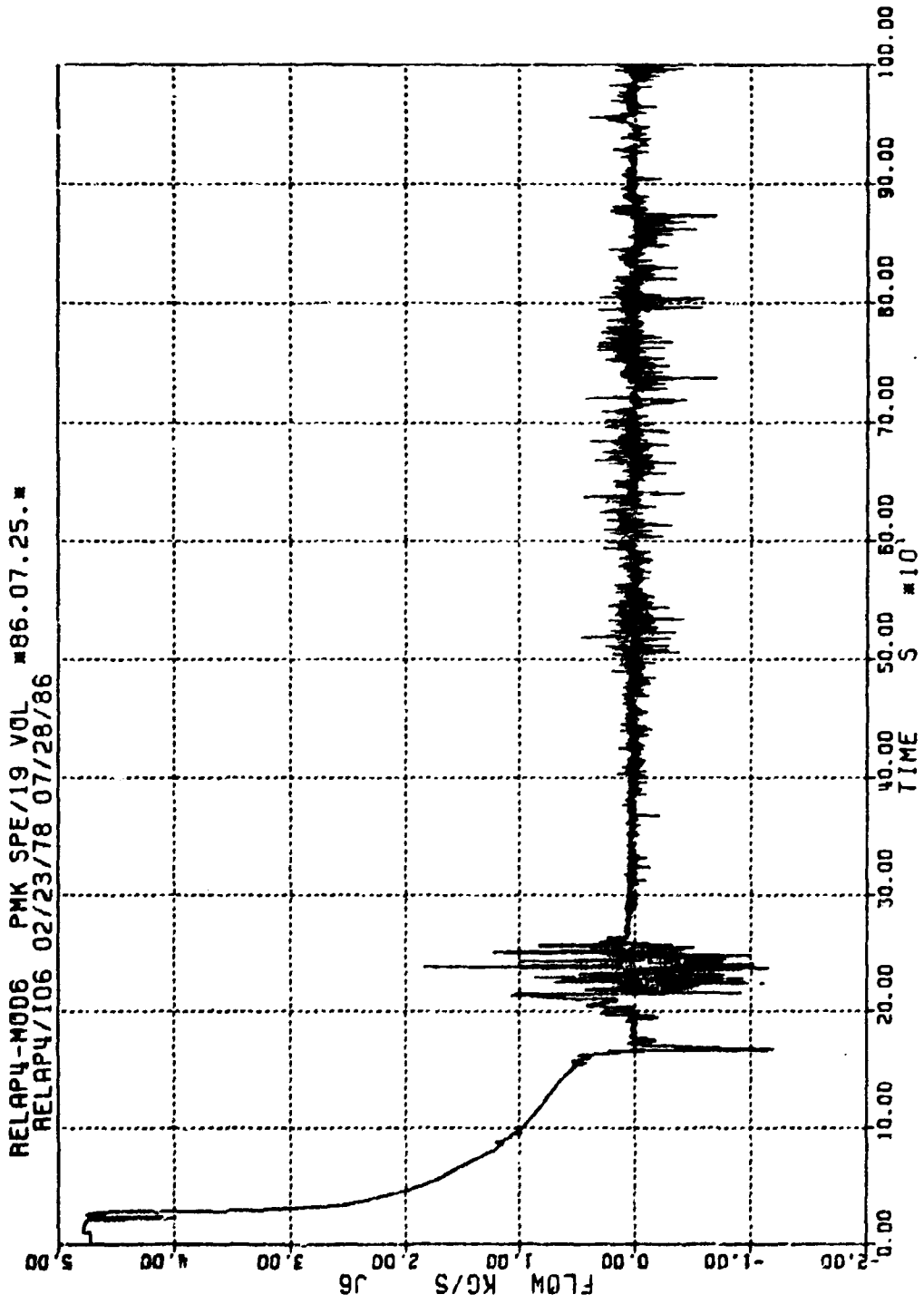


Fig. 4.25

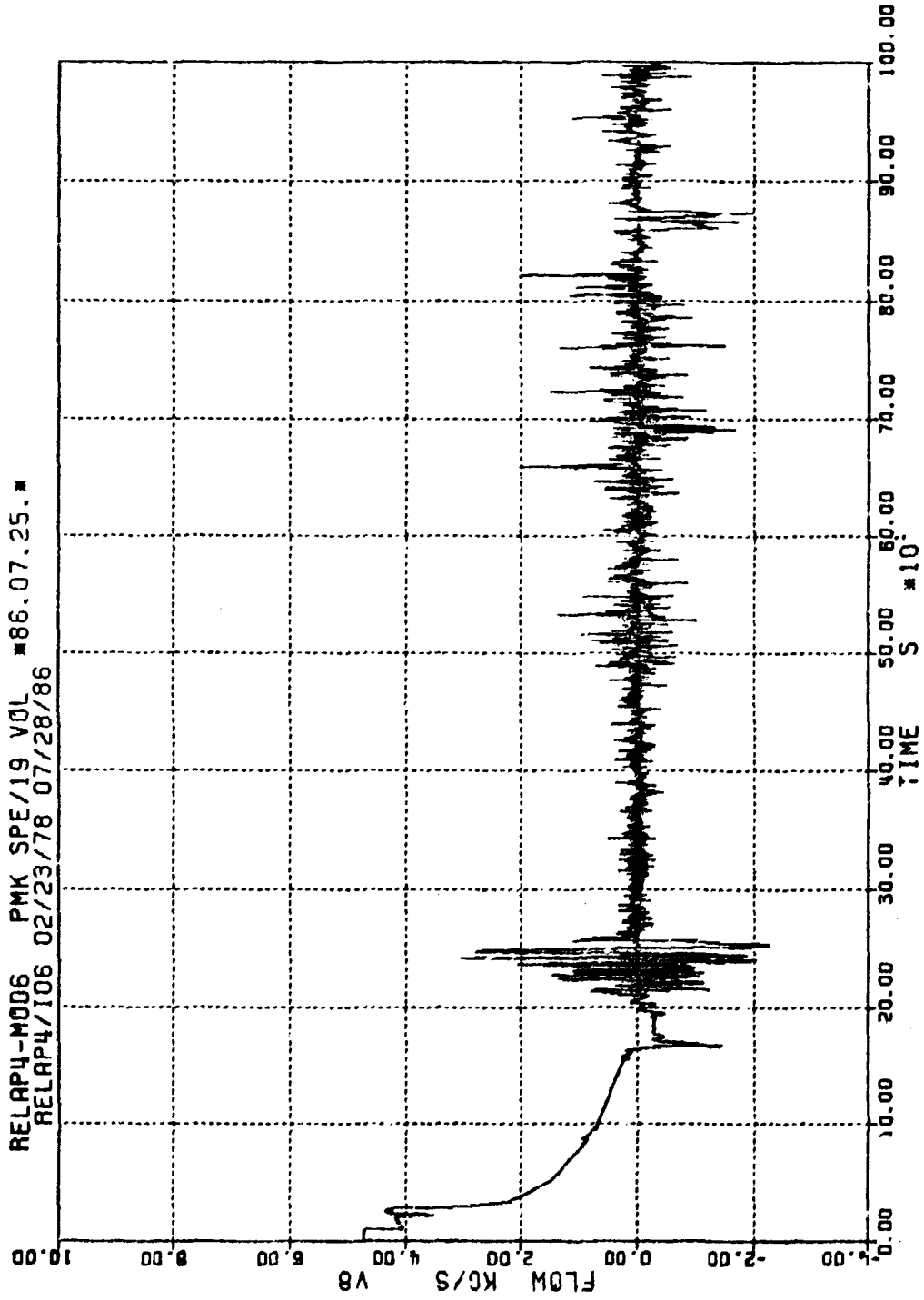


Fig. 4.26

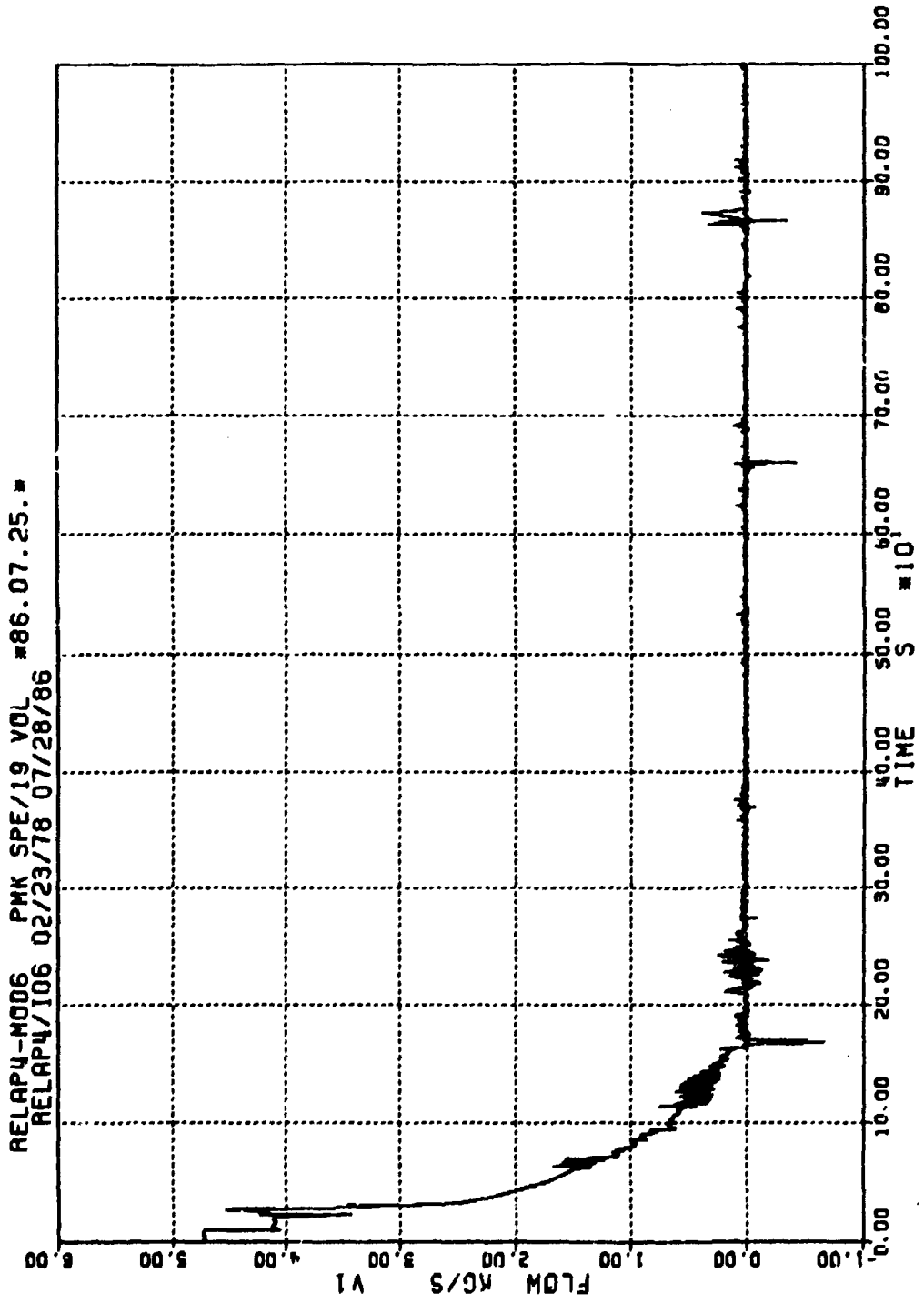


Fig. 4.27

RELAP4-MOD6 PMK SPE/19 VOL *86.07.25.*
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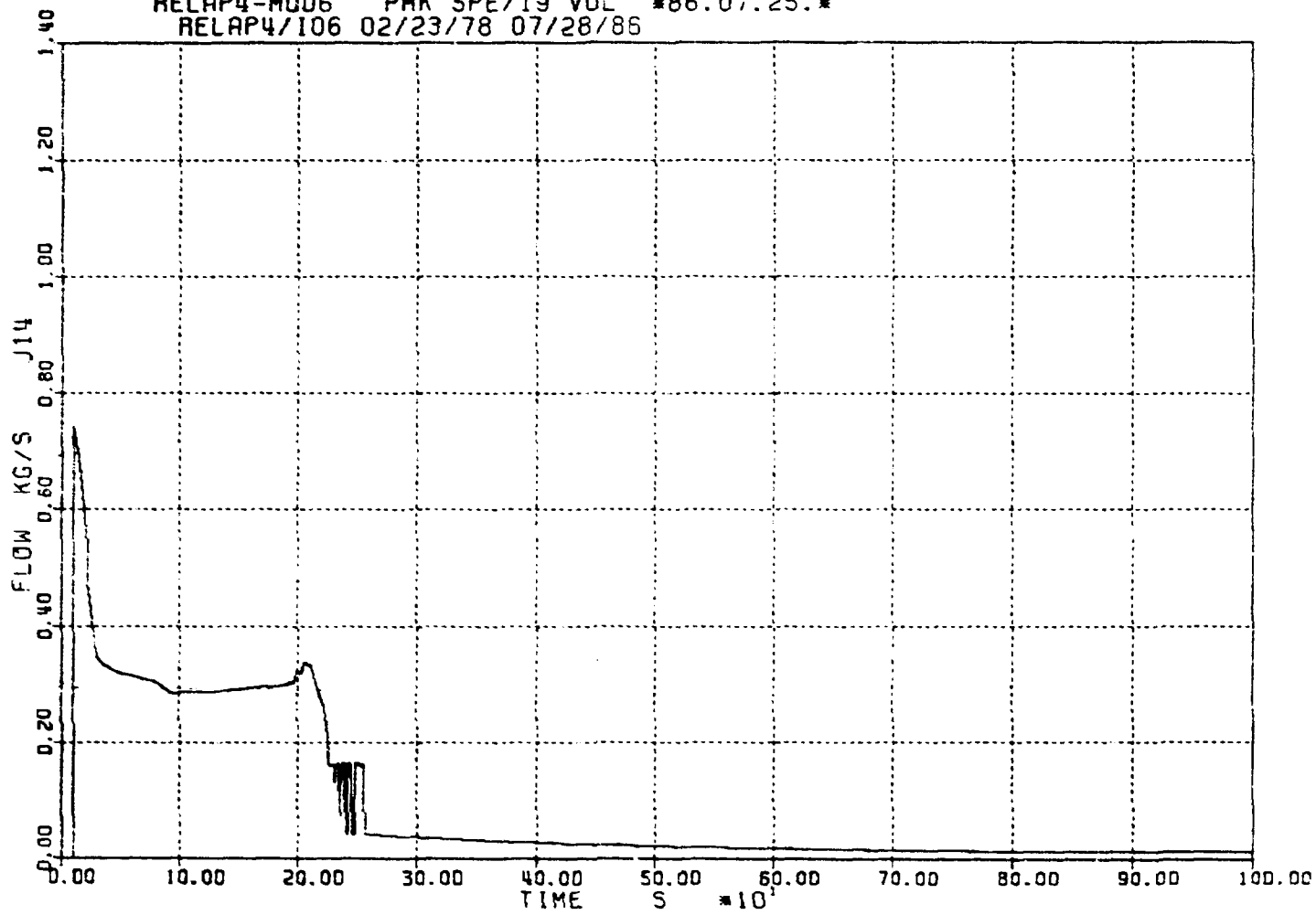


Fig. 4.28

IAEA-SPE 7.4% SBLOCA ON PMK-NVH

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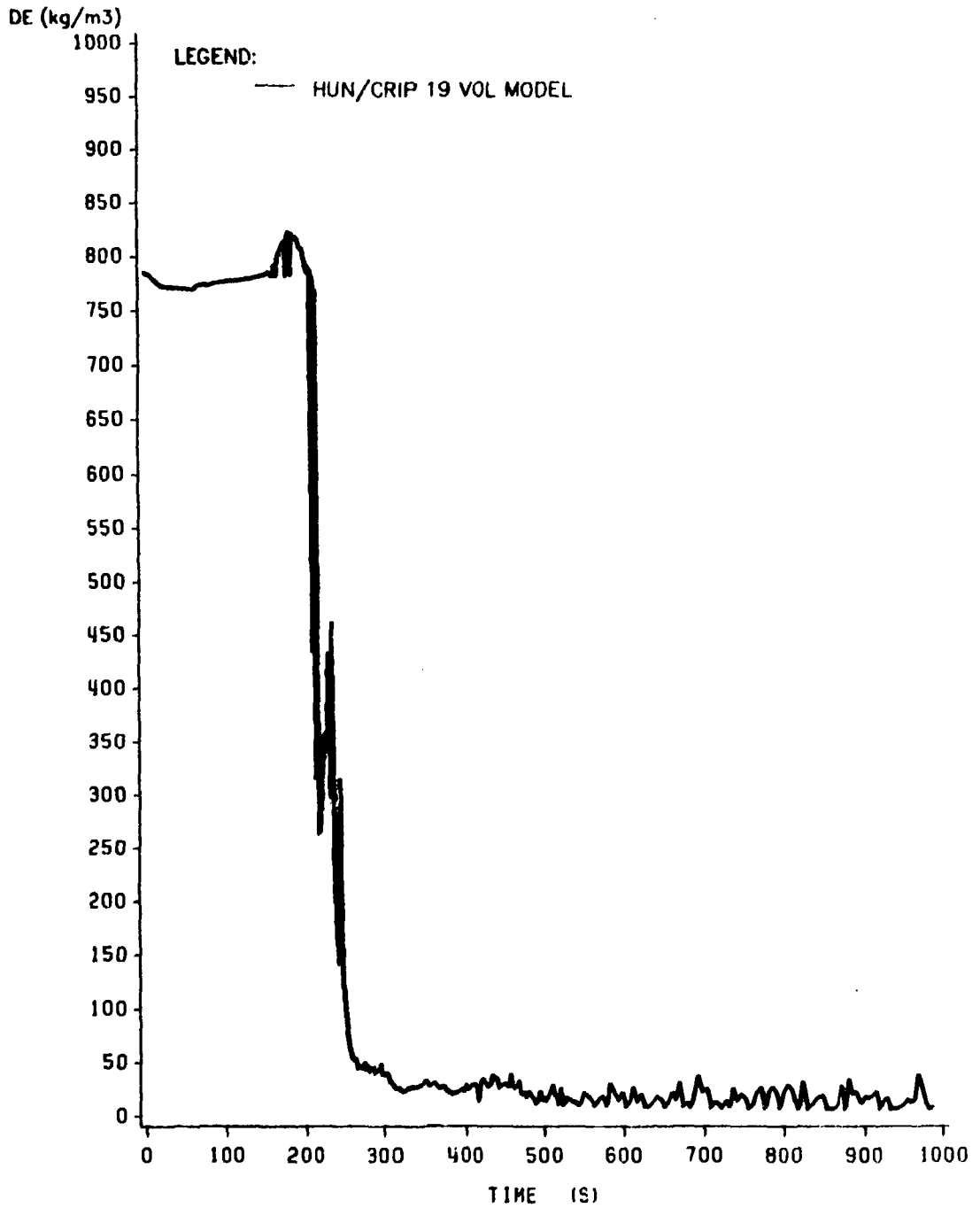


Fig. 4.29

IAEA--SPE 7.4% SBLOCA ON PMK - NVII

PL01NO-30

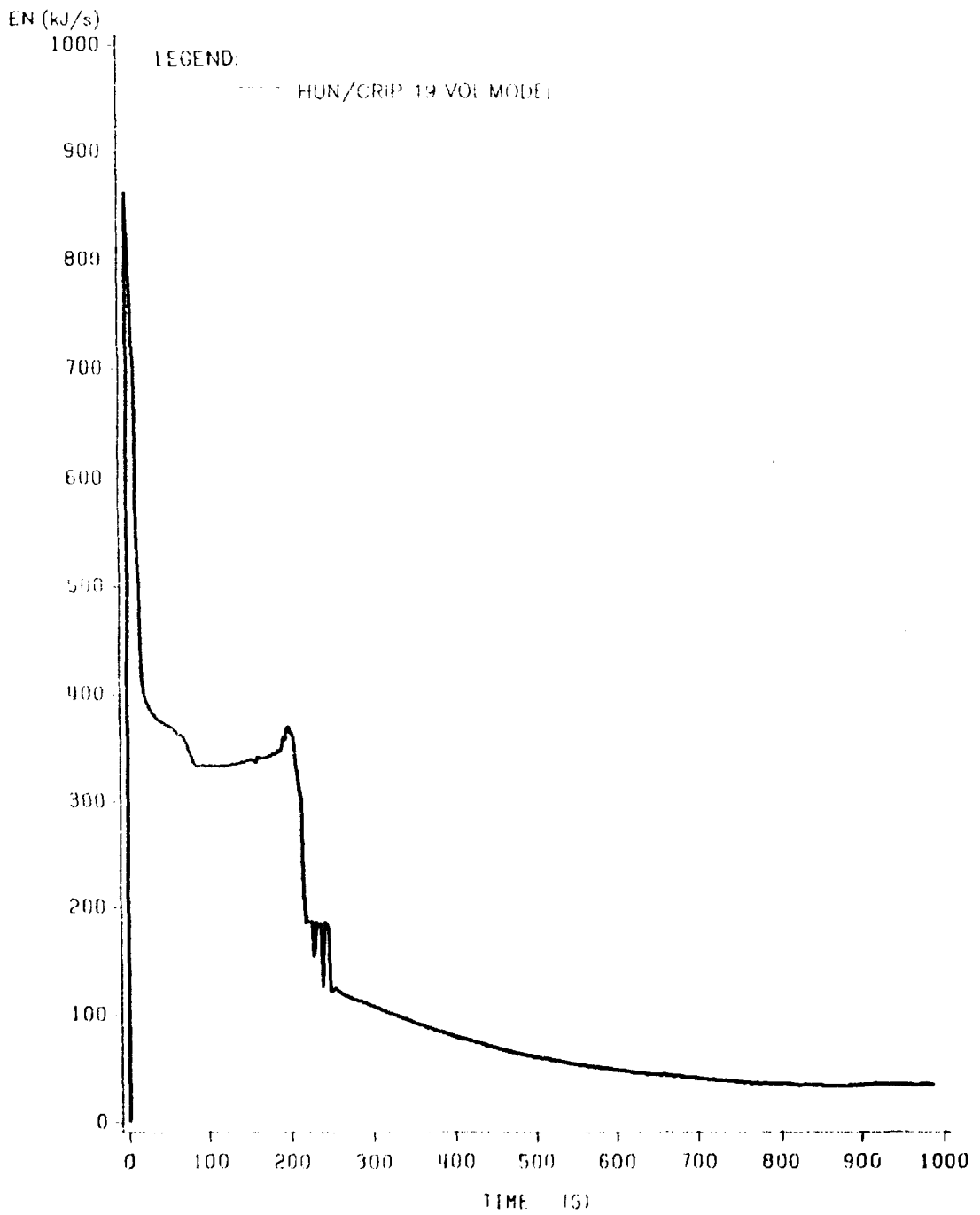


Fig. 4.30

IAEA-SPE 7.4% SBLOCA ON PMK-NVH

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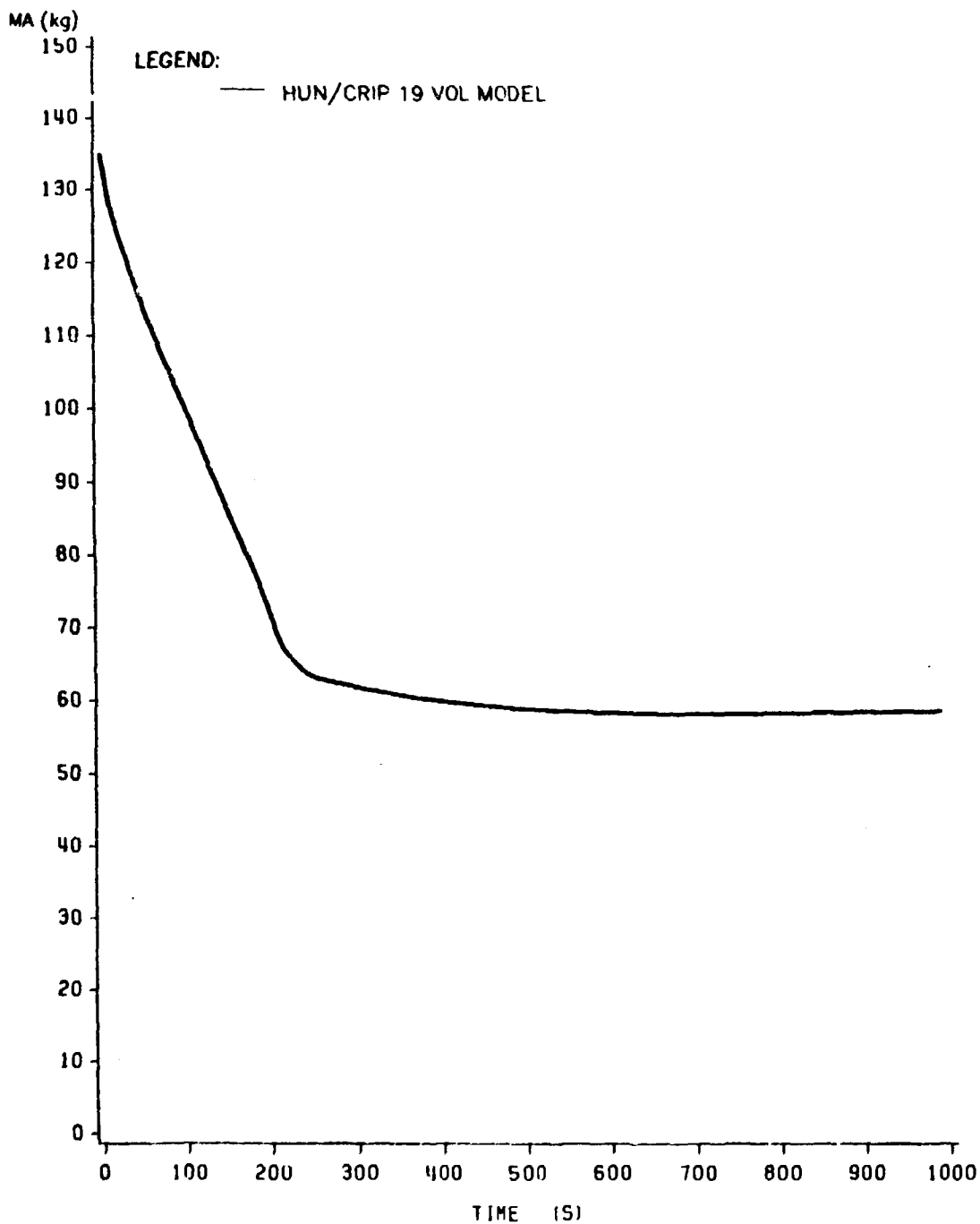


Fig. 4.31

IAEA-SPE 7.4% SBLOCA ON PMK-NVH
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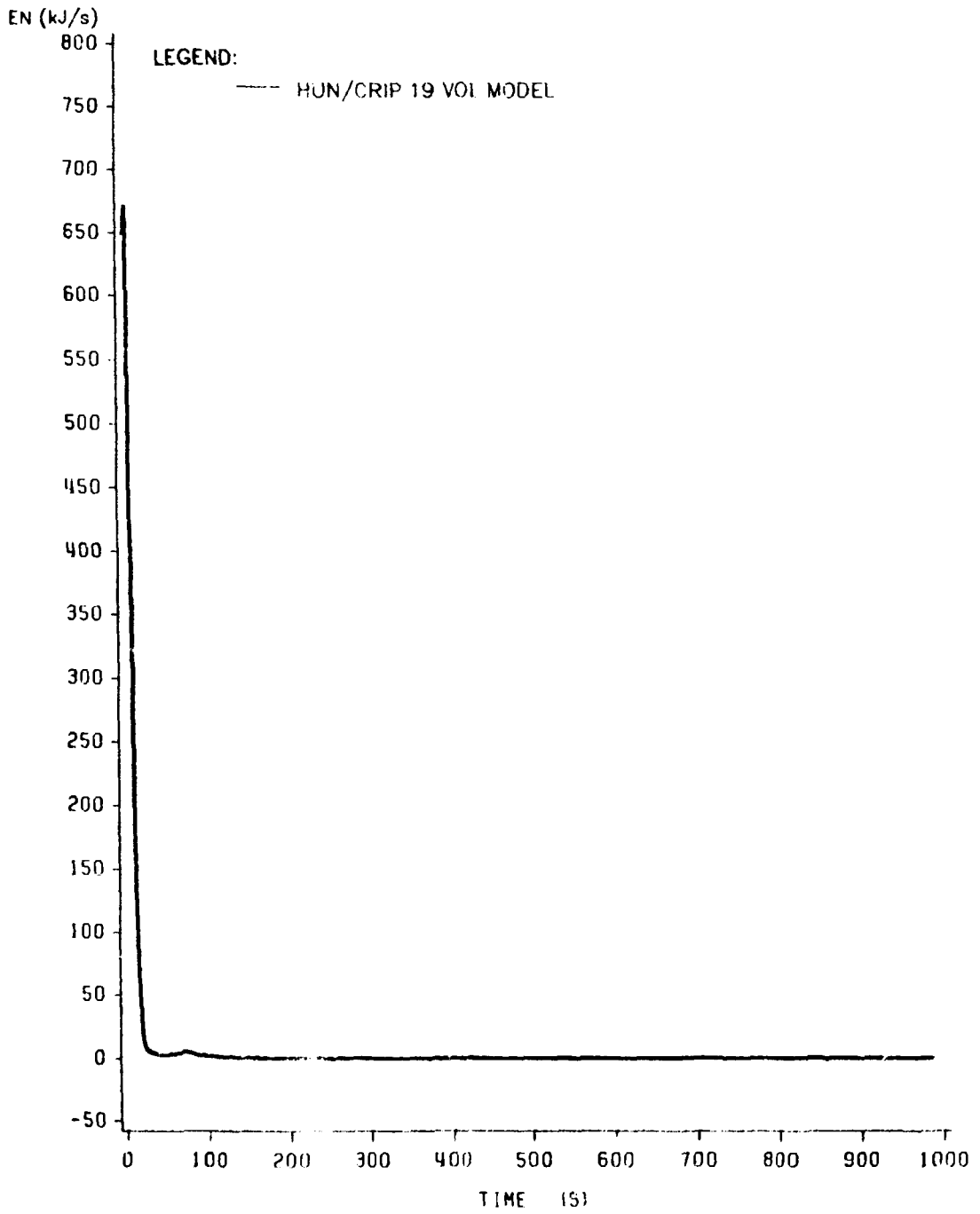


Fig. 4.32

IAEA-SPE 7.4% SBLOCA ON PMK-NVH
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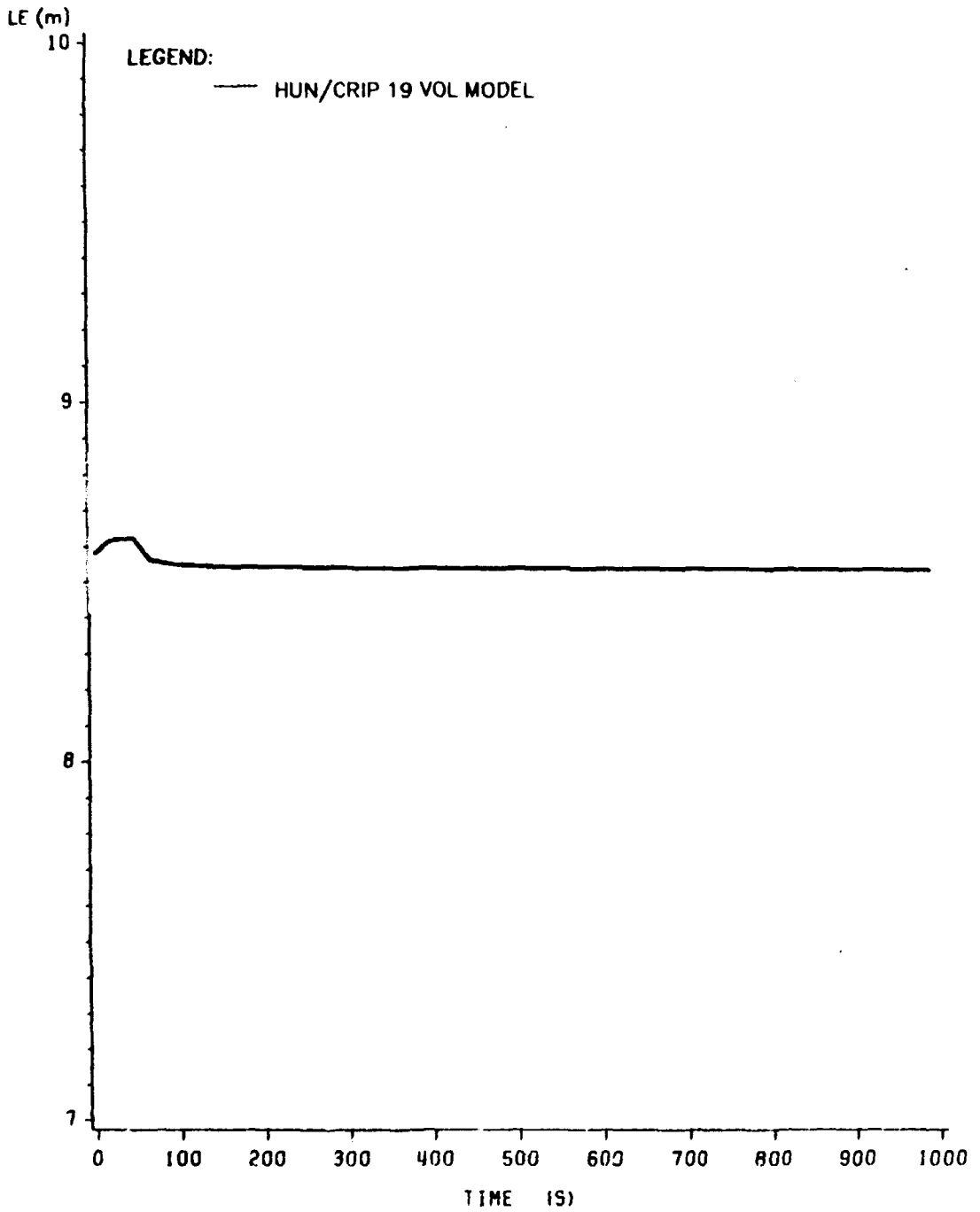


Fig. 4.33

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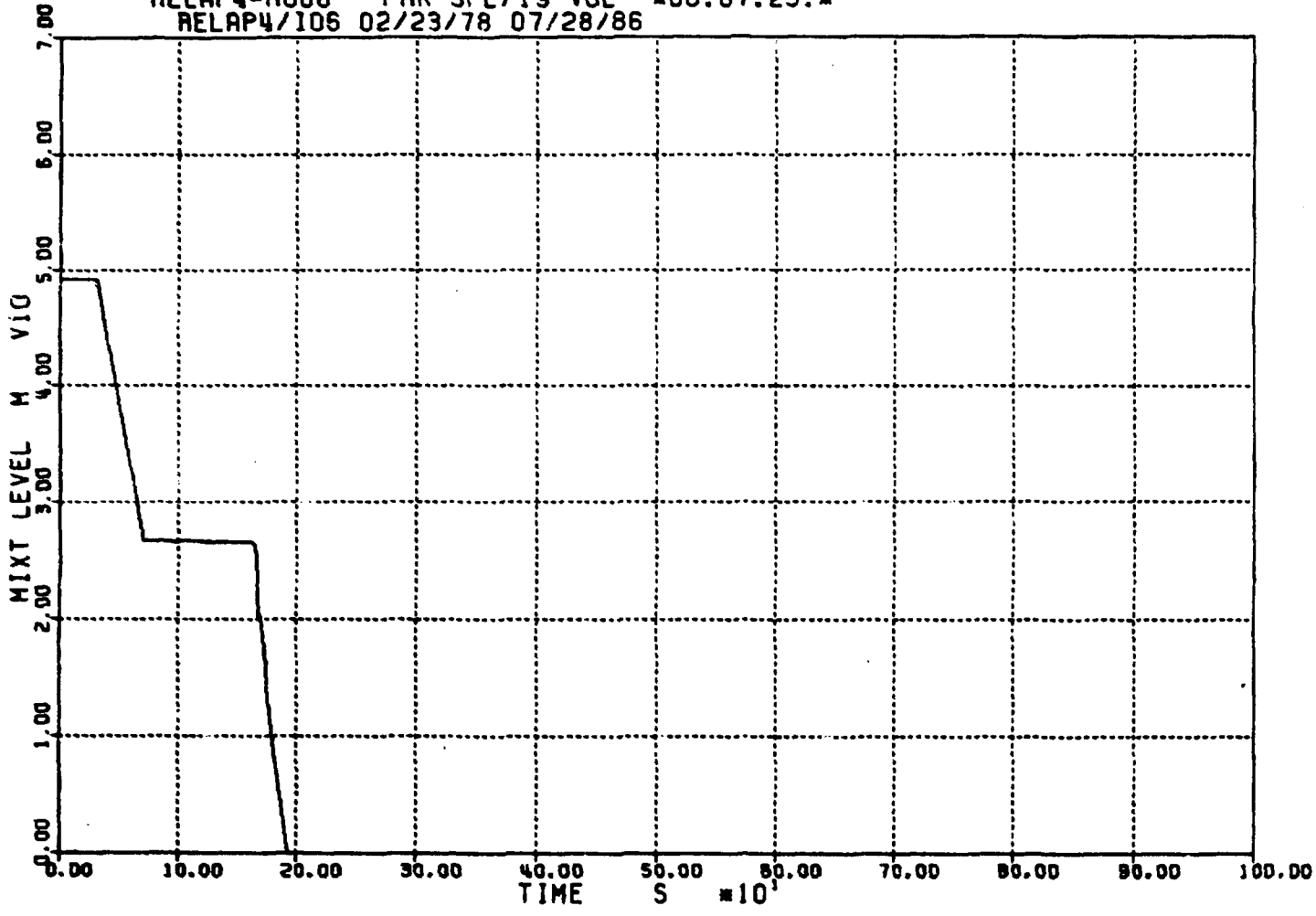


Fig. 4.34

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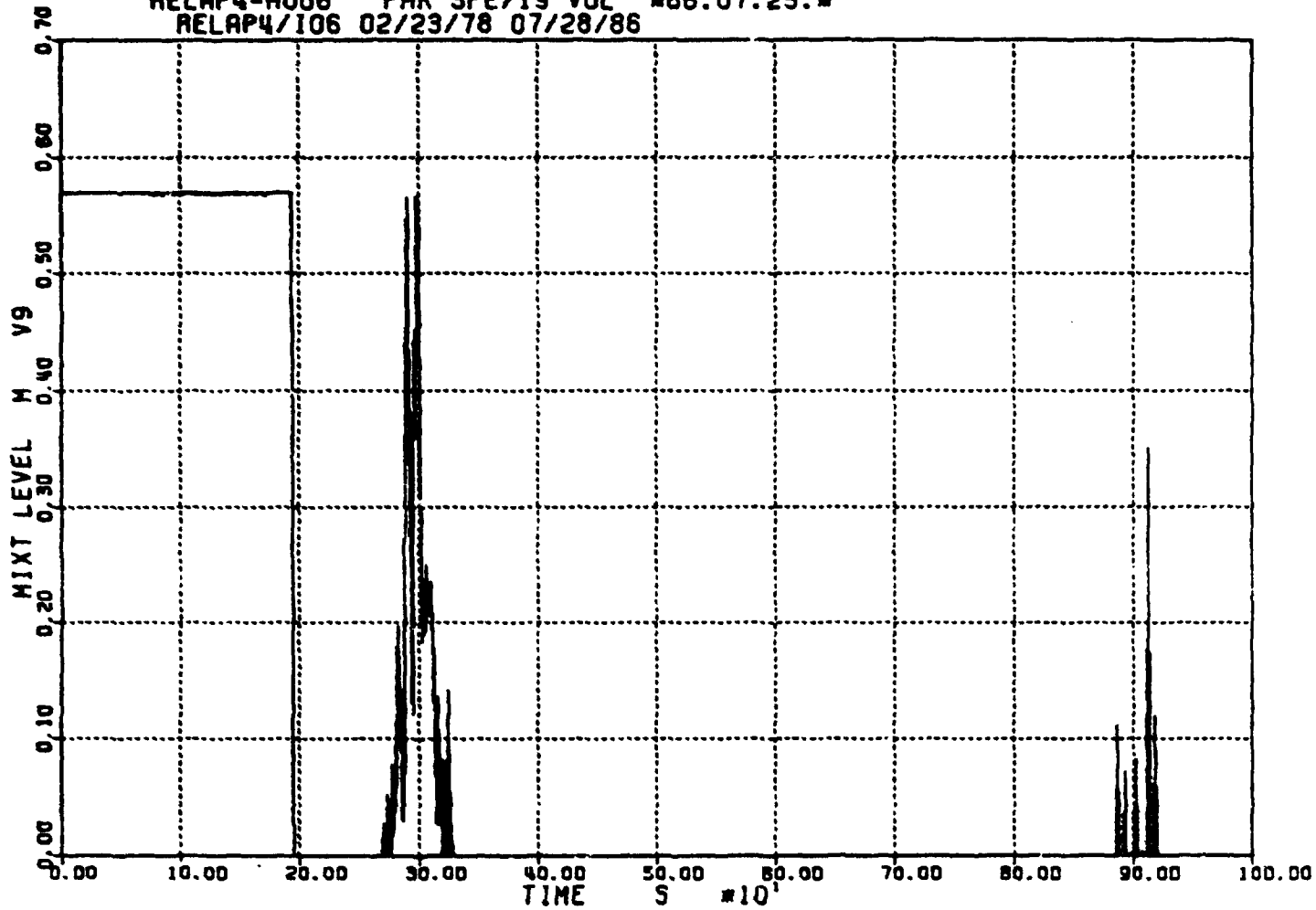


Fig. 4.35

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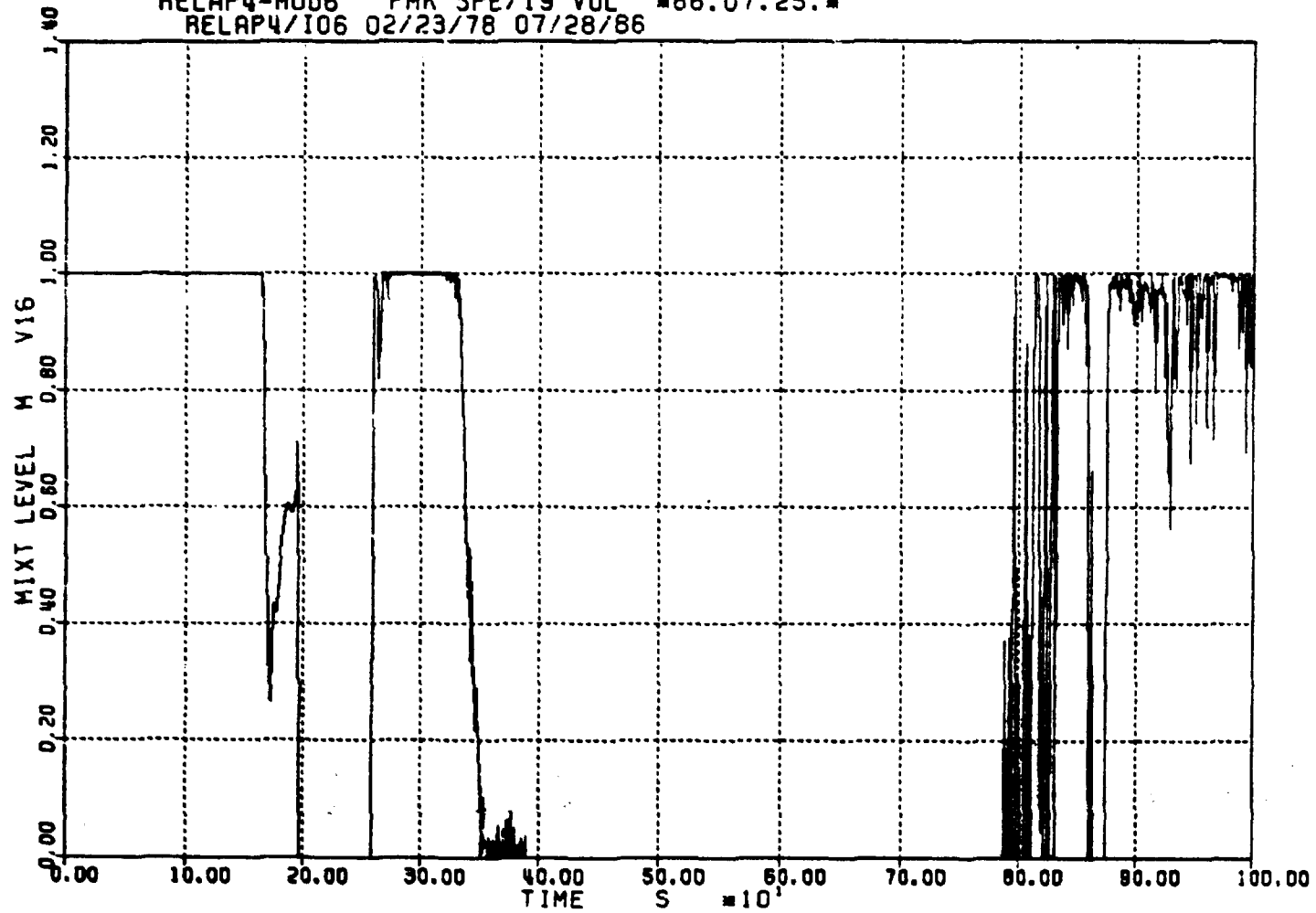


Fig. 4.36

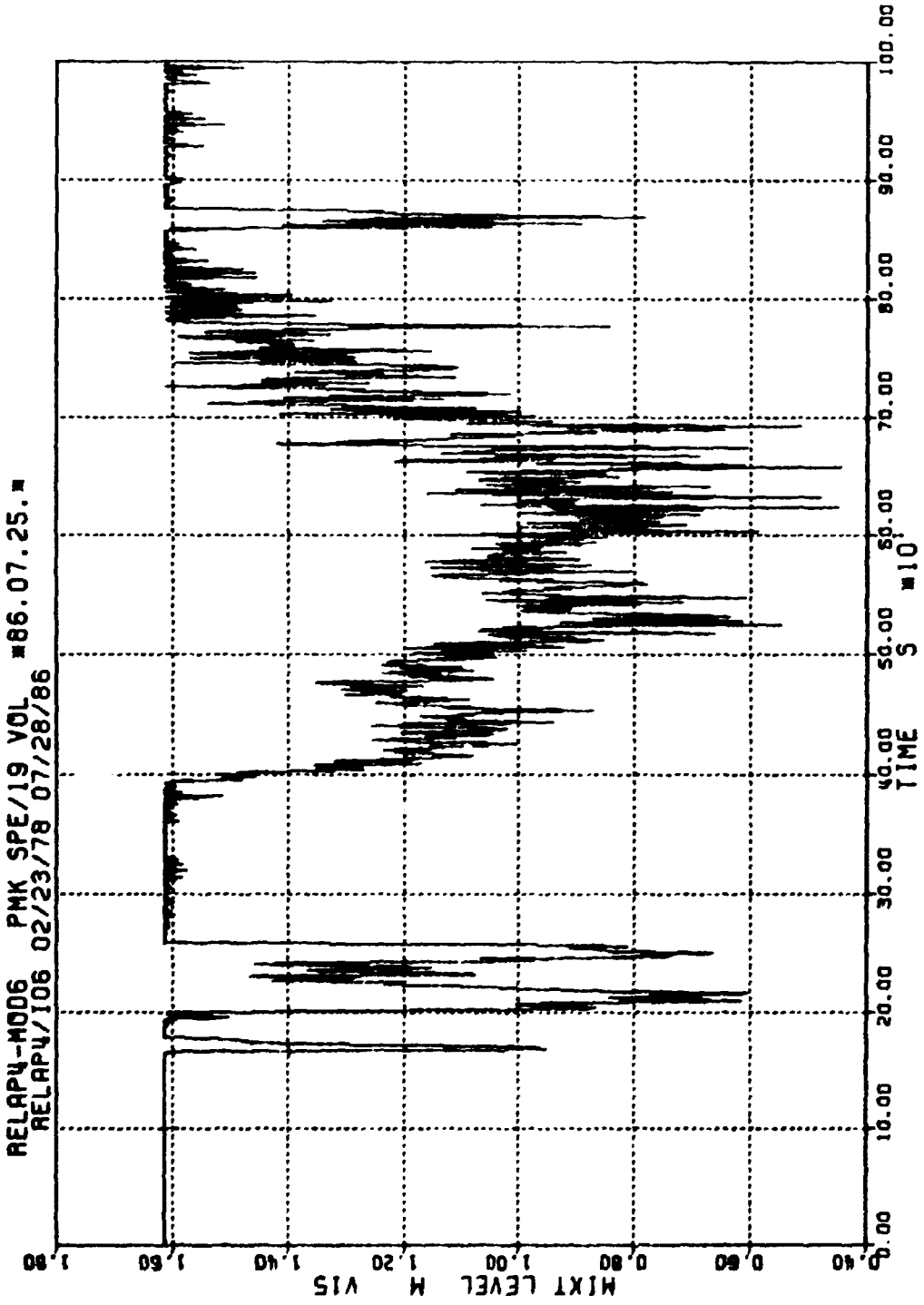


Fig. 4.37

RELAP4-MOD6 PMK SPE/19 VOL #86.07.25.*
RELAP4/I06 02/23/78 07/28/86

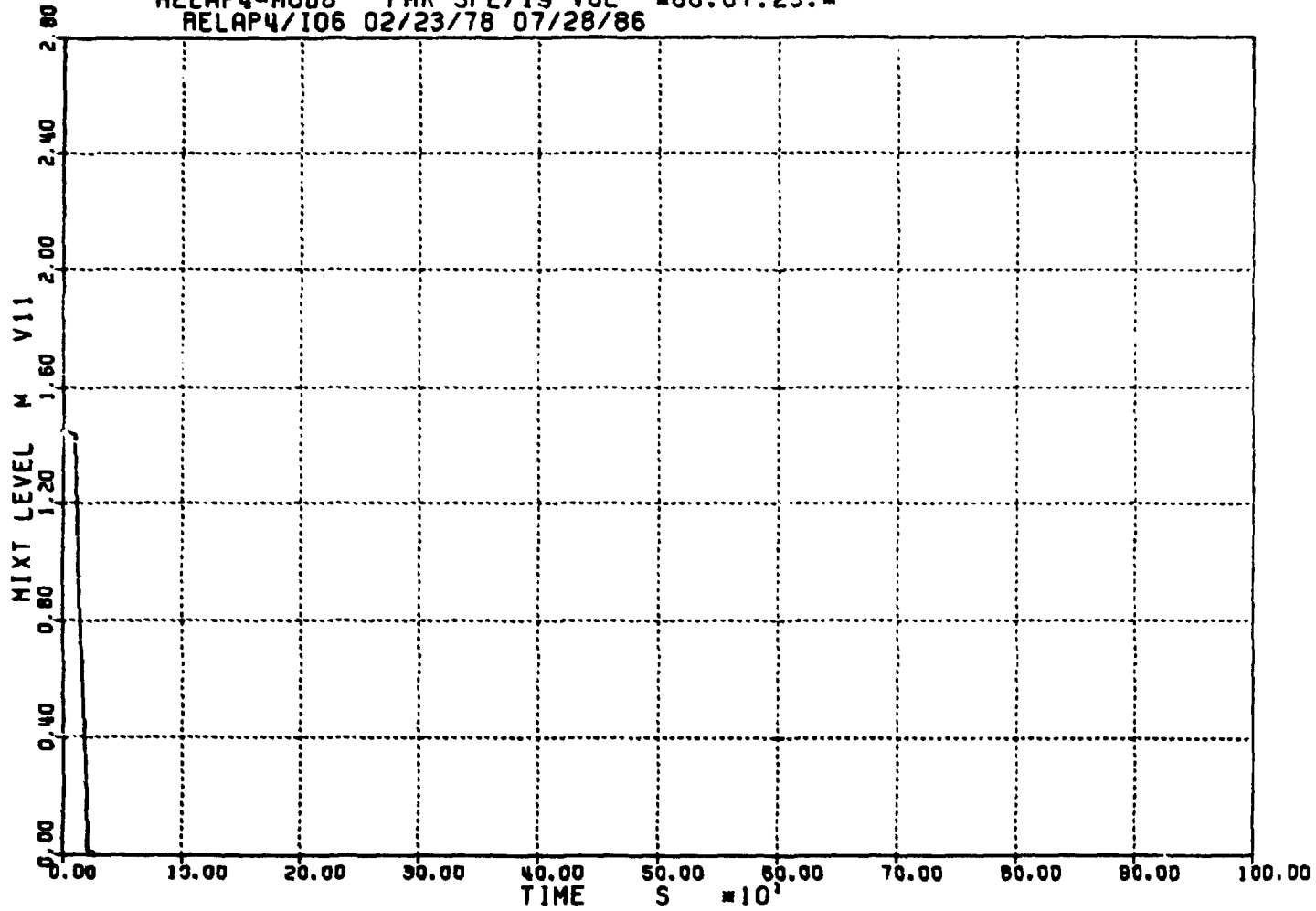


Fig. 4.38

RELAP4-M006 PMK SPE/19 VOL #86.07.25.*
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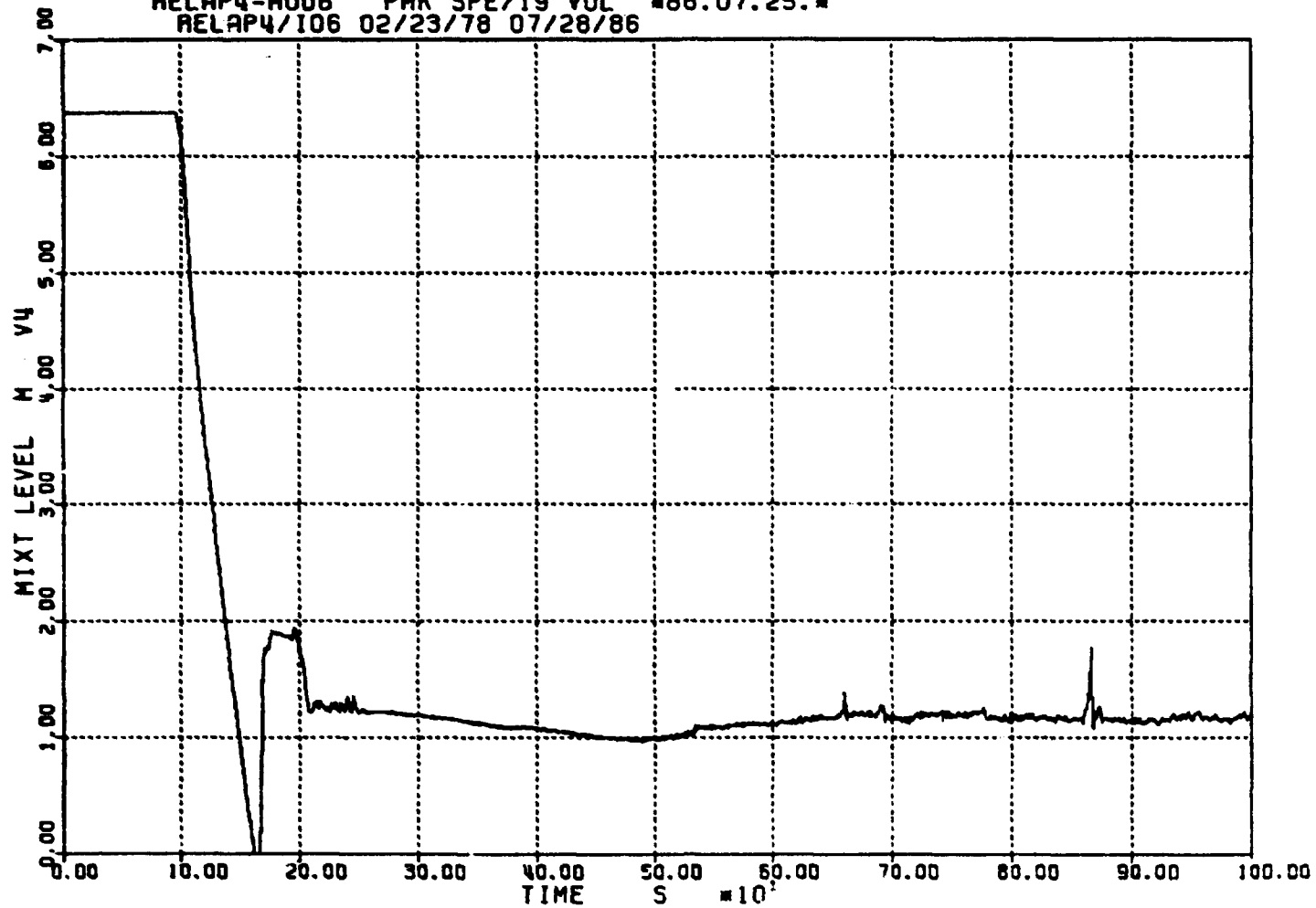


Fig. 4.39

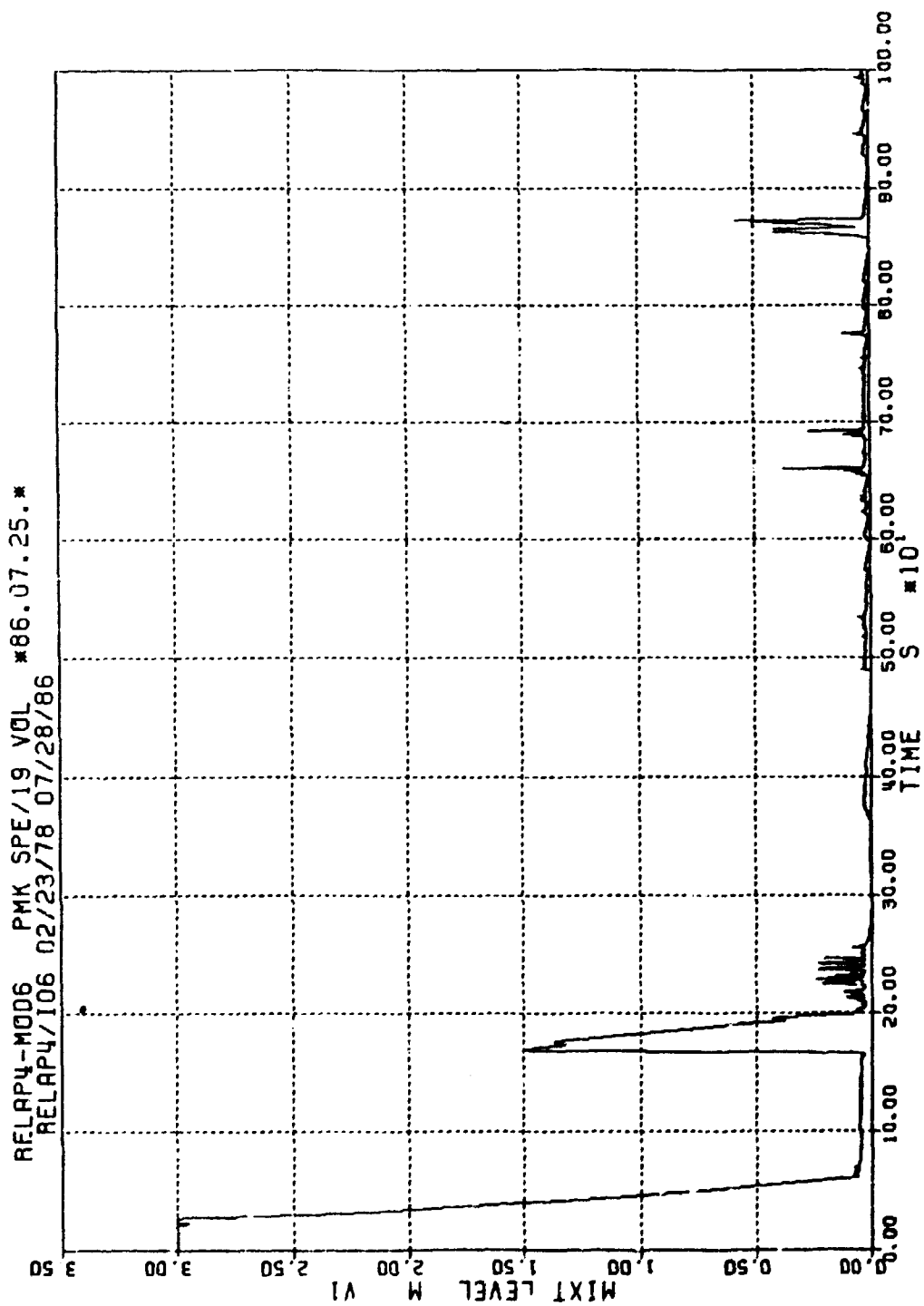


Fig. 4.40

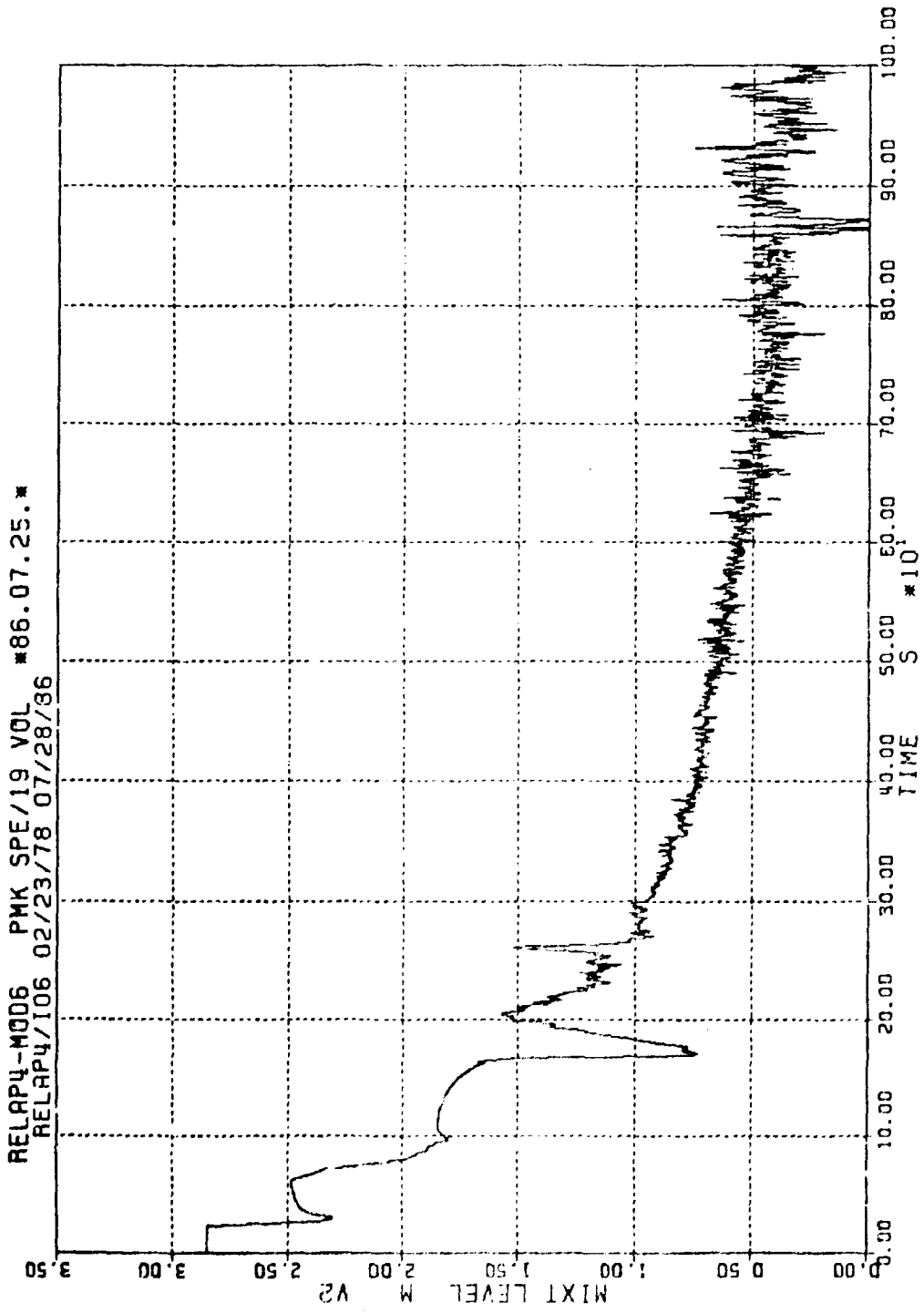


Fig. 4.41

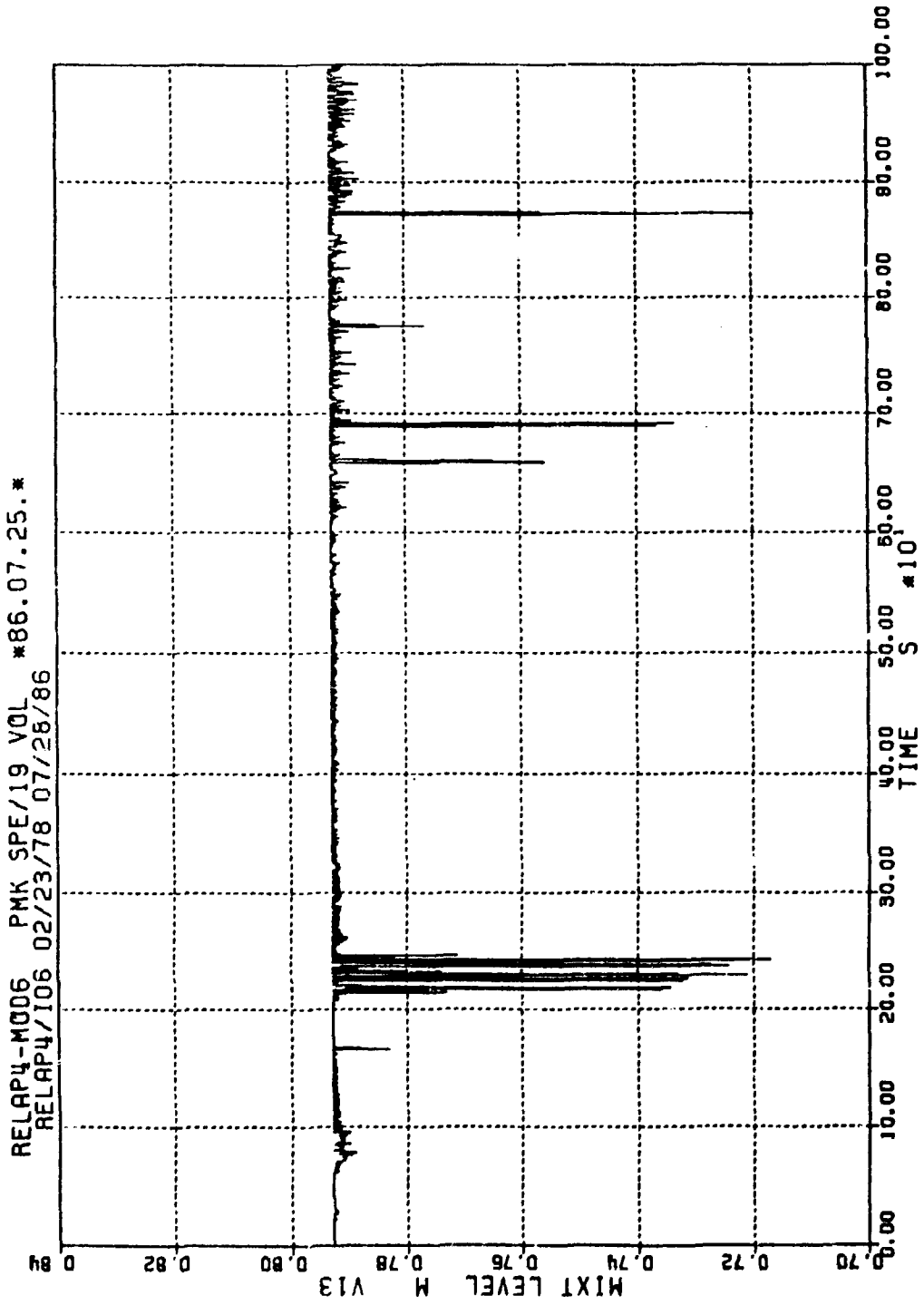


Fig. 4.42

RELAP4-MOD6 PMK SPE/19 VOL *86.07.25.*
RELAP4/I06 02/23/78 07/28/86

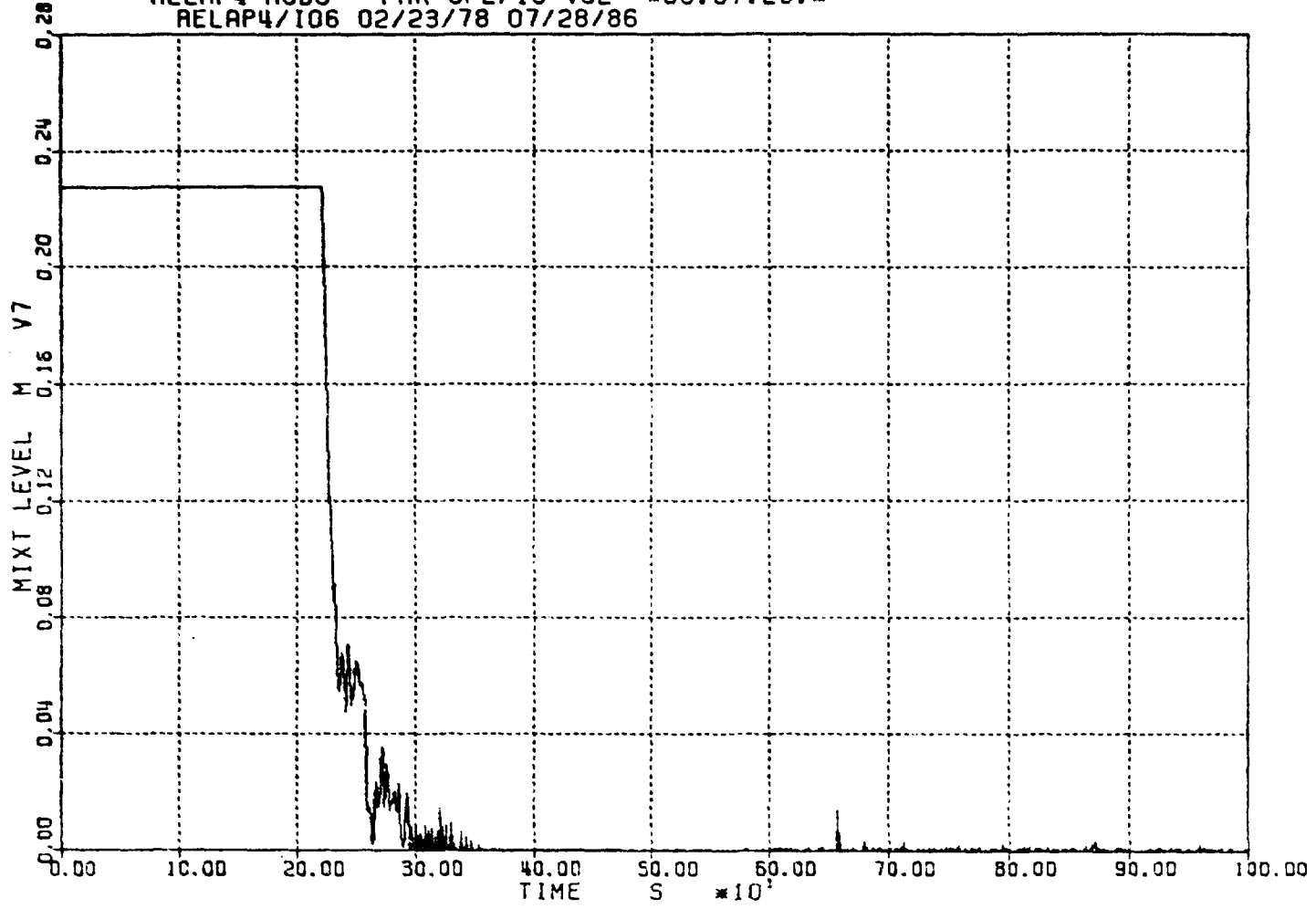


Fig.4.43

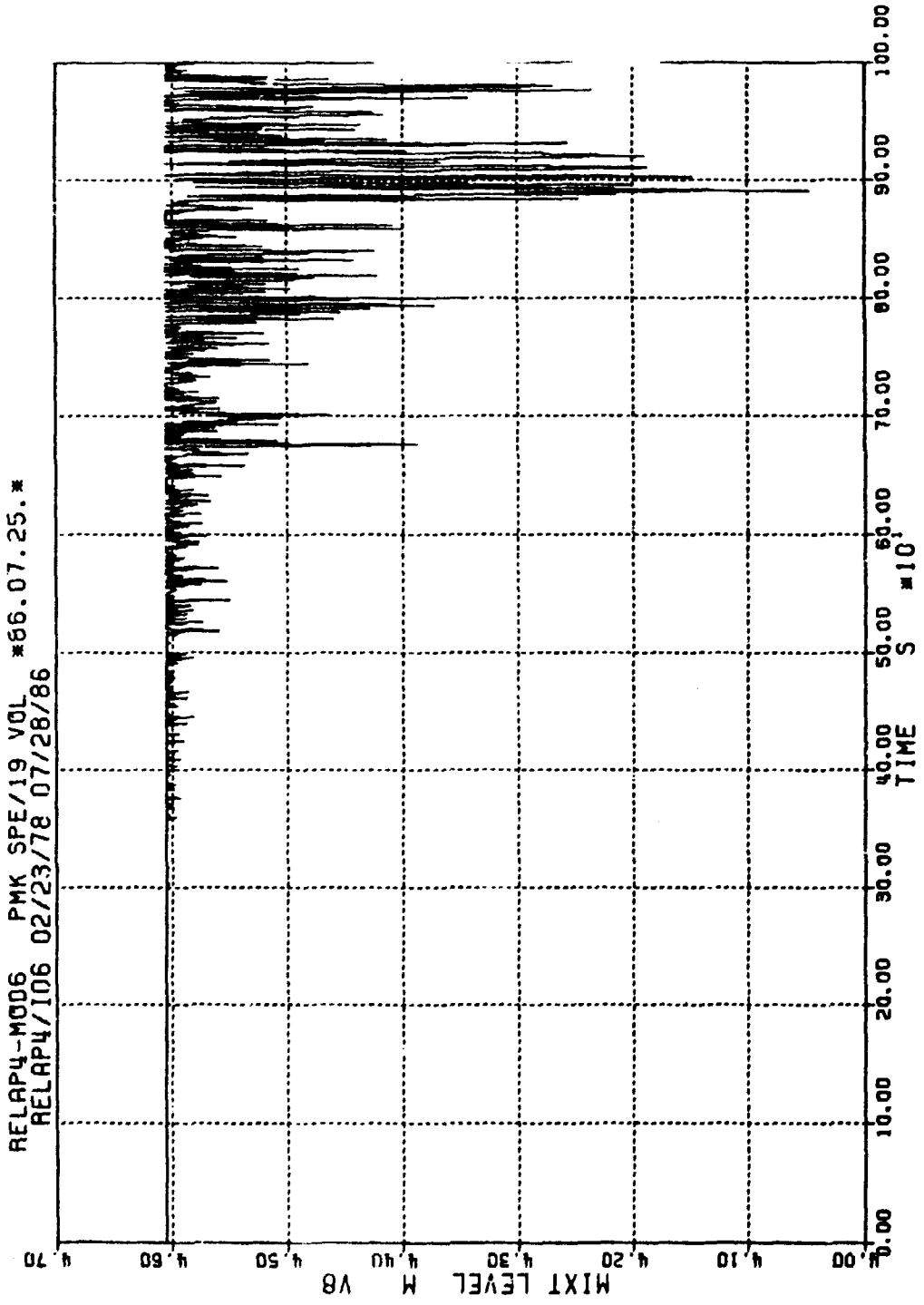


Fig. 4.44

RELAP4-M006 PMK SPE/19 VOL *86.07.25.*
RELAP4/106 02/23/78 07/28/86

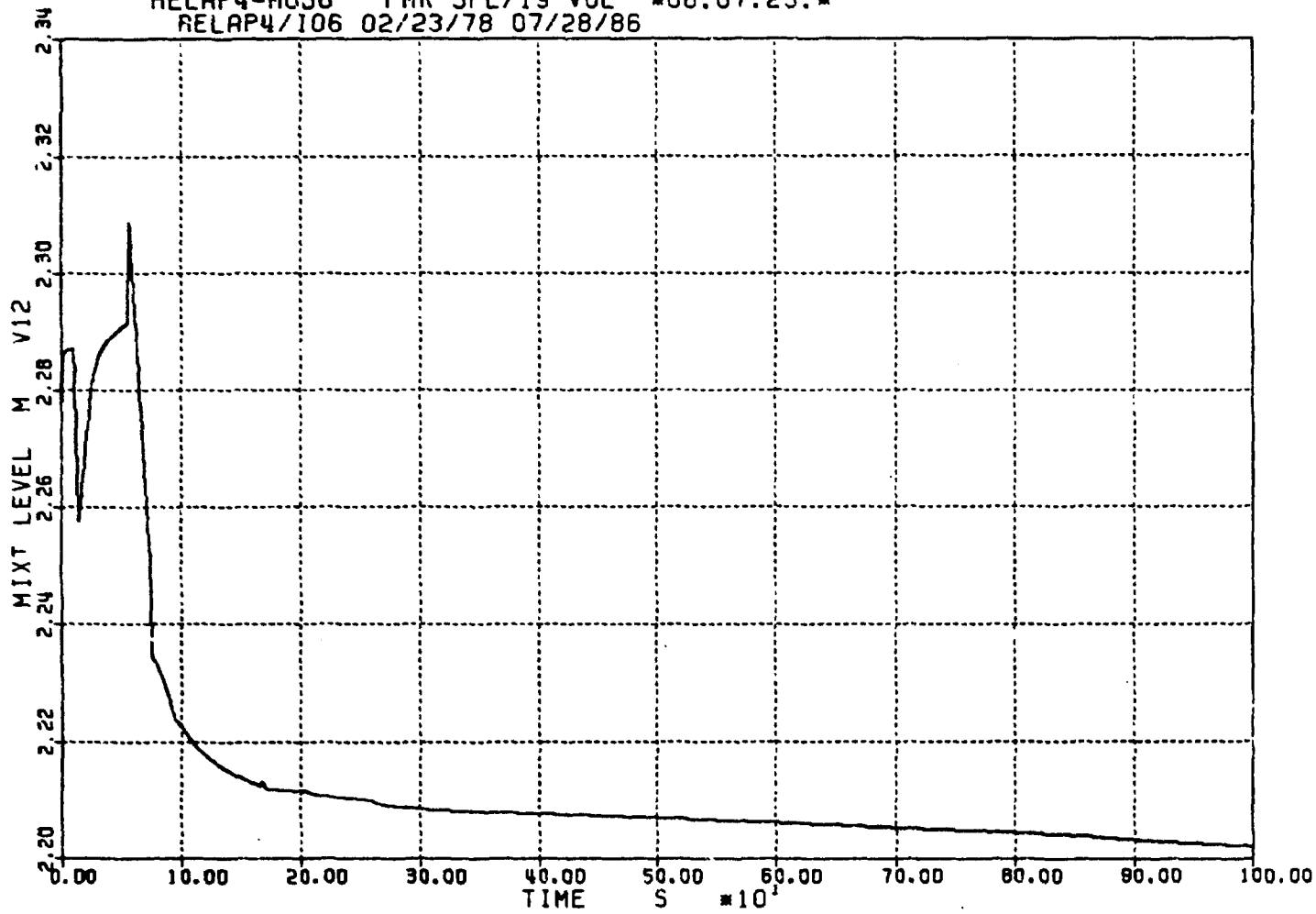


Fig. 4.45

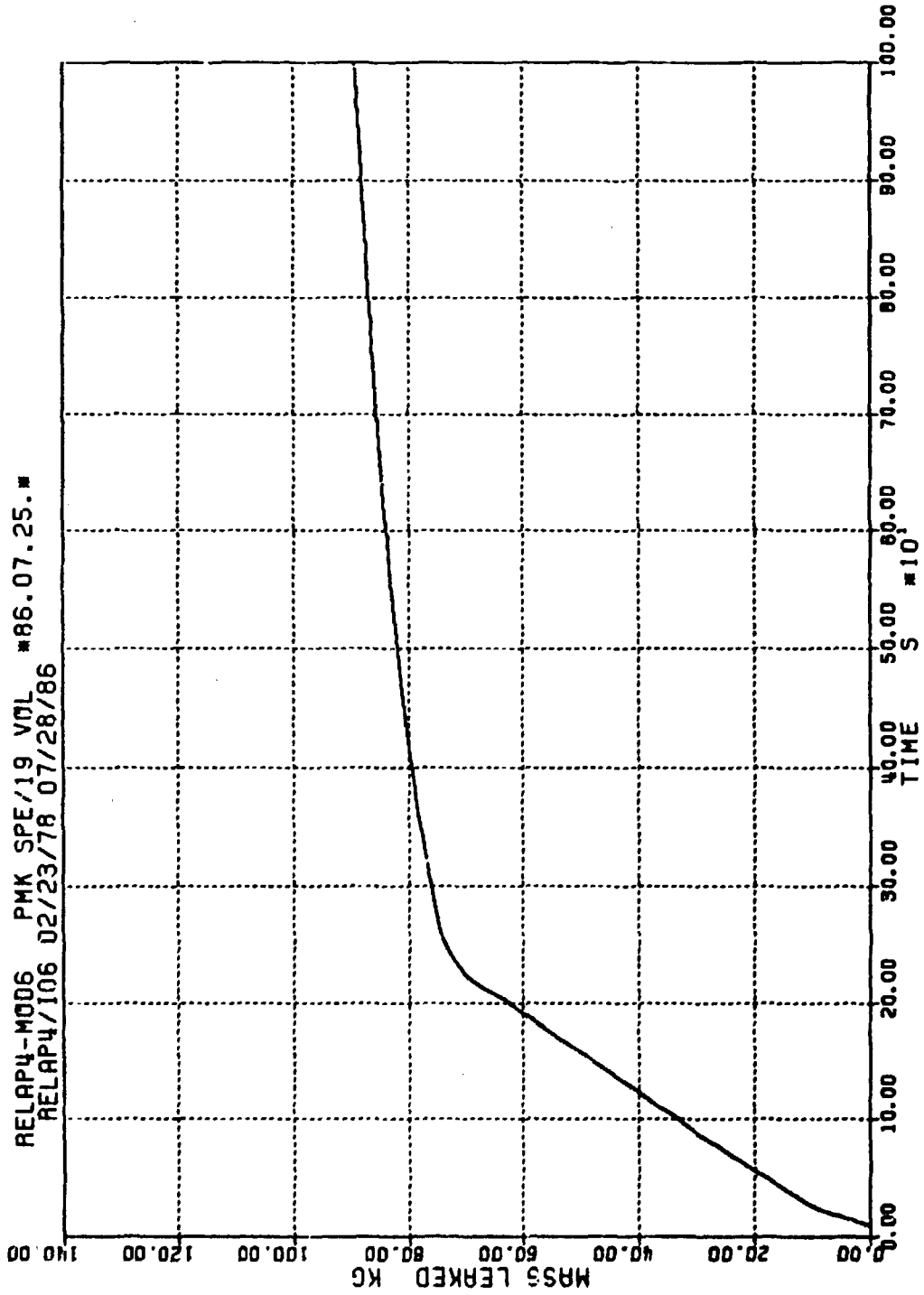


Fig. 4.46

Table 1.

Time s	Power kW
0	654.0
1	577.2
2	496.6
3	421.3
4	398.4
5	371.5
7	234.0
10	147.6
14	88.0
19	58.5
24	47.5
30	41.4
60	34.6
100	30.3
200	23.2
400	19.3
800	15.0
1000	15.0

Table 2.

Time s	Closing current mA	pump	MV12
0	11.51		
1	11.70		
2-3	12.30		
4-6	12.85		
7-10	13.44		
11-15	13.87		
16-20	14.21		
21-26	14.52		
27-32	14.86		
33-40	15.17		
41-48	15.45		
49-56	15.79		
57-66	16.12		
67-76	16.40		
77-86	16.71		
87-96	17.05		
97-106	17.36		
107-116	17.67		
117-126	18.00		
127-136	18.44		
137-146	18.96		
147-148	19.84	stopped*	
149-150	19.85		begins to close
150-995	19.85		

*At this time MV11 starts to open

Table 3.

s	kg/s	s	kg/s
0	0	61	0.014
60	0	500	0.014
		1000	0.014

Table 4.

Position [*]	1	2	3	4	5	6	7	8
p MPa	12.629	12.603	12.544	12.552	12.838	12.772	12.730	12.650

* In Reference [4], in Fig.1. /positions 2 and 3 should be changed/

Volume number [*]	1	2	3	4	5	6	7
p MPa	12.616	12.590	12.579	12.548	13.324	12.838	12.772

Volume number [*]	8	9	10	11	12	13	14
p MPa	12.750	12.650	12.629	12.607	4.671	12.603	12.790

Volume number [*]	15	16	17	18	19
p MPa	12.700	12.670	12.568	12.558	12.730

* In Fig. 3.1

Table 5.

Number of control volumes	19
Number of junctions	24
Number of check valves	5
Number of file junctions	4
Number of leak junctions	1
Number of heat slabs	16
Number of core slabs	5
Number of slabs with heat losses	4
Number of pumps	1

Table 6.

Vol. number		Junctions connected	Elevation /m/	Height /m/	Bubble rise
1	hot leg vessel side with surge line	J1, J2, J11	4.802	2.998	2
2	SG hot collector	J13, J3	5.595	2.845	2
3	SG primary tubes 1. part	J3, J21	6.362	1.831	0
4	SG cold collector and cold leg SG side	J4, J5, J15	2.077	6.363	2
5	pump with suction and delivery lines	J15, J16	-0.653	2.933	2
6	cold leg vessel side vertical part	J5, J6, J16	2.234	2.568	2
7	downcomer head	J7, J8, J17	4.770	0.228	2
8	downcomer	J8, J24	0.166	4.604	2
9	core upper part	J20, J9	2.994	0.570	2
10	upper plenum	J10, J1	3.564	4.921	2
11	pressurizer	J11	7.800	2.460	3
12	SG secondary	J17, J18, J23	6.330	2.606	1
13	hot leg SG side	J5, J13	4.802	0.793	2
14	cold leg vessel side horizontal part	J6, J7	4.802	0.046	2
15	core lower part	J9, J19	0.360	1.614	2
16	core middle part	J19, J20	1.994	1.000	2
17	SG primary tubes 2 part	J21, J22	6.362	1.831	0
18	SG primary tubes 3 part	J22, J4	6.362	1.831	0
19	lower plenum	J24, J9	0.0	0.380	2

Table 7.

Bubble rise	Alph	Vbub /ft./s/
0	0.0	0.0
1	0.8	12.0
2	0.8	3.0
3	0.8	-2.0 /complete separation/

Table 8.

Computer type			IBM 3081 /IAEA Vienna/
Code version			RELAP4/mod6-KfK
Memory region		kbyte	720
Steady state process time		s	10
Steady state CPU time		s	35
CPU time / process time /		volumes	0.184
Max. time step		s	0.2
Transient process time		s	990
Transient CPU time		s	27165
CPU time / process time /		volumes	1.444
Max. time step	10 - 20s	s	0.01
	20 - 80s	s	0.02
	80 - 600s	s	0.005
	600 - 1000s	s	0.01
Min. time step	10 - 20s	s	0.00005
	20 - 600s	s	0.0001
	600 - 1000s	s	0.0005

Table 9.

Event	Time S
Break valve opens	0.
Pressurizer empty	11.8
First reversal of core inlet flow	154.
Dryout first occurs	186.
Break flow two-phase	212.
Break uncovered	247.
Hot-leg loop seal cleared	61.5
Cold-leg loop seal cleared	200.
Core uncover starts	185.
Primary pressure equals secondary pressure	206.
Mixture level in UP drops to hot-leg elevation /6.248 m/	61.5
Mixture level in SG hot collector drops to elevation of uppermost SG tubes /8,193 m/	15.2
Scram	3.35
RPIS initiated	63.35
Pump trip simulation starts	9.95
Steam relief valve opens	46.8

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