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## COMPUTING THE EFFECTS OF A CONTAINED SODIUM SHEET FIRE: THE "FEUNA" CODE

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### ABSTRACT :

FEUNA is a computer code developed to calculate the thermodynamic effects of a sodium fire in a ventilated or unventilated containment volume.

Developed jointly by the CEA/DSN and Novatome, the FEUNA code involves two oxide formation reactions, aerosol generation and deposits, heat transfer by convection, conduction and radiation, gas inflow and outflow through the ventilation system and the relief valves.

The code was validated by comparing calculated values with the results of an actual sodium fire in a 400m<sup>3</sup> caisson.

### 1 - INTRODUCTION

With the development of the French fast neutron reactor program it soon became vital to design a computer code capable of predicting the thermodynamic effects of a contained sodium pool fire.

The FEUNA code was thus developed jointly by the CEA/DSN and Novatome to carry out safety and project calculations. This

achievement required a thorough prior knowledge of sodium combustion physics, acquired after a series of pool fires in a 400 m<sup>3</sup> caisson with various combustion surface area dimensions (the CASSANDRE program) (1).

This experimental base provided the data necessary for the code formulation, i.e. development of a combustion model, determination of the exchange coefficients between the air-aerosol system, the sodium and the containment walls, and evaluation of the aerosol deposit constants.

### 2 - MODEL HYPOTHESES

#### 2.1 - Combustion Hypotheses

- The sodium monoxide and peroxide formation reactions occur simultaneously and the proportion of sodium in monoxide form remains constant at 60 % throughout the fire.
- The aerosol formation rate is also constant. It is computed from the oxide release ratio (ratio of aerosol sodium mass to burned sodium mass) which is 40 % ; this implies that all the peroxide is present in aerosol form.
- The combustion energy is a function of the amount of heat produced by Na<sub>2</sub>O formation (104 kcal per mole) and Na<sub>2</sub>O<sub>2</sub> formation (124 kcal per mole), weighted by their respective formation percentages.
- The combustion rate depends on the oxygen concentration and temperature of the oxydant gas, and is given by the Garellis formula :

$$T(t) = T(o) \frac{nO_2(t)}{nO_2(o)} \sqrt{\frac{Tg(t)}{Tg(o)}}$$



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where :  $T(t)$  : combustion rate at instant  $t$  ( $\text{kg}\cdot\text{h}^{-1}\cdot\text{m}^{-2}$ )  
 $T(o)$  : combustion rate at initial instant ( $\text{kg}\cdot\text{h}^{-1}\cdot\text{m}^{-2}$ )  
 $nO_2(t)$  : number of moles of oxygen at instant  $t$   
 $nO_2(o)$  : number of moles of oxygen at initial instant  
 $Tg(t)$  : air temperature at instant  $t$  ( $^{\circ}\text{C}$ )  
 $Tg(o)$  : air temperature at initial instant ( $^{\circ}\text{C}$ )

- The power released from the fire is given by the relation :

$$W_F = E \cdot T(t) \cdot S_F$$

where :  $W_F$  : power output (Watt)  
 $E$  : energy released by combustion of 1 kg of sodium ( $\text{J}\cdot\text{kg}^{-1}$ )  
 $T(t)$  : combustion rate at instant  $t$  ( $\text{kg}\cdot\text{h}^{-1}\cdot\text{m}^{-2}$ )  
 $S_F$  : fire surface area ( $\text{m}^2$ )

## 2.2 - Heat Exchange Hypotheses

- The liquid sodium pool comprises a number of layers of variable thickness.
- Combustion occurs on the sodium surface (first half-layer).
- The burning sodium releases aerosols which mix with the other gases to form a homogeneous atmosphere assumed to be at the same temperature.
- Heat transfer occurs in the following manner :

### a) Downwards

by conduction through the sodium, through the combustion pan (a single layer) and through the caisson floor (also broken down into a number of layers of varying thickness).

### b) Upwards

- . by convection and radiation from the sodium to the air-aerosol system and then to the internal structures and containment walls.
- . by conduction through the walls (broken down into a number of layers of equal thickness).
- . by convection from the wall outer face to the surrounding atmosphere.

- No direct radiation occurs from the sodium pool to the vessel walls.

- All the exchanges are processed single-dimensionally.

The power exchanged by convection and radiation take the following form :

$$P = P_{\text{radiation}} + P_{\text{convection}} = (h_r + h_c) S_c \Delta\theta$$

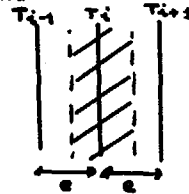
where :  $P$  : power exchanged (watts)  
 $S_c$  : source area ( $\text{m}^2$ )  
 $\Delta\theta$  : temperature difference between source and exchange medium ( $^{\circ}\text{C}$ ).  
 $h_c + h_r$  : heat exchange coefficient by natural convection and radiation ( $\text{W}\cdot\text{m}^{-2}\cdot^{\circ}\text{C}^{-1}$ )

These coefficients involve a number of absorption and emission factors which were adjusted on the basis of the CASSANDRE experiments :

$$\begin{aligned} \epsilon_a = \alpha_a &= 0.3 \text{ (gas-aerosol system radiant emission and absorption factor),} \\ \epsilon_p &= 0.3 \text{ (containment wall radiant emission factor),} \\ \epsilon_{Na} = \alpha_{Na} &= 1 \text{ (sodium radiant emission and absorption factor).} \end{aligned}$$

Heat transfers by conduction were calculated using Dusimberre's method (2) which gives the interface temperatures of the various layers through which the conduction occurs. The variation in time of the temperature  $T_i$  at a surface separating two layers is given by the thermal equilibrium in a zone extending to either side of the interface and assumed to be at temperature  $T_i$  :

$$\rho C_e \frac{dT_i}{dt} = \frac{\lambda_i}{e} (T_{i-1} - T_i) - \frac{\lambda_i}{e} (T_i - T_{i+1})$$



where :  $\rho$  : density of material ( $\text{kg.m}^{-3}$ )  
 $\lambda_i$  : thermal conductivity of material ( $\text{W.m}^{-1}.\text{K}^{-1}$ )  
 $C_e$  : specific heat of material ( $\text{J.kg}^{-1}.\text{K}^{-1}$ )  
 $e$  : layer thickness (m).

### 2.3 - Gas Hypotheses

- The gas inlet and outlet flow rates are obtained by assuming that the pressure difference between the containment and the exterior is proportional to the dynamic pressure :

$$\Delta P = K \frac{\rho V^2}{2g}$$

where :  $\Delta P$  : pressure differential (mm  $\text{H}_2\text{O}$ )  
 $\rho$  : gas density ( $\text{kg.m}^{-3}$ )  
 $V$  : gas velocity ( $\text{m.s}^{-1}$ )  
 $g$  : gravitational acceleration ( $\approx 10\text{m.s}^{-1}$ )  
 $K$  : pressure drop coefficient

- The containment volume is provided with pressure relief valves and pressurizing valves of specified surface areas, pressure drop coefficients and opening pressures.

- The gas temperature evolution is determined by assuming that the internal system energy variation per unit time is equal to the power exchanged among the sodium, gases, internal structures and walls together with the enthalpy variation of the air per unit time.  
 - The gas pressure evolution is obtained by differentiating the gas status equation.

### 3 - DESCRIPTION OF THE FEUNA CODE

The FEUNA code, written in FORTRAN, is based on the resolution of a set of first-order differential equations. For each time step it computes the following independent physical quantities :

- burned sodium mass
- oxygen mass in the containment volume
- nitrogen mass in the containment volume
- aerosol concentration in the containment volume
- air temperature
- air pressure
- sodium layer temperatures
- sodium/container and container/floor interface temperatures
- internal structure temperature
- containment wall temperatures

Euler's tangent method is used for the integration.

The remaining physical values are then computed from the values of the independent variables at instant  $t$ .

After every  $m$  consecutive integrations ( $m$  is defined as a code input) the following results are printed out in tabular form.

- Elapsed time of sodium fire
- Gas temperature ( $^{\circ}\text{C}$ )
- Gas pressure (mb)
- Combustion rate ( $\text{kg}\cdot\text{h}^{-1}\cdot\text{m}^{-2}$ )
- Burned sodium mass (kg)
- Gas density ( $\text{kg}\cdot\text{m}^{-3}$ )
- Gas inflow rate ( $\text{m}^3\cdot\text{h}^{-1}$ )
- Gas outflow rate ( $\text{m}^3\cdot\text{h}^{-1}$ )
- Oxygen molar fraction
- Aerosol mass in suspension (kg)
- Aerosol mass extracted (kg)
- Sodium surface temperature ( $^{\circ}\text{C}$ )
- Container/floor interface temperature ( $^{\circ}\text{C}$ )
- Wall inner face temperature ( $^{\circ}\text{C}$ )
- Internal structure temperature ( $^{\circ}\text{C}$ )
- Aerosol extraction rate ( $\text{mg}\cdot\text{s}^{-1}$ )
- Extracted gas mass (kg).

- Integration step 0.25
- Max.computing time 10800 s
- Printout interval 300 integrations.

Thickness of sodium layers (m) ;

0.007 0.010 0.05 0.05 0.05 0.05 0.01 0.007 0.003

Thickness of support layers (m) ;

0.003 0.007 0.01 0.01 0.01 0.02 0.02 0.02

Figure 2 compares the FEUNA computed results with the measured experimental values. The following computed and experimental curves are plotted versus time :

- oxygen molar fraction
- relative gas pressure
- sodium temperature
- gas temperature
- wall inner face temperature,

The figure shows the close agreement obtained between the two curves.

The FEUNA computer code has been applied to project design and safety analysis in the scope of the Super-Phénix program.

#### REFERENCES

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The code is capable of handling 70 equations, and 29 are used at the present time. The number of layers discriminated is limited to 30 in the sodium and containment floor, and to 70 in the walls. The code flowchart is shown in Figure 1.

#### 4 - PRACTICAL EXAMPLE - COMPARISON WITH EXPERIMENTAL RESULTS

A typical code run may be illustrated by one of the CASSANDRE experiments.

Basic experimental data :

- Liquid sodium mass 235 kg
- Containment volume 400  $\text{m}^3$
- Combustion surface area 1  $\text{m}^2$
- Wall area 336  $\text{m}^2$
- Steel combustion pan thickness 0.003 m
- Concrete wall thickness 0.26 m
- Initial combustion rate 30  $\text{kg}\cdot\text{h}^{-1}\cdot\text{m}^{-2}$

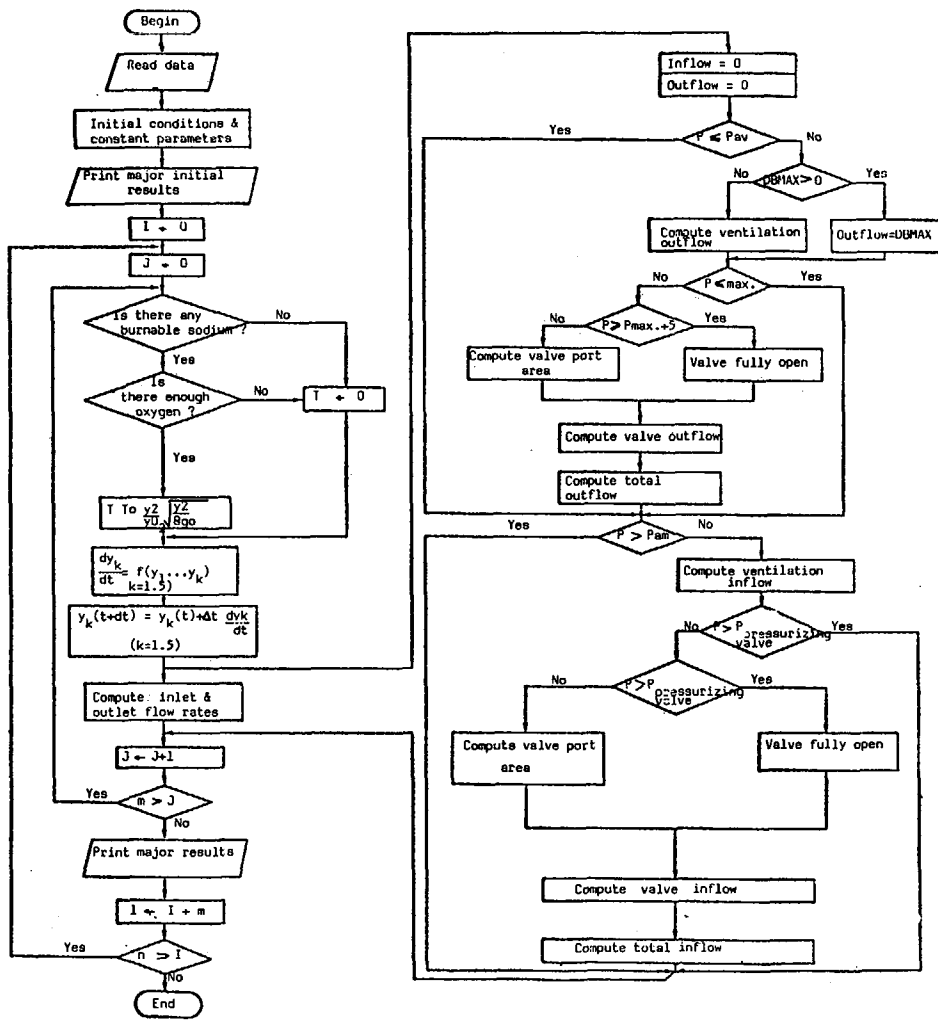


FIG. 1 - FEUNA CODE FLOWCHART

